# **Electronic Supporting Information (ESI)**

## Fabrication of core-shell $\alpha$ -MnO<sub>2</sub>@polydopamine nanocomposites

## for the efficient and ultra-fast removal of U(VI) from aqueous

## solution

Jianjun Wang\*<sup>a</sup>, Junping Ma<sup>a</sup>, Chenlu Zhang<sup>a</sup>, Xing Li<sup>a</sup>, Shuang Song<sup>a</sup>, Tao Wen<sup>a</sup>, Ming Fang<sup>a</sup>, Xiaoli Tan\*<sup>a</sup> and Xiangke Wang<sup>a</sup>

<sup>a</sup>: MOE Key Laboratory of Resources and Environmental Systems Optimization, College of Environmental Science and Engineering, North China Electric Power University, Beijing 102206, P. R. China

\*: Corresponding author. Tel (Fax): +86-10-61772890; Email: <u>wangjj2016@ncepu.edu.cn</u> (J. Wang); <u>xltan@ncepu.edu.cn</u> (X. Tan)

### **Adsorption kinetics**

The pseudo-first-order and pseudo-second-order kinetic were expressed as (S1) and (S2), respectively:

$$\ln\left(q_e - q_t\right) = \ln q_e - k_1 t \qquad (S1)$$
$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \qquad (S2)$$

where  $q_t$  and  $q_e$  (mg/g) are the amounts of U(VI) adsorbed at time t (min) and equilibrium time, respectively.  $k_1$  (min<sup>-1</sup>) and  $k_2$  (g/ (mg min)) are the rate constants of the equation (S1) and (S2), respectively.

### Adsorption isotherms

The Langmuir and Freundlich can be expressed by (S3) and (S4), respectively:

$$q_e = \frac{bq_m C_e}{1 + bC_e} \tag{S3}$$

$$q_e = K_F C_e^{\frac{1}{n}} \tag{S4}$$

where  $q_e$  (mg/g) and  $C_e$  (mg/L) are the adsorption amount of U(VI) onto adsorbent and the U(VI) equilibrium concentration in supernatant, respectively.  $q_m$  (mg/g) is the saturated monolayer adsorption amount. b (L/mg) is the Langmuir constant connected with the energy of adsorbent.  $K_F$  (mg/g) is relevant to the adsorption amount, whereas 1/n is the Freundlich constant correlated to the adsorption intensity.

The linear form of D-R isotherm is represented by the following equation (S5):

$$\ln q_{\rm e} = \ln q_m - \beta \varepsilon^2 \tag{S5}$$

where  $\beta$  is the constant of the adsorption energy (mol<sup>2</sup>/J<sup>2</sup>), related to the average energy of adsorption per mole of the U(VI) as it is transferred to the surface of the solid from infinite distance in the solution.  $\varepsilon$  is Polanyi potential, described as:

$$\varepsilon = RT \left( 1 + \frac{1}{C_e} \right) \tag{S6}$$

where R is the gas constant (8.314 J/ (mol K)). T is the absolute temperature (K).

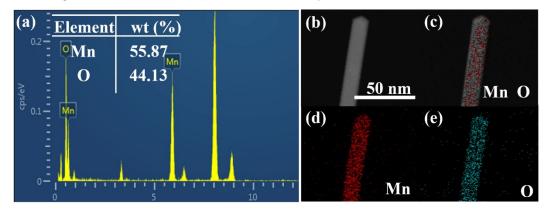


Fig S1 (a) EDX spectrum, (b) TEM and (c-e) the corresponding elemental images of as-prepared α-MnO<sub>2</sub> nanowires.

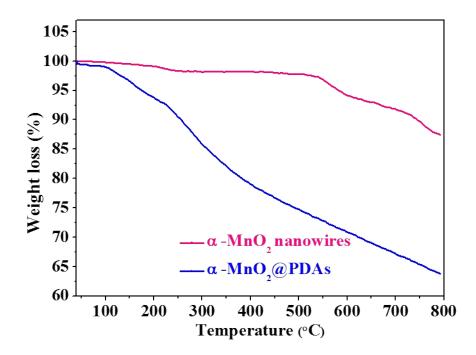
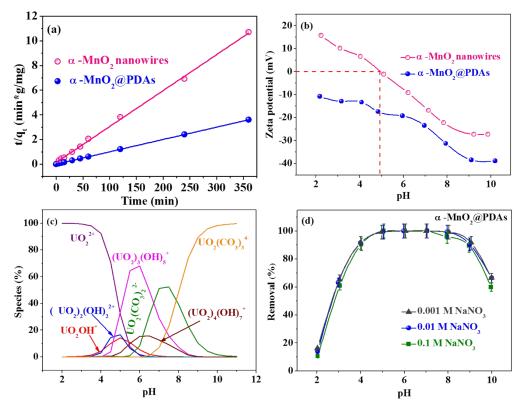


