

Electronic Supplementary Information

A noble-metal-free nanocatalyst for highly efficient and complete hydrogen evolution from $\text{N}_2\text{H}_4\text{BH}_3$

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Table S1 Catalysts composition determined by inductively coupled plasma atomic emission spectroscopic (ICP-AES).

Catalysts	Cu (wt%)	Ni (wt%)	Mo (wt%)	Cu/Ni/Mo (atomic ratio)
CuMo	26.82	0	39.64	1.01/~ /0.99
Cu _{0.8} Ni _{0.2} Mo	21.04	5.03	40.98	0.79/0.20/1.01
Cu _{0.6} Ni _{0.4} Mo	15.74	10.01	40.51	0.59/0.41/1.00
Cu _{0.5} Ni _{0.5} Mo	13.48	12.39	40.29	0.50/0.50/1.00
Cu _{0.4} Ni _{0.6} Mo	10.70	14.93	39.47	0.41/0.61/0.98
Cu _{0.3} Ni _{0.7} Mo	8.20	17.67	40.29	0.30/0.71/0.99
Cu _{0.2} Ni _{0.8} Mo	6.08	19.83	40.34	0.22/0.79/0.99
NiMo	0	24.58	40.30	~/1.00/1.00

Table S2 Catalytic activities for hydrogen generation from hydrazine brane catalyzed by different catalysts.

Catalysts	$n(\text{H}_2+\text{N}_2)/n\text{N}_2\text{H}_4\text{BH}_3$	t/min	TOF/h ⁻¹
Cu _{0.4} Ni _{0.6} Mo	6	13.9	108
Fe _{0.4} Ni _{0.6} Mo	6	15.78	95
Co _{0.4} Ni _{0.6} Mo	5.57	15.26	92
Cu _{0.4} Co _{0.6} Mo	4.37	14.28	79
Fe _{0.4} Co _{0.6} Mo	3.81	33.21	30
Cu _{0.4} Fe _{0.6} Mo	3	0.7	-
NiMo	5.14	18.1	72
Cu _{0.4} Ni _{0.6}	3.3	6.3	-
CuMo	3.3	6.9	-
Cu	3.0	8.4	-
Ni	3.0	4.5	-

Table S3 Catalytic activities for the dehydrogenation of $N_2H_4BH_3$ catalyzed by different catalysts.

Catalysts	T (K)	$n(H_2+N_2)/n(N_2H_4BH_3)$	TOF (h^{-1})	Ref.
$Rh_{0.8}Ni_{0.2}@CeO_x/rGO$	323	6.0	666.7 ^a	S1
$Ni_{0.6}Pt_{0.4}/MSC-30$	303	5.95	661.7 ^a	S4
$Ni_{0.9}Pt_{0.1}/graphene$	323	6.0	240 ^a	S2
$Ni_{0.9}Pt_{0.1}-CeO_2$	323	5.74	234 ^a	S3
$Cu_{0.4}Ni_{0.6}Mo$	323	6	108 ^a	This work
Rh_4Ni NPs	323	5.8	90.0 ^b	S5
$Ni@(Rh_4Ni-alloy)/Al_2O_3$	323	5.74	72.0 ^a	S6
$Ni_{0.77}Ru_{0.23}$ NPs	323	4.0	23.3 ^a	S7
$Ni_{0.89}Pt_{0.11}$ NPs	323	5.79	18.0 ^a	S8
$Ni_{0.89}Rh_{0.11}$ NPs	323	5.1	9.9 ^a	S7
$Ni_{0.89}Ir_{0.11}$ NPs	323	4.9	9.5 ^a	S7
$Ni_5@Pt$	323	4.4	2.3 ^a	S9

^aThe total TOF values were calculated according to the original data provided by the reports.

^bThe total TOF values were provided by the reports.

Calculation method for TOF

The turn over frequency (*TOF*) reported in this work is an apparent *TOF* value based on the number of metal (Cu + Ni + Mo) atoms in catalysts, which is calculated from the equation as follows:

$$TOF = \frac{nH_2}{n_{metal} \times t} \quad (S1)$$

Where nH_2 is the mole number of generated H_2 , n_{metal} is the total mole number of Cu, Ni, and Mo in catalyst and t is the completed reaction time in hour.

References

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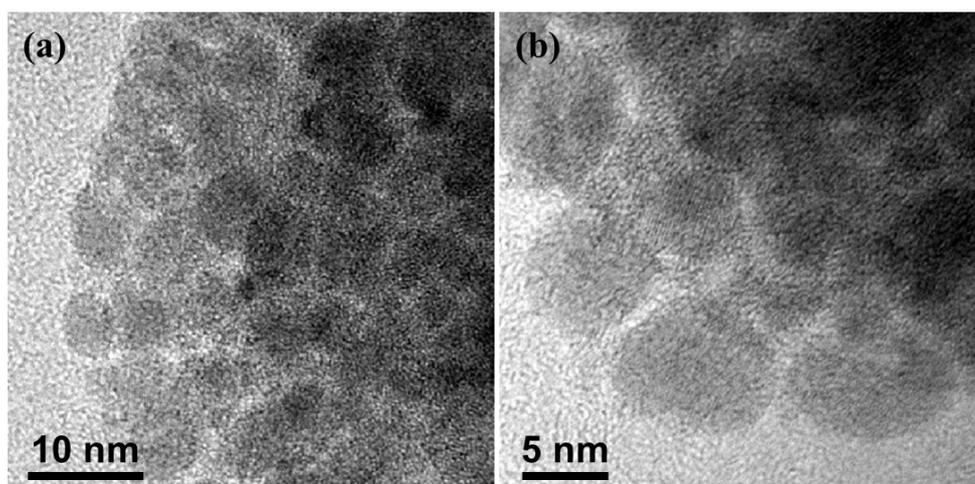


Fig. S1 (a) TEM image and (b) HRTEM image of $\text{Cu}_{0.4}\text{Ni}_{0.6}\text{Mo}$ NPs.

