

## SUPPLEMENTARY INFORMATION

### Barium-Promoted Hydrothermal Stability of Monolithic Cu/BEA Catalyst for NH<sub>3</sub>-SCR

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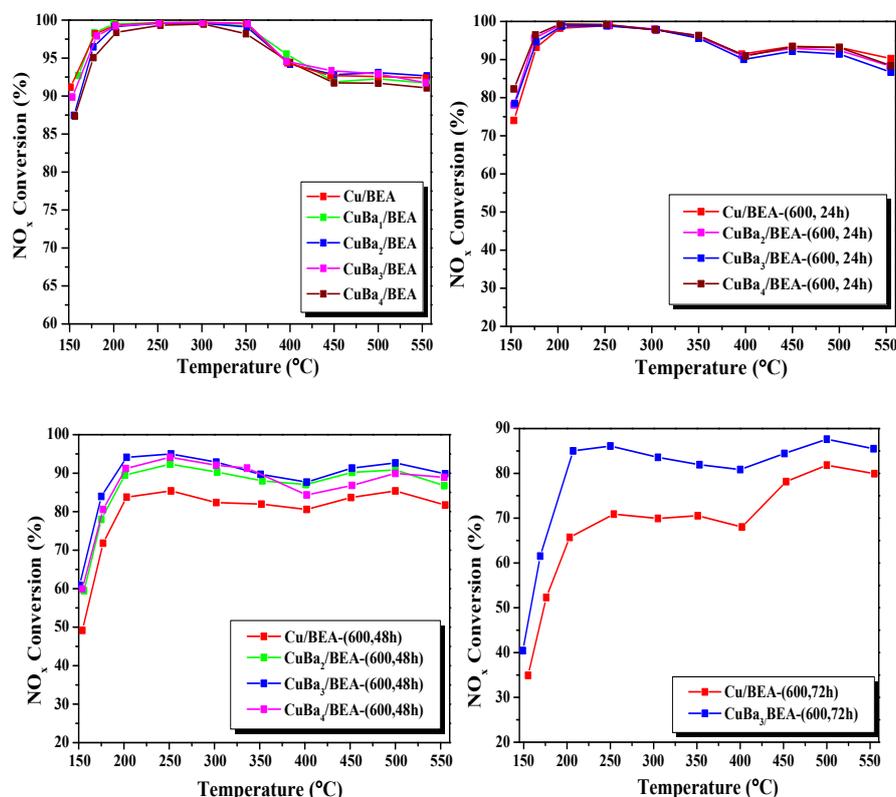
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## 1. NH<sub>3</sub>-SCR activity

Fig. S1 shows the NO<sub>x</sub> conversion as a function of reaction temperatures in NH<sub>3</sub>-SCR over the fresh and hydrothermally aged Cu/BEA and CuBa/BEA. The excellent and similar fresh activity could be achieved over all catalysts, and NO<sub>x</sub> could be converted completely (higher than 90% NO<sub>x</sub> conversion) between 175-550 °C. When the reaction temperature is above 350 °C, the decreased NO<sub>x</sub> conversion could be due to the NH<sub>3</sub> oxidation.

The hydrothermal treatment at 600 °C for different time (24h, 48h, 72h) leads to a significant loss of NO<sub>x</sub> conversion, but it could be found that it results in the less loss of activity over the CuBa/BEA than Cu/BEA (Fig. S1), demonstrating that the addition of Ba could improve the hydrothermal stability of Cu/BEA. Among these catalyst modified by the additive Ba, the best hydrothermal stability is obtained over CuBa<sub>3</sub>/BEA. And the maximum NH<sub>3</sub>-SCR activity over CuBa<sub>3</sub>/BEA-(600, 48h) is 95% NO<sub>x</sub> conversion at 250 °C and it still can remain above 87% NO<sub>x</sub> conversion between 185-550 °C.



**Fig. S1** NO<sub>x</sub> conversion as a function of the reaction temperature over the fresh and hydrothermally aged Cu/BEA and CuBa/BEA during NH<sub>3</sub>-SCR reaction conditions: 200 ppm NO, 200 ppm NH<sub>3</sub>, 10 vol.% O<sub>2</sub>, 5 vol.% H<sub>2</sub>O, GHSV = 40,000 h<sup>-1</sup>.

**Table S1**

The concentration of Cu and Ba over the fresh and hydrothermally aged Cu/BEA and CuBa/BEA analyzed by ICP-AES.

	Cu/BEA	CuBa <sub>1</sub> /BEA	CuBa <sub>2</sub> /BEA	CuBa <sub>3</sub> /BEA	CuBa <sub>4</sub> /BEA	Cu/BEA-(600, 48h)	CuBa <sub>3</sub> /BEA-(600, 48h)
Cu (wt.%)	1.94	1.94	1.90	1.94	1.93	1.82	1.89
Ba (wt.%)	-	4.71	4.46	4.66	4.77	-	4.63

## 2. EPR

Fig. S2 displays the EPR of Cu/BEA and CuBa<sub>3</sub>/BEA. Intensities of the hyperfine splitting peaks of Cu/BEA are lower than CuBa<sub>3</sub>/BEA,

indicating a reduction in the number of isolated  $\text{Cu}^{2+}$  species over Cu/BEA.

