

Supporting information

Porous Zn cathode for Li-CO₂ battery generating fuel-gas CO

Jiafang Xie, Qin Liu, Yiyin Huang, Maoxiang Wu, and Yaobing Wang*

CAS Key Laboratory of Design and Assembly of Functional Nanostructures, and Fujian Provincial Key Laboratory of Nanomaterials, State Key Laboratory of Structural Chemistry, Key Laboratory of Optoelectronic Materials Chemistry and Physics, Fujian Institute of Research on the Structure of Matter, Chinese Academy of Sciences, Fuzhou, Fujian 350002, China.

*To whom correspondence should be addressed: wangyb@fjirsm.ac.cn

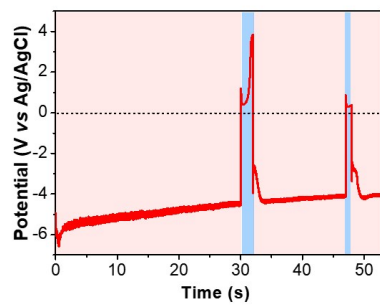


Figure S1. A typical potential vs time curve of redox-coupled electrodeposition for PF-Zn.

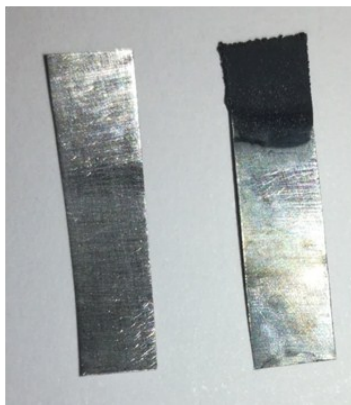


Figure S2. Typical photo of Zn foil before (left) and after (right) electrodeposition.

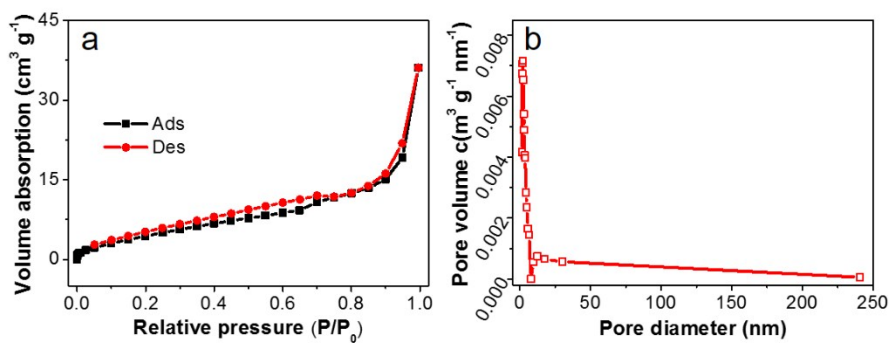


Figure S3. The N_2 adsorption-desorption isotherm and pore size distribution of PF-Zn. (a) The N_2 adsorption-desorption isotherm. (b) The pore size distribution.

PF-Zn possessed a specific surface area of $19.1 \text{ m}^2 \text{ g}^{-1}$ and three characters in isotherm curve: 1) sharply increased absorbed volume over $0.8 P/P_0$ indicated the macro pores, 2) the hysteresis loop from $0.1 P/P_0$ to $0.8 P/P_0$ indicated the meso pores, 3) sharply increased absorbed volume around $0.05 P/P_0$ indicated the micro pores. These three kinds of pores were also suggested by the pore size distribution curve and PF-Zn exhibited a total pore volume of $0.062 \text{ cm}^3 \text{ g}^{-1}$.

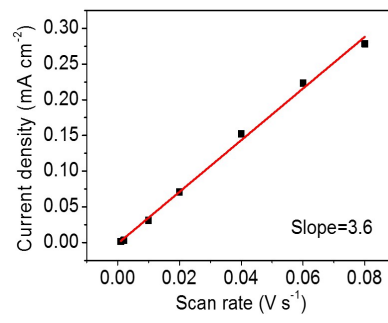


Figure S4. Double layer capacitance analysis of bare Zn foil substrate.

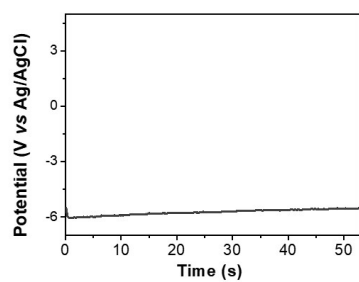


Figure S5. A typical potential vs time curve of constant cathodic current density deposition for porous Zn (P-Zn).

