

# Catalytic deoxygenation of C<sub>18</sub> fatty acid over supported metal Ni catalyst promoted by the basic sites of ZnAl<sub>2</sub>O<sub>4</sub> spinel phase

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## Experimental section

All chemicals were purchased from commercial suppliers and used as received without further purification:  $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ ,  $\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ ,  $\text{Al}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ , urea,  $\text{SiO}_2$ , and decalin (Sinopharm, AR standard), oleic acid, stearic acid, and 1-octadecanol (Aladdin, AR standard), *n*-octadecane (Aladdin,  $\geq 99.5\%$  GC standard).

### *Preparation of $\text{ZnAl}_2\text{O}_4$ support*

$\text{ZnAl}_2\text{O}_4$  support was prepared via a hydrothermal synthesis process followed by a thermal treatment. Typically,  $\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (2 mmol),  $\text{Al}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  (4 mmol), and urea (48 mmol) were dissolved into deionized water (40 mL) to form a colorless solution. The solution was then transferred into 100 mL Teflon-lined stainless autoclave and heated at 180 °C for 3 h to produce Zn-Al oxide precursor. After that, the autoclave was cooled naturally to room temperature, and the white precursor was collected by filtration, washed with deionized water to get a neutral pH, and then dried in air at 80 °C overnight. The dried material was then calcined at 750 °C for 4 h to produce the final composite oxide.

### *Preparation of $\text{Ni}/\text{ZnAl}_2\text{O}_4$ and $\text{Ni}/\text{SiO}_2$*

The preparation procedure for the two Ni-based catalysts is the same as described in Section 2.2 in the text.

Table S1. Textural properties of the Zn-Al composite oxides.

Catalyst	BET specific surface area (m <sup>2</sup> /g)	Pore volume (cm <sup>3</sup> /g)	Average pore diameter (nm)
S-120	87.8	0.17	3.9
S-140	86.1	0.22	5.1
S-160	104.2	0.20	3.8
S-180	76.5	0.19	5.0
S-200	77.1	0.20	5.1

Table S2. XPS data for Zn 2p<sub>3/2</sub> spectra of different Ni-based catalysts.

Catalysts	ZnAl <sub>2</sub> O <sub>4</sub>		ZnO	
	BE (eV)	At. (%)	BE (eV)	At. (%)
C-120	1021.6	46.8	1021.2	53.2
C-140	1021.9	50.0	1021.3	50.0
C-160	1022.2	55.1	1021.5	44.9
C-180	1022.7	58.9	1021.7	41.1
C-200	1022.7	64.8	1021.6	35.2

Table S3. The Ni content of different Ni-based catalysts and Ni species distribution.

Catalysts	Ni content (wt.%) [a]	Surface Ni content (wt.%) [b]	Ni <sup>2+</sup>		Ni <sup>0</sup>	
			BE (eV)	At. (%)	BE (eV)	At. (%)
C-120	10.8	9.2	855.3	92.1	851.9	7.9
C-140	11.0	9.2	855.6	86.1	852.1	13.9
C-160	10.5	13.5	855.7	82.2	852.5	17.8
C-180	10.6	18.0	856.2	78.1	853.5	21.9
C-200	10.3	19.6	856.2	75.0	853.1	25.0

[a] The value is determined by ICP-OES analysis.

[b] The value is determined by XPS analysis.

