

Electronic Supplementary Material (ESI)

**Coke-resistant defect-confined Ni-based nanosheet-like catalysts
derived from halloysites for CO₂ reforming of methane**

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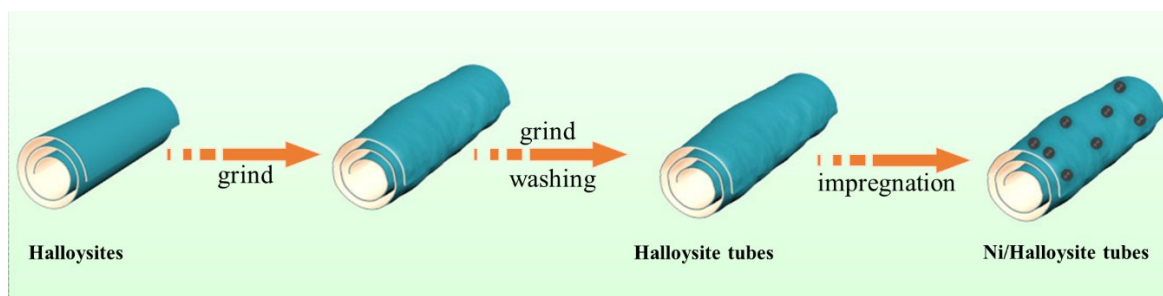
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Scheme S1. Schematic illustration of the fabrication strategy of the Ni/HA tubes.

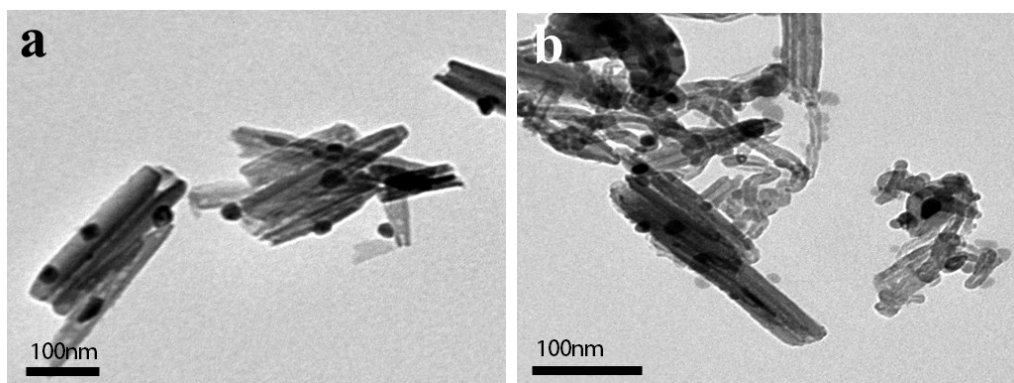


Fig. S1 TEM images of (a) Ni/HA tubes reduced at 750 °C for 1h b) Ni/HA tubes after the 20 h stability test.

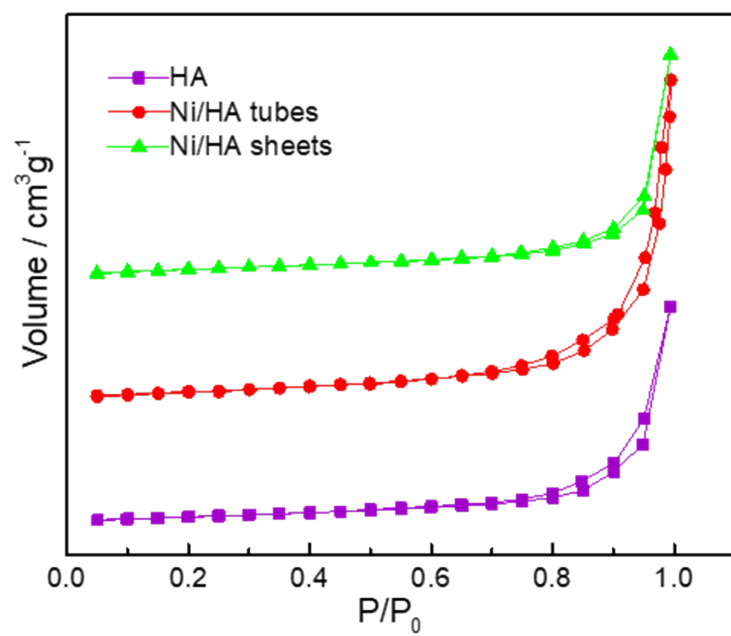


Fig. S2 N₂ sorption isotherms of HA, Ni/HA tubes and Ni/HA sheets.

