

Electronic Supplementary Material (ESI) for Catalysis Science & Technology

Supplementary Information for

Synthesis and catalytic application of alumina@SAPO-11 composite *via* the *in situ* assembly of silicoaluminophosphate nanoclusters at an alumina substrate

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1. Supplementary Figures and Tables



Fig. S1 Photographs of the products synthesized following the procedure of alumina@SAPO-11 without adding CTAB.

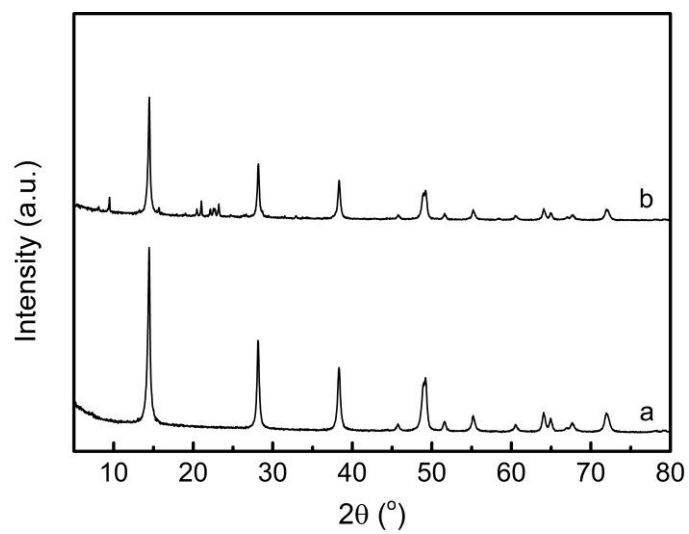


Fig. S2 XRD patterns of the alumina substrate modified without H_3PO_4 (a) and the product synthesized from alumina without H_3PO_4 modification (b).

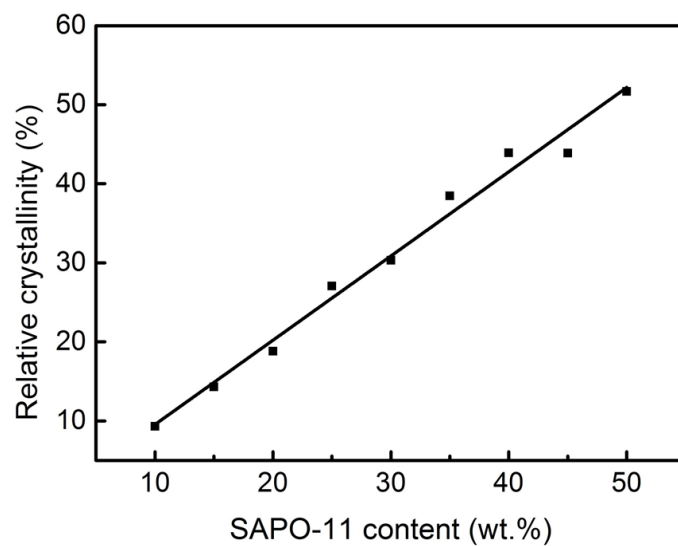


Fig. S3 The relationship between the SAPO-11 content and the relative crystallinity. This curve was obtained by plotting the relative crystallinity of SAPO-11 versus the mass fraction of SAPO-11 in a series of mechanical mixtures of pure SAPO-11 and H_3PO_4 modified alumina.