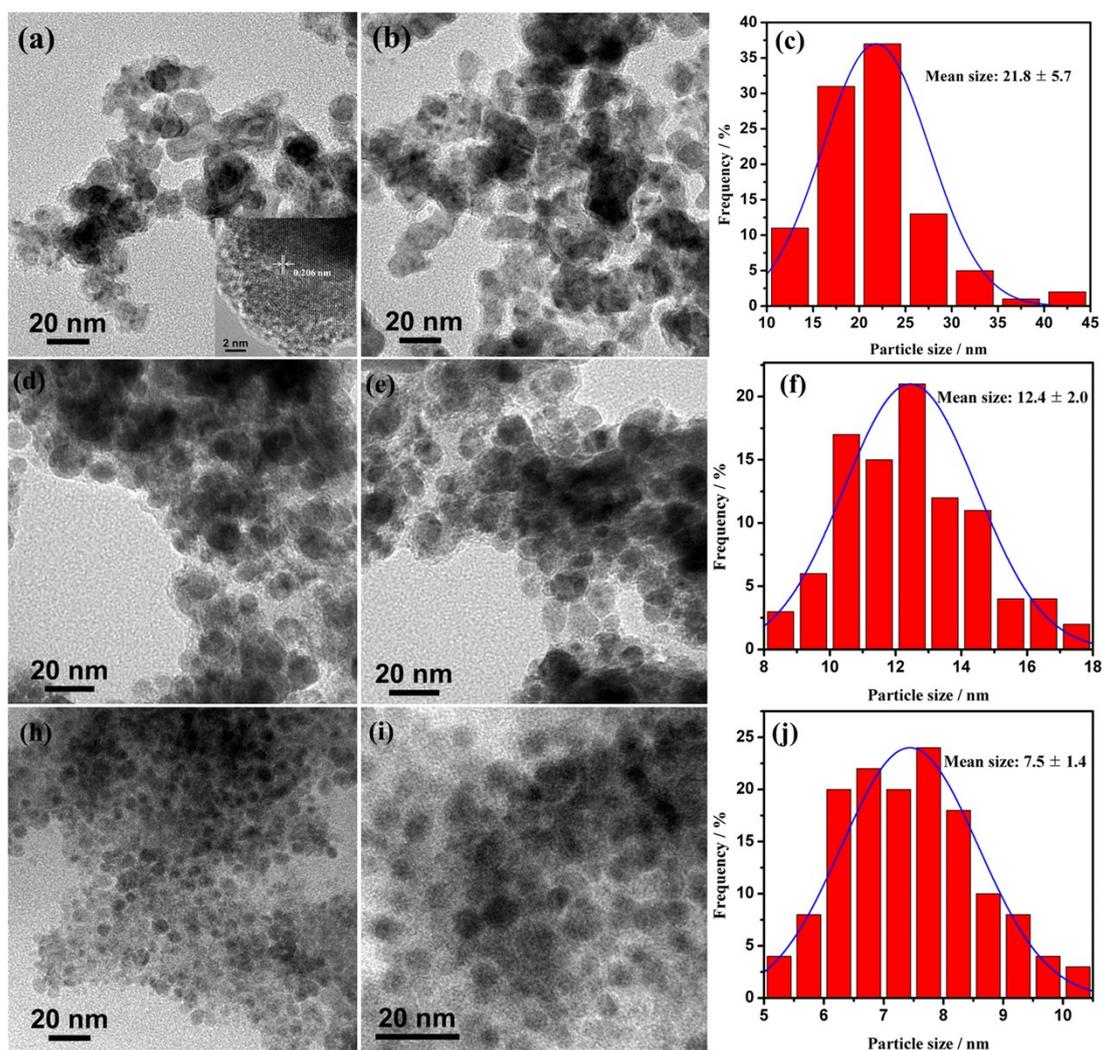


Fig. S2 TEM images and the corresponding particle size distribution of (a-b) $\text{Cu}_{0.4}\text{Ni}_{0.6}$, (d-f) $\text{Cu}_{0.4}\text{Ni}_{0.6}\text{Mo}_{0.1}$, and (h-j) $\text{Cu}_{0.4}\text{Ni}_{0.6}\text{Mo}_{0.6}$ NPs. The inset of (a) is the HRTEM image of $\text{Cu}_{0.4}\text{Ni}_{0.6}$ NPs.

