

Supporting Information

Surface Hydroxylation Induced by Alkaline-earth Metal Doping in NiO Nanocrystals and Its Application in Achieving a Wide Temperature Operation Window of Preferential CO Oxidation

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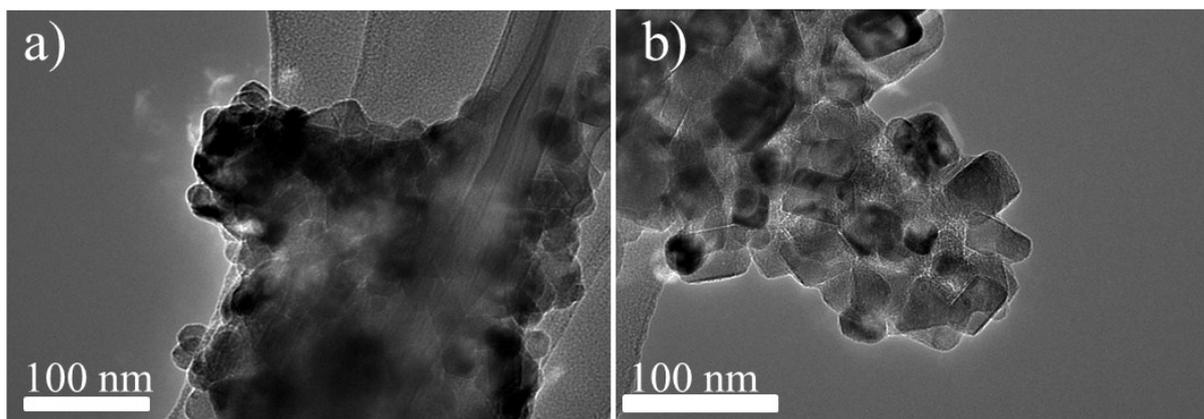


Figure S1. TEM images of $\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$ solid solution via the precipitate process of Mg after Ni.

As shown in Figure S1, we carried out the precipitate process of Mg after Ni to obtain the $\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$ samples. Although the sample presented the irregular nanosheets morphology, the nanosheets were severely accumulative which could severely hinder the exposure of active site and the support of noble metals.

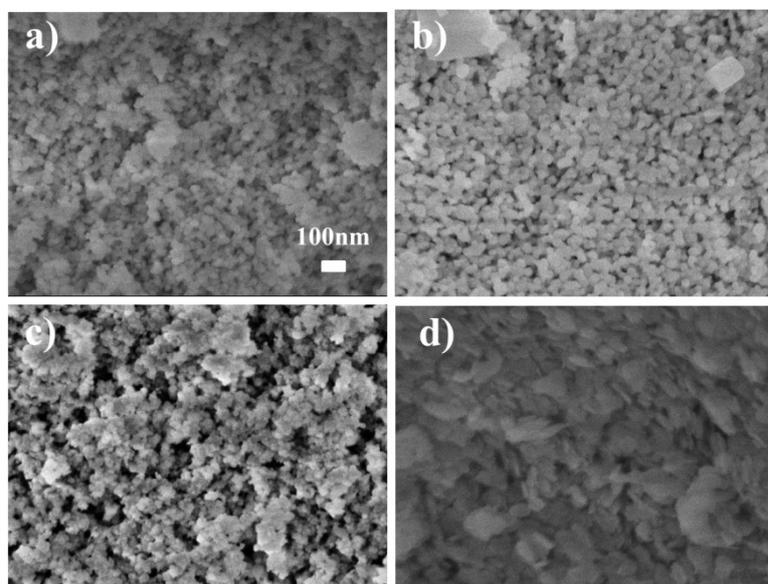


Figure S2. Scanning electron micrographs of (a) the $\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$ support, (b) $\text{Pt}/\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$ catalyst (c) Pt/NiO and (d) $\text{Pt}/\text{Mg}(\text{OH})_2$ catalyst.

SEM images of the catalysts are shown in Figure S1. $\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$ and $\text{Pt}/\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$ catalysts (Figures S1a and S1b) present uniform size. Although Pt/NiO catalyst (Figure. S1c) exhibited a similar morphology to $\text{Pt}/\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$ catalyst, the nanosheets in Pt/NiO exhibited a slight agglomeration. $\text{Pt}/\text{Mg}(\text{OH})_2$ catalyst consisted of hexagonal nanoflakes (Figure S1d). The average size of hexagonal nanoflakes was larger than those of other catalysts.