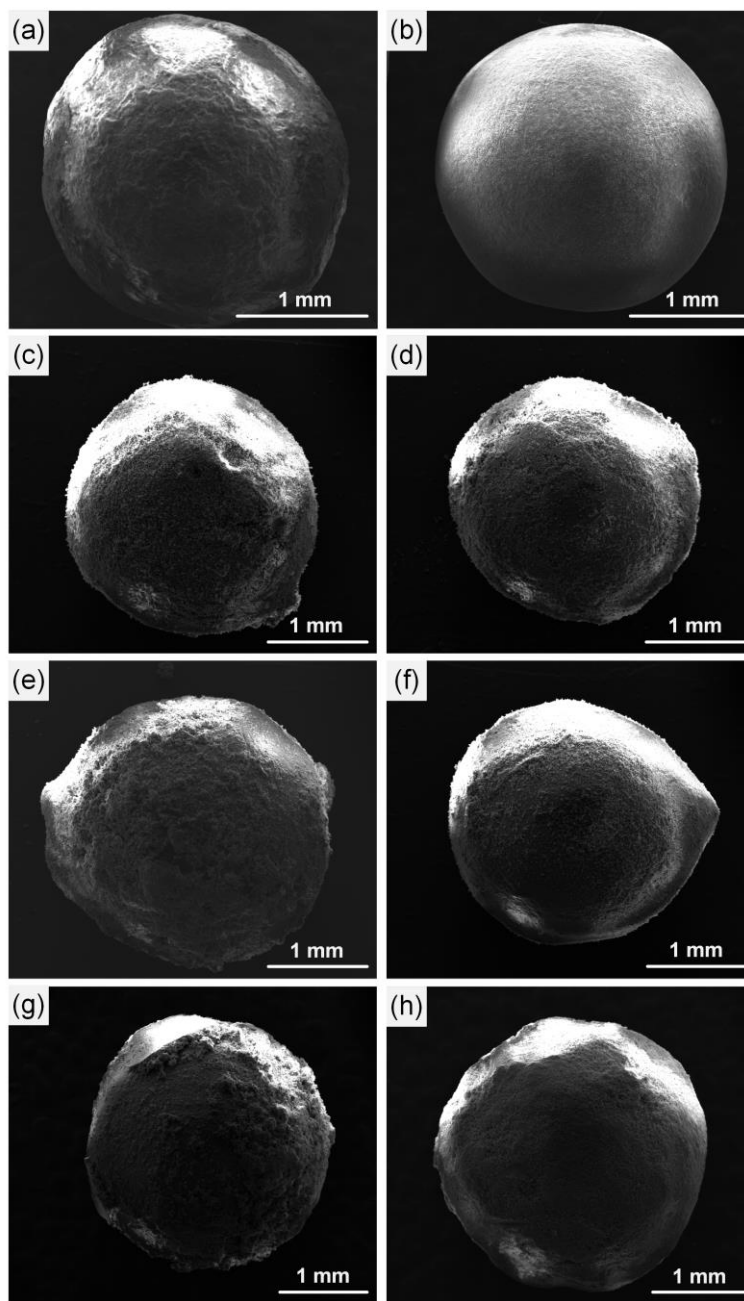


Fig. S4 SEM images of the top-view of the alumina substrate (a), the H_3PO_4 modified alumina substrate (b), and the alumina@SAPO-11 composite (c-h). *Note: In order to check the homogeneity of the alumina@SAPO-11 composite, several particles were randomly selected for taking the SEM images one by one as shown in c-h.*

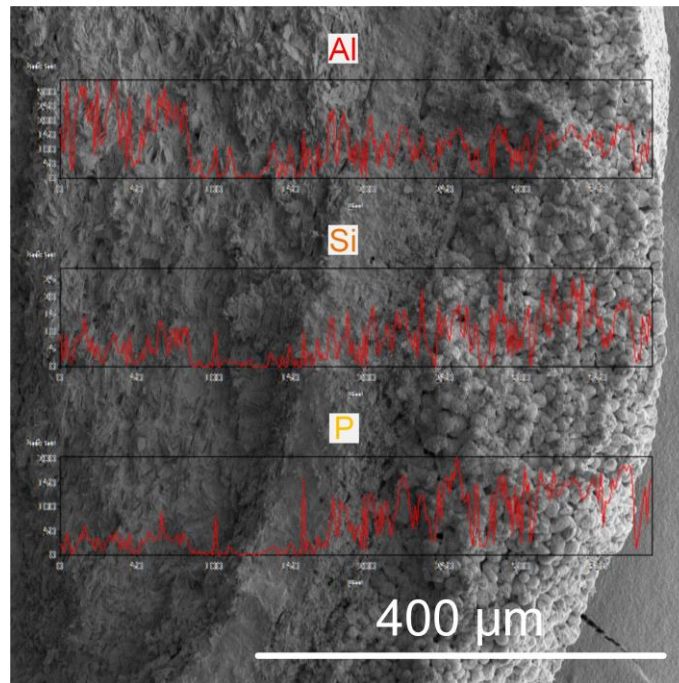


Fig. S5 Line scan analysis for SEM image of the alumina@SAPO-11 composite: Al (red), Si (orange) and P (yellow).

Table S1. Chemical compositions of alumina substrate before/after H₃PO₄ modification.

Sample	Al content ^a %	P content ^a %	Al/P ^b mol/mol
Alumina	52.7	-	∞
H ₃ PO ₄ modified alumina	48.1	3.8	16.6

Notes: ^a Determined by ICP-OES; ^b Determined by XRF.

Table S2. Textural properties of SAPO-11_{reference}, alumina@SAPO-11 and alumina-SAPO-11.

Sample	$S_{\text{BET}}^{\text{a}}$ (m ² /g)	$S_{\text{micro}}^{\text{b}}$ (cm ² /g)	S_{ext} (m ² /g)	$V_{\text{micro}}^{\text{b}}$ (cm ³ /g)	$V_{\text{meso}}^{\text{c}}$ (cm ³ /g)
SAPO-11 _{reference}	154	112	42	0.05	0.10
alumina@SAPO-11	166	41	125	0.02	0.23
alumina-SAPO-11	120	41	79	0.02	0.22

Notes: ^a BET method; ^b *t*-plot method; ^c BJH method (adsorption branch).