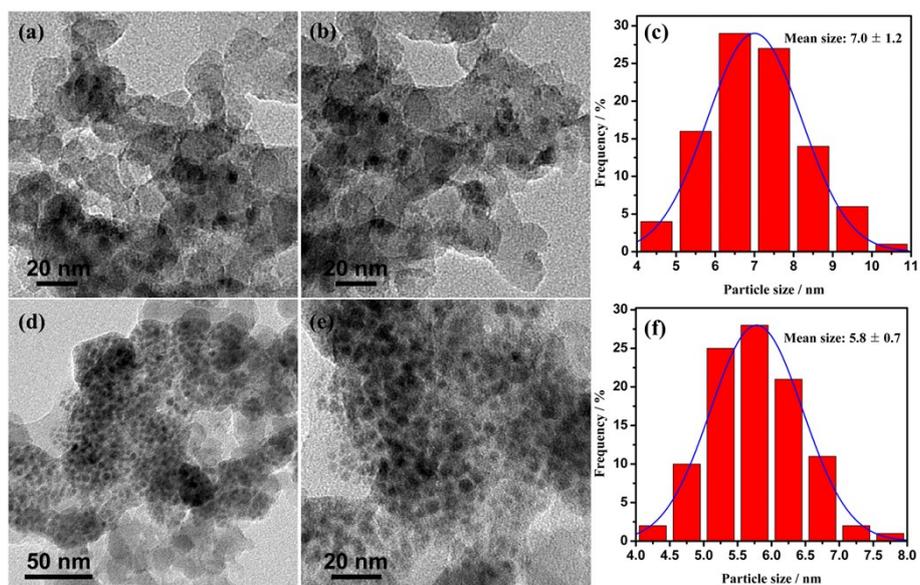


Fig. S3 TEM images and the corresponding particle size distribution of (a-c) $\text{Cu}_{0.4}\text{Ni}_{0.6}/\text{SiO}_2$ and (d-f) $\text{Cu}_{0.4}\text{Ni}_{0.6}\text{Mo}/\text{SiO}_2$ (2.0 wt%, commercial SiO_2 , 200 $\text{m}^2 \text{g}^{-1}$, Degussa).

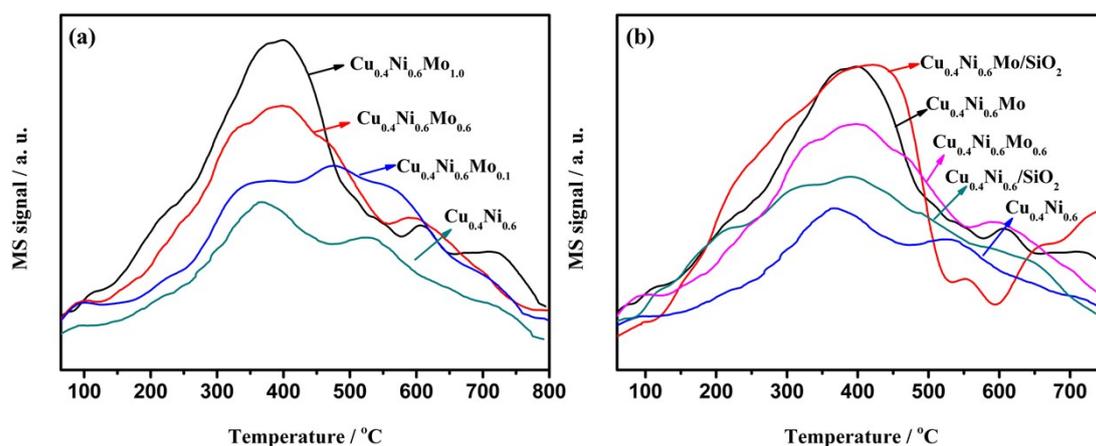


Fig. S4 CO₂-TPD mass spectra for the (a) Cu_{0.4}Ni_{0.6}Mo_x (x = 0, 0.1, 0.6, and 1.0) and (b) Cu_{0.4}Ni_{0.6}, Cu_{0.4}Ni_{0.6}/SiO₂ (2.0 wt%), Cu_{0.4}Ni_{0.6}Mo, Cu_{0.4}Ni_{0.6}Mo_{0.6}, and Cu_{0.4}Ni_{0.6}Mo/SiO₂ (2.0 wt%, commercial SiO₂, 200 m² g⁻¹, Degussa).

As shown in Fig. S4a, the basic sites of the Cu_{0.4}Ni_{0.6}Mo_x NPs (x = 0, 0.1, 0.6, and 1.0) tend to gradually strengthen with the increase of Mo content. The above TEM results (Fig. S2) show that the particle size of Cu_{0.4}Ni_{0.6}Mo_x decreases as the Mo content increases. In addition, it is also found that the strength of basic sites of the Cu_{0.4}Ni_{0.6}/SiO₂ (7.0 nm, Fig. S3c) is higher than that of Cu_{0.4}Ni_{0.6} (larger size, 21.8 nm, Fig. S2c). These results show that the basic sites of sample increase with the decrease of the particle size. To eliminate the effect of particle size on CO₂-TPD strength, the similar particle size of Cu_{0.4}Ni_{0.6}/SiO₂ (7.0 nm, Fig. S3) and Cu_{0.4}Ni_{0.6}Mo/SiO₂ (5.8 nm, Fig. S3) were synthesized and analyzed by CO₂-TPD measurement. As exhibited in Fig. S4b, the strength of basic sites of the Cu_{0.4}Ni_{0.6}Mo/SiO₂ (5.8 nm, Fig. S3), Cu_{0.6}Ni_{0.4}Mo (5.9 nm, Fig. 1b), and Cu_{0.6}Ni_{0.4}Mo_{0.6} (7.5 nm, Fig. S2) are higher than that of Cu_{0.4}Ni_{0.6}/SiO₂ (7.0 nm, Fig. S3), indicating that the introduction of Mo into Cu_{0.4}Ni_{0.6} NPs can strengthen the basic sites. Therefore, it is reasonable to conclude that the strength of basic sites of catalyst is related to not only the particle size, but also the composition of the catalyst.