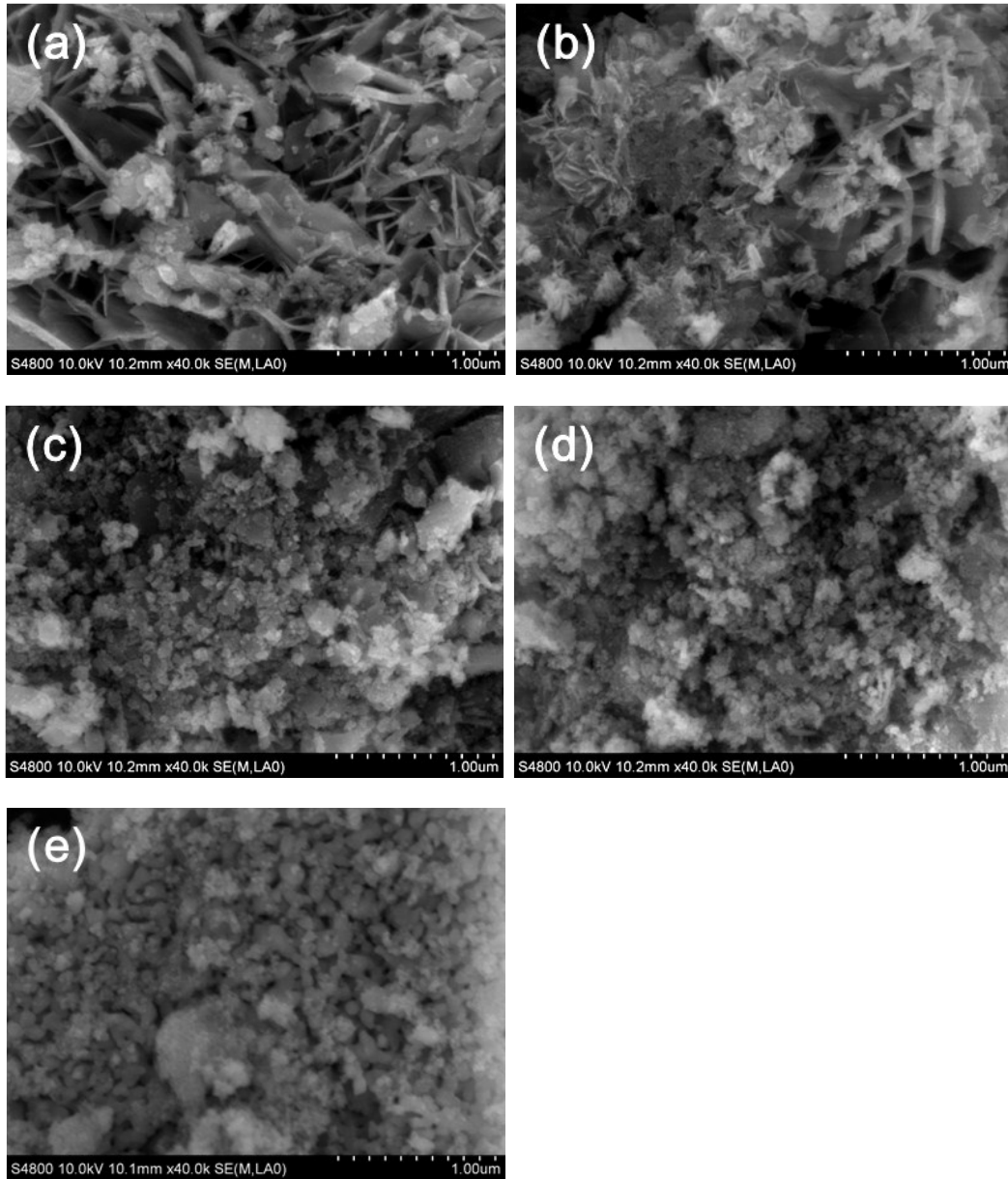


Fig. S1. SEM images of Zn-Al composite oxides: (a) S-120, (b) S-140, (c) S-160, (d) S-180, and (e) S-200.

