

Supporting Information

Encapsulation of C-N-decorated metal sub-nanoclusters/single atoms into a Metal-organic framework for highly-efficient catalysis

Xuan Qiu,[#] Jianmin Chen,[#] Xinwei Zou, Ruiqi Fang, Liyu Chen, Zhijie Chen, Kui Shen* and Yingwei Li*

State Key Laboratory of Pulp and Paper Engineering, School of Chemistry and Chemical Engineering, South China University of Technology, Guangzhou 510640, China.

[#]These authors contributed equally to this work

E-mail: *cekshen@scut.edu.cn* (K.S.), *liyw@scut.edu.cn* (Y.L.)

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Experimental Section

Chemicals

All chemicals were purchased from commercial sources and used without further purification. All solvents were analytical grade and distilled prior to use.

Synthesis of M_6L_4 (**M**: (en) $Pd(NO_3)_2$; **L**: 2,4,6-tri(pyridin-4-yl)-1,3,5-triazine)^{S1}

M_6L_4 was prepared according to the literature report.^{S1} **M** (60 mg, 0.206 mmol), **L** (43 mg, 0.137 mmol), and 10 mL water were stirred at room temperature for 24 h. The mixture was filtered and the filtrate was concentrated with evaporator to obtain the light-yellow solid.

Synthesis of MIL-101^{S2}

$Cr(NO_3)_3 \cdot 9H_2O$ (2.00 g, 5 mmol), HF (48 wt%, 5 mmol), and terephthalic acid (0.823 g, 5 mmol) were added into 24 mL deionized water. After heating at 220 °C for 8 h, the mixture was cooled first to 150 °C in 1 h, and then slowly to room temperature in 12 h. The green MIL-101 powder was isolated from the solution and washed with deionized water and ethanol, and then soaked in ethanol (95% EtOH with 5% water) at 80 °C for 24 h. The obtained solid was finally dried overnight at 150 °C under vacuum.

Synthesis of $M_6L_4 \subset MIL-101$

6.3 mg **L** was added to 8 mL n-hexane. After sonicating for 2 h, 310 mg activated MIL-101 was added. The suspension was stirred at room temperature for 20 h, to which a small amount of aqueous **M** (7 mg) solution (0.40 mL) was added dropwise under vigorous stirring. Afterwards, the suspension was stirred for another 72 h. The

obtained solid was washed with water, and activated by heating at 150 °C for 12 h under dynamic vacuum.

Synthesis of PCN \subset M

The M₆L₄ \subset MIL-101 hybrids were treated at 250°C under H₂ flow for 2 h. The heating rate and cooling rate were 0.5 °C/min. The obtained hybrids were washed with H₂O and ethanol, and then dried at room temperature. PCN \subset M hybrids with different Pd contents were synthesized according to the above protocol by varying the amount of precursors. The obtained hybrids were named as XPCN \subset M (X = 0.33, 0.51, 0.64, 0.82), where X represents the actual Pd weight percentage, as measured by atomic absorption spectrometry (AAS). For 0.33PCN \subset M, 0.51PCN \subset M, 0.64PCN \subset M and 0.82PCN \subset M, the added **L** precursor was 3.0 mg, 4.7 mg, 6.3 mg and 7.4 mg, and the **M** mass was 3.5 mg, 5.2 mg, 7 mg and 8.6 mg, respectively. The theoretical Pd loading, the actual Pd loading and the doping efficiency were shown in Table S2.

Synthesis of Pd/MIL-101

310 mg MIL-101 was soaked in M₆L₄ aqueous solution (33 mg M₆L₄ in 8 mL H₂O). After stirring for 24 h, the suspension was filtered and washed with H₂O for several times. The obtained solid was washed with water, activated by heating at 150 °C for 12 h under dynamic vacuum, and then heated at 250 °C in H₂ for 2 h. The heating rate and cooling rate were both 0.5 °C/min. The theoretical Pd loading, the actual Pd loading and the doping efficiency were shown in Table S2.

Nitrobenzene hydrogenation reaction

Typically, nitrobenzene (0.1 mmol) and catalyst (0.0015 mmol Pd) were added to a Schlenk tube. Ethanol (2 mL) was then added under hydrogen at room temperature. Then an hydrogen balloon was connected to the Schlenk tube. The reaction mixture was stirred at room temperature for the desired time. Afterwards, the reaction liquid was collected by centrifugation. the solid catalyst was washed with ethyl acetate (3 × 5 mL). The liquid was all collected and concentrated in vacuo. The crude product was quantified by GC-MS analysis.

Heterogeneity of the catalyst

To verify whether the catalysis of 0.64PCN \subset M was truly heterogeneous, the solid catalyst was filtered from the reaction solution after 2 min (Con. 52%) in nitrobenzene hydrogenation reaction. The reaction was continued with the filtrate in the absence of solid catalyst for an additional 5 min. The solution in the absence of solid did not exhibit any further reactivity. The results demonstrated that the reaction proceeded mostly on the heterogeneous surface.

Catalytic hydrogenation of furfural

Typically, FFA (0.52 mmol), catalyst (Pd/FFA = 1.15×10^{-3}) and water (4 mL) were added to a 10 mL stainless steel autoclave equipped with a magnetic stirrer, a pressure gauge, and an automatic temperature controller. Then the autoclave was sealed and purged with hydrogen at low pressure for several times to remove air. Then the autoclave was purged with H₂ for the desired pressure and then set to the

desired temperature. After reaction, the autoclave was cooled to room temperature and the reaction liquid was collected by centrifugation. The solid catalyst was washed with ethyl acetate (3×5 mL). The liquid was all collected and concentrated in vacuo. The crude product was quantified by GC-MS analysis.

The conversions and selectivities were calculated based on the moles of furfural. The conversion of furfural (mol%) and cyclopentanone selectivity (mol%) were calculated using the following equations:

$$\text{Furfural conversion} = \left(1 - \frac{\text{Moles of furfural}}{\text{Moles of furfural loaded}} \right) \times 100\%$$

$$\text{Cyclopentanone yield} = \frac{\text{Moles of cyclopentanone}}{\text{Moles of furfural loaded}} \times 100\%$$

Recycling of the catalysts

The recyclability of the catalysts was tested for the nitrobenzene hydrogenation reaction and the catalytic hydrogenation of furfural under the investigated reaction conditions as described above except using the recovered catalysts. Each time, the catalyst was separated from the reaction mixture by centrifugation at the end of catalytic reaction, thereafter, washed with ethyl acetate and ethanol, dried at room temperature. The catalyst powder was reused as catalyst for a new run.

Materials characterization

BET surface area measurements were performed with N₂ adsorption/desorption isotherms at 77 K on a Micromeritics ASAP 2020M instrument. Prior to analysis, the samples were degassed at 150 °C for 12 h. Powder X-ray diffraction patterns of the

samples were recorded on a Bruker D8 ADVANCR using Cu K α radiation (40 kV, 40 mA).

The size and morphology of the materials were determined by a scanning electronic microscope (SEM, **Merlin** from **Zeiss**) equipped with an energy dispersive X-ray detector (EDS, X-MaxN20 from Oxford), Transmission Electron Microscopy (TEM) (JEM-2100F, JEOL, Tokyo, Japan) as well as cold field-emission spherical-aberration corrected TEM (Cold FEG Cs corrected TEM) (JEM-ARM200F, Japan) were operated at an accelerating voltage of 200 kV. Energy dispersive X-ray spectroscopy (EDX) was performed to locate elemental distribution of Pd, Cr and N with an SDD-type EDX detector. The attainable energy-resolution of the EDX detector is 130 eV. The identification and quantitation of products were performed on a GC-MS spectrometer (Agilent Technologies 7890B-5977A equipped with a 0.25 mm \times 30 m HP-5MS capillary column).

