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Supplementary Information

2 Role of Al-based coagulants on hybrid ozonation-coagulation
3 (HOC) process for WWTP effluent organic matter and
4 ibuprofen removal

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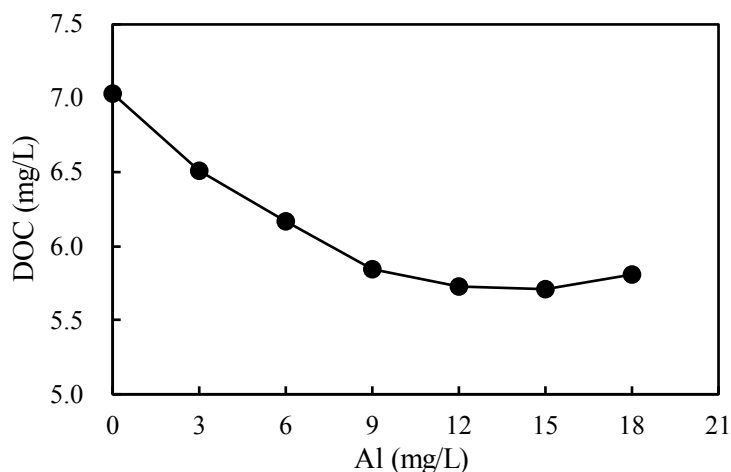
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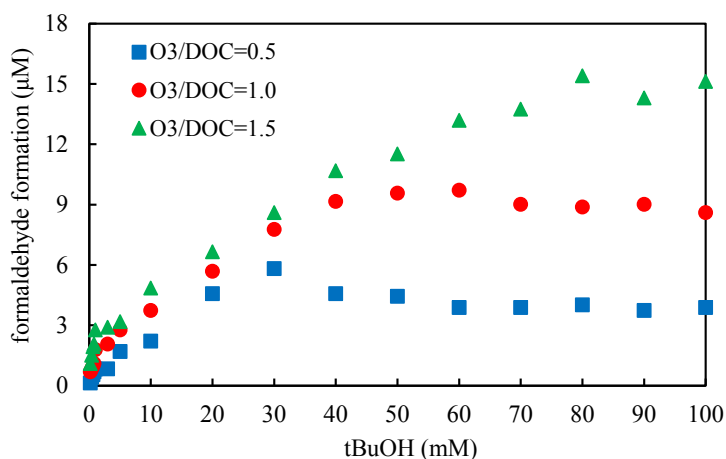


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Fig. S1 DOC removal performance at different Al dosages at pH 8

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Fig. S2 Formaldehyde formation at different tBuOH dosages

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33 **Text.S1.** UV/H₂O₂ experiment procedures

34 UV/H₂O₂ experiment was used to obtain $\sum k_i[S_i]$. UV/H₂O₂ was used to generate

35 •OH, and this experiment was conducted in ultrapure water. Experimental details

36 were modified based on previous work¹. A Low-pressure mercury lamp (254 nm, 40

37 W, Cnlight) positioned 5 cm above the water surface of the reactor (ϕ 5× 4 cm). The

38 solution was adjusted to have concentrations of 12 mg/L [Al], 1 µM pCBA and 2 mM

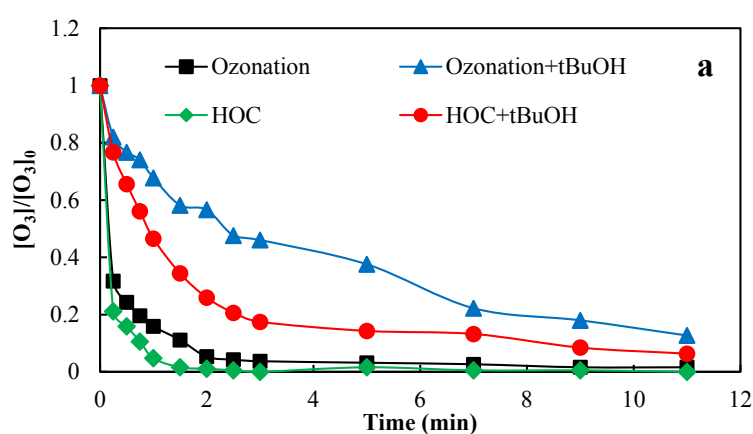
39 phosphate buffer (pH=8).