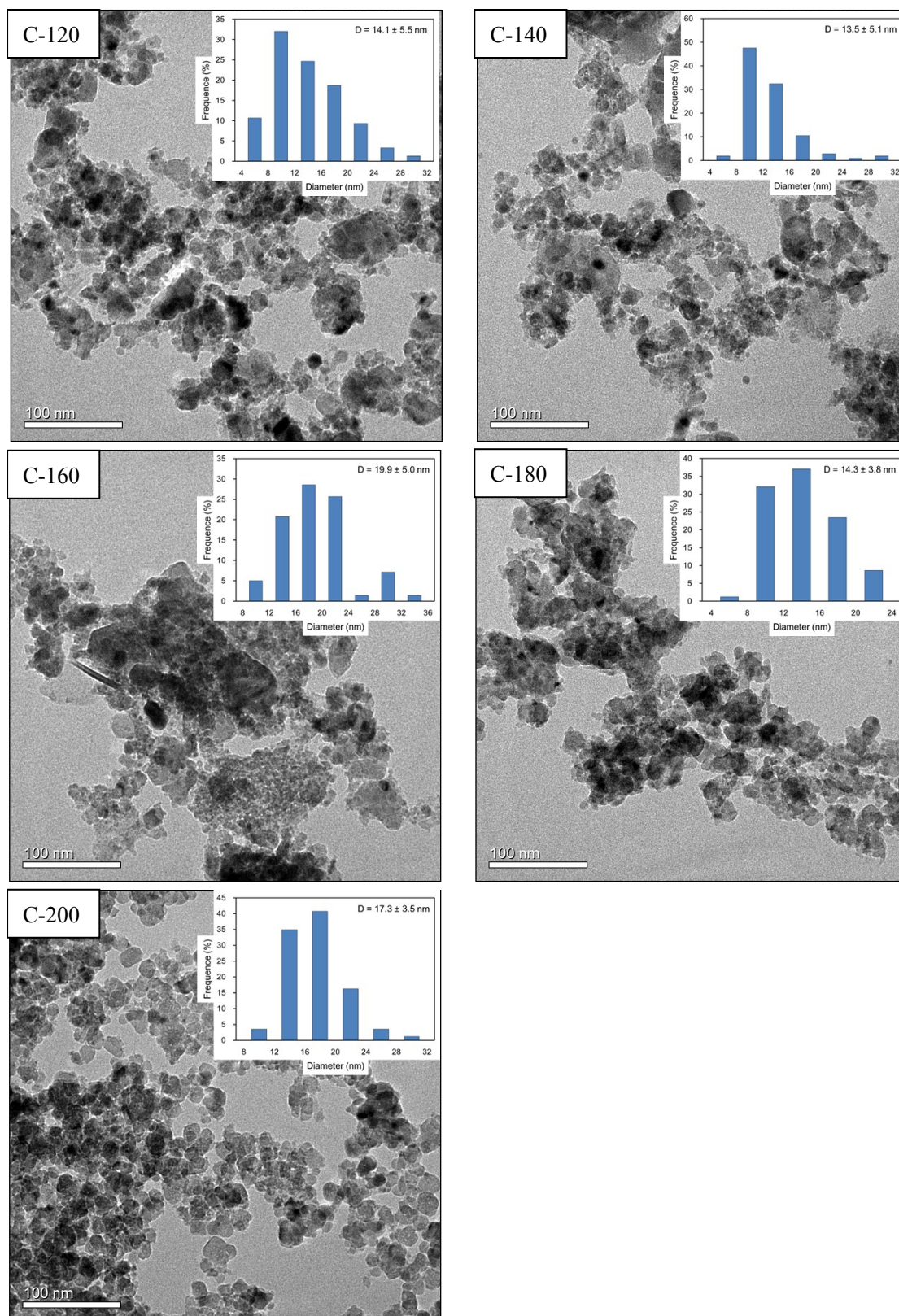


Fig. S2. TEM images of the reduced Ni-based catalysts and their histograms of Ni particle size distribution (inset).