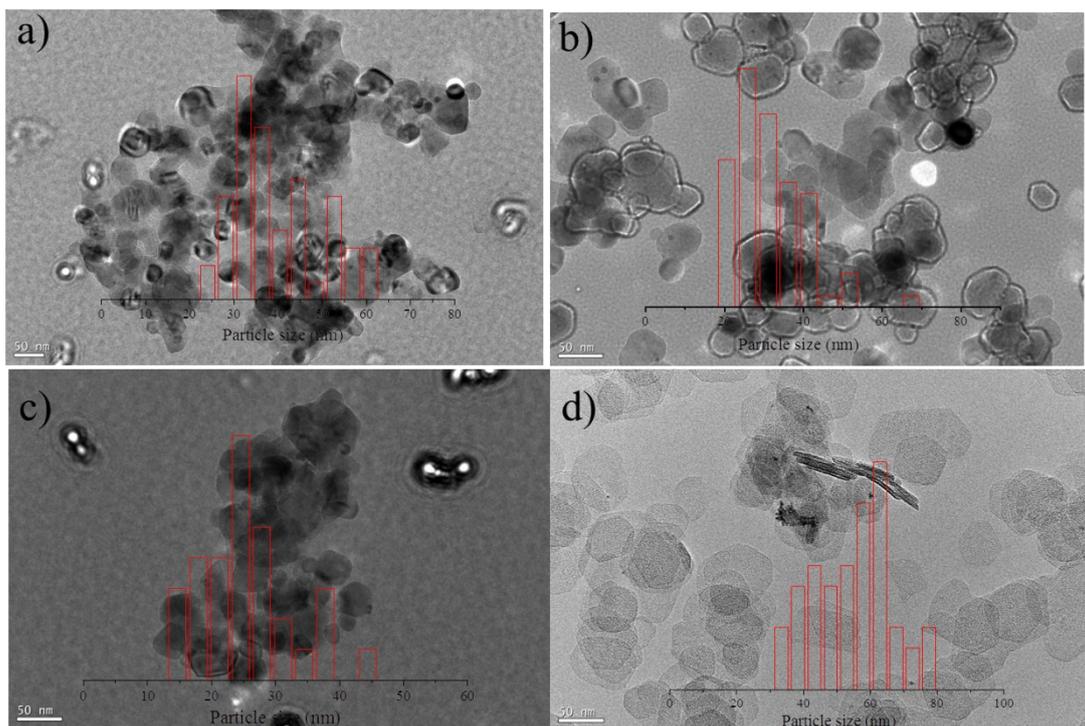


Figure S3. TEM images of (a) $\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$, (b) $\text{Pt}/\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$, (c) Pt/NiO , and (d) $\text{Pt}/\text{Mg}(\text{OH})_2$ that show the estimated particle sizes.

The particle size distribution for $\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$ support is about 30-40 nm. After supporting Pt, particle size distribution has not changed. This result indicates that supporting Pt catalyst had no distinct effect on the particle size. The particle size distributions for Pt/NiO and $\text{Pt}/\text{Mg}(\text{OH})_2$ catalysts, are about 20-30 and 50- 60 nm, respectively. The particle size distribution of $\text{Pt}/\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$ catalyst is between Pt/NiO and $\text{Pt}/\text{Mg}(\text{OH})_2$.

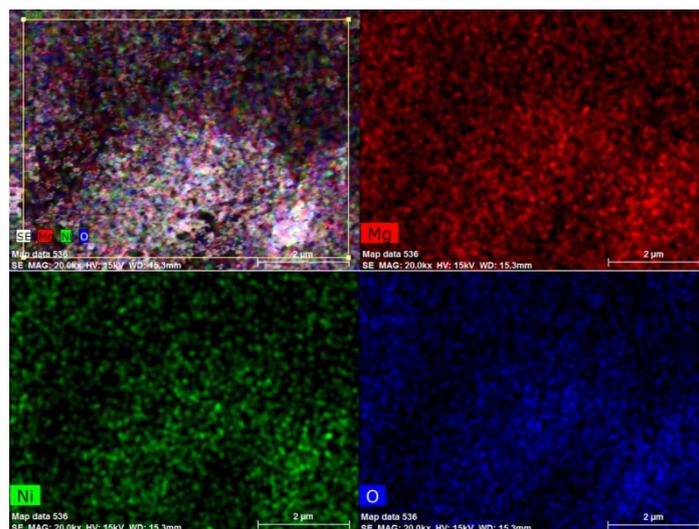


Figure S4. SEM elemental mapping of $\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$ solid solution.