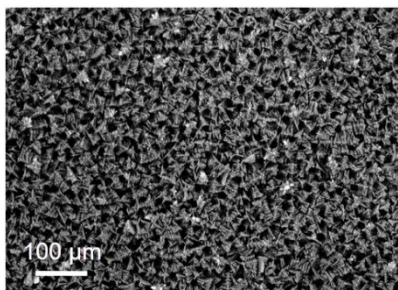


Figure S6. SEM image of P-Zn.

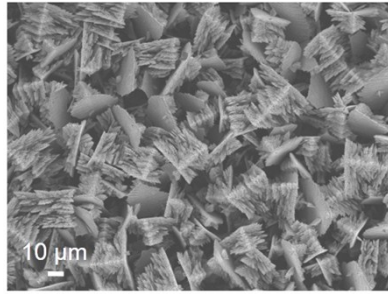


Figure S7. SEM image of P-Zn with higher magnification.

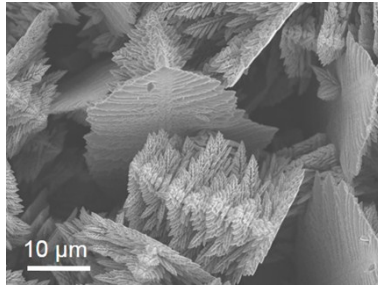


Figure S8. SEM image of P-Zn with further higher magnification.

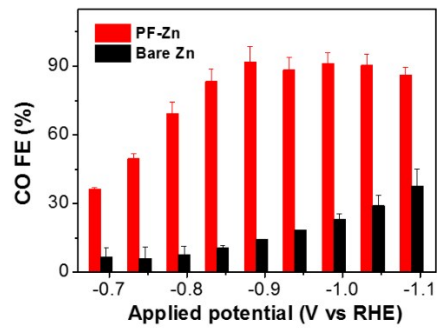


Figure S9. Electrochemical CO₂-to-CO electrochemical evaluation on PF-Zn in 0.1 M KHCO₃ with error bar.

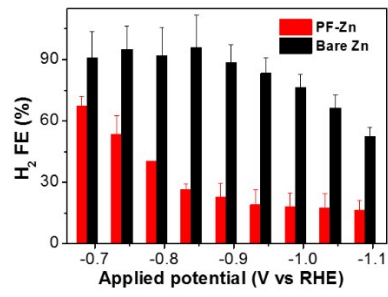


Figure S10. Electrochemical hydrogen evolution during CO₂-to-CO electrochemical evaluation on PF-Zn in 0.1 M KHCO₃ with error bar.

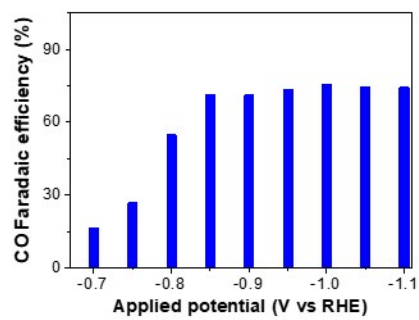


Figure S11. Electrochemical CO₂-to-CO electrochemical evaluation on P-Zn in 0.1 M KHCO₃.

Table S1. Reported Zn catalysts for electrochemical CO₂ reduction

Catalyst	Electrolyte	Max CO FE (overpotential)	Tafel slope	Reference
PF-Zn	0.1 M KHCO₃	94% (780 mV)	181 mV dec⁻¹	This work
P-Zn	0.1 M KHCO ₃	75% (880 mV)	209 mV dec ⁻¹	This work
<i>h</i> -Zn	0.5 M KHCO ₃	85.4% (840 mV)	NM	<i>Angew. Chem. Int. Ed.</i> ¹
LiET-Zn	0.1 M KHCO ₃	71% (690 mV)	149 mV dec ⁻¹	<i>ACS Nano</i> ²
Reduced nanoporous ZnO	0.25 M K ₂ SO ₄	92% (1100 mV)	221 mV dec ⁻¹	<i>Electrochem. Commun.</i> ³
Zn dendrites	0.1 M KHCO ₃	79% (990 mV)	260 mV dec ⁻¹	<i>ACS Catal.</i> ⁴
Bi	[EMIM]BF ₄	95% (165 mV)	139 mV dec ⁻¹	<i>J. Am. Chem. Soc.</i> ⁵
Cu ₄ Bi	0.5 M NaHCO ₃	~85% (590 mV)	NM	<i>Angew. Chem. Int. Ed.</i> ⁶
Porous hollow fibre copper	0.3 M KHCO ₃	72% (290 mV)	93 mV dec ⁻¹	<i>Nat. Commun.</i> ⁷
Oxidized-derived Ag	0.1 M KHCO ₃	80% (490 mV)	77 mV dec ⁻¹	<i>Angew. Chem. Int. Ed.</i> ⁸
MoSeS monolayers	EMIMBF ₄ :H ₂ O=4:96(mol)	45% (940 mV)	NM	<i>Angew. Chem. Int. Ed.</i> ⁹
Co ₃ O ₄ -CDots-C ₃ N ₄	0.5 M KHCO ₃	89% (490 mV)	NM	<i>Nat. Commun.</i> ¹⁰

Notes: NM: not mentioned.