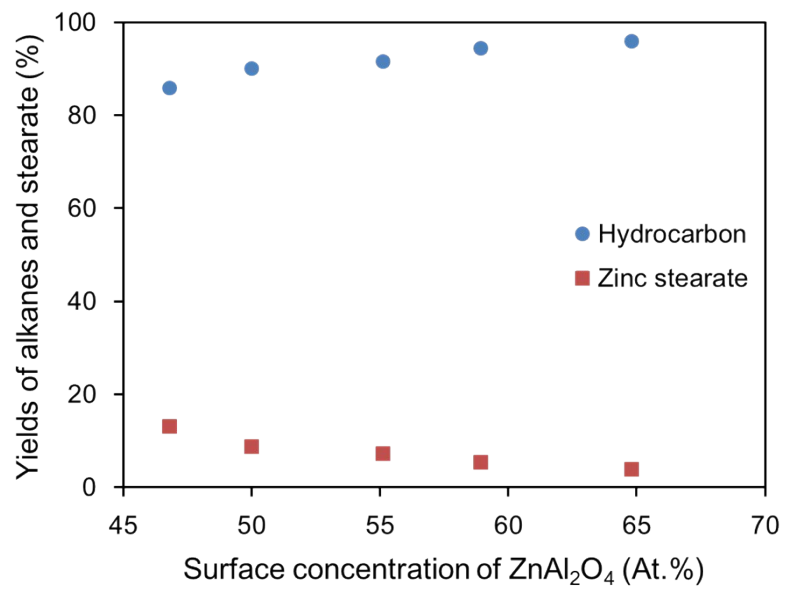


Fig. S3. Yields of heptadecane and zinc stearate as a function of surface concentration of ZnAl<sub>2</sub>O<sub>4</sub> on Ni-based catalysts.



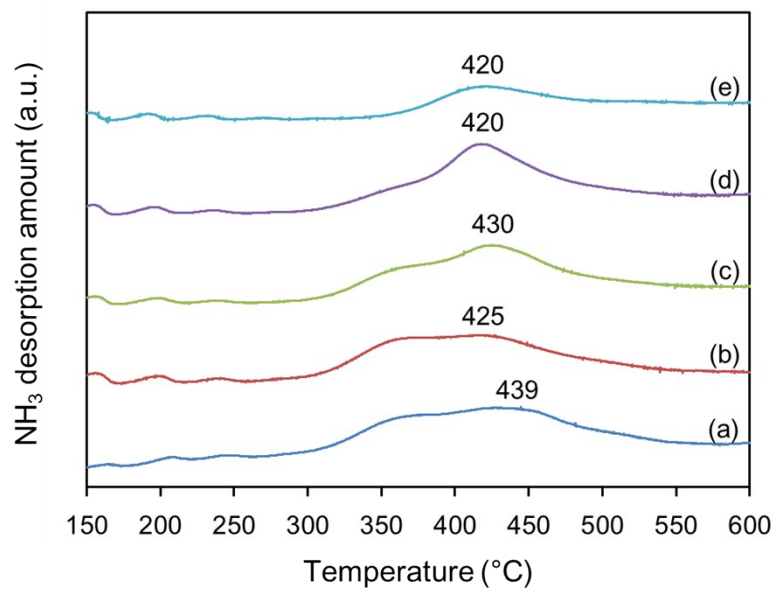


Fig. S4. NH<sub>3</sub>-TPR profiles of Zn-Al composite oxides: (a) S-120, (b) S-140, (c) S-160, (d) S-180, and (e) S-200.