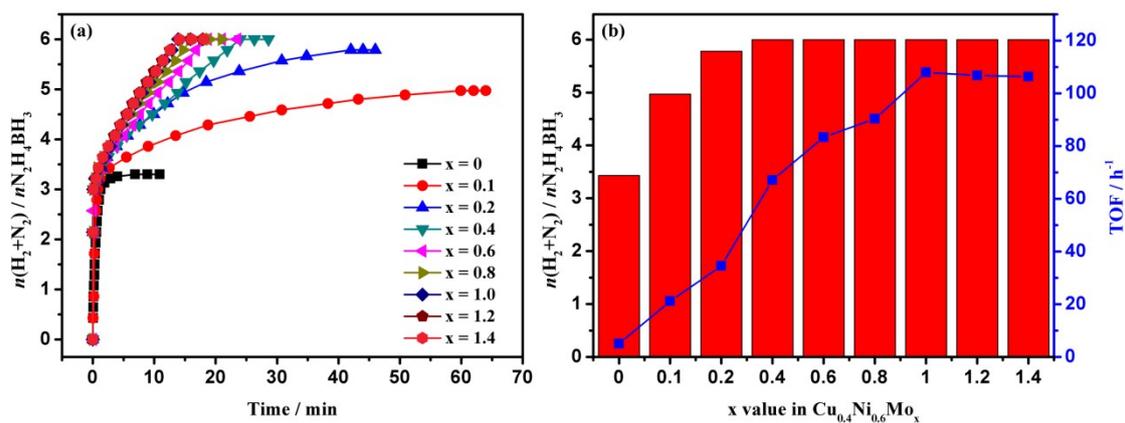


Fig. S5 (a) Time-course plots and (b) Mo-content dependence of $n(\text{H}_2 + \text{N}_2)/n\text{NH}_4\text{BH}_3$ and TOF values for the dehydrogenation of $\text{N}_2\text{H}_4\text{BH}_3$ aqueous solution (0.2 M, 5 mL) catalyzed by $\text{Cu}_{0.4}\text{Ni}_{0.6}\text{Mo}_x$ catalysts with different Mo molar contents in the presence of NaOH (2.0 M) at 323K ($x = n_{\text{Mo}}/n_{\text{Cu+Ni}}$; $n_{\text{Cu+Ni}} = 0.1$ mmol).

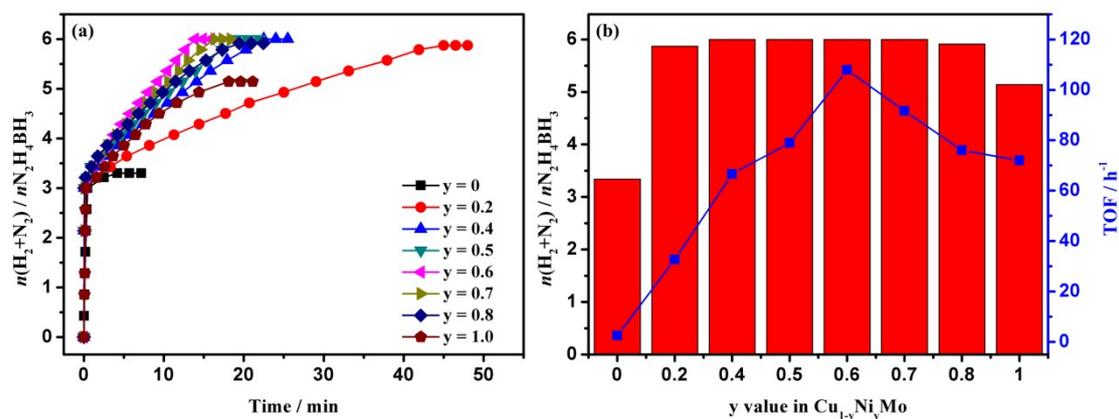


Fig. S6 (a) Time-course plots and (b) Cu/Ni compositional dependence of $n(\text{H}_2 + \text{N}_2)/n\text{NH}_4\text{BH}_3$ and TOF values for the dehydrogenation of $\text{N}_2\text{H}_4\text{BH}_3$ aqueous solution (0.2 M, 5 mL) catalyzed by $\text{Cu}_{1-y}\text{Ni}_y\text{Mo}$ NPs with different compositions of Cu and Ni in the presence of NaOH (2.0 M) at 323 K ($n_{\text{metal}}/n_{\text{N}_2\text{H}_4\text{BH}_3} = 0.2$).

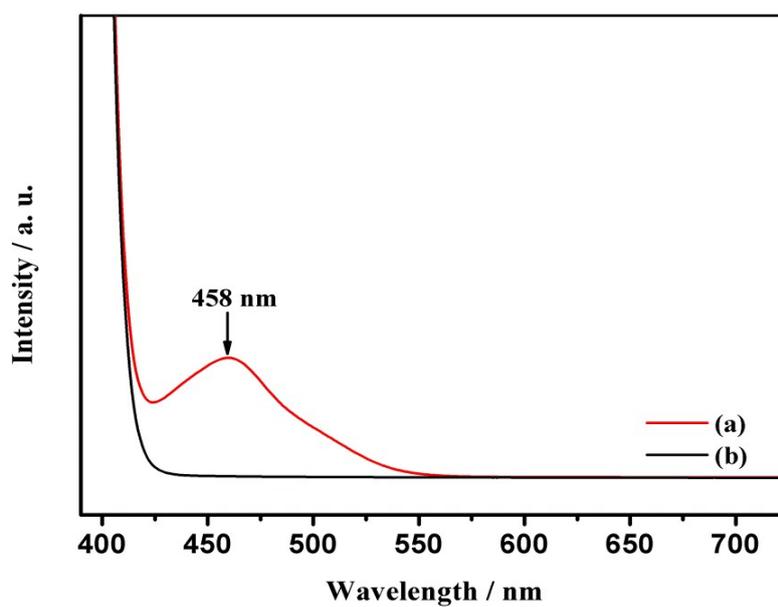


Fig. S7 UV-Vis spectra of $N_2H_4BH_3$ (a) before and (b) after the completion of $N_2H_4BH_3$ dehydrogenation reaction catalyzed by the $Cu_{0.4}Ni_{0.6}Mo$ NPs. After the catalytic reaction, the reaction solution was obtained by centrifuging the reaction suspension to separate the solution and the $Cu_{0.4}Ni_{0.6}Mo$ NPs.