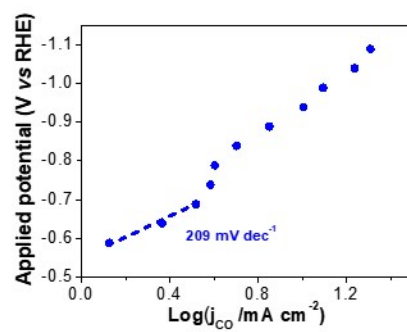


Figure S12. Tafel analysis about CO₂-to-CO electrochemical evaluation on P-Zn in 0.1 M KHCO₃.

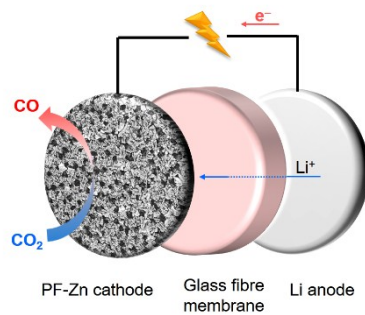


Figure S13. Schematic of the Li-CO₂ battery with PF-Zn cathode. The electrolyte: TEGDME and 1 M LiTFSI.



Figure S14. Photo of cathodic shell of coin-type cell used in the Li-CO₂ battery test.

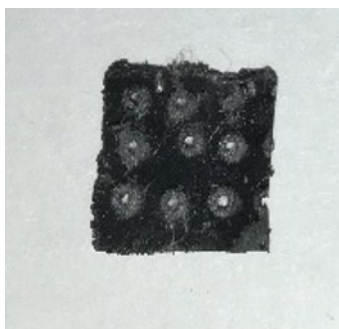


Figure S15. Photo of PF-Zn used in battery test.

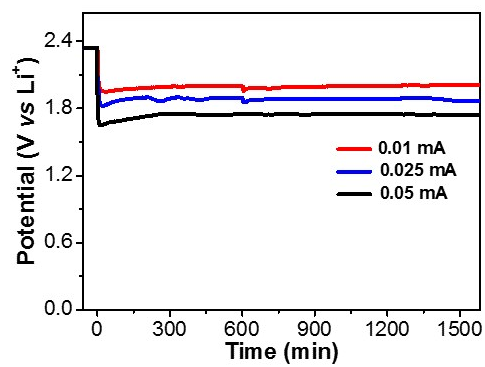


Figure S16. Galvanostatic discharge potentials of Li-CO₂ batteries with PF-Zn cathodes under several currents.

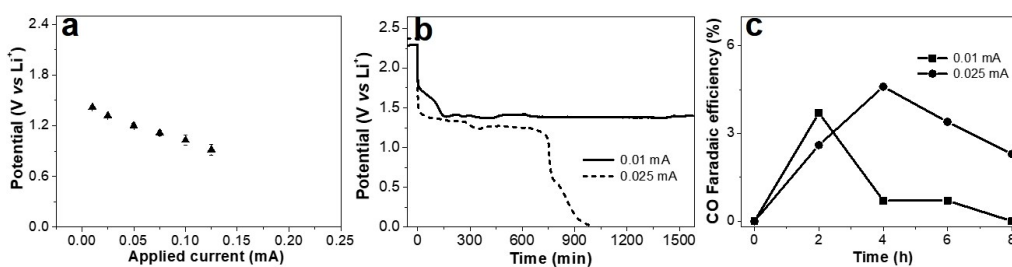


Figure S17. Galvanostatic discharge of Li-CO₂ batteries with bare Zn cathodes. (a) Discharge potentials profiles. (b) Discharge potential variation at long-term tests. (c) Max CO FE at several-currents during 10-h discharge.

The smaller CO generation with lower FE during Li-CO₂ batteries discharge (Fig. 4, S17, and S18) than during electrochemical evaluation (Fig. 3) was observed in both PF-Zn and bare Zn cathodes. This lower selectivity of CO generation from Li-CO₂ battery ($2\text{Li}^+ + 2\text{CO}_2 \rightarrow \text{Li}_2\text{CO}_3 + \text{CO}$) may be owing to the slow kinetics resulted from Li₂CO₃ forming and depositing on catalyst surface.