Fig S2 TG curves of  $\alpha\text{-}MnO_2$  nanowires and  $\alpha\text{-}MnO_2@PDAs.$ 



**Fig S3** (a) Pseudo-second-order kinetic plots of U(VI) removal on  $\alpha$ -MnO<sub>2</sub> nanowires and  $\alpha$ -MnO<sub>2</sub>@PDAs, (b) The zeta potential of  $\alpha$ -MnO<sub>2</sub> nanowires and  $\alpha$ -MnO<sub>2</sub>@PDAs and (c) the relative distribution of U(VI) species in aqueous solution as a function of pH, (d) The effect of ion strength (0.001, 0.01 and 0.1 mol/L NaNO<sub>3</sub>) on U(VI) adsorption onto  $\alpha$ -MnO<sub>2</sub>@PDAs at T = 298 K, m/V = 0.1 g/L,  $C_0$ (U(VI)) = 10 mg/L.

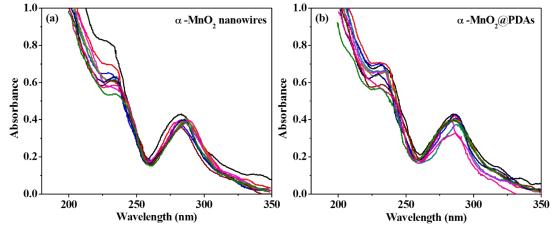


Fig S4 The titration spectra of 0.1 M (a) α-MnO<sub>2</sub> nanowires and (b) α-MnO<sub>2</sub>@PDAs in the pH range 3.36-9.11 at 298 K.

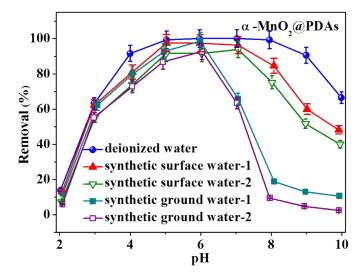
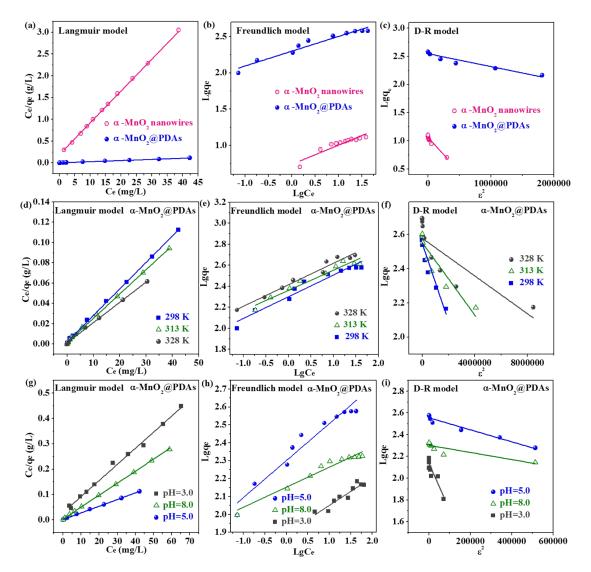


Fig S5 The removal efficiency of U(VI) by  $\alpha$ -MnO<sub>2</sub>@PDAs in deionized water and different imitative uranium-containing wastewater in the pH range of 2.0 – 10.0. m/V = 0.1 g/L,  $C_0(U(VI)) = 10 \text{ mg/L}$ , and T = 298 K.



**Fig S6** Langmuir, Freundlich and D-R models simulation of (a, b, c) U(VI) adsorption on  $\alpha$ -MnO<sub>2</sub> nanowires and  $\alpha$ -MnO<sub>2</sub>@PDAs at pH = 5.0 ± 0.05, *T* = 298 K, (d, e, f) U(VI) adsorption on  $\alpha$ -MnO<sub>2</sub>@PDAs at different temperature, and (g, h, i) U(VI) adsorption on  $\alpha$ -MnO<sub>2</sub>@PDAs at three different pH values. All experiments were at *m*/V = 0.1 g/L and *I* = 0.01 M NaNO<sub>3</sub>.