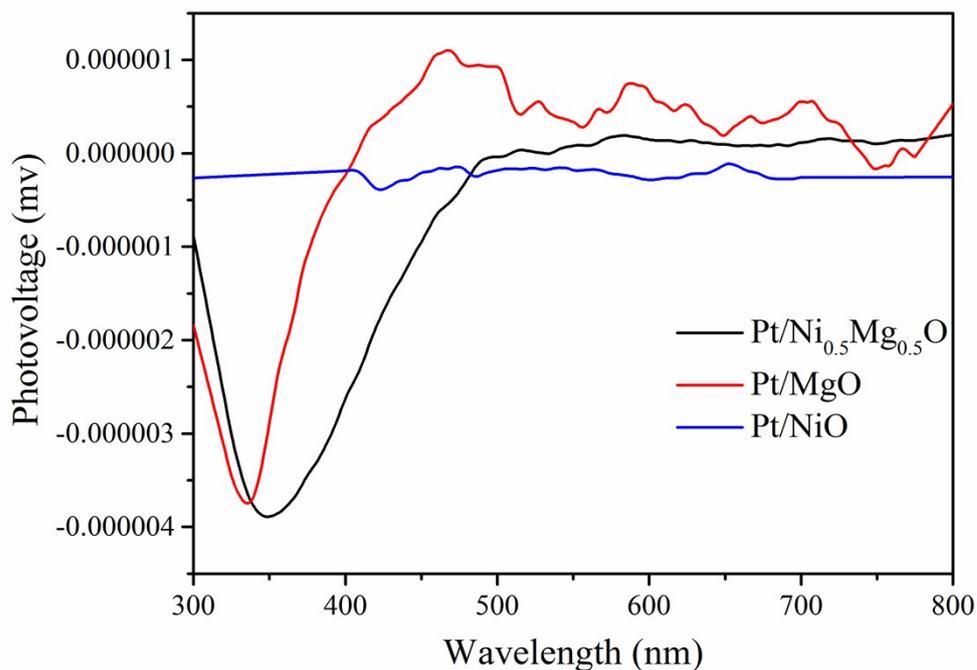


Figure S5. Surface photovoltage spectra (SPV) of Pt/Ni_{0.5}Mg_{0.5}O, Pt/MgO and Pt/NiO catalysts.

For the SPV response, a positive signal implies a positive charge accumulation at the surface of the sample. On the contrary, a negative signal is produced due to the negative charge accumulation at the surface. For Pt/Ni_{0.5}Mg_{0.5}O catalyst, a weak negative SPV response arises between 300 and 488 nm, which implies a negative charge accumulation at the surface. Pt/MgO performs the similar behavior to Pt/Ni_{0.5}Mg_{0.5}O. However, Pt/NiO has no SPV response. Therefore, the electron is supplied from the magnesium ions to the active metal in the catalyst and strengthens CO adsorption.

