

**Supplementary material for**

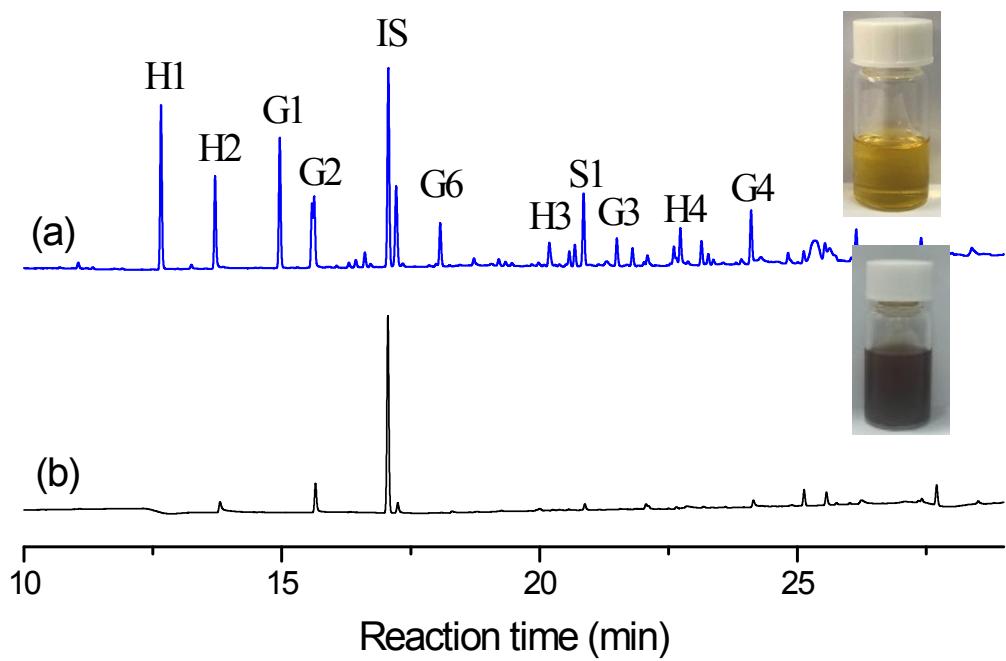
**Hydrogenolysis of biorefinery corncob lignin into aromatic phenols over activated carbon-supported nickel**

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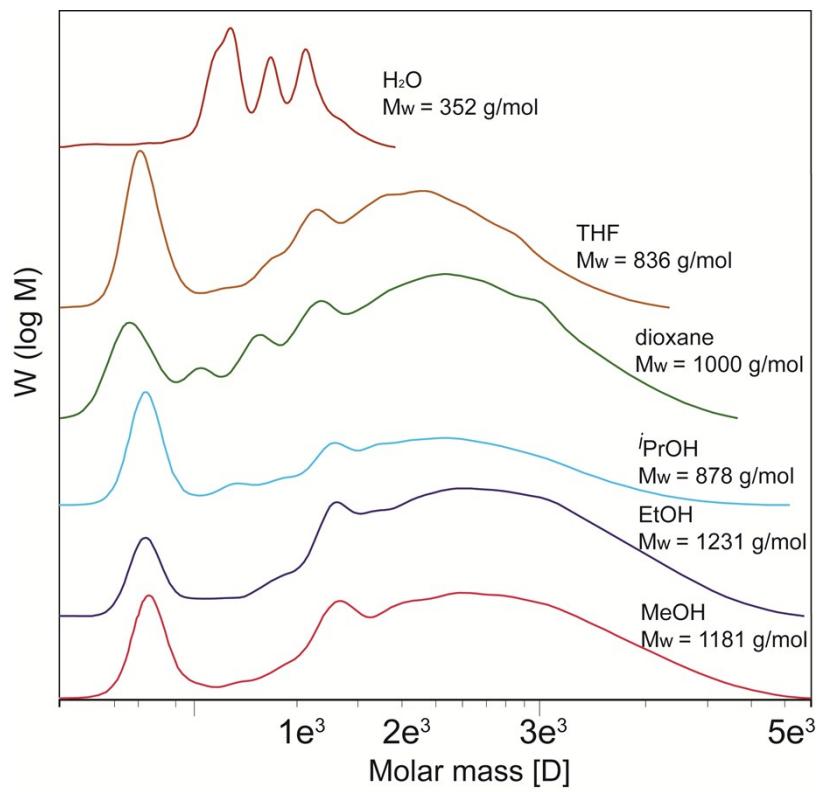
‡ These authors contribute equally to this work.