The Pd contents in the samples were measured quantitatively by atomic absorption spectroscopy (AAS) on a HITACHI Z-2300 instrument. XPS spectra were recorded on ESCALAB 250Xi from Thermo Fisher-VG Scientific using Mono Al K α as the X-ray source. Elemental analysis was performed on an Elementar Vario EL III equipment by weighing samples of 0.2-0.3 mg and packing with aluminium foil for the measurement. All materials were degassed at 150 °C for 12 h before measurement. TGA-DSC was performed on a Q600 SDT from TAINC under N₂ atmosphere. H₂-TPR measurements were performed on DAS-7200. The samples were pre-treated under an Ar atmosphere at 150 °C for 1 h to clean the surface, followed by cooling

down to room temperature. The flow of 10% H₂/Ar (50 mL/min) was then switched into the system, and the samples were heated up to 800 °C from room temperature at a rate of 10 °C/min.

The X-ray absorption data at the Pd *K* - edge of the samples were recorded at room temperature in transmission mode and in the fluorescent mode with silicon drift fluorescence detector at beam line BL14W1 of the Shanghai Synchrotron Radiation Facility (SSRF), China. The station was operated with a Si(311) double crystal monochromator. During the measurement, the synchrotron was operated at energy of 3.5 GeV and a current between 150-210 mA. The photon energy was calibrated with the first inflection point of Pd K-edge in Pd metal foil.

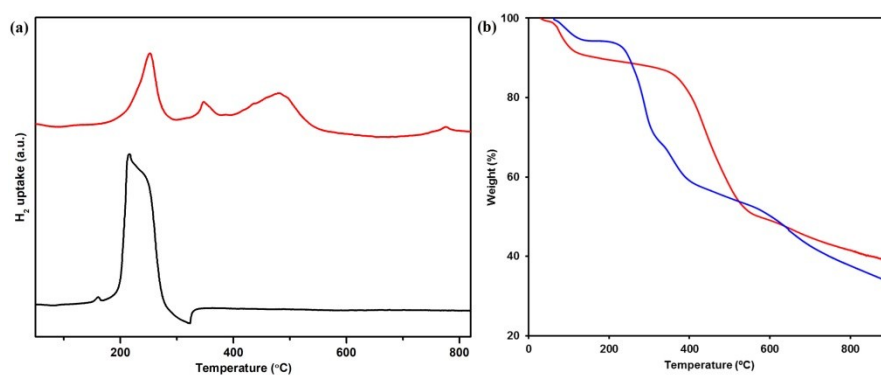


Fig. S1 (a) TPR patterns of M₆L₄ (black curve) and M₆L₄⊂MIL-101 (red curve); (b) TGA results of MIL-101 (red curve) and M₆L₄ (blue curve).

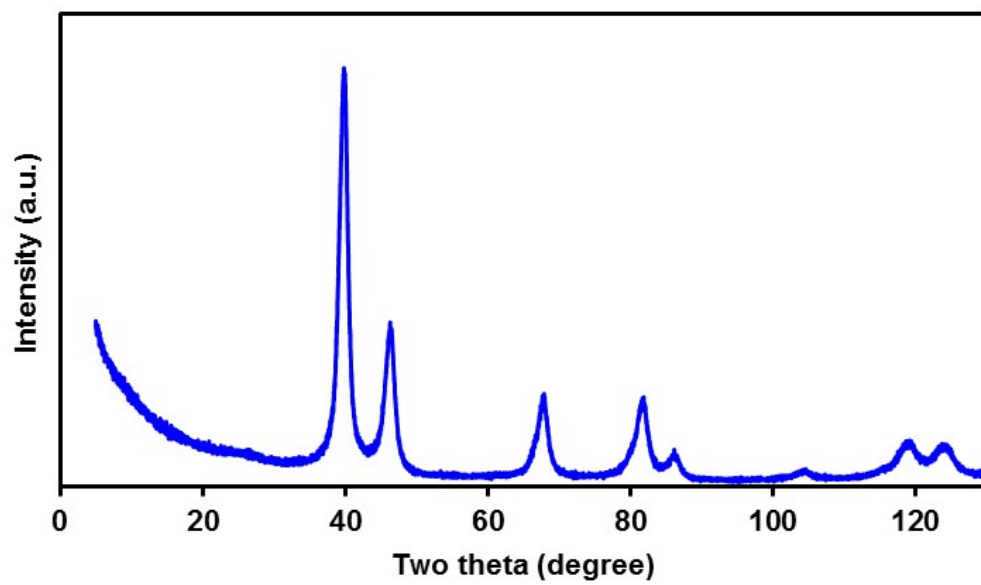


Fig. S2 PXRD patterns of Pd/C-N.