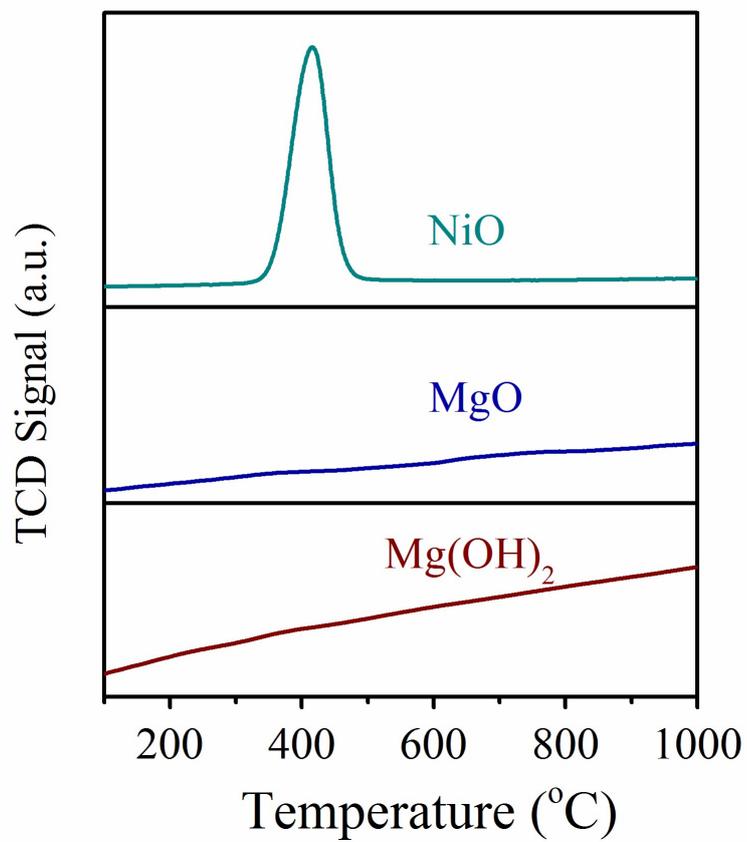


Figure S6. H₂-TPR profiles of the contrast samples NiO, MgO, and Mg(OH)₂.

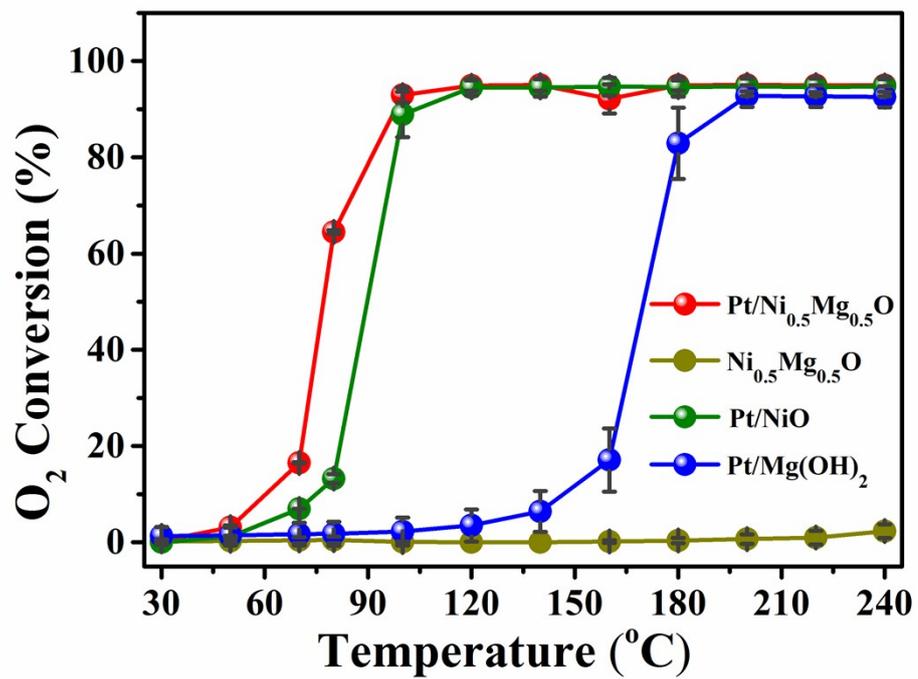


Figure S7. O₂ conversion of all catalysts.