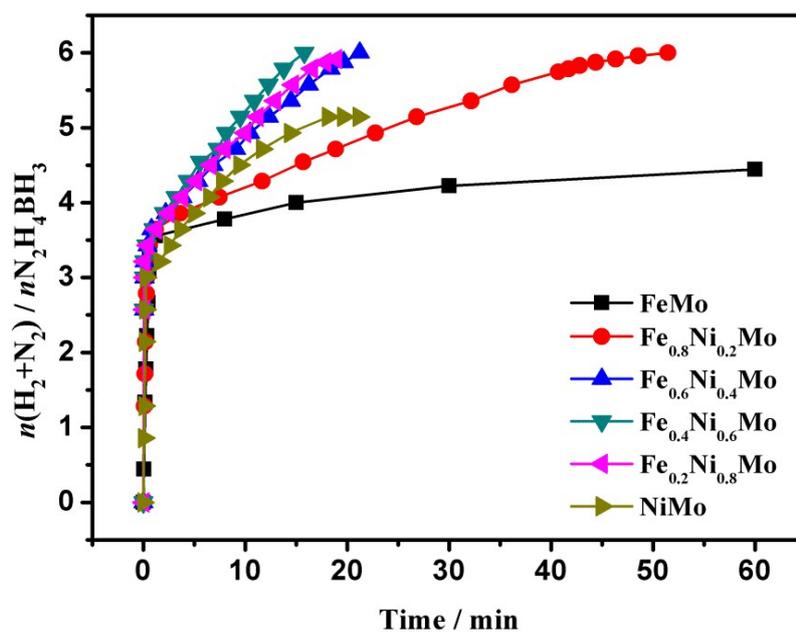


Fig. S8 Time-course plots for the dehydrogenation of $N_2H_4BH_3$ aqueous solution (0.2 M, 5 mL) catalyzed by $Fe_{1-y}Ni_yMo$ NPs with different compositions of Fe and Ni in the presence of NaOH (2.0 M) at 323 K ($n_{metal}/n_{N_2H_4BH_3} = 0.2$).

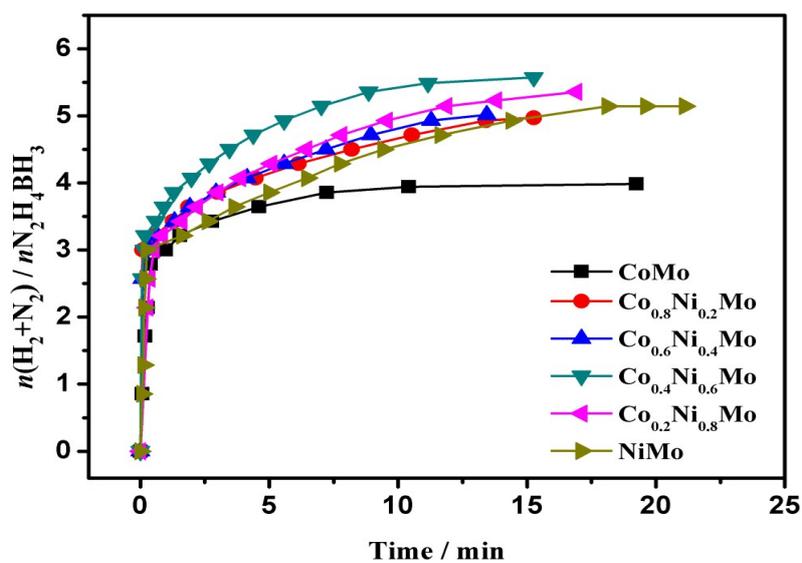


Fig. S9 Time-course plots for the dehydrogenation of $N_2H_4BH_3$ aqueous solution (0.2 M, 5 mL) catalyzed by $Co_{1-y}Ni_yMo$ NPs with different compositions of Co and Ni in the presence of NaOH (2.0 M) at 323 K ($n_{metal}/n_{N_2H_4BH_3} = 0.2$).

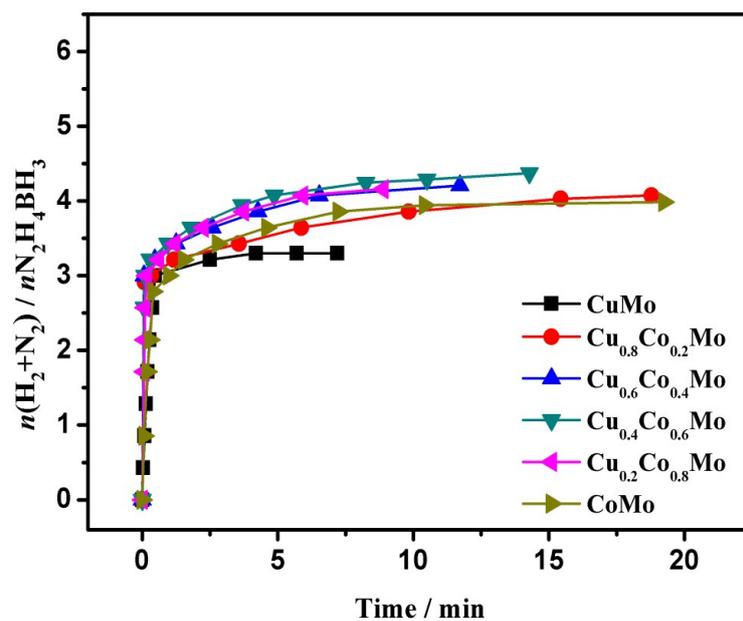


Fig. S10 Time-course plots for the dehydrogenation of $\text{N}_2\text{H}_4\text{BH}_3$ aqueous solution (0.2 M, 5 mL) catalyzed by $\text{Cu}_{1-y}\text{Co}_y\text{Mo}$ NPs with different compositions of Cu and Co in the presence of NaOH (2.0 M) at 323 K ($n_{\text{metal}}/n_{\text{N}_2\text{H}_4\text{BH}_3} = 0.2$).

