Ultrafine $\mathbf{N i M o O}_{\mathbf{x}}$ nanoparticles confined in mesoporous carbon for the<br>reduction of nitroarenes: Effect of the composition and accessibility of the active sites<br>Shuna Li, Yipin Lv, Guolong Song, Cuncheng Li, Daowei Gao* and<br>Guozhu Chen*

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[^0]Table S1. The XPS parameters of Ni 2 p and Mo 3d over different catalysts.

| Area ${ }^{\text {d }}$ (\%) |  | Binding energy ${ }^{\text {b }}$ (eV) |  |  | Sample | Binding energy ${ }^{\text {a }}$ (eV) |  |  | Area ${ }^{\text {c (\%) }}$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathrm{Ni}^{2+}$ | $\mathrm{Ni}^{0}$ | $\mathrm{Ni}(\mathrm{OH})_{2}$ | NiO | $\mathrm{Ni}^{0}$ |  | $\mathrm{Mo}^{0}$ | $\mathrm{Mo}^{++}$ | $\mathrm{Mo}^{6+}$ | $\mathrm{Mo}^{0}$ | $\mathrm{MoO}_{\mathrm{x}}$ |
| 96.4 | 3.6 | 856.2 | 855 | 853.0 | $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 230.7 | 232.4 | 235.9 | 22.0 | 88 |
| 82.2 | 17.8 | 856.1 | 854.4 | 852.9 | $\begin{gathered} \mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}- \\ 450 \end{gathered}$ | 230.6 | 232.3 | 235.5 | 33.6 | 66.4 |
| 67.5 | 32.5 | 856.4 | 854.5 | 852.7 | $\begin{gathered} \mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}- \\ 750 \end{gathered}$ | 230.6 | 232.3 | 235.7 | 36.3 | 63.7 |

${ }^{\text {a }}$ The binding energy of $\mathrm{Mo} 3 \mathrm{~d}_{3 / 2}$.
${ }^{\mathrm{b}}$ The binding energy of Ni $2 \mathrm{p}_{5 / 2}$.
${ }^{\mathrm{c}}$ The difference of valence of Mo species. Area $=\mathrm{Mo}^{\mathrm{x}} /\left(\mathrm{Mo}^{0}+\mathrm{Mo}^{4+}+\mathrm{Mo}^{6+}\right)$.
${ }^{\mathrm{d}}$ The difference of valence of Ni species. Area $=\mathrm{Ni}^{\mathrm{x}} /\left(\mathrm{Ni}^{0}+\mathrm{Ni}^{2+}\right)$.

Table S2. The kinetic constants and TOF of $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ at different concentration of $\mathrm{NaBH}_{4}$.

| Samples | Catalyst <br> amount <br> $(\mathrm{mg})$ | Concentration <br> of <br> $\mathrm{NaBH}_{4}$ <br> $\left({\left.\mathrm{~mol} \cdot \mathrm{~L}^{-1}\right)}\right.$ | Concentration <br> of <br> $4-\mathrm{NP}$ <br> $\left(\mathrm{mol} \cdot \mathrm{L}^{-1}\right)$ | $\mathrm{Time}^{\mathrm{a}}$ <br> $(\mathrm{min})$ | k <br> $\left(\mathrm{min}^{-1}\right)$ | K <br> $\left(\mathrm{min}^{-1} \cdot \mathrm{~g}^{-1}\right)$ | $\mathrm{TOF}^{\mathrm{b}} \times 10^{3}$ <br> $\left(\mathrm{~s}^{-1}\right)$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.5 | 0.005 | 0.012 | 8.5 | 0.10 | 200 | 42.6 |
| $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.5 | 0.01 | 0.012 | 6.0 | 0.19 | 380 | 60.4 |
| $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.5 | 0.02 | 0.012 | 2.0 | 0.48 | 960 | 175.8 |
| $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.5 | 0.03 | 0.012 | 2.3 | 0.41 | 820 | 157.5 |
| $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.5 | 0.04 | 0.012 | 1.9 | 0.49 | 980 | 190.7 |

${ }^{a}$ Calculated at $50 \%$ of the conversion.
${ }^{\mathrm{b}}$ Calculated on the basis of total catalyst and conversion rate of $50 \%$.