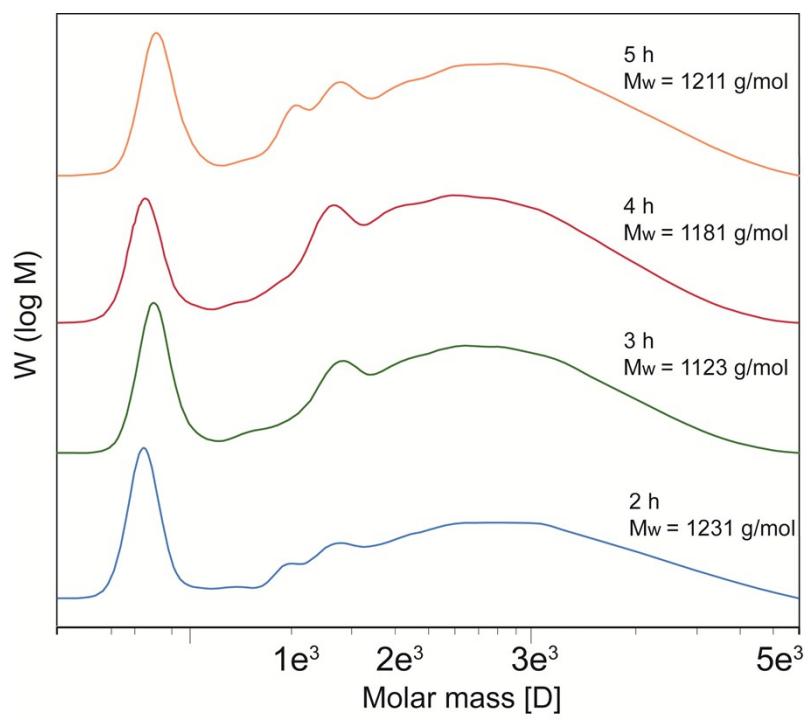
**Fig. S1** Gas chromatogram and peak identification of the lignin monomers from the catalytic hydrogenolysis of biorefinery corncob lignin (a) with Ni/AC (reaction condition from Table 1, entry 1), and (b) without catalyst (reaction condition from Table 1, entry 2). IS represents internal standard.



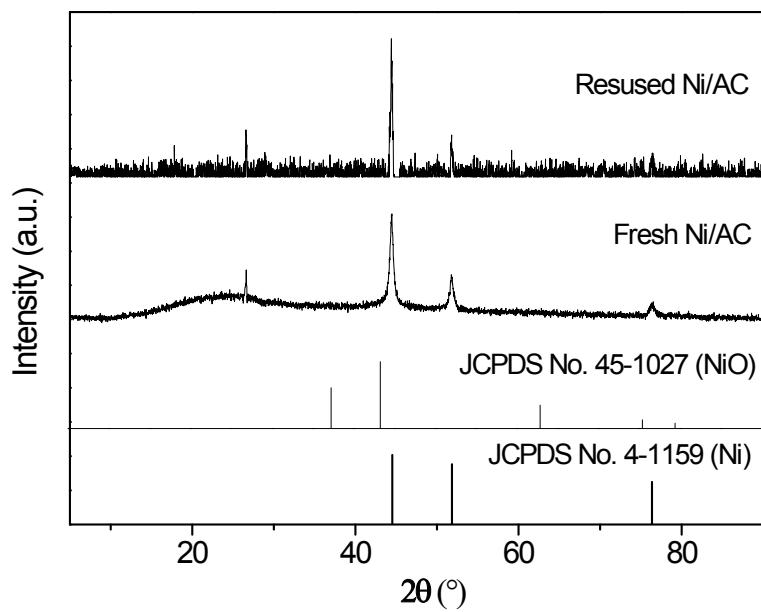
**Fig. S2** Images of biorefinery corncob lignin after catalytic hydrogenolysis reaction over the Ni/AC catalyst.



