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## **Supplementary materials for**

# Comparative study of naproxen degradation by the UV/chlorine and the UV/ $H_2O_2$ advanced oxidation processes

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ESI negative mode

### Text S1. The operating conditions of UPLC-QTOF MS under ESI negative mode.

The chromatographic separation was achieved using a C-18 column (Waters acquity BEH, 1.7 µm). The mobile phase consisted of 0.1% formic acid water (A) and methanol (B), with a gradient elution of A/B from 95/5 (v/v) to 5/95 for 20 min. The sample injection volume was 0.3 µL. The Ion Mobility-Q-TOFMS was operated under the following conditions: ESI negative mode, capillary 2.5 kV, source temperature 110 °C, desolvation temperature 350 °C, sampling cone 30 V, cone gas flow 30 L/Hr, desolvation gas flow 700 L/Hr, nebulizer gas flow 6 bar, trap collision energy 4 eV, transfer collision energy 2 eV, trap gas flow 2 mL/min, lock spray capillary 2.5 kV, collision energy 4 eV, trap MSMS collision energy ramp 4~30eV.

#### Text S2. The calculation of EE/O.

Electrical Energy per Order (EE/O) was applied to compare the cost of the UV/chlorine and UV/H<sub>2</sub>O<sub>2</sub> AOPs for the removal of 90% NPX. The total EE/O includes electrical energy for UV irradiation (EE/O<sub>UV</sub>) and equivalent electrical energy for oxidant consumption (EE/O<sub>oxidant</sub>). The calculation of EE/O, EE/O<sub>UV</sub> and EE/O<sub>oxidant</sub> followed eqs s1-s4.

$$EE/O = EE/O_{UV} + EE/O_{oxidant} (kWh/m^3)$$
(S1)

$$EE/O_{UV} = \overline{V * log^{\text{ind}}([NPX]t/[NPX]0} \text{ (kWh/m^3)}$$
(S2)

$$EE/O_{oxidant} = Eq_{oxidant} * Oxidant/O (kWh/m^3)$$
(S3)

$$Oxidant/O = \overline{log^{[m]}([NPX]t/[NPX]0} (mg/L) \qquad \Box \qquad (S4)$$

where EE/O<sub>UV</sub>, and EE/O<sub>oxidant</sub> are the electrical energy consumptions by UV irradiation and oxidant (chlorine or H<sub>2</sub>O<sub>2</sub>), respectively, kWh/m<sup>3</sup>; P is electronic energy input of UV lamps, kW (photoelectric conversion efficiency of the reactor was 25.0%, P = UV irradiance / 25.0%) <sup>s1</sup>; V is the reaction volume, L; t is the reaction time, h; [NPX]<sub>0</sub> and [NPX]<sub>t</sub> are the NPX concentrations at 0 h and t h, respectively, mg/L; [Oxidant]<sub>0</sub> is the concentration of oxidant, mg/L, Eq<sub>oxidant</sub> is the equivalent electric energy consumption to produce per milligram of oxidant, kWh/mg (Eq<sub>chlorine</sub> = 11.6 × 10<sup>-6</sup> kWh/mg <sup>s2</sup>, Eq<sub>H2O2</sub> = 10.8 × 10<sup>-6</sup> kWh/mg <sup>s3</sup>); Oxidant/O is the oxidant required for per order magnitude elimination of NPX, mg/L).

[Ovidant]]

	Rate constants (M <sup>-1</sup> s <sup>-1</sup> )								
Scavenger	НО•	Cl•	ClO•	Cl <sub>2</sub> -	CO₃-				
HCO <sub>3</sub> -	$8.5\times10^{6\text{s}4}$	$2.2\times10^{8}{}^{\rm s5}$	600 s <sup>5</sup>	$8.0\times10^{7\text{s6}}$	-				
TBA	$6.0\times 10^{8\text{s4}}$	$3.0\times10^{8s7}$	$1.3\times 10^{7\mathrm{s}9}$	700 s <sup>8</sup>	$9.6  imes 10^{4  s9}$				

Table S1. Reactivities between scavengers and involved radicals in the processes.

рН	HOCl (µM)	OCl <sup>-</sup> (µM)
6	48.5	1.5
7	38	12
9	1.5	48.5

Table S2. Concentrations of HOCl and OCl<sup>-</sup> at different pHs with 50  $\mu$ M chlorine dosage.

Water treatment	dosage	CO <sub>3</sub> • (M)	HO• (M)	Cl• (M)	$\operatorname{Cl}_2^{\bullet}(M)$	ClO• (M)
	control	1.62 × 10 <sup>-13</sup>	9.40 × 10 <sup>-14</sup>	0	0	0
UV/H <sub>2</sub> O <sub>2</sub>	1 mM	$2.45 \times 10^{-12}$	$8.05 \times 10^{-14}$	0	0	0
	5 mM	$7.42 \times 10^{-12}$	5.11 × 10 <sup>-14</sup>	0	0	0
	control	4.74 × 10 <sup>-12</sup>	9.28 × 10 <sup>-14</sup>	$2.83 \times 10^{-14}$	$1.82 \times 10^{-13}$	9.00 × 10 <sup>-13</sup>
UV/chlorine	1 mM	1.65 × 10 <sup>-11</sup>	$7.59 \times 10^{-14}$	$1.56 \times 10^{-14}$	$4.57 \times 10^{-14}$	6.83 × 10 <sup>-13</sup>
	5 mM	2.02 × 10 <sup>-11</sup>	3.94 × 10 <sup>-14</sup>	7.65 × 10 <sup>-15</sup>	7.04 × 10 <sup>-15</sup>	5.05 × 10 <sup>-13</sup>