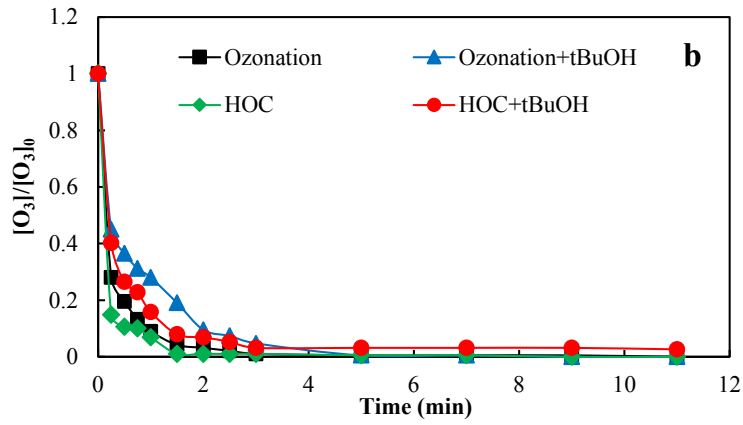
40 During the UV/H₂O₂ experiment, the rate of •OH generation can be calculated
 41 from Eq. (S1)².

$$42 \quad r_{OH\cdot} = \Phi_{OH} \cdot I_0 \cdot f_{H_2O_2} (1 - e^{-A}) \quad (S1)$$

43 Where Φ_{OH} is the quantum yield of •OH at 254 nm, and Φ_{OH} is 1.00 in the bulk
 44 solution³. I_0 is the incident light intensity at 254 nm, and it was measured by an
 45 illuminometer (ST-51X, SENTRY, Taiwan); A is the fraction of light absorbed by the
 46 bulk solution, and is given by $A = 2.303b(\epsilon_{H_2O_2}C_{H_2O_2} + \epsilon_{HO_2^-}C_{HO_2^-} + \epsilon_S C_S)$, where
 47 $\epsilon_{H_2O_2} = 17.9-19.6 \text{ M}^{-1} \text{ cm}^{-1}$, $\epsilon_{HO_2^-} = 220 \text{ M}^{-1} \text{ cm}^{-1}$, $\epsilon_S C_S$ is the absorbance of other
 48 compounds in the water matrix at 254 nm, and b is the water path length. In this case,
 49 AlCl₃•6H₂O had no UV adsorption at 254 nm. Parameter $f_{H_2O_2}$ is the fraction of
 50 absorbed light that is absorbed by H₂O₂ and HO₂⁻, and is given by
 51 $f_{H_2O_2} = 2.303b(\epsilon_{H_2O_2}C_{H_2O_2} + \epsilon_{HO_2^-}C_{HO_2^-})/A$. Based on Eq.(S1), •OH formation during
 52 UV/H₂O₂ experiment can be obtained in both ultrapure water and WWTP effluent
 53 (Fig. S5).

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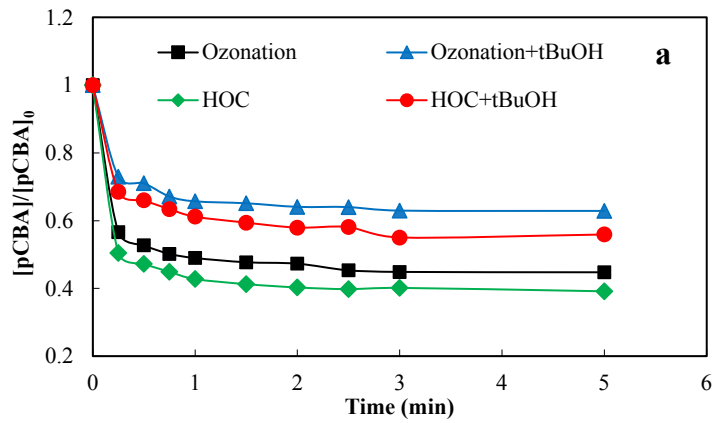
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Fig. S3 Ozone depletion at pH 8 in the ozonation and HOC processes.

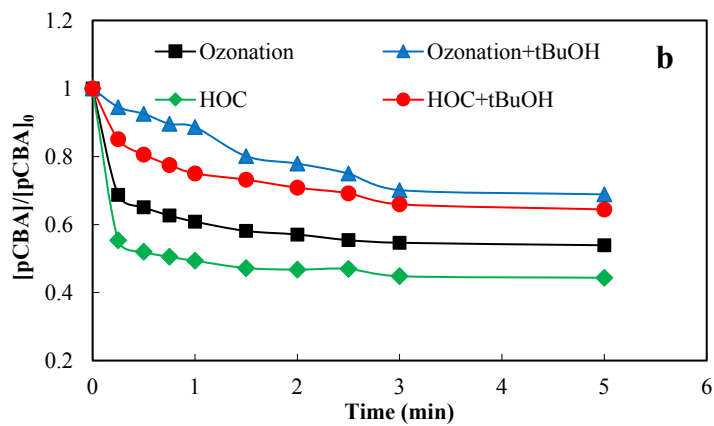
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a: ultrapure water; b: WWTP effluent. tBuOH dosage: 10mM.