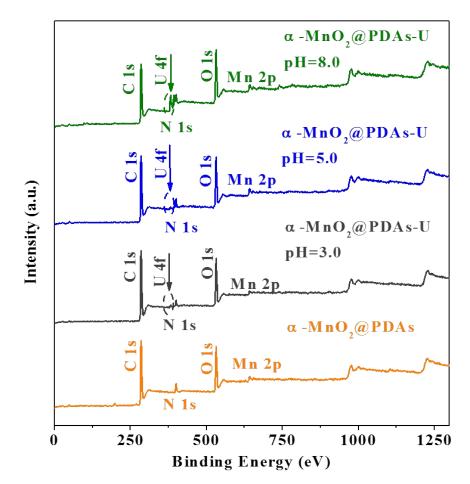


Fig S7 XPS survey spectra of  $\alpha\text{-MnO}_2 @PDAs$  before and after U(VI) adsorption.

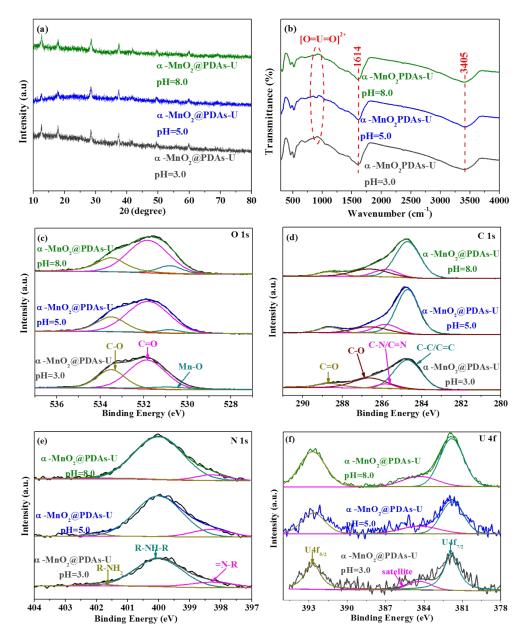


Fig S8 (a) XRD patterns and (b) FT-IR spectra of  $\alpha$ -MnO<sub>2</sub>@PDAs before and after U(VI) adsorption at different pH. High-resolution XPS spectra of (c) O 1s, (d) C 1s, (e) N 1s and (f) U 4f of  $\alpha$ -MnO<sub>2</sub>@PDAs after U(VI) adsorption at different pH.

In Fig S7c, the variable quantity of C-O in diverse pH abided by the order: pH 5.0 (14.65%) > 8.0 (12.52%) > 3.0 (8.19%). Similarly, as shown in Fig S7d, the total content of C-N/C=N and C-O bonds displayed more or less changes whether under acidic or alkaline environment, which changed to lower content from 33.30% to 31.47% (pH 3.0), 26.05% eV (pH 5.0) and 30.02% (pH 8.0), respectively. The above phenomenon was consistent with the adsorption result (Fig 4c), and the trends were attributed to the different amount of the reacted active groups for U(VI) species. As observed in Fig S7f, the presence of U 4f centered at ~281.8 of U  $4f_{7/2}$ , ~392.7 of U  $4f_{5/2}$  of U(VI) were observed, respectively.

lons		Synthetic ground				Real sea		
Synthetic groun water-1 (mM)		water-2 (mM)	Synthetic surface water-1 (mM)	Synthetic surface water-2 (mM)	Deionized water (M)	water (mM)		
HCO <sub>3</sub> -	0.43	0.43	0.26	0.26	0	-		
CO32-	0	0.50	0	0.33				
SO4 <sup>2-</sup>	0.36	0.36	0.07	0.07	0	-		
NO <sub>3</sub> -	0.21	0.21	0.12	0.12	0.01	-		
Cl-	0.64	0.64	0.34	0.34	0	-		
Ca <sup>2+</sup>	0.66	0.66	0.33	0.33	0	-		
Mg <sup>2+</sup>	0.24	0.24	0.24	0.24	0	-		
Na+	0.42	0.42	0.23	0.23	0.01	-		
K+	0.20	0.20	0.03	0.03	0	-		
рН	6.67	7.43	7.17	7.82	7.03	7.04		
Table S2 Structural properties of $\alpha$ -MnO <sub>2</sub> nanowires and $\alpha$ -MnO <sub>2</sub> @PDAs.								
	Adsorbents	BET surface area	Maximum pore size	Pore volume	Average pore	e size		
		(m²/g)	(n <b>m</b> )	(cm <sup>3</sup> /g)	(n <b>m</b> )			
-	$\alpha$ -MnO <sub>2</sub> nanowires	30.78	99.64	0.12	21.98			
	α-MnO₂@PDAs	22.79	95.48	0.06	12.85			

 Table S1 The concentrations of different ions in deionized water and different imitative uranium-containing wastewater.