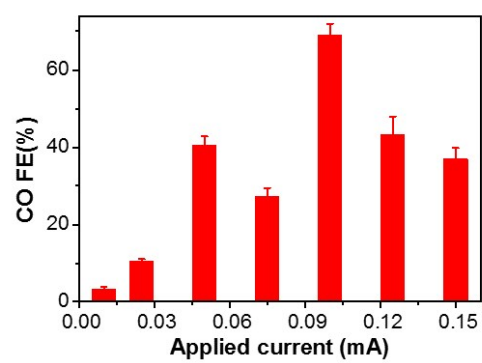


Figure S18. Max CO FE from Li-CO₂ batteries with PF-Zn cathodes at several currents during 10-h discharge with error bar.

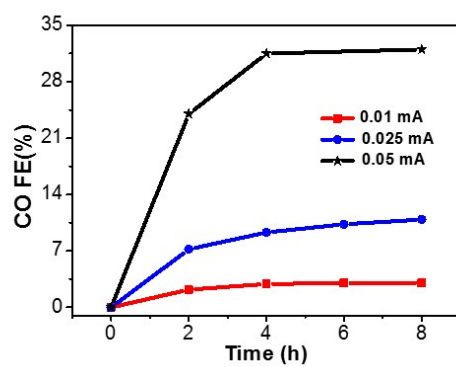


Figure S19. Max CO FE from Li-CO₂ batteries with PF-Zn cathodes at several currents during 10-h discharge.

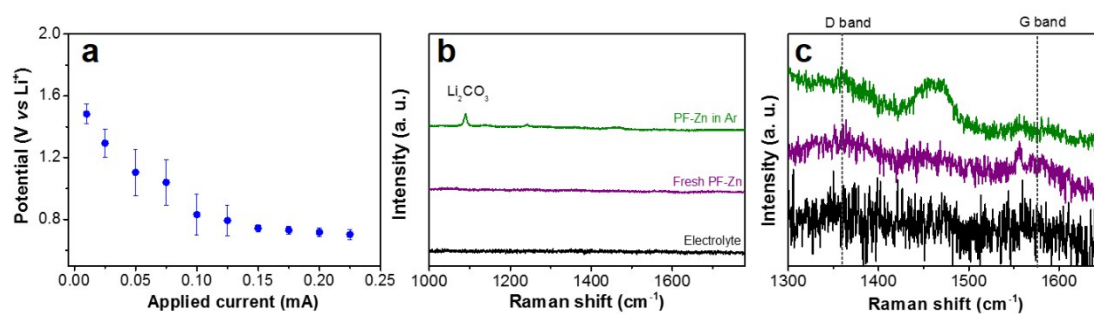


Figure S20. Galvanostatic discharge test of batteries with PF-Zn cathodes in Ar. (a) Discharge potentials profiles. (b) Raman spectra of PF-Zn after discharge tests. (c) High-resolution Raman spectra of PF-Zn in (b).

The control experiment with Ar supply instead of CO₂ filled cell was carried out, and the results revealed that 1) the discharge voltages were much lower than in CO₂, 2) no carbon-contained gas products (such as CO, CH₄, and C₂H₄) were detected, 3) H₂ was identified as the only gas product, 4) Li₂CO₃ and C were detected on the PF-Zn after the battery discharge in Ar. Based on above experiments, the electrolyte is possibly decomposed in our case, but the decomposition products do not contain CO. So CO generation from Li-CO₂ battery with PF-Zn cathode originated, most likely, from CO₂ reduction.

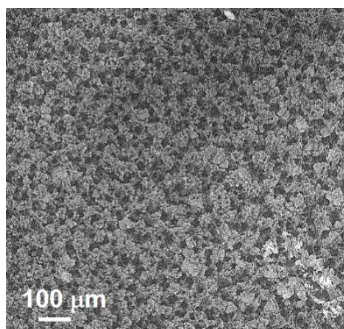


Figure S21. SEM image of PF-Zn cathode after battery discharge.

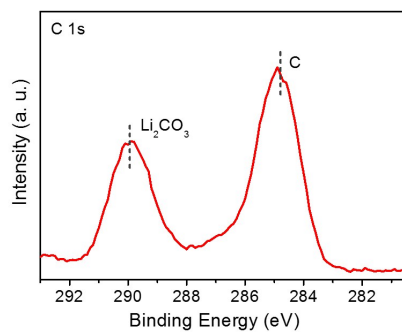


Figure S22. XPS spectrum of C 1s for PF-Zn after battery discharge.

References

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