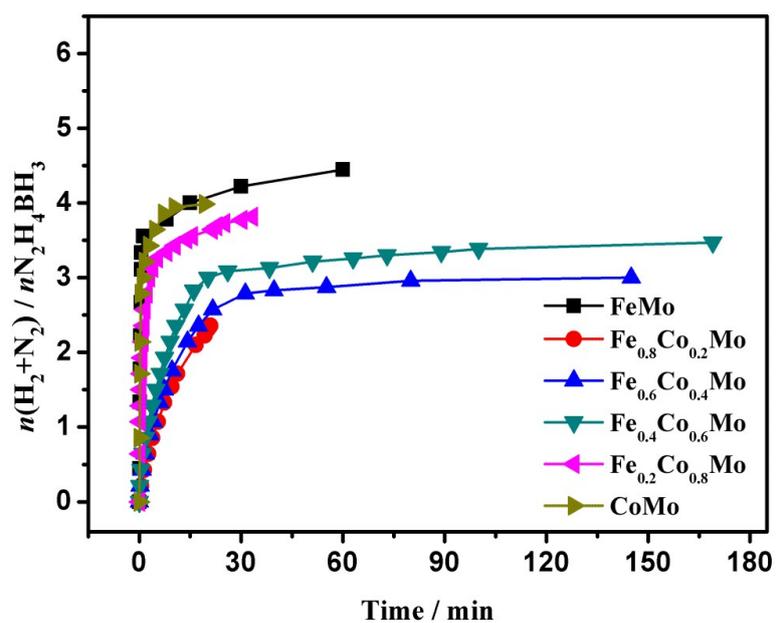


Fig. S11 Time-course plots for the dehydrogenation of $N_2H_4BH_3$ aqueous solution (0.2 M, 5 mL) catalyzed by $Fe_{1-y}Co_yMo$ NPs with different compositions of Fe and Co in the presence of NaOH (2.0 M) at 323 K ($n_{metal}/n_{N_2H_4BH_3} = 0.2$).

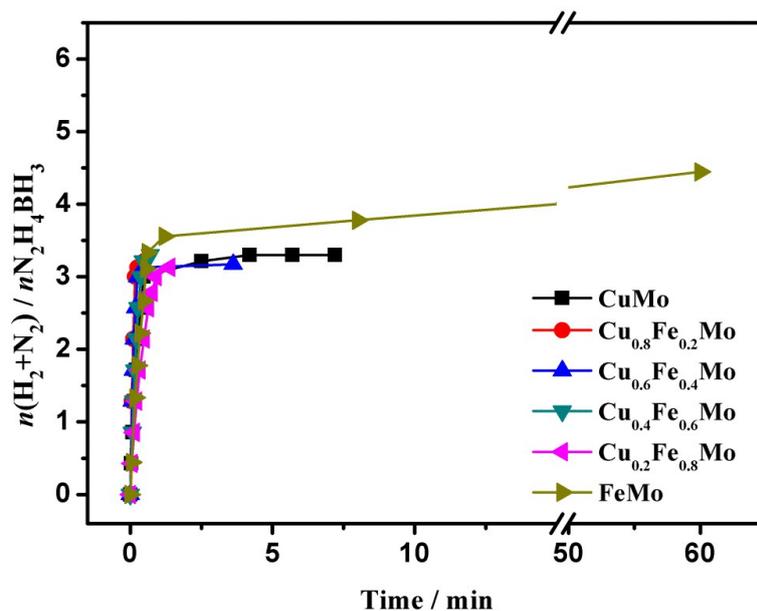


Fig. S12 Time-course plots for the dehydrogenation of $\text{N}_2\text{H}_4\text{BH}_3$ aqueous solution (0.2 M, 5 mL) catalyzed by $\text{Cu}_{1-y}\text{Fe}_y\text{Mo}$ NPs with different compositions of Cu and Fe in the presence of NaOH (2.0 M) at 323 K ($n_{\text{metal}}/n_{\text{N}_2\text{H}_4\text{BH}_3} = 0.2$).

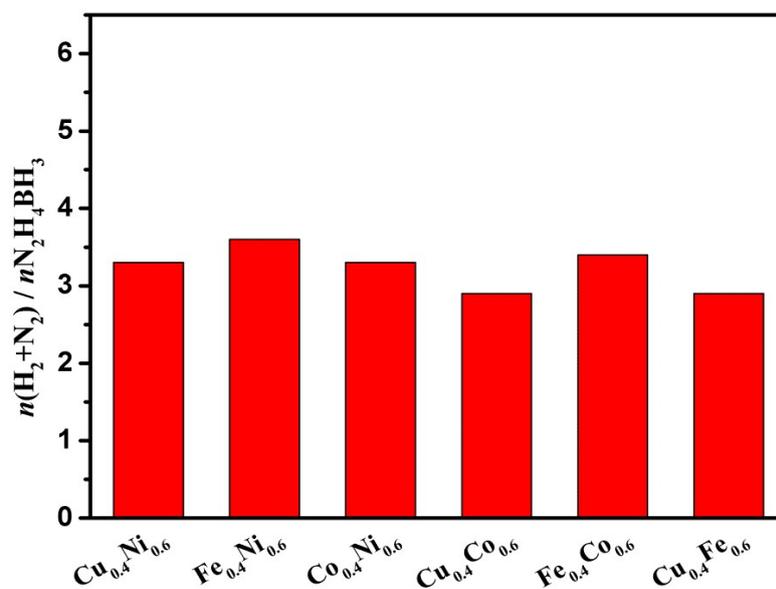


Fig. S13 Time-course plots for the dehydrogenation of N₂H₄BH₃ aqueous solution (0.2 M, 5 mL) catalyzed by different catalysts in the presence of NaOH (2.0 M) at 323 K ($n_{\text{metal}}/n_{\text{N}_2\text{H}_4\text{BH}_3} = 0.1$).