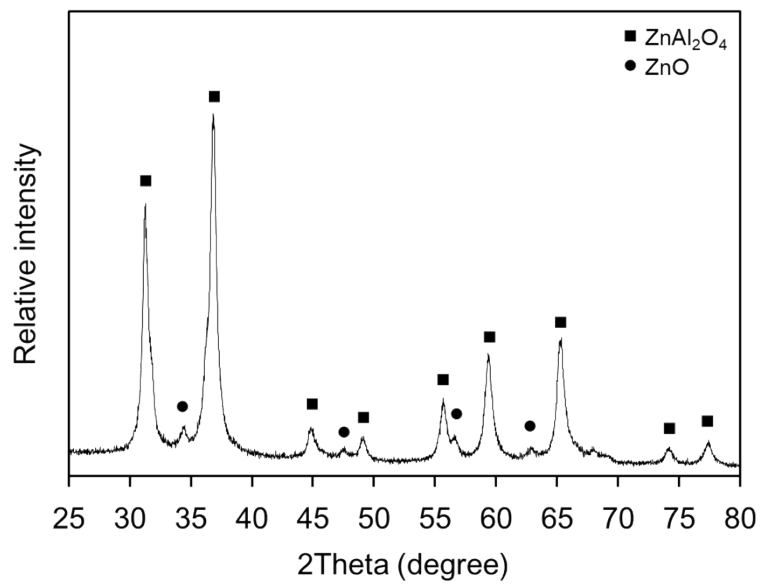


Fig. S5. XRD pattern of ZnAl<sub>2</sub>O<sub>4</sub> support.

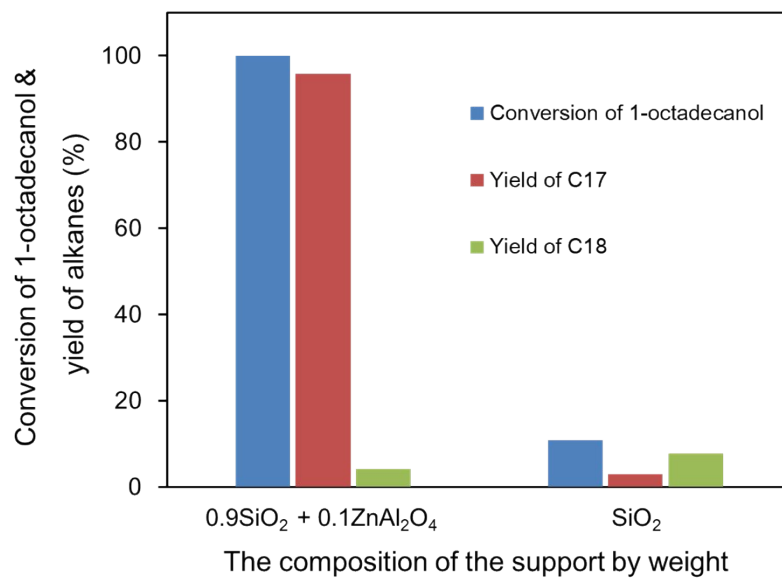


Fig. S6. The effect of addition amount of ZnAl<sub>2</sub>O<sub>4</sub> on the catalytic deoxygenation of 1-octadecanol. Reaction conditions: 1-octadecanol (2.0 g), decalin (30.0 g), catalyst (0.2 g), temperature (280 °C), H<sub>2</sub> pressure (2.5 MPa), and stirring at 600 r/min for 6 h.