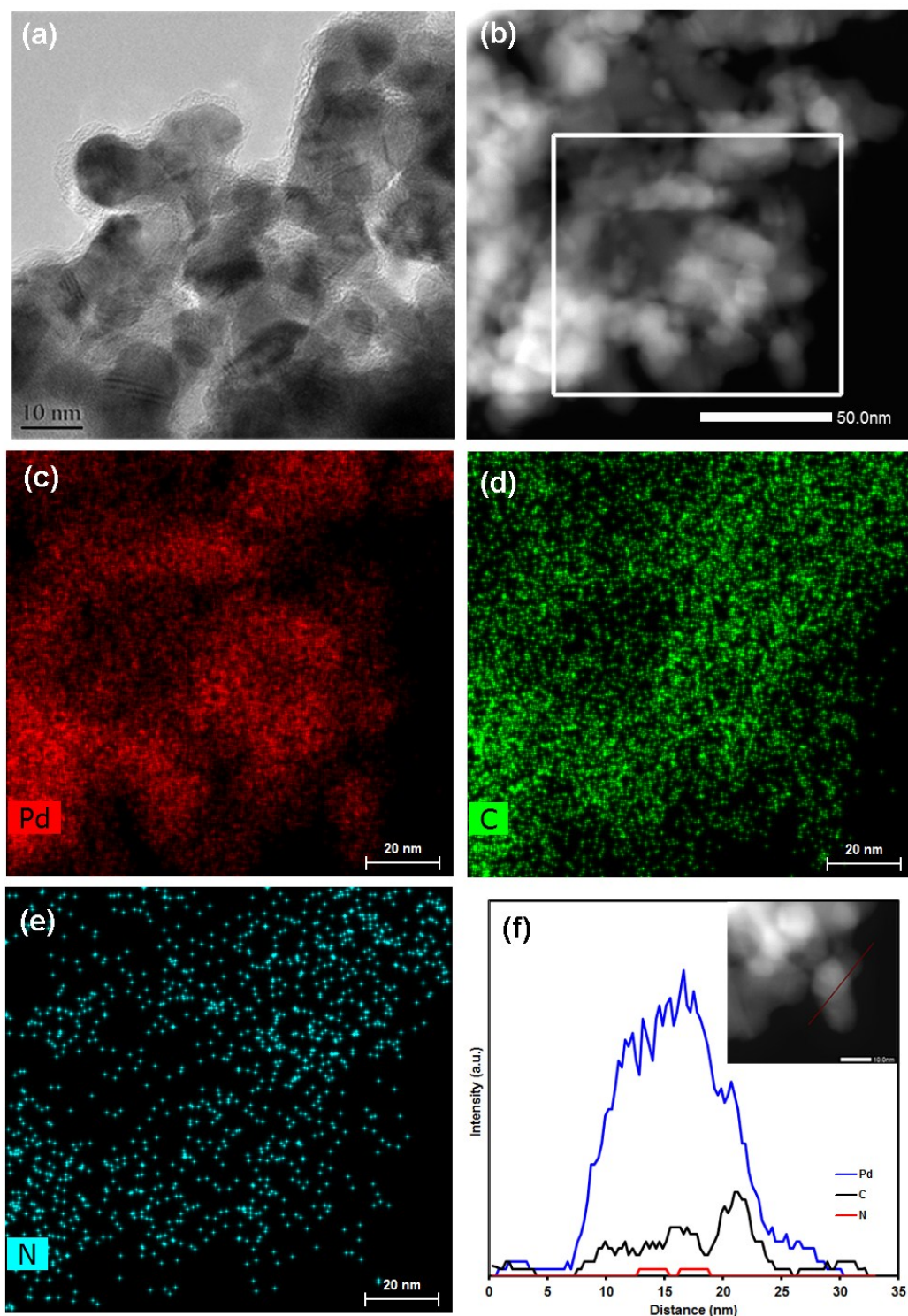


Fig. S3 (a) TEM image of Pd/C-N. (b) HAADF-STEM image of Pd/C-N and (c-e) corresponding EDX elemental mapping images of Pd, C, and N. (f) Elemental line-scanning spectra of Pd/C-N along the direction marked by a red line (inset).

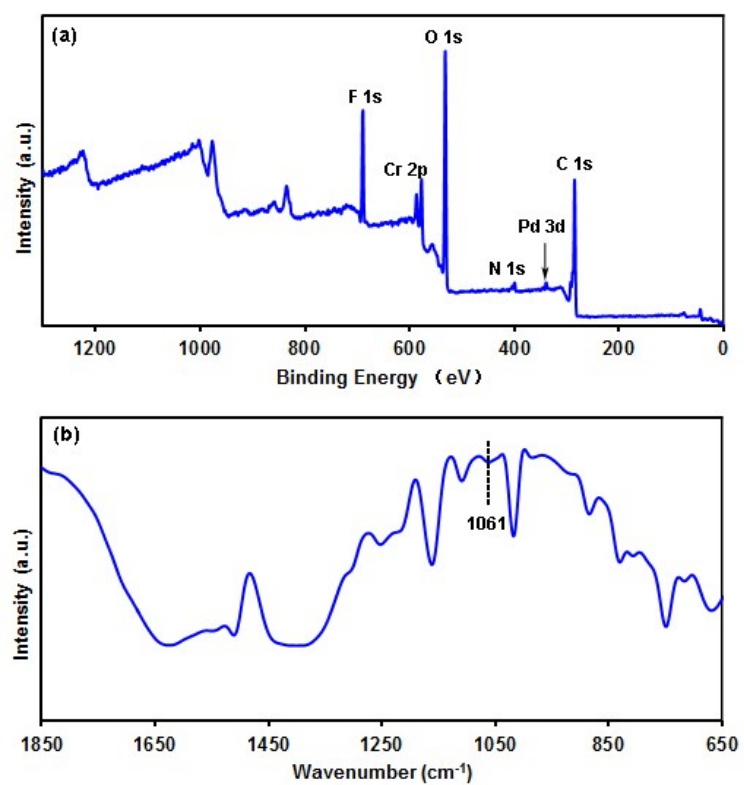


Fig. S4 (a) XPS and (b) FT-IR spectrum of the $M_6L_4@MIL-101$.

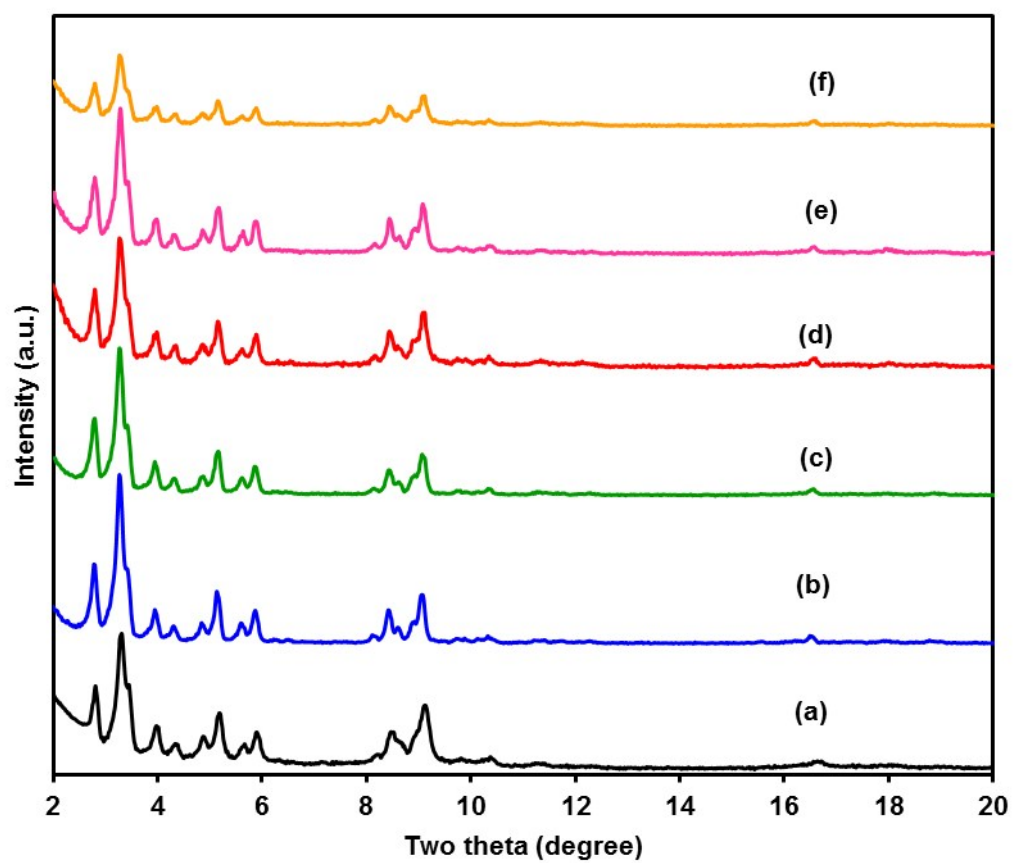


Fig. S5 PXR D patterns of (a) MIL-101, (b) 0.82PCN⊂M, (c) 0.64PCN⊂M, (d) 0.51PCN⊂M, (e) 0.33PCN⊂M and (f) the reused 0.64PCN⊂M.