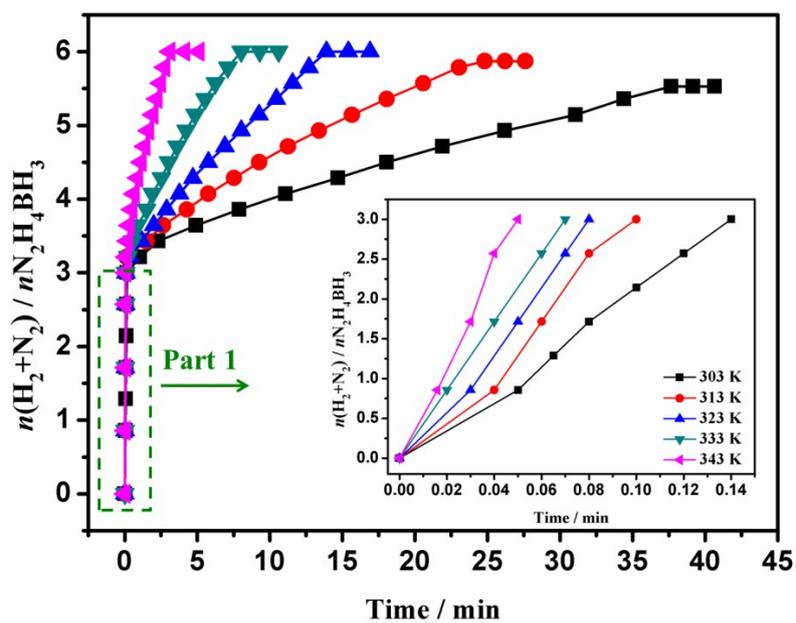


Fig. S14 Time-course plots for the dehydrogenation of $N_2H_4BH_3$ aqueous solution (0.2 M, 5 mL) catalyzed by $Cu_{0.4}Ni_{0.6}Mo$ catalysts in the presence of NaOH (2.0 M) at different temperatures ($n_{metal}/n_{N_2H_4BH_3} = 0.2$). Inset shows the enlarged region with part 1 to see clearly.

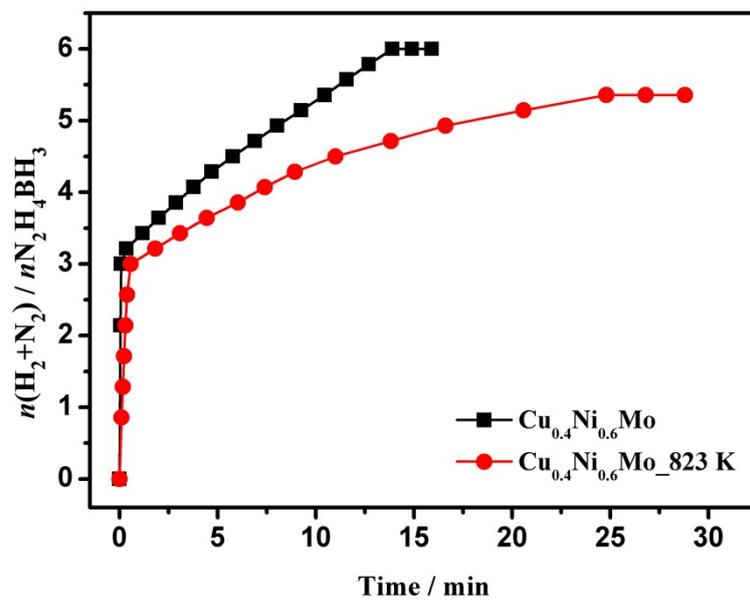


Fig. S15 Time-course plots for the dehydrogenation of $\text{N}_2\text{H}_4\text{BH}_3$ aqueous solution (0.2 M, 5 mL) catalyzed by $\text{Cu}_{0.4}\text{Ni}_{0.6}\text{Mo}$ NPs before and after heat treatment at 823 K in the presence of NaOH (2.0 M) at 323 K ($n_{\text{metal}}/n\text{N}_2\text{H}_4\text{BH}_3 = 0.2$).

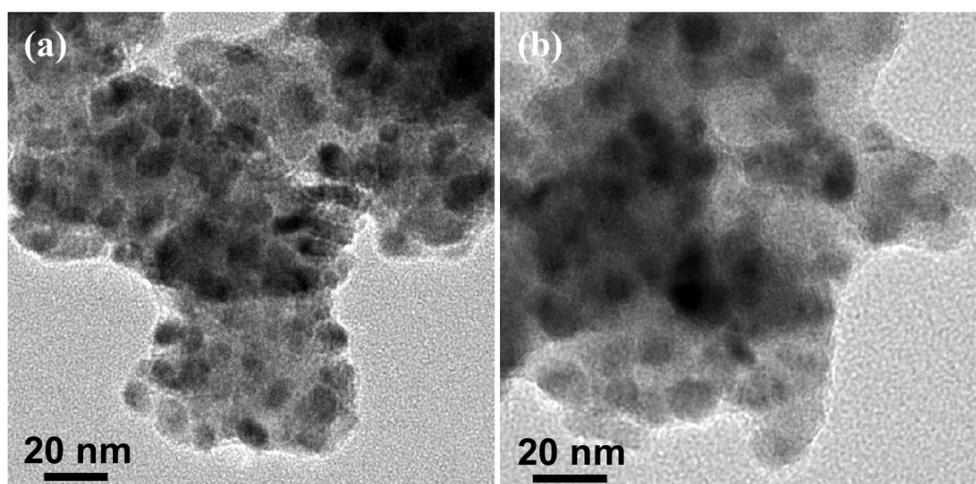


Fig. S16 (a,b) TEM images of $\text{Cu}_{0.4}\text{Ni}_{0.6}\text{Mo}$ NPs after heat treatment at 823 K for 3 h under Ar atmosphere in tube furnace.