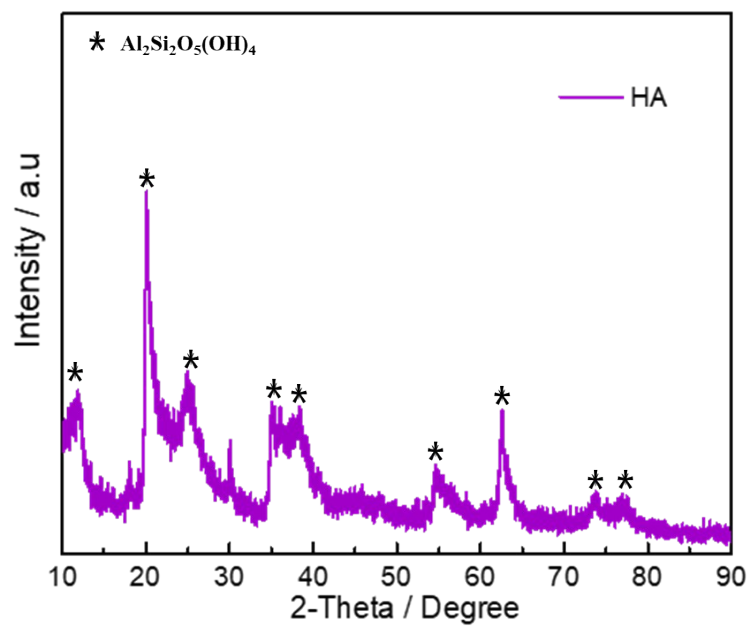


Fig. S3 XRD patterns of HA.

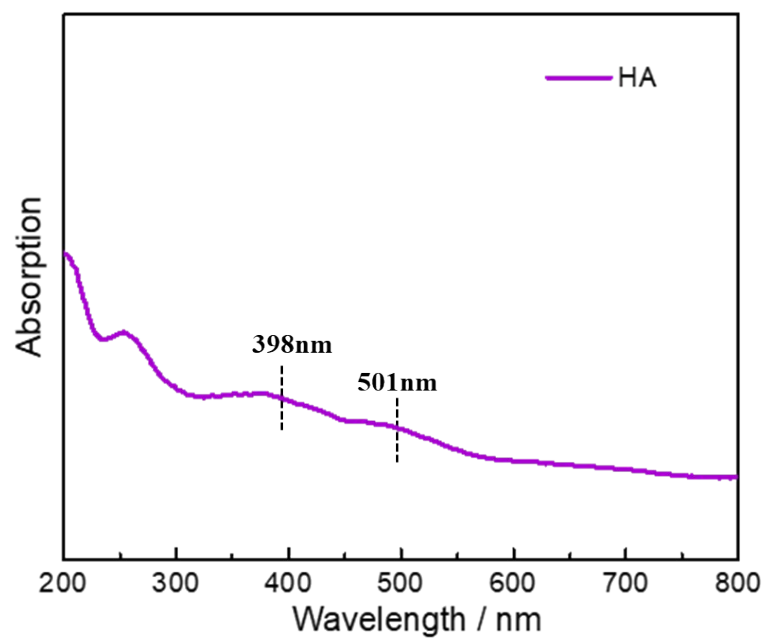


Fig. S4 UV-Vis spectra of HA.