Table S3 Parameters of pseudo-first-order kinetic and pseudo-second-order kinetic models for U(VI) adsorption onto  $\alpha$ -MnO<sub>2</sub> nanowires and  $\alpha$ -MnO<sub>2</sub>@PDAs.

MINO <sub>2</sub> @PDAS.							
Adsorbents	Pseudo-first-order			Pseudo-second-or	Pseudo-second-order		
	<i>k</i> <sub>1</sub>	<i>q</i> <sub>e</sub>	R <sup>2</sup>	k2	<i>q</i> <sub>e</sub>	<i>R</i> <sup>2</sup>	
	(1/min)	(mg/g)		(g/ (mg min))	(mg/g)		
$\alpha$ -MnO <sub>2</sub> nanowires	0.13	31.98	0.974	0.0060	34.36	0.999	
α-MnO₂@PDAs	0.94	99.05	0.999	0.0233	100.0	~1	

\_

Table S4 Comparisons of U(VI) adsorption capacities of  $\alpha$ -MnO<sub>2</sub>@PDAs with other nanomaterials.

Adsorbents	$q_m$ (mg/g)	Conditions
mSiO <sub>2</sub> /PDA <sup>1</sup>	286.5	рН = 5.5 <i>, Т</i> = 298 К
MnO <sub>2</sub> <sup>2</sup>	39.8	pH = 3.8, <i>T</i> = 298 K
GO/MnO <sub>2</sub> <sup>2</sup>	185.2	pH = 3.8, <i>T</i> = 298 K
PDA <sup>3</sup>	34.21	pH = 4.0, <i>T</i> = 298 K
PDA/GO <sup>3</sup>	145.39.00	pH = 4.0, <i>T</i> = 298 K
Fe <sub>3</sub> O <sub>4</sub> @PDA <sup>4</sup>	71.00	pH = 5.0, <i>T</i> = 293 K
$\alpha$ -MnO $_2$ nanowires (in this work)	13.51	pH = 5.0, <i>T</i> = 298 K
$\alpha$ -MnO <sub>2</sub> @PDAs (in this work)	383.14	рН = 5.0, <i>T</i> = 298 К

Table S5 Thermodynamic parameters for U(VI) adsorption onto  $\alpha$ -MnO<sub>2</sub> nanowires and  $\alpha$ -MnO<sub>2</sub>@PDAs.

Adsorbents	<i>q<sub>m</sub></i> (mg/g)	<i>Т</i> (К)	рН	$\Delta H^o$	$\Delta S^{o}$	$\Delta G^{o}$
				(KJ/mol)	(J/ (mol K))	(KJ/mol)
α-MnO₂ nanowires	13.51	298	5.0			-2.04
α-MnO₂@PDAs	383.14	298	5.0	9.91	78.70	-13.76
	418.41	313	5.0	9.91	78.70	-14.29
	502.51	328	5.0	9.91	78.70	-16.13

#### Notes and references

- 1. L. Bai, S. Duan, W. Jiang, M. Liu, S. Wang, M. Sang, X. Gong, J. Li and S. Xuan, Applied Surface Science, 2017, **426**, 1121-1132.
- 2.
- N. Pan, L. Li, J. Ding, S. Li, R. Wang, Y. Jin, X. Wang and C. Xia, *Journal of Hazard Mater*, 2016, **309**, 107-115. Z. Zhao, J. Li, T. Wen, Z. Chen, K. Wang and A. Xu, *Colloid and Surface A: Physicochemical and Engineering* 3. Aspects, 2015, 482, 258-266.
- 4. D. Yang, X. Wang, N. Wang, G. Zhao, G. Song, D. Chen, Y. Liang, T. Wen, H. Wang, T. Hayat, A. Alsaedi, X. Wang and S. Wang, Journal of Cleaner Production, 2018, 172, 2033-2044.