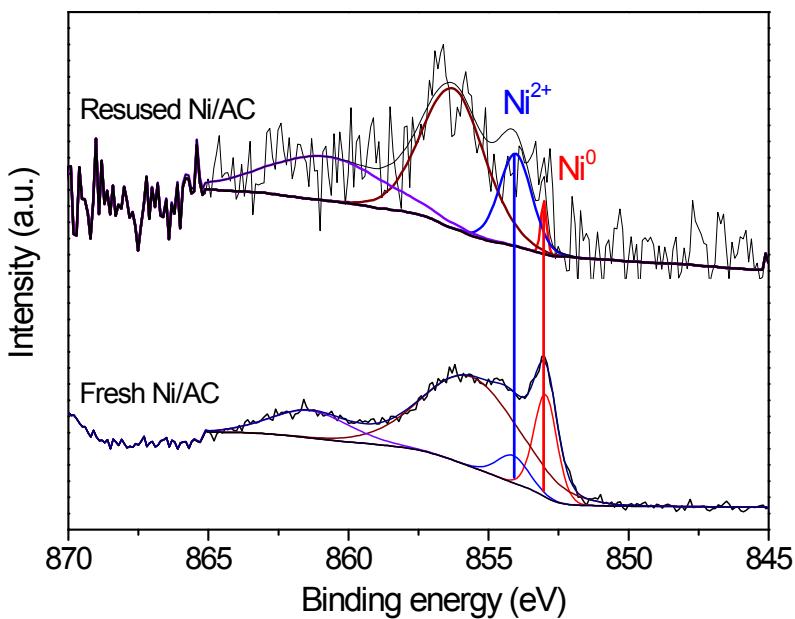
**Fig. S3** The molecular weight distribution of lignin oily product from catalytic hydrogenolysis of biorefinery corncob lignin with different solvents. Reaction conditions unless specified otherwise: lignin (50 mg), Ni/AC catalyst (10 mg), solvent (10 mL), 240 °C, 4 h, H<sub>2</sub> (3 MPa).



**Fig. S4** The molecular weight distribution of lignin oily product from catalytic hydrogenolysis of biorefinery corncob lignin with various reaction times. Reaction condition: lignin (50 mg), Ni/AC catalyst (10 mg), MeOH (10 mL), 240 °C, H<sub>2</sub> (3 MPa).

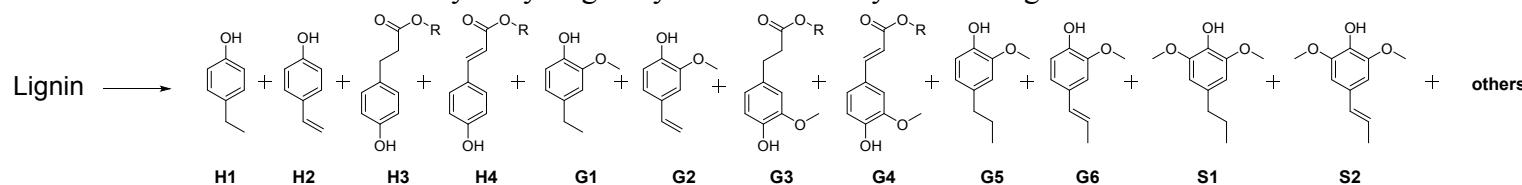


**Fig. S5** XRD patterns of the fresh and reused Ni/AC catalyst.



**Fig. S6** XPS spectra of the fresh and reused Ni/AC catalyst. The peaks at 852.9 eV and 854.2 eV are assigned to Ni<sup>0</sup> and Ni<sup>2+</sup>, respectively. The analysis of the XPS results show that Ni<sup>0</sup> occupied about 80 wt% based the total content of Ni<sup>0</sup> and Ni<sup>2+</sup> for Ni 2p of the fresh Ni/AC catalyst, which is higher than that of the reused Ni/AC catalyst (Ni<sup>0</sup> occupied about 14 wt% based the total content of Ni<sup>0</sup> and Ni<sup>2+</sup>).