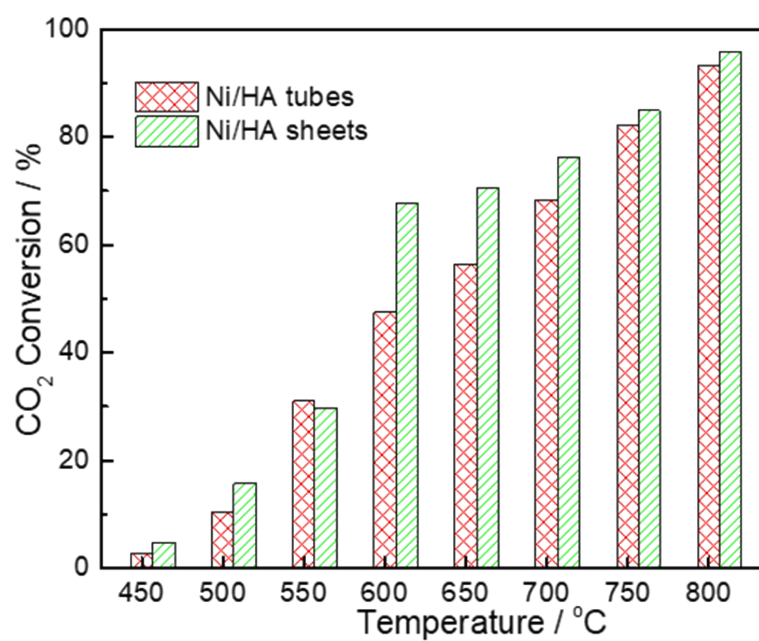


Fig. S5 Effects of reaction temperature on CO₂ conversion over the catalysts.

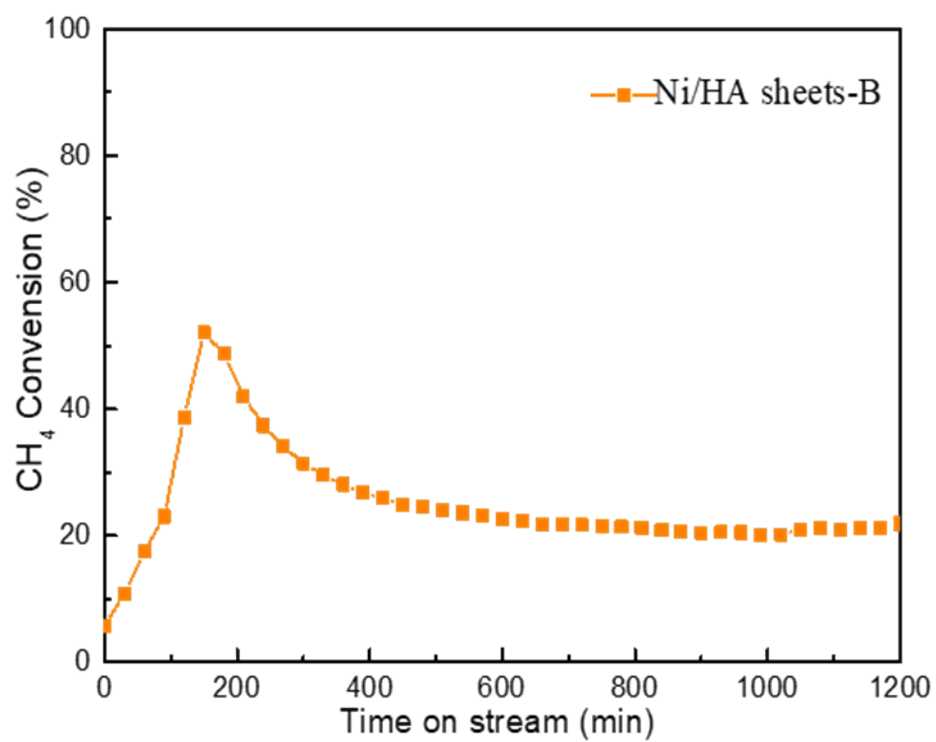


Fig. S6 CH₄ reforming of methane stability of the Ni/ HA sheets-B catalyst: CH₄ conversion as a function of reaction time (GHSV = 15,000 mL h⁻¹gcat⁻¹, 750 °C, 1 atm).