Table S3. Product distributions of *n*-octane over Pt/alumina@SAPO-11 and Pt/alumina-SAPO-11.^a

	Pt/alumina@SAPO-11	Pt/alumina-SAPO-11
Conversion (%)	66.9	45.9
Product composition w_i^b		
2-MC ₇	35.4	41.6
3-MC ₇	38.8	37.6
4-MC ₇	10.2	8.5
2,5-DMC ₆	5.0	3.4
2,4-DMC ₆	4.1	2.4
2,3-DMC ₆	2.4	1.2
2,2-DMC ₆	0.9	0.1
<i>i</i> -C ₅	1.8	2.6
<i>n</i> -C ₅	1.1	1.9
2-MC ₅	0.1	0.0
3-MC ₅	0.0	0.0
<i>n</i> -C ₆	0.0	0.1
2-MC ₆	0.1	0.2
3-MC ₆	0.1	0.2
<i>n</i> -C ₇	0.0	0.2
Total	100.0	100.0

Notes: ^a Reaction conditions: Tests were conducted in a continuous flow tubular fixed-bed micro-reactor, $W_{\text{cat}} = 5$ g, 1.5 MPa, 360 °C, H₂/*n*-octane volumetric ratio 300, weight hourly space velocity 1.5 h⁻¹; ^b w_i is the mass fraction of component *i* in the liquid product.

Table S4. Results of *n*-octane hydroisomerization over Pt/alumina@SAPO-11 and Pt/alumina-SAPO-11 at the same level of conversion of 41%.^a

	Pt/alumina@SAPO-11	Pt/alumina-SAPO-11
Selectivity (%)		
S_{MB}^b	85.5	85.7
S_{DB}^b	8.2	6.1
S_C^b	6.3	8.2
S_{DB}/S_C	1.3	0.7
MON ^c	34.7	33.3
RON ^c	28.9	27.9

Notes: ^a Reaction conditions: Tests were conducted in a continuous flow tubular fixed-bed micro-reactor, $W_{cat} = 5$ g, 1.5 MPa, 360 °C, H_2/n -octane volumetric ratio 300, weight hourly space velocity 4.0 and 2.0 h^{-1} , respectively; ^b S_{MB} , S_{DB} and S_C correspond to the total selectivity to mono-branched C_8 isomers, total selectivity to di-branched C_8 isomers, and total selectivity to cracking products, respectively, at 41% conversion of *n*-octane; ^c MON (motor octane number) and RON (research octane number) are calculated according to the following formula: octane number = $\sum(a_i w_i)$, in which a_i is the octane number of component i and w_i is the mass fraction of component i ;¹ and the RON and MON data for each component in the liquid product are adapted from *Technical Data Book-Petroleum Refining* by API (American Petroleum Institute).

Table S5. Product distributions of *n*-octane over Pt/alumina@SAPO-11 and Pt/alumina-SAPO-11.^a

	Pt/alumina@SAPO-11	Pt/alumina-SAPO-11
Conversion (%)	41.3	41.6
Product composition w_i^b		
2-MC ₇	38.1	41.7
3-MC ₇	39.6	39.1
4-MC ₇	11.1	8.0
2,5-DMC ₆	2.8	3.0
2,4-DMC ₆	2.9	1.8
2,3-DMC ₆	1.8	1.1
2,2-DMC ₆	1.1	0.1
<i>i</i> -C ₅	1.4	1.6
<i>n</i> -C ₅	0.9	2.1
2-MC ₅	0.1	0.1
3-MC ₅	0.1	0.0
<i>n</i> -C ₆	0.0	0.1
2-MC ₆	0.0	0.9
3-MC ₆	0.1	0.2
<i>n</i> -C ₇	0.0	0.2
Total	100.0	100.0

Notes: ^a Reaction conditions: Tests were conducted in a continuous flow tubular fixed-bed micro-reactor, $W_{\text{cat}} = 5$ g, 1.5 MPa, 360 °C, H₂/*n*-octane volumetric ratio 300, weight hourly space velocity 4.0 and 2.0 h⁻¹, respectively; ^b w_i is the mass fraction of component *i* in the liquid product.

Table S6. Acidity properties of Pt/alumina@SAPO-11 and Pt/alumina-SAPO-11 determined by Py-IR.

Sample	Amount ($\mu\text{mol/g}$) and distribution of acid sites					
	Total acid sites (200 °C)			Medium and strong acid sites (350 °C)		
	B	L	B + L	B	L	B + L
Pt/alumina@SAPO-11	18.3	66.0	84.3	10.2	23.2	33.4
Pt/alumina-SAPO-11	11.0	70.4	81.4	5.7	29.3	35.0

2. References

- 1 R. Sun, S. Shen, D. Zhang, Y. Ren and J. Fan, *Energy Fuels*, 2015, **29**, 7005-7013.