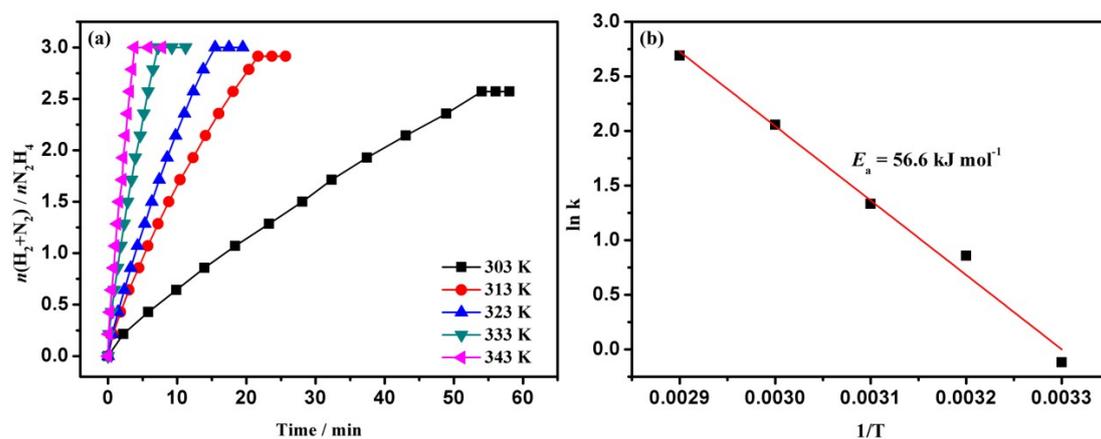


Fig. S17 (a) Time-course plots for the dehydrogenation of $\text{N}_2\text{H}_4 \cdot \text{H}_2\text{O}$ aqueous solution (0.2 M, 5 mL) catalyzed by $\text{Cu}_{0.4}\text{Ni}_{0.6}\text{Mo}$ catalysts in the presence of NaOH (2.0 M) at different temperatures ($n_{\text{metal}}/n_{\text{N}_2\text{H}_4} = 0.2$). (b) The corresponding Arrhenius plot.

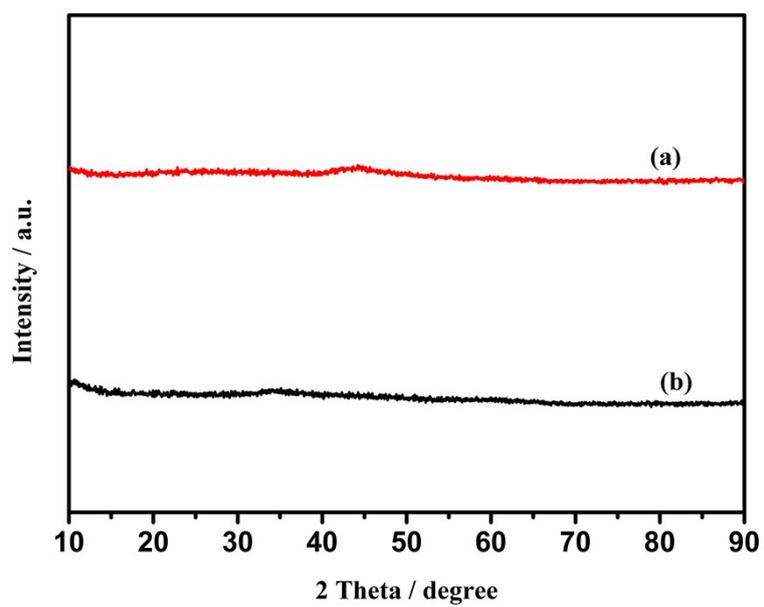


Fig. S18 X-ray diffraction patterns of $\text{Cu}_{0.4}\text{Ni}_{0.6}\text{Mo}$ NPs (a) before and (b) after the durability test.

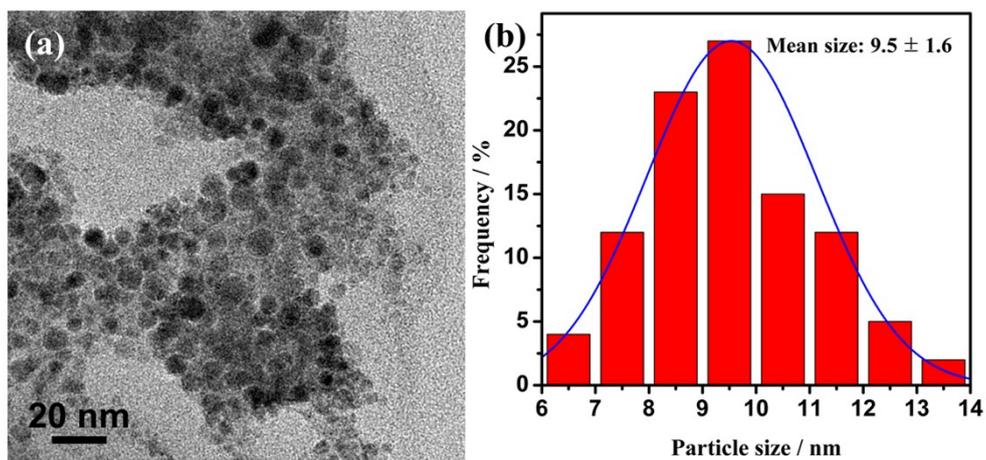


Fig. S19 (a) TEM image and (b) the corresponding particle size distribution of $\text{Cu}_{0.4}\text{Ni}_{0.6}\text{Mo}$ NPs after the durability test.