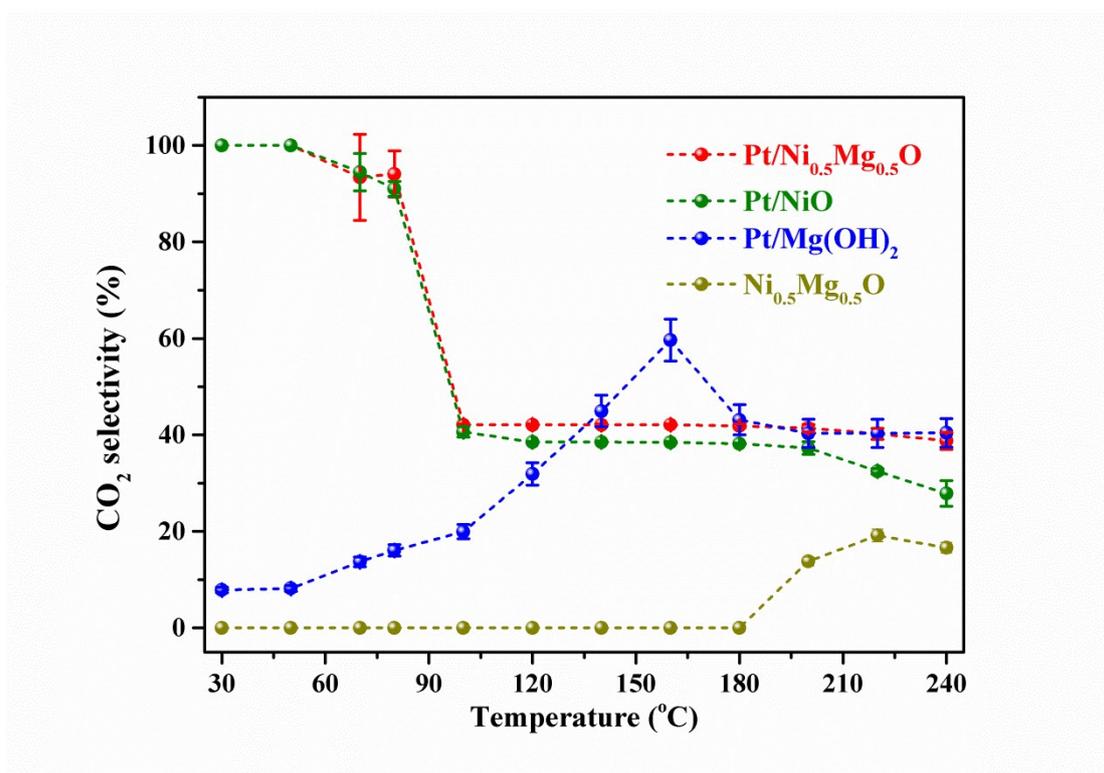


Figure S8. CO₂ selectivity of four catalysts. PROX reactions were performed over the four catalysts at C:O₂ ratios of 1:1.25 and a GHSV of 80000 h⁻¹.

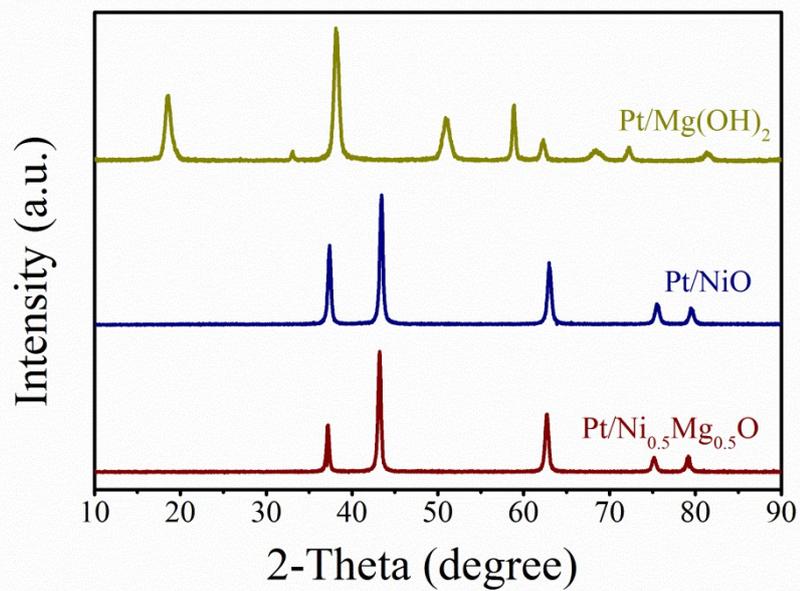


Figure S9. XRD patterns of the catalysts used Pt/Ni_{0.5}Mg_{0.5}O, Pt/NiO, and Pt/Mg(OH)₂.