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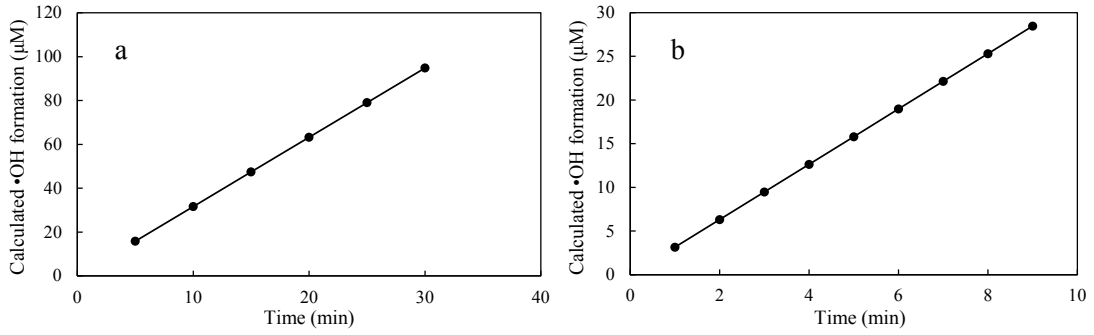
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Fig. S4 pCBA decomposition at pH=8 in the ozonation and HOC processes.

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a: ultrapure water; b: WWTP effluent

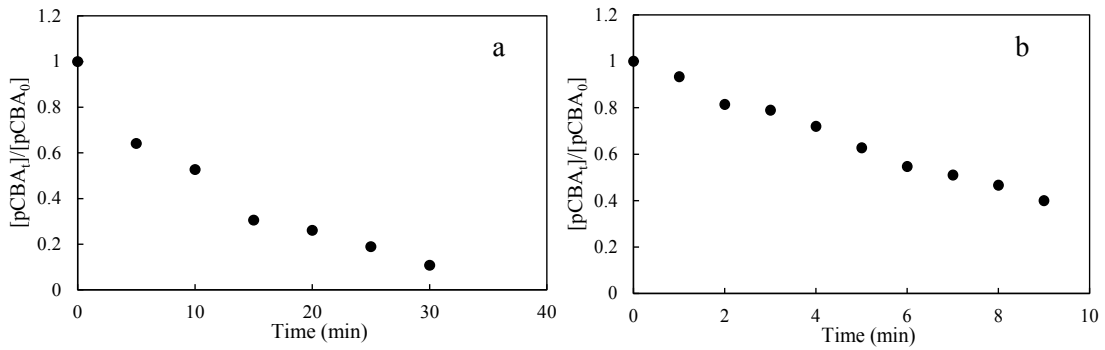
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65 **Fig. S5** •OH formation during UV/H₂O₂ experiment in ultrapure water (a) and
 66 WWTP effluent (b)

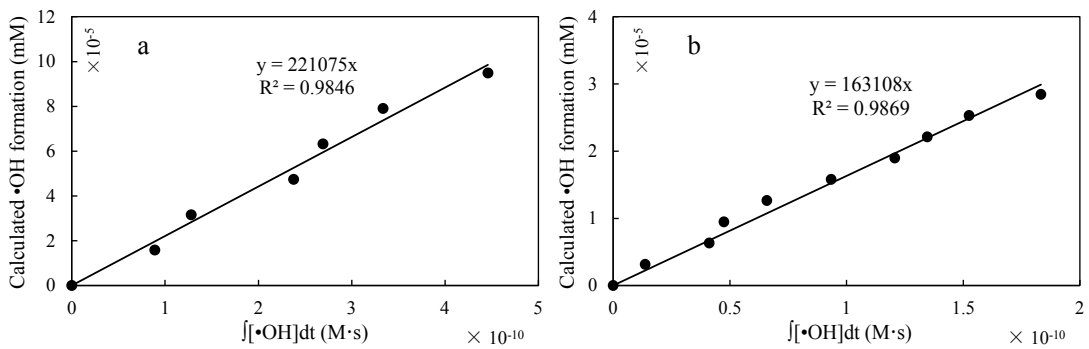
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69 **Fig. S6** pCBA removal during UV/H₂O₂ experiment in ultrapure water (a) and
 70 WWTP effluent (b)