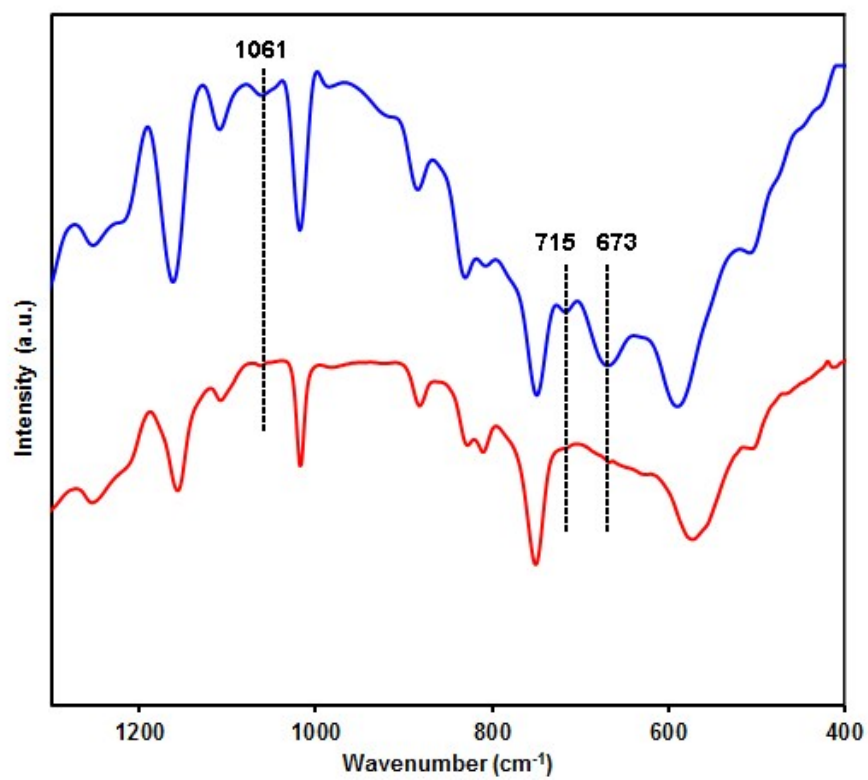


Fig. S6 FT-IR spectra of the M₆L₄-MIL-101 (blue line) and 0.64PCN-M (red line).

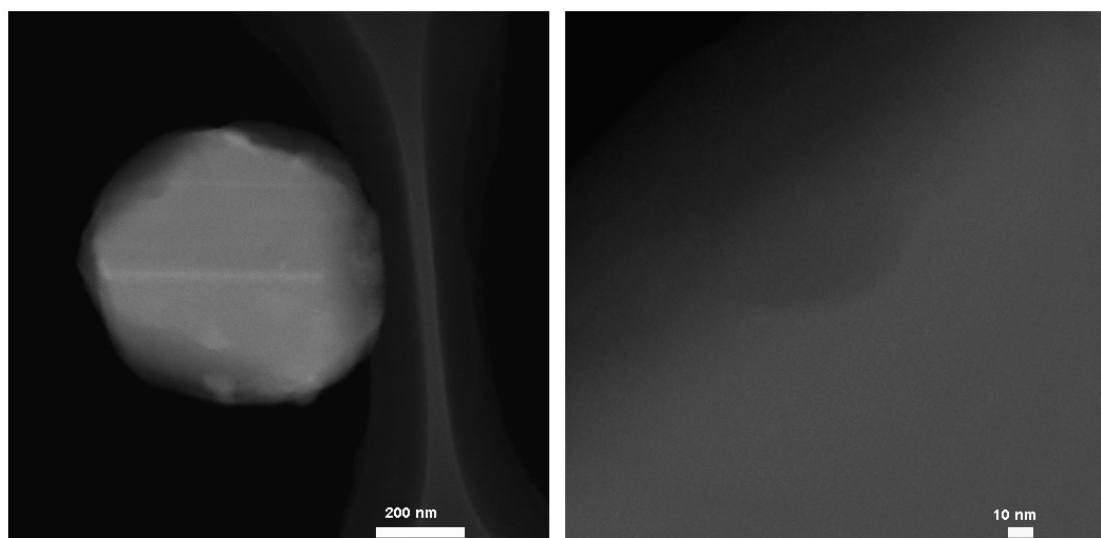


Fig. S7 HAADF-STEM images of $M_6L_4@MIL-101$.

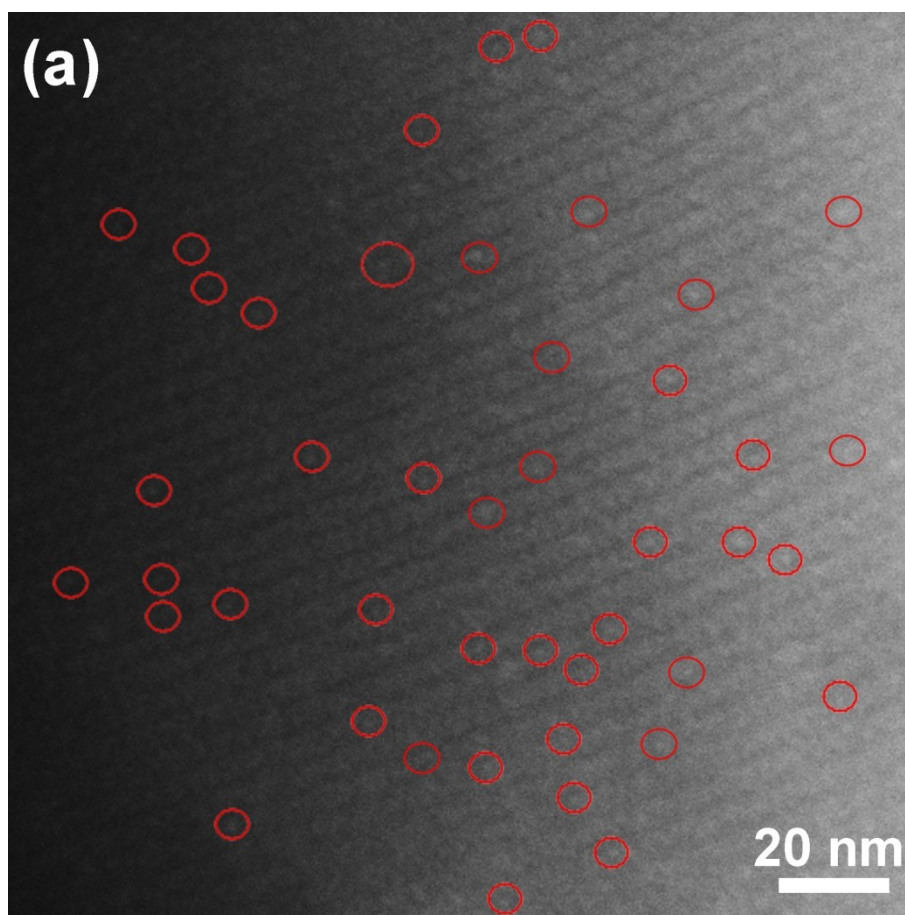


Fig. S8 (Enlarged Fig. 1a) HAADF-STEM images of ultrathin cuts from 0.33PCN \subset M.