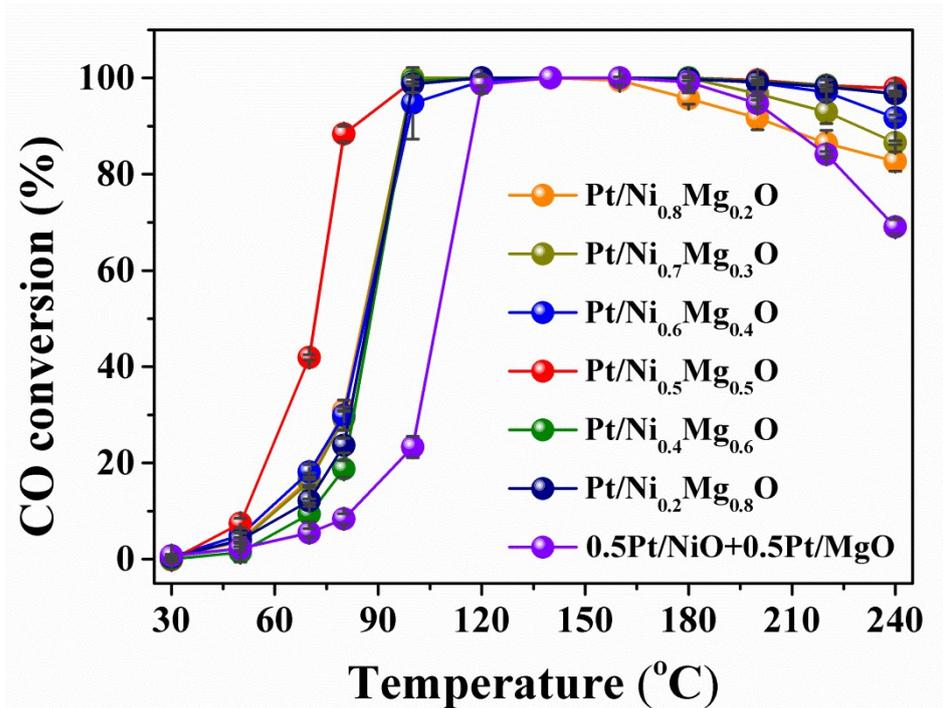


Figure S10. CO conversions of Pt supported Ni_{1-x}Mg_xO (0, 0.2, 0.3, 0.4, 0.5, 0.6, 0.8)

solid solutions for CO oxidation reactions in H₂-rich condition.

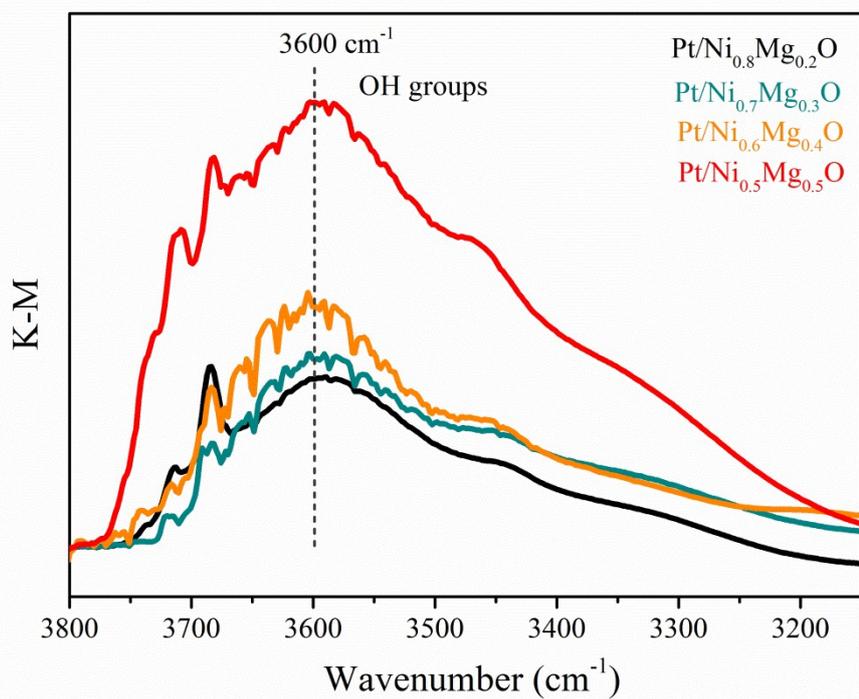


Figure S11. DRIFTS recorded for Pt/Ni_{1-x}Mg_xO (x = 0.2, 0.3, 0.4, 0.5) under the CO-PROX measurement conditions (i.e., 1 % CO, 1.25 % O₂ and 50 % H₂ in He balance) at 30 °C.