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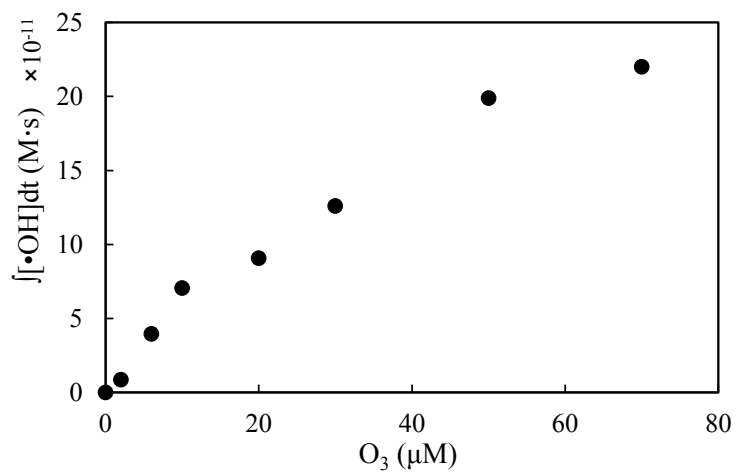


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73 **Fig. S7** $\sum k_i[S_i]$ calculation in (a) ultrapure water ($P = 1\text{E-}5$) and (b) WWTP effluent
 74 ($P = 1\text{E-}7$) (Calculated •OH formation vs. $\int[\bullet\text{OH}]dt$), the slope indicates $\sum k_i[S_i]$

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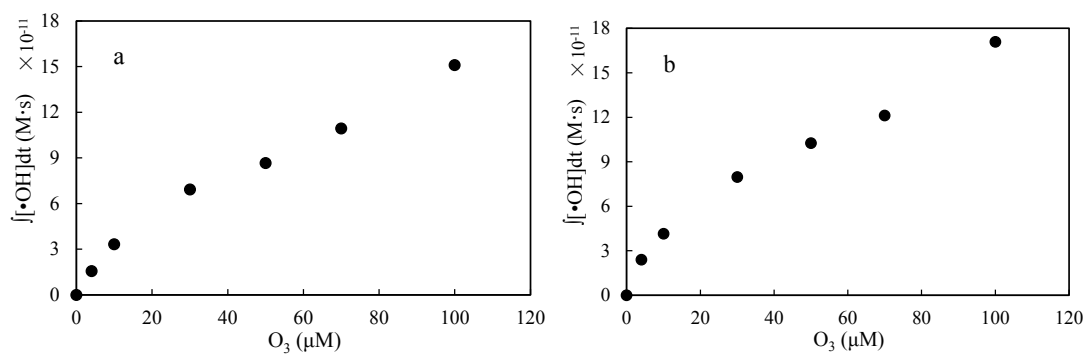
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78 **Fig. S8** ∫[•OH]dt at different ozone dosages in the HOC process in the ultrapure water

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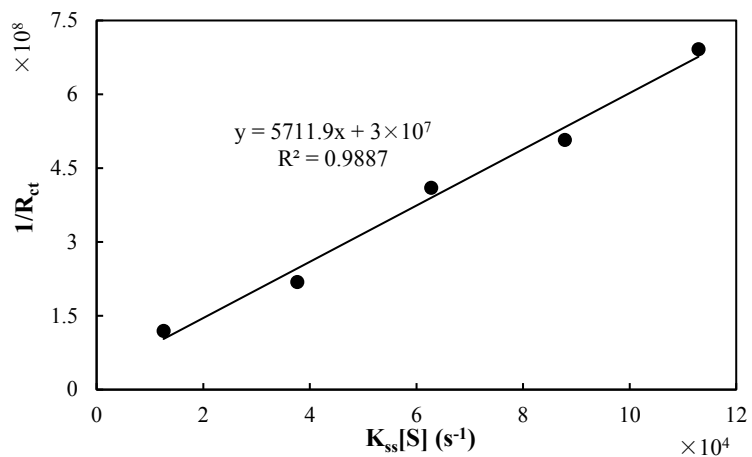
81 **Fig. S9** ∫[•OH]dt at different ozone dosages in the HOC process in WWTP effluent. a:

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without AlCl₃•6H₂O; b: with AlCl₃•6H₂O

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86 **Fig. S10** The plots of $1/R_{ct}$ vs. $(k_{SS}[S])$ in ultrapure water without $AlCl_3 \cdot 6H_2O$ ($P =$

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5E-4)

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89 References

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