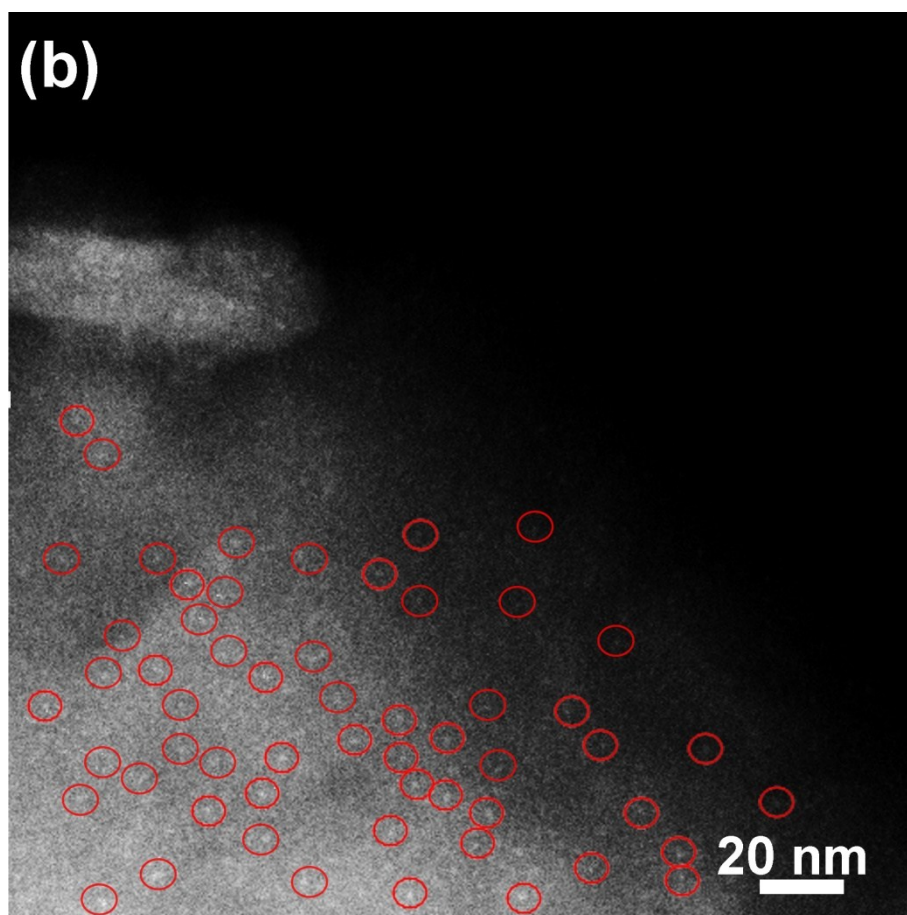


Fig. S9 (Enlarged Fig. 1b) HAADF-STEM images of ultrathin cuts from 0.51PCN@M.

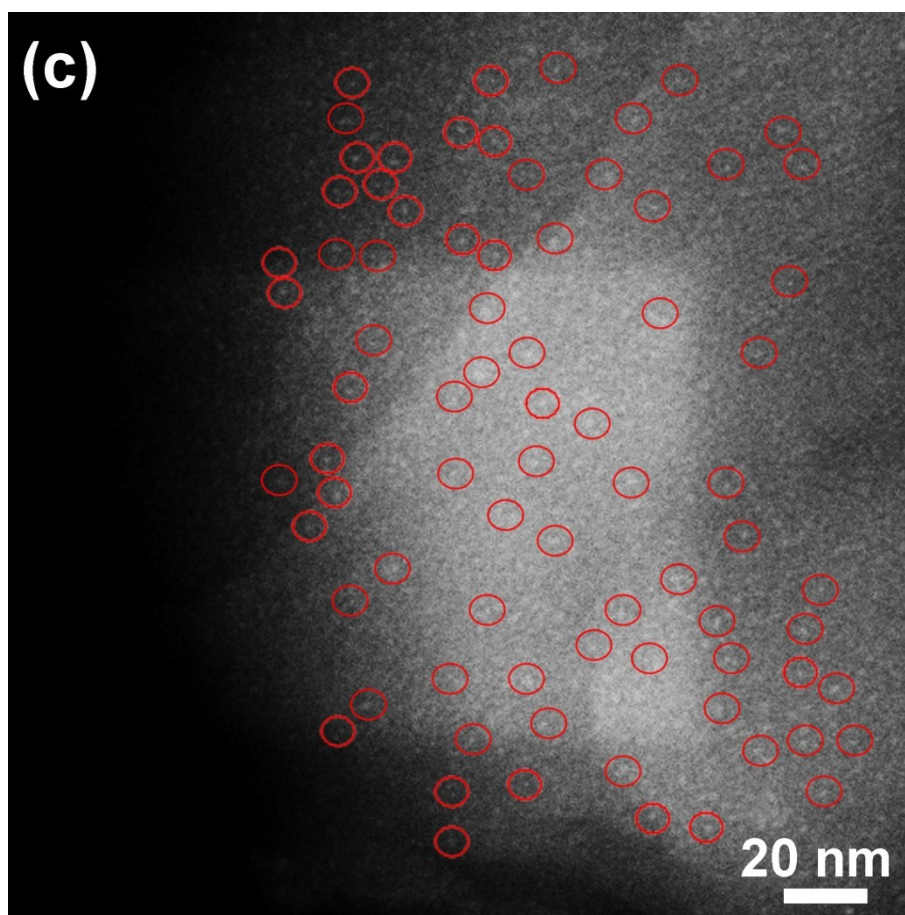


Fig. S10 (Enlarged Fig. 1c) HAADF-STEM images of ultrathin cuts from 0.64PCN@M.

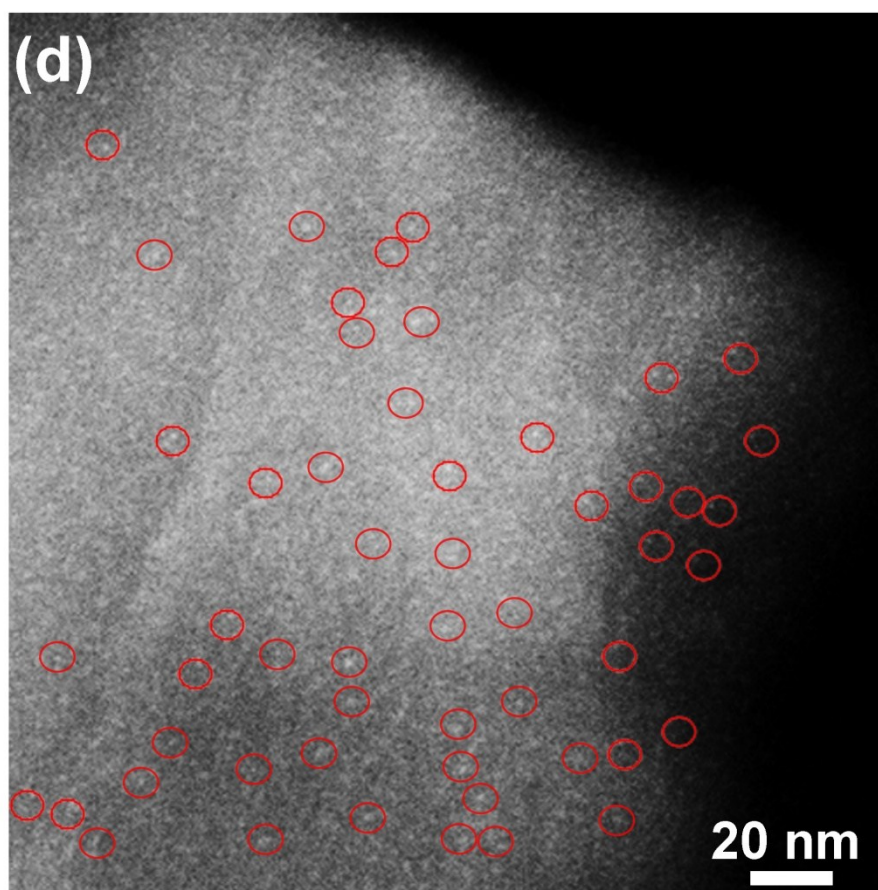


Fig. S11 (Enlarged Fig. 1d) HAADF-STEM images of ultrathin cuts from 0.82PCN \subset M.