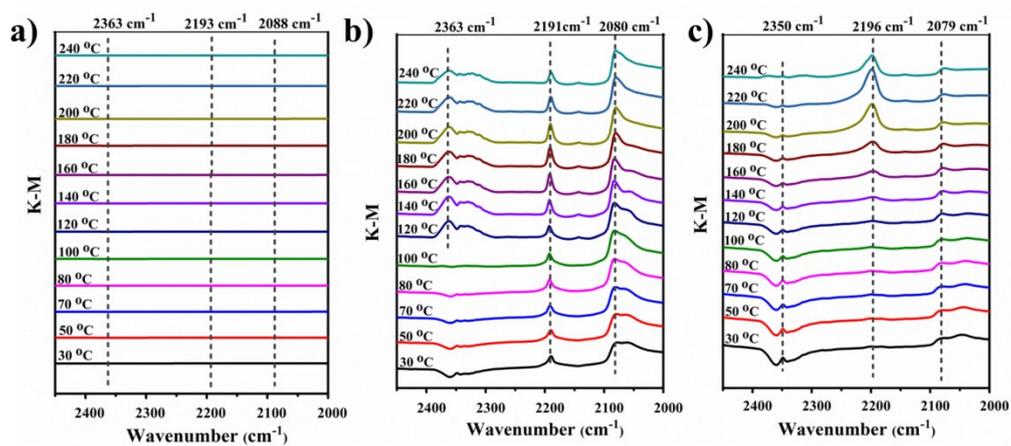


Figure S12. DRIFT spectra recorded for (a) $\text{Ni}_{0.5}\text{Mg}_{0.5}\text{O}$, (b) Pt/NiO, and (c) Pt/Mg(OH)₂ as a function of temperature under operando PROX conditions (i.e., 1 % CO, 1.25 % O₂ and 50 % H₂ in He balance).

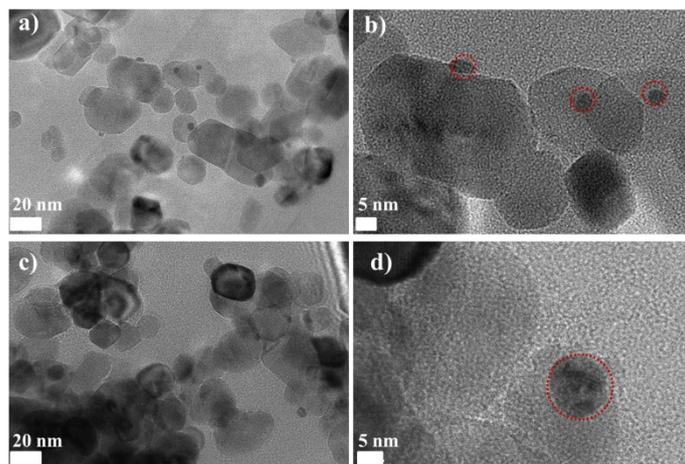


Figure S13. TEM images of the Pt/Ni_{0.5}Mg_{0.5}O and Pt/NiO after the stability test for 50 h.

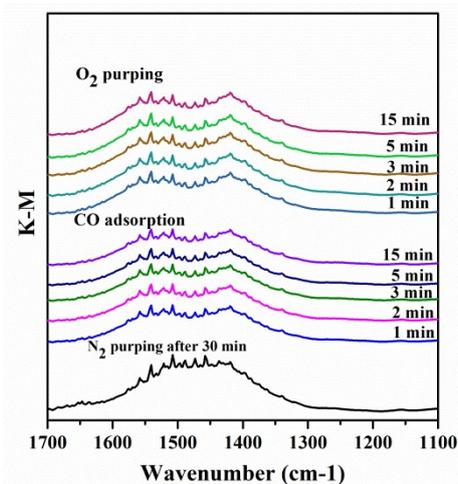


Figure S14. In situ DRIFTS study of N_2 purging, CO adsorption, O_2 removal on the $Pt/Ni_{0.5}Mg_{0.5}O$ catalyst. (CO flow rate, 10 mL min^{-1} ; catalyst mass, 20 mg; temperature, $140 \text{ }^\circ\text{C}$).