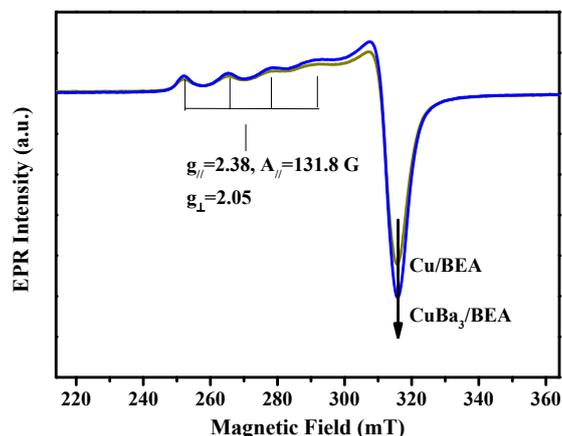


Fig. S2 EPR spectra of Cu/BEA and CuBa<sub>3</sub>/BEA recorded at -150 °C.

**Table S2**

The surface chemical composition and contents of isolated  $\text{Cu}^{2+}$  species over Cu/BEA and CuBa<sub>3</sub>/BEA.

Sample	<sup>a</sup> Isolated $\text{Cu}^{2+}$ concentration on surface*
Cu/BEA	1.00
CuBa <sub>3</sub> /BEA	1.25

<sup>a</sup> Calculated by EPR spectroscopy; \* The isolated  $\text{Cu}^{2+}$  content on Cu/BEA is defined as 1.00.

### 3. TEM

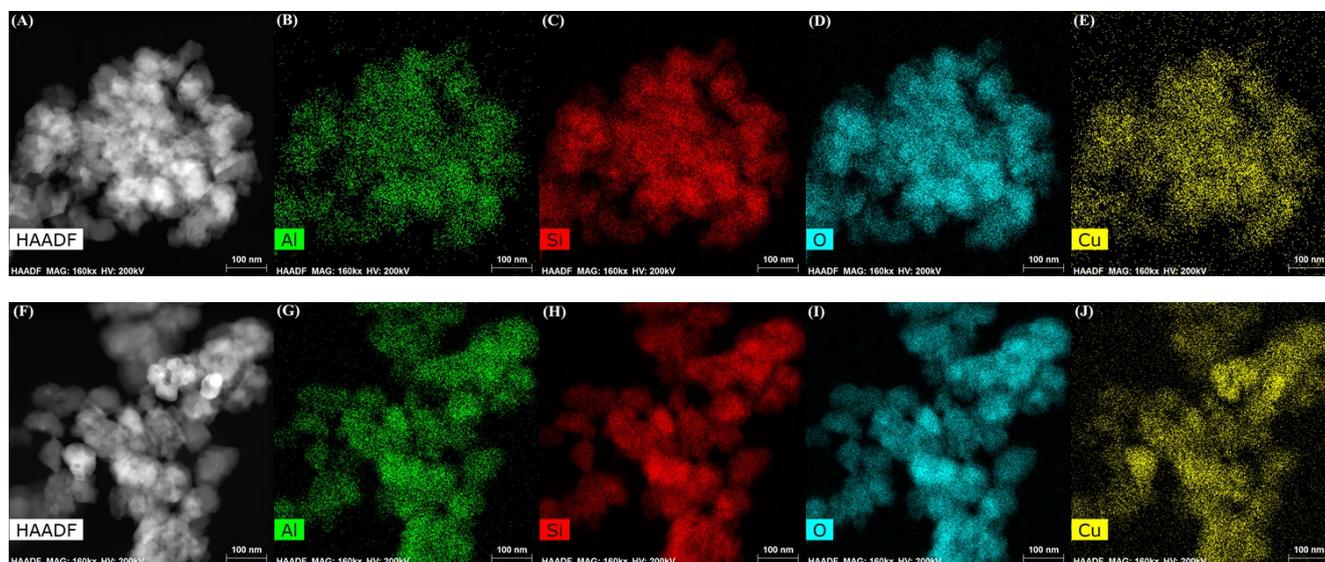


Fig. S3. HAADF-STEM image combined with the EDS elemental mapping over Cu/BEA (A)-(E) and CuBa/BEA (F)-(J).

Distributions of Al, Si, O and Cu species in the same region over fresh Cu/BEA and CuBa/BEA are simultaneously investigated by the HRTEM-STEM combined with EDS elemental mapping images (Fig. S3). Higher distributions of Al, Si, O and Cu species over Cu/BEA from elemental mapping image (Fig. S3B-E) could be observed than CuBa/BEA. Fig. S3B-D suggest that the better zeolite structure over Cu/BEA, which is consistent with the XRD. The more complete BEA structure is favor for more acid sites, which also corresponding to the

NH<sub>3</sub>-TPD (Fig 3) and NH<sub>3</sub>-adsorption (Fig 4). Furthermore, compared with CuBa/BEA, more bright copper region over Cu/BEA-HT are detected (Fig. S3J). Combined with the O element mapping image (Fig. S3I), some bright copper regions coincide with some rich O regions, which could be due to formation of the copper oxides during the preparation process. So it demonstrates that more copper oxides are presented in CuBa/BEA. But the H<sub>2</sub>-TPR and XRD have no obvious presence of copper oxides, so a small amount of copper species is produced in the fresh CuBa/BEA. More copper oxides are disadvantaged for the higher activity of the hydrothermally treated catalyst.