**Table S1** Products distribution of catalytic hydrogenolysis of biorefinery corncob lignin with different solvent.<sup>a</sup>

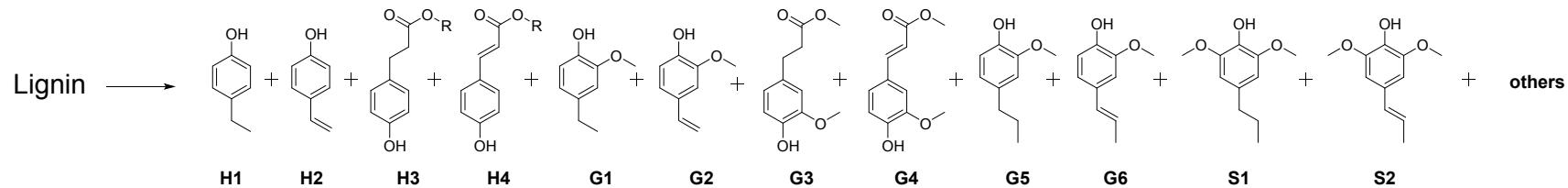


Entry	Catalyst	Solvent	The distribution and yields of phenolic monomers (wt%) <sup>b</sup>														Others	Total monomers yield (wt%)	
			Ethyl/vinyl phenol and guaiacol					Methyl coumarate/ferulate and derivatives					Propyl/propenyl guaiacol and syrinol						
			H1	H2	G1	G2	Total yield (wt%)	H3	H4	G3	G4	Total yield (wt%)	G5	G6	S1	S2	Total yield (wt%)		
1	Ni/C	MeOH	0.5	0.8	2.3	0.9	4.5	1.3 <sup>c</sup>	0.7 <sup>c</sup>	0.7 <sup>c</sup>	0.9 <sup>c</sup>	3.6	0.4	0.4	1.8	0.1	2.7	1.3	12.1
2	Ni/C	EtOH	0.3	0.4	1.0	0.4	2.1	0.6 <sup>e</sup>	0.4 <sup>d</sup>	0.5 <sup>d</sup>	0.8 <sup>d</sup>	2.3	0.4	0.4	0.7	0.2	1.7	2.3	8.4
3	Ni/C	iPrOH	0.5	0.8	1.4	0.6	3.3	0.2 <sup>f</sup>	0.1 <sup>e</sup>	0.4 <sup>e</sup>	0.7 <sup>e</sup>	1.4	0.4	0.3	0.9	0.3	1.9	3.7	10.3
4	Ni/C	THF	0.3	0.6	0.8	0.4	2.1	0.2 <sup>g</sup>	trace <sup>f</sup>	0.3 <sup>f</sup>	trace <sup>f</sup>	0.5	0.4	0.8	0.8	0.3	2.3	0.9	5.8
5	Ni/C	Dioxane	0.1	--	0.5	--	0.6	--	--	--	--	0	0.8	--	0.2	--	1.0	1.5	3.1
6	Ni/C	H <sub>2</sub> O	0.8	--	1.9	--	2.7	--	--	--	--	0	0.8	--	0.5	--	1.3	2.5	6.5
7	None	MeOH	--	1.7	--	2.1	3.8	--	0.3	--	0.4	0.7	--	0.3	--	0.2	0.5	1.2	6.2
8	AC	MeOH	--	1.4	--	1.8	3.2	--	0.2	--	0.1	0.3	--	0.2	--	--	0.2	1.6	5.3
9 <sup>g</sup>	Ni/C	MeOH	0.1	1.2	0.6	1.3	3.2	--	0.3	--	0.9	1.2	--	0.7	--	0.3	1.0	1.2	6.6

<sup>a</sup> Reaction conditions: lignin (50 mg), catalyst (10 mg), solvent (10 mL), 240 °C, 4 h. <sup>b</sup> Representing the monomer yield is based on total lignin content. <sup>c</sup>

R=CH<sub>3</sub>. <sup>d</sup> R=CH<sub>2</sub>CH<sub>3</sub>. <sup>e</sup> R=CH<sub>3</sub>CHCH<sub>3</sub>. <sup>f</sup> R=H. <sup>g</sup> Reaction performed under N<sub>2</sub> (0 MPa).