In situ DRIFTS was carried out to identify the active species by analyzing the spectral range of $1700\text{-}1100 \text{ cm}^{-1}$. In a typical steady test, the powder sample (ca. 20 mg) was purged in N_2 for 30 min at room temperature and a background spectrum was collected via 48 scans at 4 cm^{-1} resolution. The reaction gas with 10 % CO/N_2 was introduced into the in situ chamber (10 mL min^{-1}) and heated to $140 \text{ }^\circ\text{C}$. Once the CO adsorption lasted 15 min, the gas channel was switched immediately to 20 % O_2/N_2 . These peaks hardly were observed change significantly when undergo the process of 10 % CO/N_2 shifting to 20 % O_2/N_2 compared to the treatment of N_2 . The reason for this phenomenon is the presence of surface bicarbonates, which have lower thermal stability in comparison to carbonate species. The surface bicarbonates would favor a faster desorption of CO_2 , leaving the surface available for further chemisorptions, through which the CO oxidation is accelerated.

Table S1. Particulate properties of the catalysts used.

Samples	Surface area (m²/g)	Pore volume (cm³/g)	Pore diameter (nm)
Pt/Ni_{0.5}Mg_{0.5}O	24	0.14	27
Ni_{0.5}Mg_{0.5}O	27	0.13	26
Pt/NiO	19	0.11	22
Pt/Mg(OH)₂	73	0.43	19

Table S2. Structural Refinement Results for Pt/Ni_{1-x}Mg_xO Using GSAS software

Samples	Cell parameters	Rp	Rwp	χ^2
	a (Å)			
Pt/NiO	4.1795(8)	0.0618	0.0839	4.418
Pt/Ni _{0.8} Mg _{0.2} O	4.1839(8)	0.0438	0.0588	2.845
Pt/Ni _{0.7} Mg _{0.3} O	4.1872(1)	0.0507	0.0668	3.703
Pt/Ni _{0.6} Mg _{0.4} O	4.1910(2)	0.0594	0.0851	4.778
Pt/Ni _{0.5} Mg _{0.5} O	4.1915(7)	0.0490	0.0694	3.429
Pt/Ni _{0.4} Mg _{0.6} O	4.1945(6)	0.0385	0.0542	3.814
Pt/Ni _{0.2} Mg _{0.8} O	4.1995(6)	0.0517	0.0749	4.532
Pt/ MgO	4.2087(6)	0.0485	0.0697	2.250

Table S3. Comparison of catalytic performance in CO-PROX over Pt/Ni_{0.5}Mg_{0.5}O and those catalysts reported in literature.

Sample	Pt loading wt. %	Amount of catalyst (mg)	Space Velocity (ml.g _{cat} ⁻¹ .h ⁻¹)	Operation temperature window (CO conversion >99.0%)	ref
Pt/Ni _{0.5} Mg _{0.5} O	0.5	50	80000	100-220 °C	This work
Pt/NiO	0.5	50	80000	100-180 °C	This work
Pt/Mg(OH) ₂	0.5	50	80000	200-240 °C	This work
Pt/Ti _{0.5} Ce _{0.5} O ₂	0.6	100	17000	-	1
Pt-Ni-Al	0.5	undefined	12,000	200 °C	2
Pt/Co ₃ O _{4-x}	2.0	undefined	42857	110–130 °C	3
Pt-Ni/CNT-OX	2.0	50	48,000	95–120 °C	4
Pt-Mg/Al ₂ O ₃	2.0	undefined	60000	-	5
M-Pt-Ni/Al ₂ O ₃	1.0	undefined	16000	100-150 °C	6
Pt/xCeO ₂ – (1-x)Nb ₂ O ₅	1.0	100	17000	-	7
Pt ₃ Co/MgO	3.0	50	-	120-160 °C	8
PtFeNi/CNTs-p	3.0	60	25000	-	9
Pt/CuCrO _x	2.0	100	60000	160-200 °C	10
Pt– Ni/GMMSiO ₂	2.0	100	24000	95-120 °C	11

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