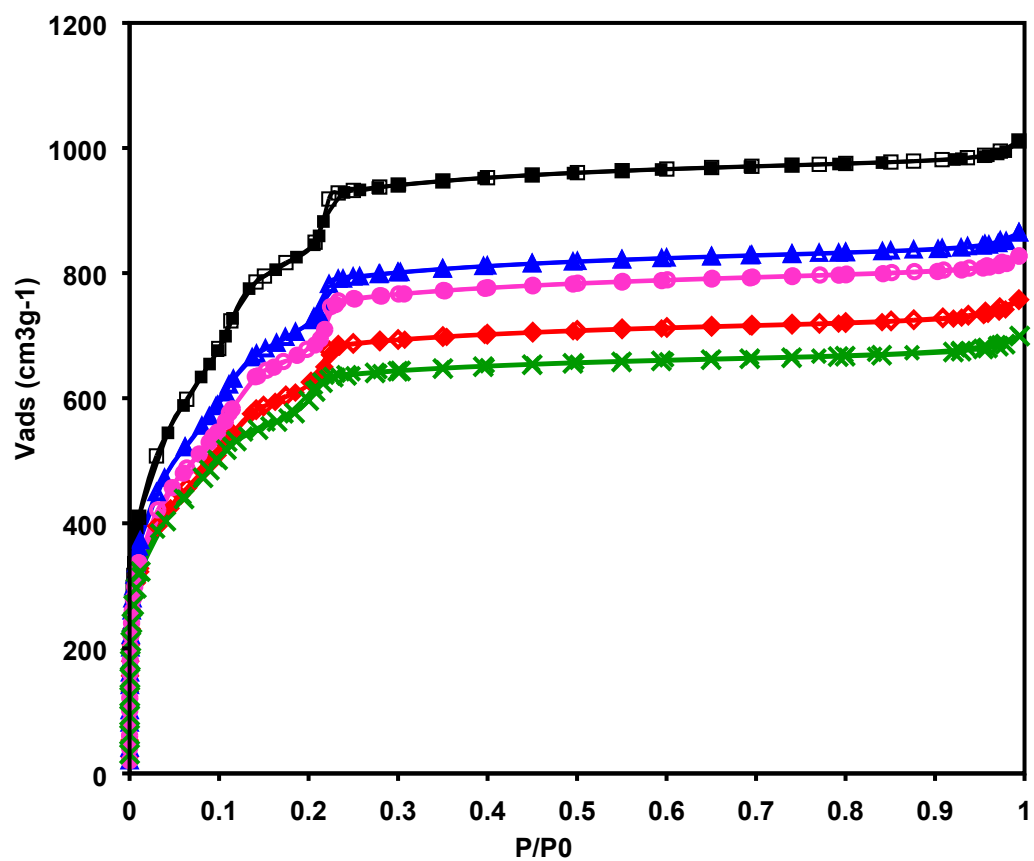


Fig. S12 Nitrogen adsorption/desorption isotherms at 77 K for the MIL-101 and PCN-M hybrids: \square for parent MIL-101, Δ for 0.33PCN-M, \circ for 0.51PCN-M, \diamond for 0.64PCN-M, \times for 0.82PCN-M.

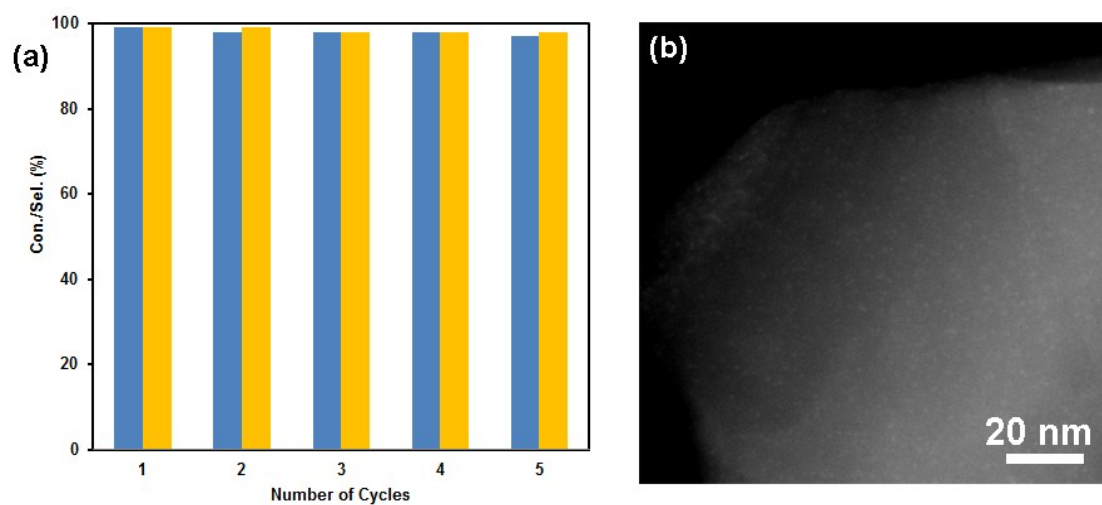


Fig. S13 (a) The conversion and selectivity of nitrobenzene hydrogenation over the 0.64PCN \subset M, blue for conversion, and yellow for selectivity. (b) The STEM image of the reused 0.64PCN \subset M catalyst after the 5th run.

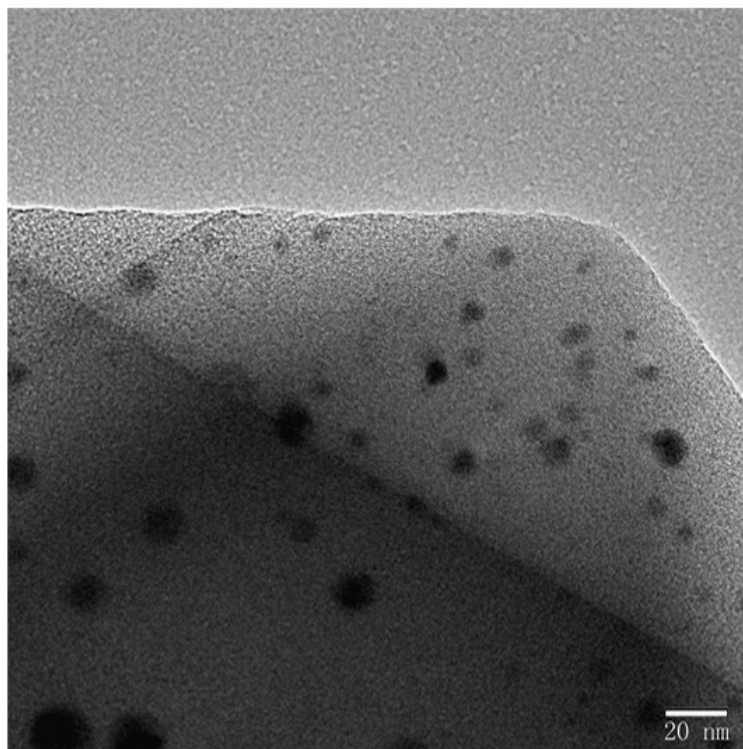


Fig. S14 TEM image of Pd/MIL-101.