Table S3. The kinetic constants and TOF of $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ under different amount of catalyst in the reduction reaction.

| Samples | Catalyst amount (mg) | Concentration of $\mathrm{NaBH}_{4}$ ( $\mathrm{mol} \cdot \mathrm{L}^{-1}$ ) | $\begin{gathered} \text { Concentration } \\ \text { of } \\ 4-\mathrm{NP} \\ \left(\mathrm{~mol} \cdot \mathrm{~L}^{-1}\right) \\ \hline \end{gathered}$ | Time $\qquad$ <br> (min) | $\begin{gathered} \mathrm{k} \\ \left(\min ^{-1}\right) \end{gathered}$ | $\underset{\left(\mathrm{min}^{-1} \cdot \mathrm{~g}^{-1}\right)}{\mathrm{K}}$ | $\begin{gathered} \mathrm{TOF}^{\mathrm{b}} \times 10^{3} \\ \left(\mathrm{~s}^{-1}\right) \end{gathered}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.0625 | 0.02 | 0.012 | 12.3 | 0.07 | 1120 | 235.6 |
| NiMoO ${ }_{\text {x }} / \mathrm{MC}-\mathrm{PL}$ | 0.125 | 0.02 | 0.012 | 7.8 | 0.12 | 968 | 185.8 |
| $\mathrm{NiMoO}_{\mathbf{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.25 | 0.02 | 0.012 | 4.5 | 0.27 | 1080 | 161 |
| $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.5 | 0.02 | 0.012 | 2.0 | 0.48 | 960 | 175.8 |
| $\mathrm{NiMoO}_{x} / \mathrm{MC}-\mathrm{PL}$ | 1.0 | 0.02 | 0.012 | 1.3 | 1.06 | 1060 | 125.5 |

${ }^{a}$ Calculated at $50 \%$ of the conversion.
${ }^{\mathrm{b}}$ Calculated on the basis of total catalyst and conversion rate of $50 \%$.

Table S4. The kinetic constants and TOF of $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ under different amount of 4-NP.

| Samples | Catalyst <br> amount <br> $(\mathrm{mg})$ | Concentration <br> of <br> $\mathrm{NaBH}_{4}$ <br> $\left(\mathrm{~mol} \cdot \mathrm{~L}^{-1}\right)$ | Amount <br> of <br> $4-\mathrm{NP}$ <br> $(\mu \mathrm{L})$ | $\mathrm{Time}^{\mathrm{a}}$ <br> $(\mathrm{min})$ | k <br> $\left(\mathrm{min}^{-1}\right)$ | K <br> $\left(\mathrm{min}^{-1} \cdot \mathrm{~g}^{-1}\right.$ <br> $)$ | $\mathrm{TOF}^{\mathrm{b}} \times 10^{3}$ <br> $\left(\mathrm{~s}^{-1}\right)$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.5 | 0.02 | 10 | 1.1 | 0.77 | 1540 | 329.4 |
| $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.5 | 0.02 | 15 | 2.4 | 0.67 | 1340 | 150.9 |
| $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.5 | 0.02 | 20 | 1.8 | 0.52 | 1040 | 201.3 |
| $\mathrm{NiMoO}_{\mathrm{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.5 | 0.02 | 25 | 2.9 | 0.46 | 920 | 124.9 |
| $\mathrm{NiMoO}_{\mathbf{x}} / \mathrm{MC}-\mathrm{PL}$ | 0.5 | 0.02 | 30 | 4.3 | 0.25 | 500 | 84.0 |

${ }^{a}$ Calculated at $50 \%$ of the conversion.
${ }^{\mathrm{b}}$ Calculated on the basis of total catalyst and conversion rate of $50 \%$.


Fig. S1. XRD patterns of various morphologies of $\mathrm{NiMoO}_{x} /$ SBA-15 $(\mathrm{a}, \mathrm{b})$ in the small-angle and wide-angle.


Fig. S2. The EDS analysis of NiMoS/MC-PL.


Fig. S3. The reduction of 4-NP recorded every 1.5 min with different concentration of the $\mathrm{NaBH}_{4}(\mathrm{a}-\mathrm{e})$; Time dependent conversion of 4-NP over the catalysts (f); The relationship between the $A_{t} / A_{0}$ and reaction time $(g)$; Plots of $\ln \left(C_{t} / \mathrm{C}_{0}\right)$ versus reaction time at different concentration of $\mathrm{NaBH}_{4}$ for reduction $4-\mathrm{NP}$ (h).


Fig. S4. The reduction of 4-NP recorded every 1.5 min with different amount of catalyst (a-e); Plots of conversion versus time over the different amount of catalyst (f); The relationship between the $\ln \left(\mathrm{C}_{\mathrm{t}} / \mathrm{C}_{0}\right)$ and reaction time for reduction 4-NP $(\mathrm{g})$; The correlation between the k and amount of catalyst (h).


Fig. S5. The reduction of 4-NP recorded every 1.08 min with different amount of 4-

NP (a-e); Plots of conversion versus time over the different amount 4-NP (f); The relationship between the $\ln \left(\mathrm{C}_{\mathrm{t}} / \mathrm{C}_{0}\right)$ and reaction time (g); The correlation between the k and amount of 4-NP (h).


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