**Table S2** Products distribution of catalytic hydrogenolysis of biorefinery corncob lignin with different reaction temperature.<sup>a</sup>

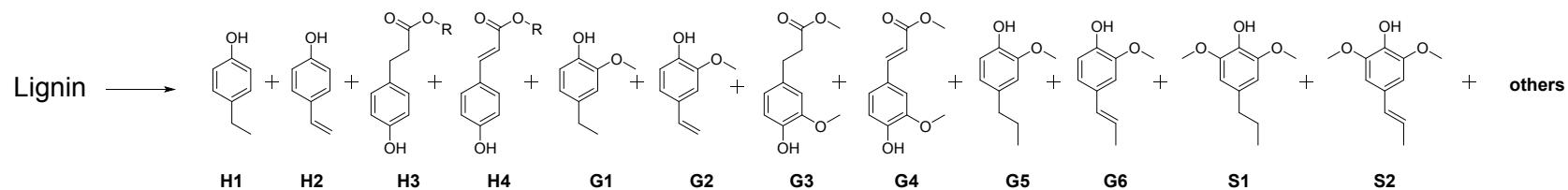


Entry	Tem. (°C)	The distribution and yields of phenolic monomers (wt%) <sup>b</sup>												Others	Total monomers yield (wt%)			
		Ethyl/vinyl phenol and guaiacol					Methyl coumarate/ferulate and derivatives				Propyl/propenyl guaiacol and syrinol							
		H1	H2	G1	G2	Total yield (wt%)	H3	H4	G3	G4	Total yield (wt%)	G5	G6	S1	S2	Total yield (wt%)		
1	220	0.3	0.5	1.1	0.5	2.4	1.2	0.4	0.6	0.7	2.9	0.2	1.3	--	0.2	1.7	1.0	8.0
2	230	0.9	1.0	1.0	0.7	3.6	1.2	0.6	0.3	0.8	2.9	0.4	0.8	0.4	0.5	2.1	1.8	10.4
3	240	0.5	0.8	2.3	0.9	4.5	1.3	0.7	0.7	0.9	3.6	0.4	0.4	1.8	0.1	2.7	1.3	12.1
4	260	0.5	0.8	1.2	0.3	2.8	1.0	0.7	0.7	1.1	3.5	0.4	0.4	0.9	1.0	2.7	2.0	11.0
5	280	0.8	--	1.7	0.2	2.7	1.1	0.6	1.3	0.9	3.9	0.4	0.8	0.8	0.6	2.6	1.5	10.7

<sup>a</sup> Reaction conditions: lignin (50 mg), catalyst (10 mg), solvent (10 mL), MeOH, 4 h, 3 MPa (H<sub>2</sub>).

<sup>b</sup> Representing the monomer yield is based on total lignin content.

**Table S3** Products distribution of catalytic hydrogenolysis of biorefinery corncob lignin with different reaction time.<sup>a</sup>

