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## Supplementary Information

Role of Al-based coagulants on hybrid ozonation-coagulation  
(HOC) process for WWTP effluent organic matter and ibuprofen  
removal

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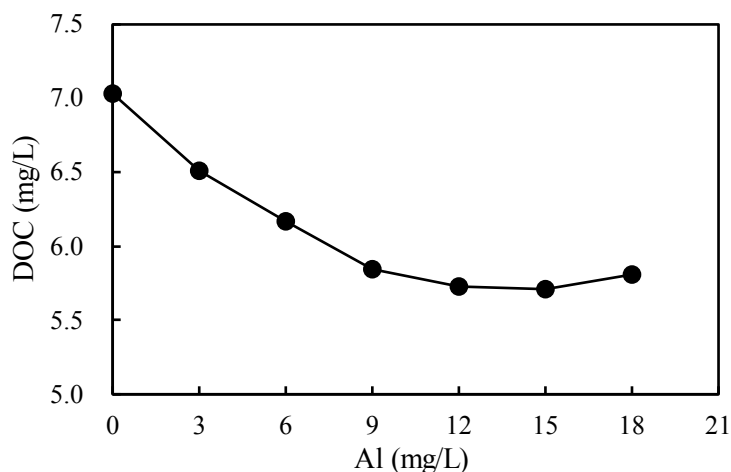
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Number of pages:7

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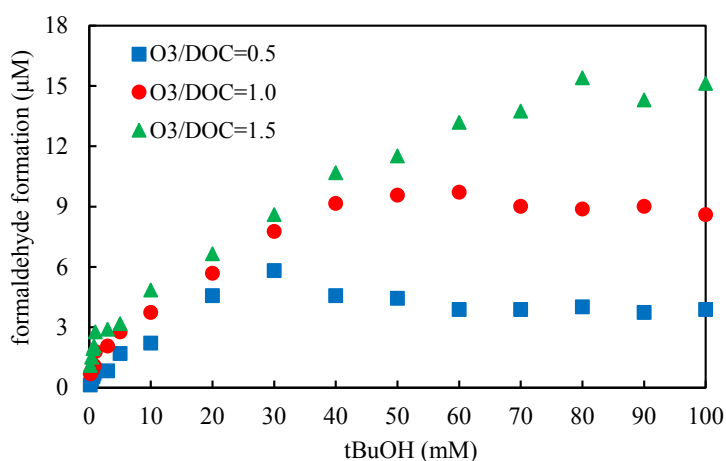


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**Fig. S1** DOC removal performance at different Al dosages at pH 8

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**Fig. S2** Formaldehyde formation at different tBuOH dosages

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33 **Text.S1.** UV/H<sub>2</sub>O<sub>2</sub> experiment procedures

34 UV/H<sub>2</sub>O<sub>2</sub> experiment was used to obtain  $\sum k_i[S_i]$ . UV/H<sub>2</sub>O<sub>2</sub> was used to generate

35 •OH, and this experiment was conducted in ultrapure water. Experimental details were

36 modified based on previous work<sup>1</sup>. A Low-pressure mercury lamp (254 nm, 40 W,

37 Cnlight) positioned 5 cm above the water surface of the reactor ( $\phi$  5 × 4 cm). The

38 solution was adjusted to have concentrations of 12 mg/L [Al], 1 µM pCBA and 2 mM

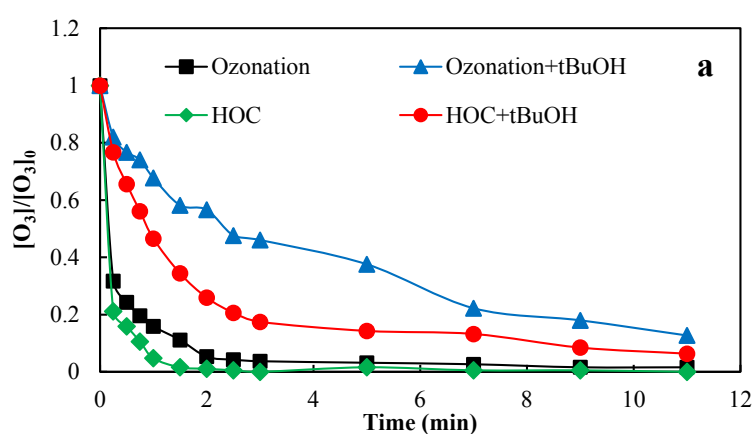
39 phosphate buffer (pH=8).