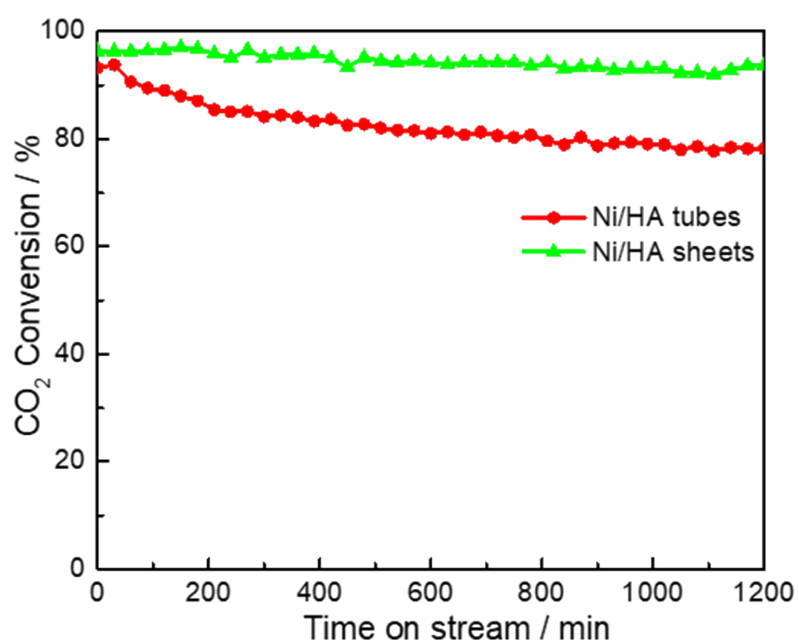


Fig. S7 CO₂ reforming of methane stability of the catalysts: CO₂ conversion as a function of reaction time (GHSV = 15,000 mL h⁻¹gcat⁻¹, 750 °C, 1 atm).

Table S1 Comparison of the previously reported Ni catalysts.

Catalysts	Temp. (°C)	Time X (h)	CH ₄ conv.	CH ₄ conv.	References
			(%)	(%)	
			T=0h	T=Xh	
Ni/ZrO ₂	750	12	53	33	ref. 1
10Ni15Ce/illite	800	4	88	84	ref. 2
Ni/SiO ₂ -F	700	6	62	56	ref. 3
LaNi _{0.4} Ce _{0.6} O ₃	800	10	91	80	ref. 4
10Ni15La/illite	800	25	80	78	ref. 5
Ni/HA sheets	750	20	89	88	This work

Table S2 Comparison of TOF_{CH₄} of the previously reported Ni catalysts.

Catalysts	Temp. (°C)	Time X (h)	TOF _{CH₄} ^c (h ⁻¹)	References
Ni/SBA-16	700	100	1728	ref. 6
Ni–MgO–ZrO ₂	800	5	1577	ref. 7
Co/Al ₂ O ₃	750	20	1584	ref. 8
Ni/HA sheets	750	20	2175	This work

Table S3 The TOF_{CH₄} of the as-prepared catalysts during the DRM reaction at 500 °C and textural properties of the spent catalysts.

Catalysts	Temp. (°C)	Time X (h)	Surface area ^a (m ² g ⁻¹)	Ni dispersion ^b (%)		TOF _{CH₄} ^c (h ⁻¹)	
				t = 10 min	t = 360 min	t = 10min	t = 360min
Ni/HA tubes	550	6	51	0.98%	0.37%	790	624
Ni/HA sheets	550	6	55	0.33%	0.34%	2175	2169

^a Specific surface area of the spent catalysts after the 20 h stability test determined by the BET method.

^b Ni dispersion were measured by H₂ pulse chemisorption.

^c The value of TOF was tested at 550°C with CH₄ flowing of 45 ml/min.