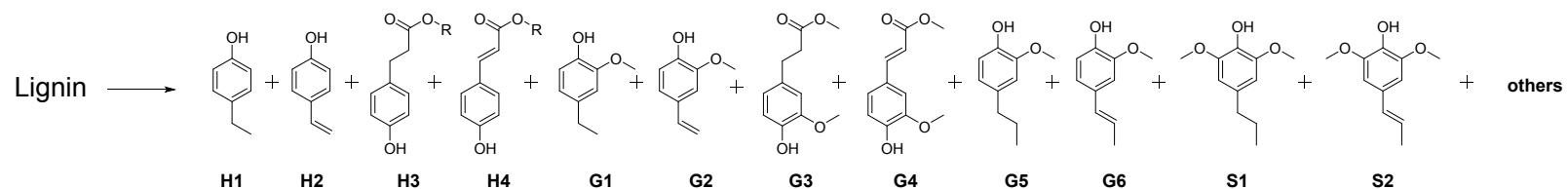


Entry	Time (h)	The distribution and yields of phenolic monomers (wt%) <sup>b</sup>														Others	Total monomers yield (wt%)		
		Ethyl/vinyl phenol and guaiacol					Methyl coumarate/ferulate and derivatives					Propyl/propenyl guaiacol and syrinol							
		H1	H2	G1	G2	Total yield (wt%)	H3	H4	G3	G4	Total yield (wt%)	G5	G6	S1	S2	Total yield (wt%)			
1	2	1.2	1.1	0.5	1.2	4.0	1.2	0.5	0.2	0.6	2.5	--	0.7	--	0.3	1.0	1.2	8.7	
2	3	1.2	1.1	1.0	0.8	4.1	1.2	0.5	0.6	0.8	3.1	0.3	0.8	0.3	0.4	1.8	1.7	10.7	
3	4	0.5	0.8	2.3	0.9	4.5	1.3	0.7	0.7	0.9	3.6	0.4	0.4	1.8	0.1	2.7	1.3	12.1	
4	5	1.1	0.9	1.7	0.4	4.1	1.2	0.4	0.6	0.8	3.0	0.4	0.8	0.3	0.5	2.0	2.0	11.1	

<sup>a</sup> Reaction conditions: lignin (50 mg), catalyst (10 mg), solvent (10 mL), 240 °C, MeOH, 3 MPa (H<sub>2</sub>).

<sup>b</sup> Representing the monomer yield is based on total lignin content.

**Table S4** Products distribution of catalytic hydrogenolysis of biorefinery corncob lignin with different run times.<sup>a</sup>



Run time	The distribution and yields of phenolic monomers (wt%) <sup>b</sup>													Others	Total monomers yield (wt%)		
	Ethyl/vinyl phenol and guaiacol					Methyl coumarate/ferulate and derivatives					Propyl/ propenyl guaiacol and syrinol						
	H1	H2	G1	G2	Total yield (wt%)	H3	H4	G3	G4	Total yield (wt%)	G5	G6	S1	S2	Total yield (wt%)		
1	0.5	0.8	2.3	0.9	4.5	1.3	0.7	0.7	0.9	3.6	0.4	0.4	1.8	0.1	2.7	1.3	12.1
2	0.1	0.8	2.0	0.7	3.6	1.1	0.6	0.5	0.8	3.0	0.7	0.3	1.4	0.2	2.6	2.4	11.6
3	--	1.3	2.1	0.5	3.9	1.1	0.6	0.6	0.8	3.1	0.5	0.3	1.3	0.1	2.2	1.1	10.3
4	--	1.4	2.3	0.6	4.3	1.2	0.8	0.2	1.2	3.4	--	0.7	0.4	0.1	1.2	3.0	11.9
5	--	1.5	1.8	0.7	4.0	1.1	0.7	0.3	1.0	3.1	--	0.7	0.4	--	1.1	3.2	11.4
6	--	1.5	1.6	0.5	3.6	1.1	0.7	0.2	0.9	2.9	--	0.7	0.4	--	1.1	3.9	11.5

<sup>a</sup> Reaction conditions: lignin (50 mg), catalyst (10 mg), solvent (10 mL), 240 °C, MeOH, 3 MPa (H<sub>2</sub>), 4 h.

<sup>b</sup> Representing the monomer yield is based on total lignin content.

**Table S5** The assignments of main lignin and lignin monomers  $^{13}\text{C}$ - $^1\text{H}$  correlation signals in the 2D HSQC NMR spectra in Fig. 3.