Table S3. Simulated molar concentration of reactive species with different bicarbonate dosages

Tuble 5 il Water quality parameters of the feat water sample.									
	$\mathrm{NH_4^+}$	Mg <sup>2+</sup>	Ca <sup>2+</sup>	F-	Cl-	NO <sub>2</sub> -	Br	NO <sub>3</sub> -	HCO <sub>3</sub> -
Concentration									

0.44

16.03

0.06

n.d.

10.79

58.56

33.13

DOC

0.628

Table S4. Water quality parameters of the real water sample.

n.d.

Note: n.d. means undetectable.

(mg/L)

0.04

Table S5. Accurate mass measurement of product ions of NPX and its transformed products as determined

by HPLC/ESI-IT-TOFMS.

	RT	[M-H] <sup>-</sup> (m/z)		Elemental	D 10		
Compound	(min)	Theoretical	Experimental	formula	Proposed Structure	UV/chlorine	UV/H <sub>2</sub> O <sub>2</sub>
236	1.865	235.0150	235.0162	C <sub>12</sub> H <sub>8</sub> O <sub>3</sub> Cl	H <sub>3</sub> C O OH	$\checkmark$	
252	2.168	251.0101	251.0111	C <sub>12</sub> H <sub>8</sub> O <sub>4</sub> Cl	H <sub>3</sub> C <sub>0</sub> Cl OH OH	$\checkmark$	
220ª	2.691	219.0649	219.0657	$C_{12}H_{11}O_4$	H <sub>3</sub> C O (OH) <sub>3</sub>		$\checkmark$
264	3.915	263.0544	263.0556	$C_{13}H_{11}O_6$	H <sub>3</sub> C <sub>0</sub> H <sub>0</sub> (OH) <sub>3</sub>		
216	4.642	215.0692	215.0708	$C_{13}H_{11}O_3$	H <sub>3</sub> C O		
204ª	5.102	203.0689	203.0708	$C_{12}H_{11}O_3$	H <sub>3</sub> C O (OH) <sub>2</sub>		
220 <sup>b</sup>	5.384	219.0644	219.0657	$C_{12}H_{11}O_4$	H <sub>3</sub> C O (OH) <sub>3</sub>		$\checkmark$
232ª	5.622	231.0647	231.0657	C <sub>13</sub> H <sub>11</sub> O <sub>4</sub>	H <sub>3</sub> C O O H O H	$\checkmark$	$\checkmark$





Figure S1. UV-vis absorption spectrum of NPX in aqueous phase.



**Figure S2**. Degradation of NPX and NB by UV/chlorine AOP in pure water at different pHs. Conditions: [chlorine]<sub>0</sub> = 50  $\mu$ M, [NPX]<sub>0</sub> = 5  $\mu$ M, [NB]<sub>0</sub> = 1  $\mu$ M, [Phosphate buffer]<sub>0</sub> = 2 mM.

![](_page_12_Figure_0.jpeg)

**Figure S3**. Degradation of NPX by the UV/H<sub>2</sub>O<sub>2</sub> AOP in pure water at different pHs. Conditions:  $[H_2O_2]_0 = 50 \ \mu\text{M}$ ,  $[\text{NPX}]_0 = 5 \ \mu\text{M}$ ,  $[\text{phosphate buffer}]_0 = 2 \ \text{mM}$ .

![](_page_13_Figure_0.jpeg)

**Figure S4.** Competition kinetics of NPX versus the reference compound DMOB at pH 10 by CIO•. Direct UV photolysis and chlorination have been subtracted. Conditions:  $[chlorine]_0 = 300 \ \mu M$ ,  $[NPX]_0 = [DMOB]_0 = 5 \ \mu M$ .  $[TBA]_0 = 0.5 \ mM$ .

![](_page_14_Figure_0.jpeg)

**Figure S5.** The degradation kinetics of NPX by chlorination with addition of bromide and chloride in pure water at pH 7. Conditions: [chlorine]<sub>0</sub> = 50  $\mu$ M, [NPX]<sub>0</sub> = 5  $\mu$ M, [bromide]<sub>0</sub> = 10  $\mu$ M, [chloride]<sub>0</sub> = 5 mM.

![](_page_15_Figure_0.jpeg)

Figure S6. Total ion chromatogram (TIC) under ESI negative mode.

![](_page_16_Figure_0.jpeg)

![](_page_17_Figure_0.jpeg)

![](_page_18_Figure_0.jpeg)

Figure S7. MS and MS2 spectra of the degradation products of NPX by the UV/chlorine and UV/ $H_2O_2$ AOPs under ESI negative mode.

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