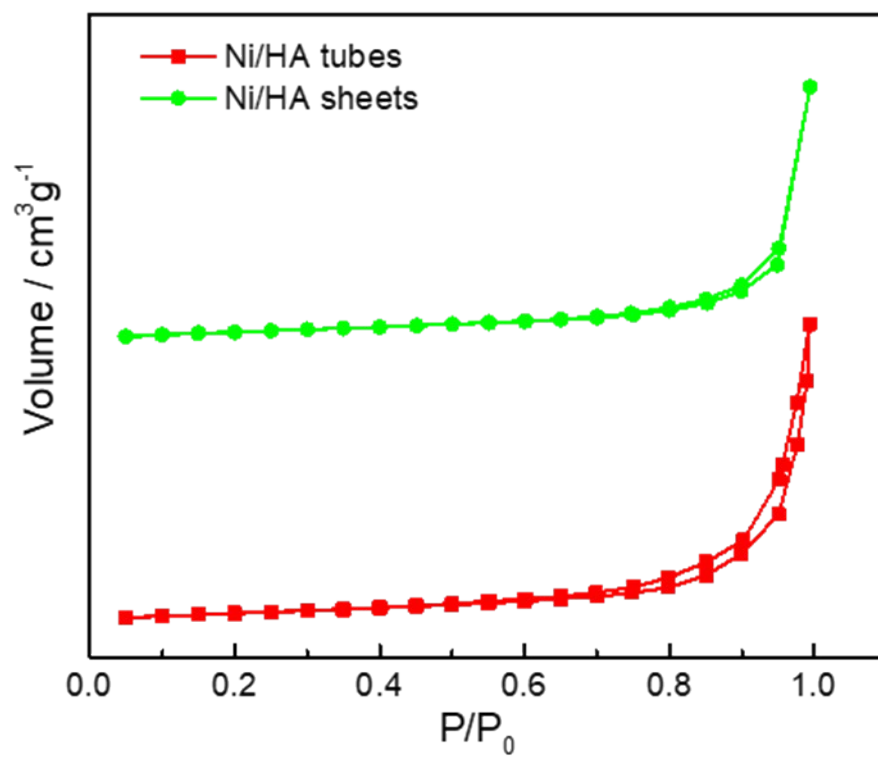


Fig. S8 N₂ sorption isotherms of the spent catalysts after the 20 h stability test.

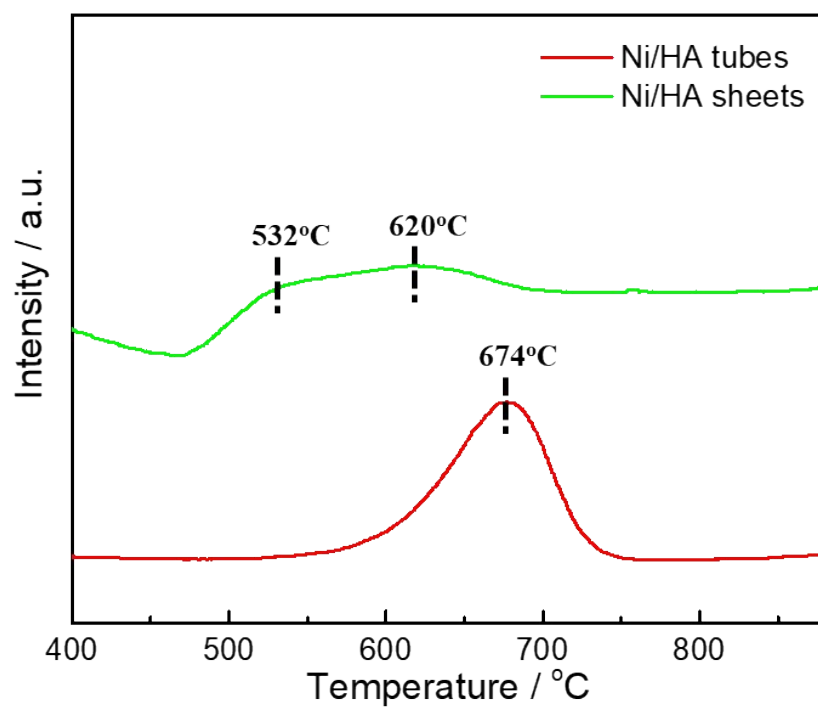


Fig. S9 O₂-TPO profiles of the spent catalysts after the 20 h stability test.