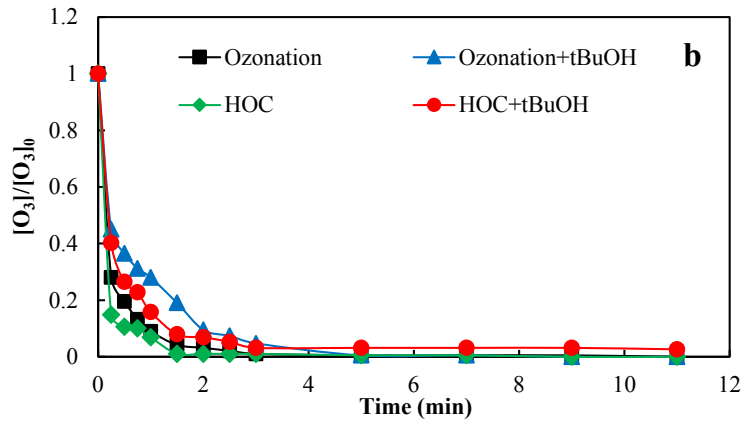
40 During the UV/H<sub>2</sub>O<sub>2</sub> experiment, the rate of •OH generation can be calculated  
 41 from Eq. (S1)<sup>2</sup>.

$$42 \quad r_{OH\cdot} = \Phi_{OH} \cdot I_0 \cdot f_{H_2O_2} (1 - e^{-A}) \quad (S1)$$

43 Where  $\Phi_{OH}$  is the quantum yield of •OH at 254 nm, and  $\Phi_{OH}$  is 1.00 in the bulk  
 44 solution<sup>3</sup>.  $I_0$  is the incident light intensity at 254 nm, and it was measured by an  
 45 illuminometer (ST-51X, SENTRY, Taiwan);  $A$  is the fraction of light absorbed by the  
 46 bulk solution, and is given by  $A = 2.303b(\epsilon_{H_2O_2}C_{H_2O_2} + \epsilon_{HO_2\cdot}C_{HO_2\cdot} + \epsilon_S C_S)$ , where  
 47  $\epsilon_{H_2O_2} = 17.9-19.6 \text{ M}^{-1} \text{ cm}^{-1}$ ,  $\epsilon_{HO_2\cdot} = 220 \text{ M}^{-1} \text{ cm}^{-1}$ ,  $\epsilon_S C_S$  is the absorbance of other  
 48 compounds in the water matrix at 254 nm, and  $b$  is the water path length. In this case,  
 49 AlCl<sub>3</sub>•6H<sub>2</sub>O had no UV adsorption at 254 nm. Parameter  $f_{H_2O_2}$  is the fraction of  
 50 absorbed light that is absorbed by H<sub>2</sub>O<sub>2</sub> and HO<sub>2</sub><sup>-</sup>, and is given by  
 51  $f_{H_2O_2} = 2.303b(\epsilon_{H_2O_2}C_{H_2O_2} + \epsilon_{HO_2\cdot}C_{HO_2\cdot})/A$ . Based on Eq.(S1), •OH formation during  
 52 UV/H<sub>2</sub>O<sub>2</sub> experiment can be obtained in both ultrapure water and WWTP effluent (Fig.  
 53 S5).

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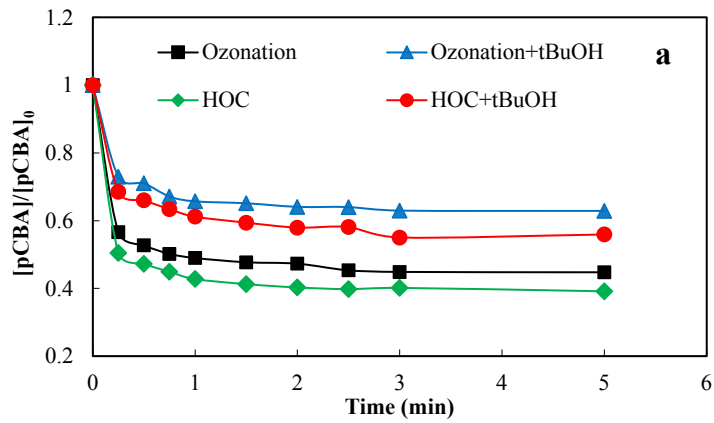
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**Fig. S3** Ozone depletion at pH 8 in the ozonation and HOC processes.

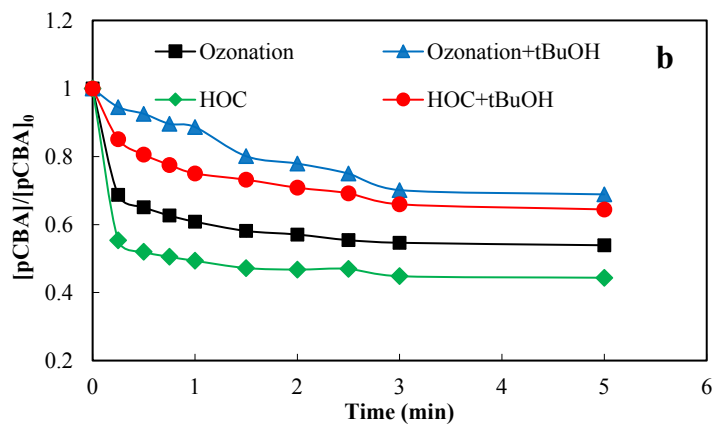
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a: ultrapure water; b: WWTP effluent. tBuOH dosage: 10mM.