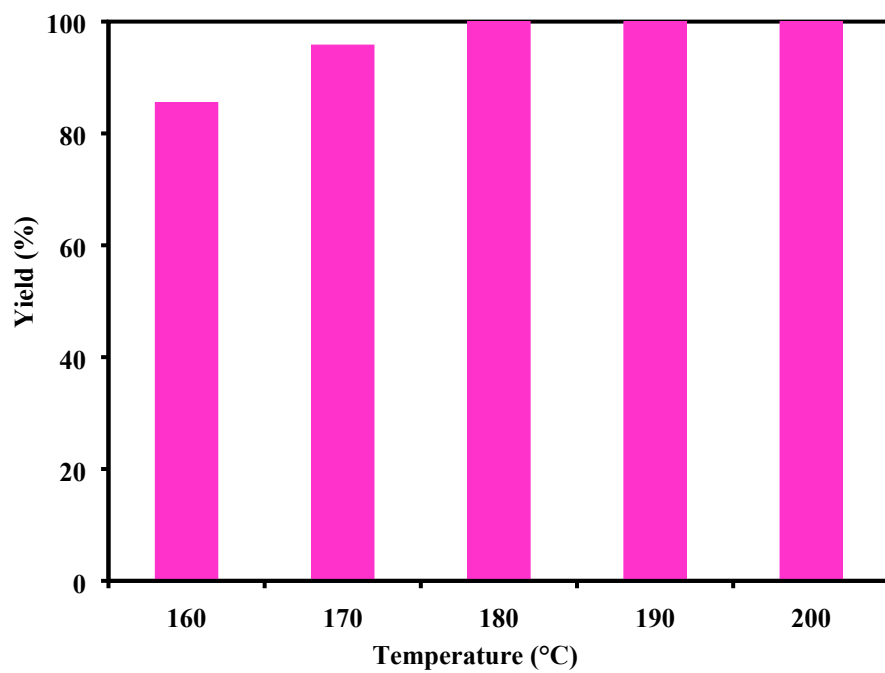


Fig. S15 Effect of temperature on CPO yield over 0.64PCN⊂M. Reaction conditions:

FFA (0.52 mmol) , Pd/FFA = 1.15×10^{-3} , water (4 mL), 0.8 MPa H₂, 24 h.

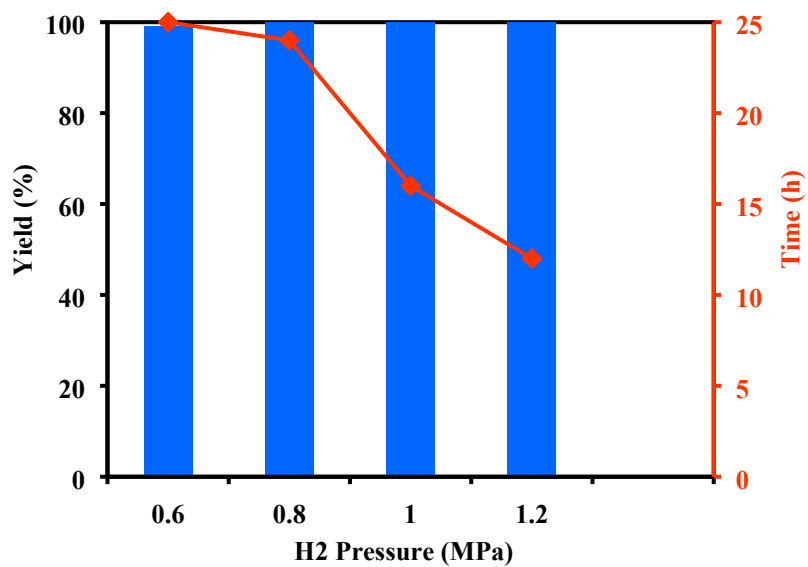


Fig. S16 Effect of hydrogen pressure on CPO yield over 0.64PCN \subset M. Reaction conditions: FFA (0.52 mmol), Pd/FFA = 1.15×10^{-3} , water (4 mL), 180 °C.

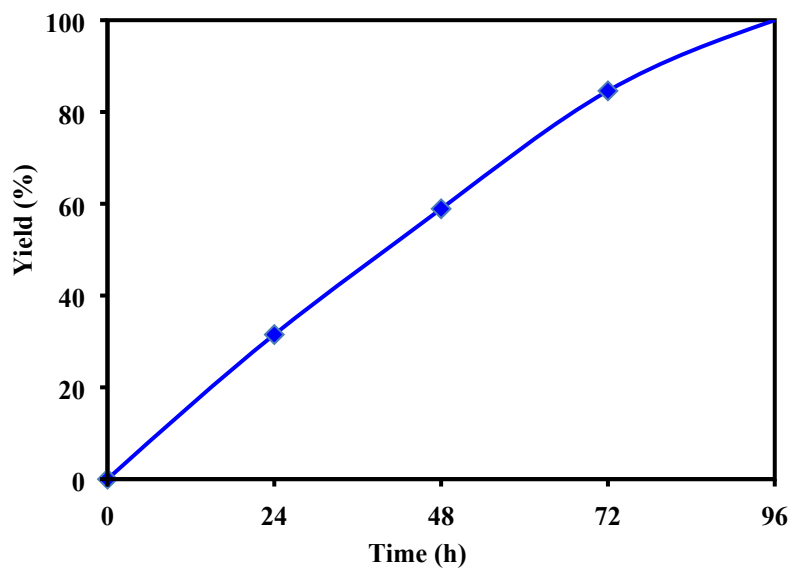


Fig. S17 CPO yield as a function of reaction time. Reaction conditions: FFA (0.52 mmol), Pd/FFA = 1.15×10^{-3} , water (4 mL), 180 °C, 1 atm H₂.

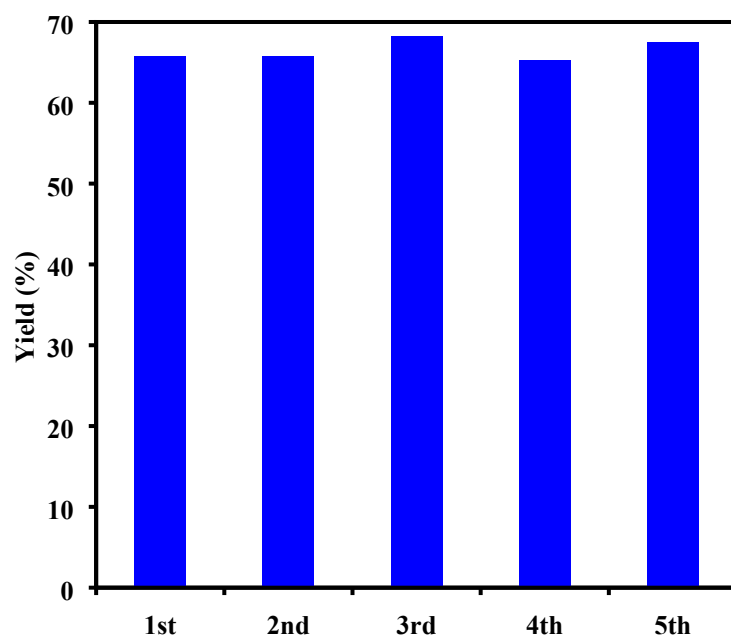


Fig. S18 Reuse of the 0.64PCN \subset M catalyst in FFA hydrogenation. Reaction conditions: FFA (0.52 mmol), Pd/FFA = 1.15×10^{-3} , water (4 mL), 180 °C, 0.8 MPa H₂. Each reaction was terminated at 12 h.