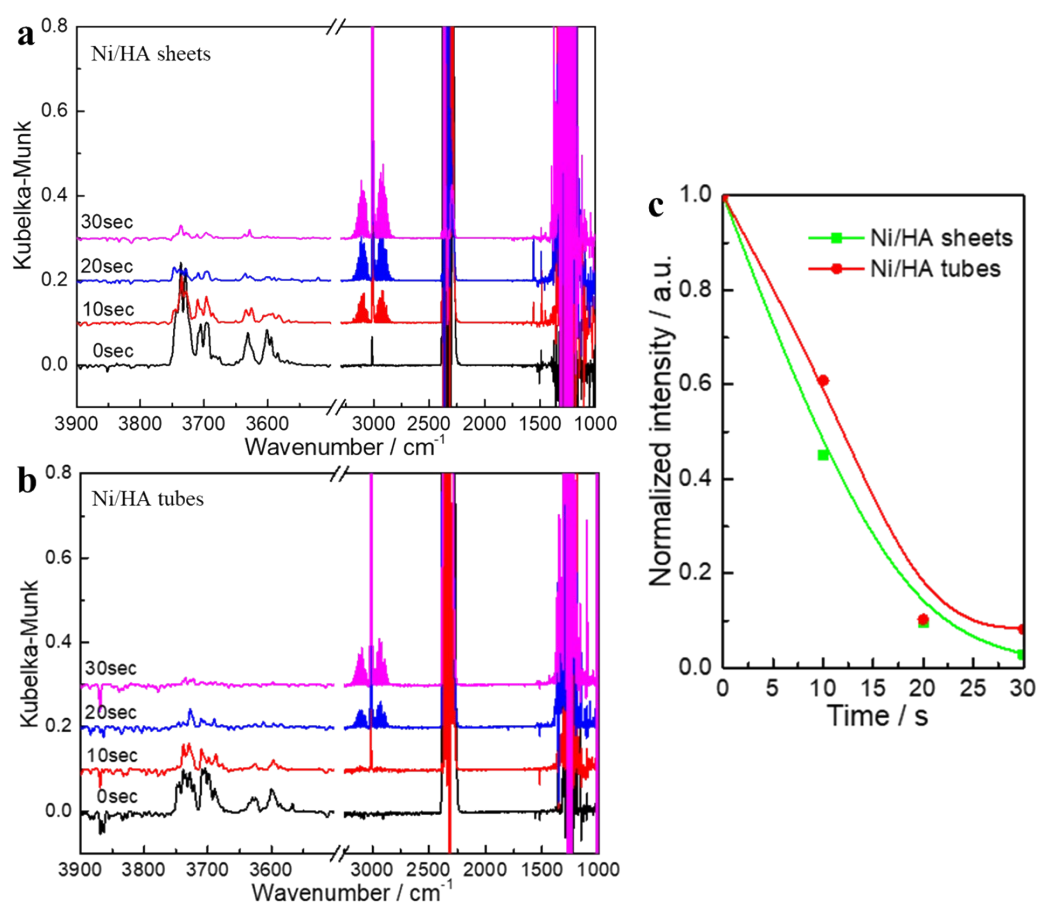


Fig. S10 *In situ* DRIFTS spectra of transient reactions over (a) Ni/HA sheets; (b) Ni/HA tubes catalysts after the CO₂ adsorption at 500 °C for 1 h and then exposed to CH₄; (c) consumption rate of Si-OH species over the Ni/HA sheets and Ni/HA tubes catalysts upon passing CH₄.

In situ DRIFTS of transient reactions over Ni/HA sheets and Ni/HA tubes catalysts was carried out to clarify the reaction mechanisms. First, the sample in the DRIFTS cell was pre-treated at 300 °C under a 50 ml/min N₂ atmosphere and kept at this temperature for 30 min. Then, the catalysts were pre-adsorbed by CO₂ at 500 °C for 1 h. After that, CH₄ introduced into the cell and spectra were obtained by collecting 16 scans with a resolution of 4 cm⁻¹. From the *in situ* DRIFTS spectra, the gas phase CH₄ can be easily discerned at wavenumbers 3015 and 1304 cm⁻¹ and CO₂ peaks appeared at 2360 and 2340 cm⁻¹, respectively (Fig. S10a-b). The intensity of Si-OH peaks at 3694-3800 cm⁻¹ over both the Ni/HA sheets and Ni/HA tubes disappeared while exposing to CH₄. In addition, the intensity of Si-OH over Ni/HA sheets decreases rapidly than that of Ni/HA tubes with flowing CH₄ stream due to the strong interaction between Ni and HA sheets (Fig. S10c). We can also conclude that bidentate formate species at 2878 cm⁻¹ dominate over bicarbonates detected at 1419 and 1224 cm⁻¹ on the surface of the catalysts. It means that H^{*} is produced via dissociation of CH₄ on Ni particles which accelerates the formation of transition from bicarbonate.

Reference

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