Labels	$\delta_{\text{C}}/\delta_{\text{H}}$ (ppm)	Assignment
OMe	55.5/3.69	C-H in methoxyls (-OCH <sub>3</sub> )
A <sub><math>\alpha</math></sub>	71.6/4.85	C <sub><math>\alpha</math></sub> -H <sub><math>\alpha</math></sub> in $\beta$ -O-4 substructures (A)
A <sub><math>\beta</math></sub>	86.6/4.09	C <sub><math>\beta</math></sub> -H <sub><math>\beta</math></sub> in $\beta$ -O-4 substructures (A)
A <sub><math>\gamma</math></sub>	59.5/3.1-3.79	C <sub><math>\gamma</math></sub> -H <sub><math>\gamma</math></sub> in $\beta$ -O-4 substructures (A)
B <sub><math>\gamma</math></sub>	62.4/3.69	C <sub><math>\gamma</math></sub> -H <sub><math>\gamma</math></sub> in phenylcoumaran substructures (B)
S <sub>2,6</sub>	103.7/6.65	C <sub>2,6</sub> -H <sub>2,6</sub> in syringyl units (S)
S' <sub>2,6</sub>	106.3/7.17	C <sub>2,6</sub> -H <sub>2,6</sub> in oxidized syringyl units (S')
G <sub>2</sub>	110.7/6.92	C <sub>2</sub> -H <sub>2</sub> in guaiacyl units (G)
G <sub>5</sub>	114.5/6.68	C <sub>5</sub> -H <sub>5</sub> in guaiacyl units (G)
G <sub>6</sub>	119.0/6.77	C <sub>6</sub> -H <sub>6</sub> in guaiacyl units (G)
G/S <sub>1</sub> (7)	28.3/2.48	C <sub>7</sub> -H <sub>7</sub> in compounds <b>G1</b> and <b>H1</b>
G/S <sub>1</sub> (8)	16.4/1.14	C <sub>8</sub> -H <sub>8</sub> in compounds <b>G1</b> and <b>H1</b>
H/G <sub>2</sub> (7)	136.1/6.72	C <sub>7</sub> -H <sub>7</sub> in compounds <b>G2</b> and <b>H2</b> (Chemdraw)
H <sub>3</sub>	128.3/6.97	C <sub>2,6</sub> -H <sub>2,6</sub> in compounds <b>H3</b>
	115.9/6.77	C <sub>3,5</sub> -H <sub>3,5</sub> in compounds <b>H3</b>
	29.4/2.73	C <sub>7</sub> -H <sub>7</sub> in compounds <b>H3</b>
	35.2/2.55	C <sub>8</sub> -H <sub>8</sub> in compounds <b>H3</b>
G <sub>3</sub>	111.9/6.74	C <sub>2</sub> -H <sub>2</sub> in compounds <b>G3</b>
	114.8/6.58	C <sub>5</sub> -H <sub>5</sub> in compounds <b>G3</b>
	119.7/6.57	C <sub>6</sub> -H <sub>6</sub> in compounds <b>G3</b>
	29.4/2.73	C <sub>7</sub> -H <sub>7</sub> in compounds <b>G3</b>
	35.2/2.55	C <sub>8</sub> -H <sub>8</sub> in compounds <b>G3</b>
pCA/H <sub>4</sub>	129.9/7.51	C <sub>2,6</sub> -H <sub>2,6</sub> in compounds <b>H4</b> and <b>pCA</b>
	115.5/6.78	C <sub>3,5</sub> -H <sub>3,5</sub> in compounds <b>H4</b> and <b>pCA</b>
	143.9/7.53	C <sub>7</sub> -H <sub>7</sub> in compounds <b>H4</b> and <b>pCA</b>
	115.2/6.28	C <sub>8</sub> -H <sub>8</sub> in compounds <b>H4</b> and <b>pCA</b>
FA/G <sub>4</sub>	111.0/7.28	C <sub>2</sub> -H <sub>2</sub> in compounds <b>G4</b> and <b>pCA</b>
	122.2/7.11	C <sub>6</sub> -H <sub>6</sub> in compounds <b>G4</b> and <b>pCA</b>
	144.0/7.45	C <sub>7</sub> -H <sub>7</sub> in compounds <b>G4</b> and <b>pCA</b>

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	116.5/6.40	C <sub>8</sub> -H <sub>8</sub> in compounds <b>G4</b> and <b>pCA</b>
	51.1/3.62	C(O)OMe in compounds H/ <b>G4</b>
G/S <sub>5</sub> (7)	37.5/2.43	C <sub>7</sub> -H <sub>7</sub> in compounds <b>G5</b> and <b>S5</b>
G/S <sub>5</sub> (8)	24.9/1.55	C <sub>8</sub> -H <sub>8</sub> in compounds <b>G5</b> and <b>S5</b>
G/S <sub>5</sub> (9)	13.9/0.87	C <sub>9</sub> -H <sub>9</sub> in compounds <b>G5</b> and <b>S5</b>

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