Table S1. The element contents of the Pd/C-N hybrids derived from M₆L₄.

	C	N	H	Pd
Sample	content	content	content	content
	(wt%) ^a	(wt%) ^a	(wt%) ^a	(wt%) ^b
Pd/C-N	26.40	8.14	3.20	56.90

^a Measured by elemental analysis.

^b Measured by AAS.

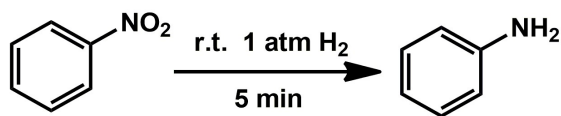
Table S2. The actual Pd contents in the PCN \subset M hybrids measured by AAS.

Sample	Theoretical Pd content (%)	Actual Pd content (%)	Doping percentage (%)
0.33PCN \subset M	0.40	0.33	83
0.51PCN \subset M	0.60	0.51	85
0.64PCN \subset M	0.80	0.64	80
0.82PCN \subset M	1.00	0.82	82
Pd/MIL-101	2.20	0.57	26

Table S3. BET surface areas and pore volumes of the materials.

Sample	S_{BET} ($\text{m}^2 \text{ g}^{-1}$)	Pore volume ($\text{cm}^3 \text{ g}^{-1}$)
MIL-101	2988	1.56
0.33PCN \subset M	2559	1.33
0.51PCN \subset M	2424	1.28
0.64PCN \subset M	2221	1.17
0.82PCN \subset M	2112	1.08

Table S4. Hydrogenation of nitrobenzene (**1a**) to aniline (**3a**)^a



Entry	Catalyst	Solvent	Yield (%)	TOF (h ⁻¹)
1	MIL-101	CH ₃ OH	<1	-
2	0.64PCN⊂M	Toluene	76	614
3	0.64PCN⊂M	CH ₃ OH	>99	800
4	0.64PCN⊂M	CH ₃ CH ₂ OH	60	480
5	0.64PCN⊂M	H ₂ O	88	704
6	0.64PCN⊂M	Ethyl acetate	24	192
7	0.82PCN⊂M	CH ₃ OH	97	776
8	0.33PCN⊂M	CH ₃ OH	56	448
9	0.51PCN⊂M	CH ₃ OH	76	655
10	Pd/MIL-101	CH ₃ OH	16	128
11	Pd/C	CH ₃ OH	6	51

^a Reaction conditions: nitrobenzene (0.1 mmol), 1 atm H₂, room temperature, 5 min, 2 ml solvent, Pd/substrate = 1.5 mol%.

Table S5. Summary of the catalytic performance of typical Pd-based catalysts for hydrogenation of nitrobenzene.

Catalyst	Pd loading (wt%)	Solvent, <i>T</i> (°C)	H ₂ pressure (kPa)	Time (h)	Conversion (%)	Selectivity (%)	TOF ^b (h ⁻¹)	Note
0.64PCN⊂M	0.64	methanol, r.t.	101.3	0.083	>99	>99	800	this work ^a
0.82PCN⊂M	0.82	methanol, r.t.	101.3	0.083	97	>99	776	this work ^a
0.33PCN⊂M	0.33	methanol, r.t.	101.3	0.083	56	>99	448	this work ^a
0.51PCN⊂M	0.51	methanol, r.t.	101.3	0.083	76	>99	655	this work ^a
Pd@NKZPDB-1	0.03	methanol, r.t.	101.3	3	89.2	100	129	Ref ³
1 at% Pd-coated Ni	Unknown	methanol, r.t.	101.3	6	100	Unknown	367	Ref ⁴
Pd/PVDF-EC	0.9	water, r.t.	Unknown	2.5	98	100	92	Ref ⁵
Pd/PEG catalyst	3.75	EtOH, r.t.	101.3	2(3)	93(100)	93(100)	71(83)	Ref ⁶
Pd ^o -in-UiO-66	1.0	THF, r.t.	101.3	3	100	99	165	Ref ⁷
HMMS-NH ₂ -Pd	2.34	EtOH, r.t.	101.3	1	100	>99	100	Ref ⁸
Pd/C	10	EtOH, r.t.	101.3	2	100	>99	50	Ref ⁸
Fe ₃ O ₄ @SiO ₂ -SH-Pd	3.81	EtOH, r.t.	101.3	0.83	100	>99	168	Ref ⁹
Pd(0)-CF	0.73	EtOH, 35 ± 2°C	1000	2.67	52	>99	162	Ref ¹⁰
Pd(0)-EGCG _{0.2} -CF	1.1	EtOH, 35 ± 2°C	1000	2.67	98	>99	306	Ref ¹⁰
Pd/γ-Al ₂ O ₃	1.0	EtOH, 35 ± 2°C	1000	2.67	100	>95	312	Ref ¹⁰
Pd/SiO ₂	1.0	EtOH, 35 ± 2°C	1000	2.67	88	>95	275	Ref ¹⁰
Pd/γ-Al ₂ O ₃ /Fe ₃ O ₄ /SiO ₂	1.0	EtOH, 20°C	200	0.5	99	92	206	Ref ¹¹
Pd@Fe ₃ O ₄	Unknown	EtOH, r.t.	101.3	1	>99	—	49	Ref ¹²
(Pd/bpy) ₁₀	Unknown	EtOH, 24°C	122	5.3	>99	—	225	Ref ¹³
Fe ₃ O ₄ -NH ₂ -Pd	8.43	EtOH, r.t.	101.3	0.75	>99	>99	83	Ref ¹⁴
Pd/γ-Fe ₂ O ₃ /urea-MCF	5	MeOH, 25°C	689	16	>98	>98	6	Ref ¹⁵

Pd NPs	Unknown	MeOH, 25°C	101.3	4	Yield: 98	252	Ref ¹⁶
Pd/Fe ₃ O ₄	2.3	EtOH, 25-40°C	101.3	2-3	Yield: 99	50	Ref ¹⁷
Pd /SiO ₂	Unknown	EtOH, r.t	101.3	1	Yield:27.2	24	Ref ¹⁸
HMMS-salpr-Pd	5.12	EtOH, r.t	101.3	1	Yield:>99	106	Ref ¹⁹

^a Reaction conditions: nitrobenzene (0.1 mmol), 1 atm H₂, room temperature, 5 min, 2 ml solvent, Pd/substrate = 1.5 mol%.

^b TOF of the catalyst was calculated as the number of moles of product per mol of Pd per hour.

Table S6. Summary of the reaction results of FFA hydrogenation to CPO over different catalysts.

Catalyst	Metal loading (wt%)	H ₂ Pressure (MPa)	T (°C)	Note
Co/ZrO ₂ -La ₂ O ₃	8.8	2	160	Ref ^{S20}
CuNi _{0.5} @C	unkown	5	130	Ref ²¹
Au/TiO ₂ -A	0.1	4	160	Ref ²²
5%Pd-10%Cu/C	1	3	160	Ref ²³
Ru/MIL-101	3	4	160	Ref ²⁴
Cu-Co-CP-500	5	2	170	Ref ²⁵
CuZnAl-500-0.5		4	150	Ref ²⁶
Cu-Ni-Al		4	140	Ref ²⁷
G-134A	44	8	175	Ref ²⁸
NiCu-50/SBA-15		4	160	Ref ²⁹
Ru/C		2.5	165	Ref ^{S30}
Pt/C and Pt/Al ₂ O ₃		8	160	Ref ^{S31}

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