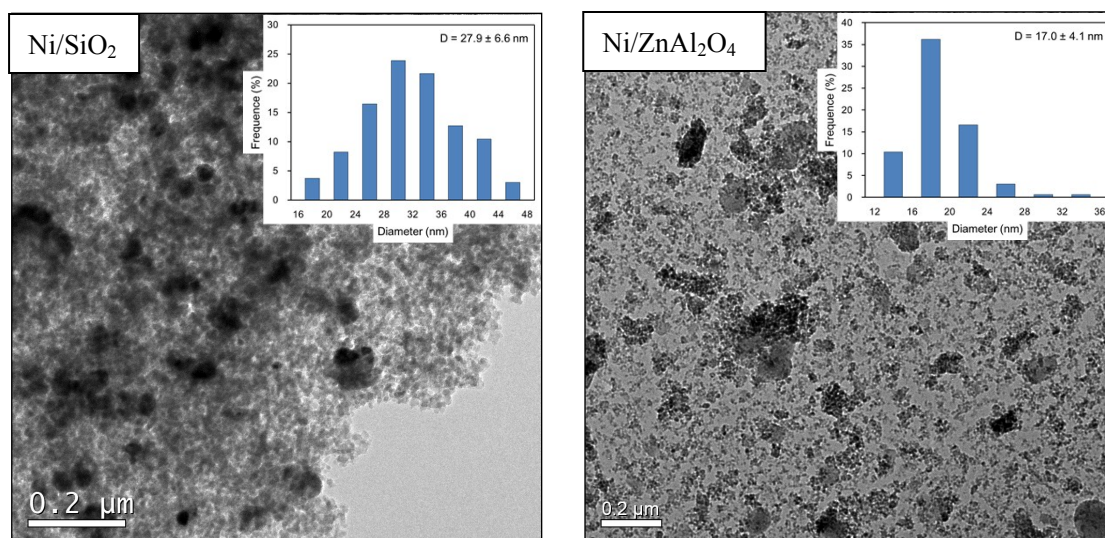


Fig. S7. TEM images of the reduced Ni-based catalysts and their histograms of Ni particle size distribution (inset).

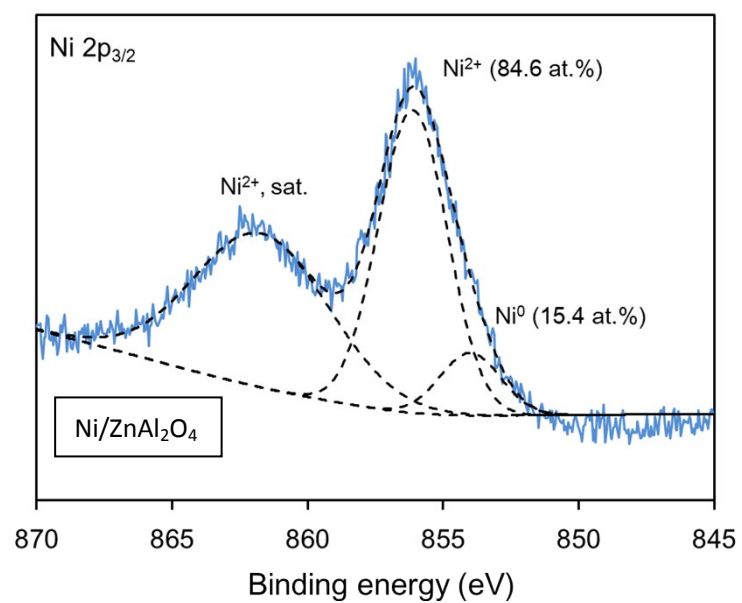
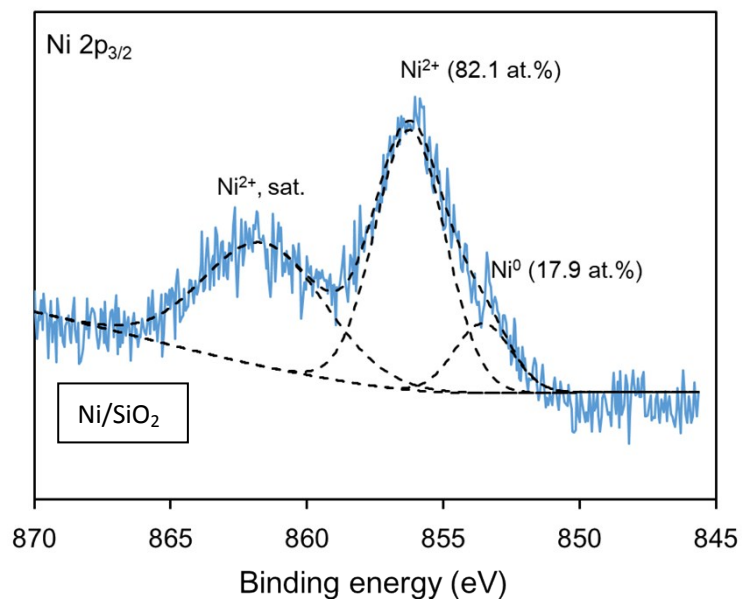


Fig. S8. Ni  $2p_{3/2}$  XPS spectra of Ni/SiO<sub>2</sub> and Ni/ZnAl<sub>2</sub>O<sub>4</sub> catalysts.