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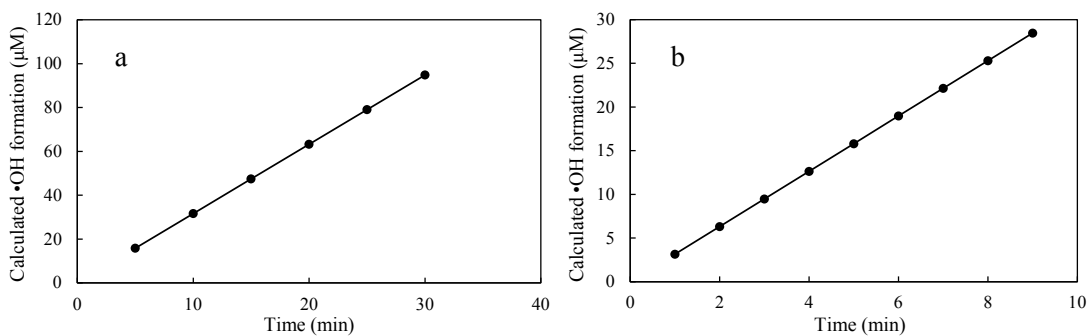
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**Fig. S4** pCBA decomposition at pH=8 in the ozonation and HOC processes.

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a: ultrapure water; b: WWTP effluent

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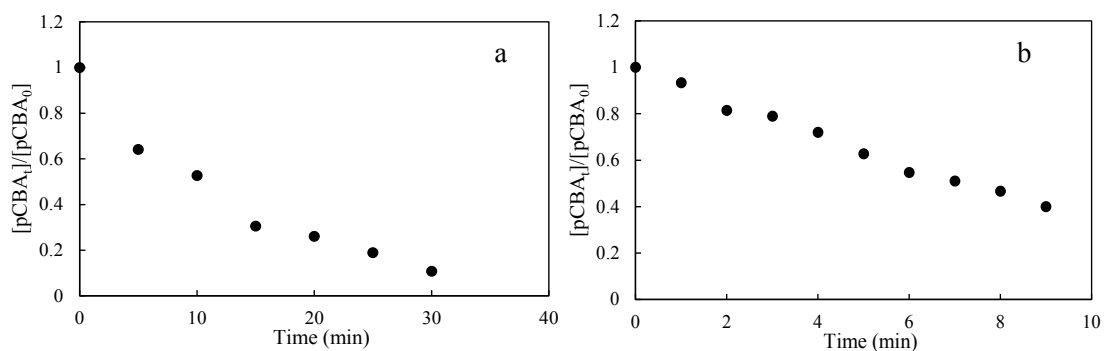
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65 **Fig. S5** •OH formation during UV/H<sub>2</sub>O<sub>2</sub> experiment in ultrapure water (a) and

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WWTP effluent (b)

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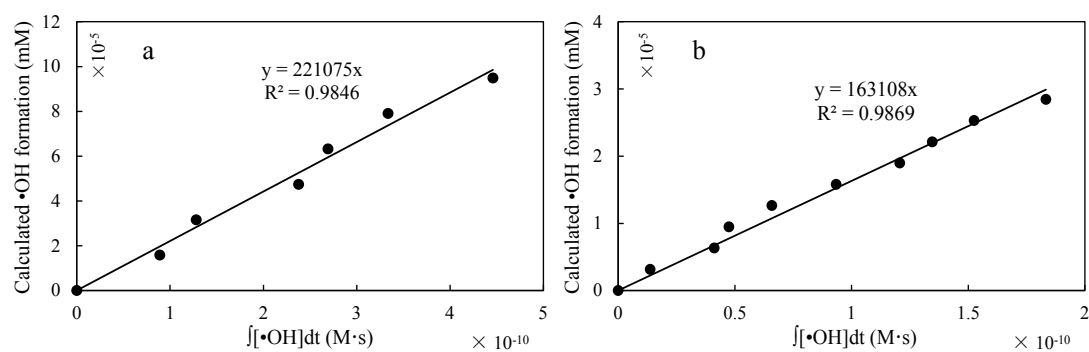
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69 **Fig. S6** pCBA removal during UV/H<sub>2</sub>O<sub>2</sub> experiment in ultrapure water (a) and

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WWTP effluent (b)

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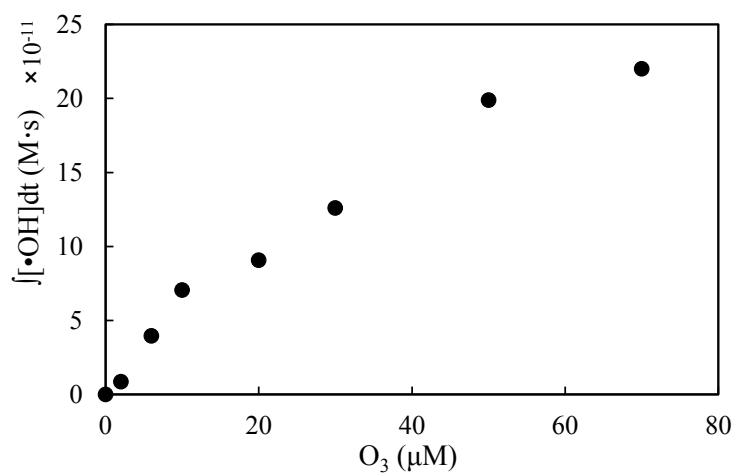
73 **Fig. S7**  $\sum k_i[S_i]$  calculation in (a) ultrapure water ( $P = 1E-5$ ) and (b) WWTP effluent

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( $P = 1E-7$ ) (Calculated •OH formation vs.  $\int[\bullet\text{OH}]dt$ ), the slope indicates  $\sum k_i[S_i]$

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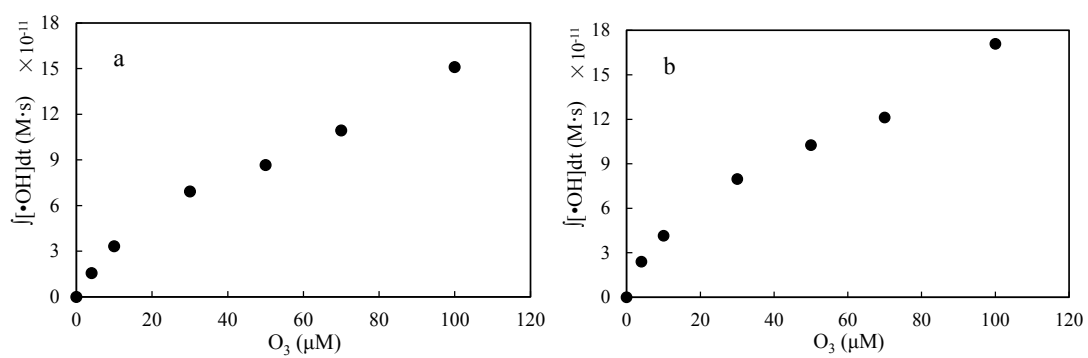
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78 **Fig. S8**  $\int[\bullet\text{OH}]\text{dt}$  at different ozone dosages in the HOC process in the ultrapure water

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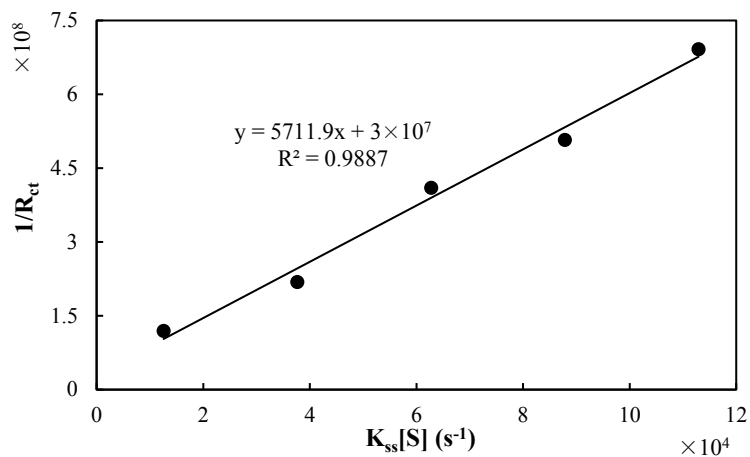
81 **Fig. S9**  $\int[\bullet\text{OH}]\text{dt}$  at different ozone dosages in the HOC process in WWTP effluent. a:

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without  $\text{AlCl}_3 \cdot 6\text{H}_2\text{O}$ ; b: with  $\text{AlCl}_3 \cdot 6\text{H}_2\text{O}$

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86 **Fig. S10** The plots of  $1/R_{ct}$  vs.  $(k_{SS}[S])$  in ultrapure water without  $AlCl_3 \cdot 6H_2O$  ( $P =$   
 87  $5E-4$ )

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