Supporting Information

## Enhanced stability and separation efficiency of graphene oxide membranes in organic solvent nanofiltration

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		Materials	Thickness	Solvent permeance $(L m^{-2} h^{-1} bar^{-1})$	Rejection
Yang al. <sup>S1</sup>	et	HLGO	8 nm	7.5 (methanol)	99% for Chrysoidine G (249 g mol <sup>-1</sup> )
Aba al. <sup>S2</sup>	et	GO hollow fiber membrane (wet)	1.5 μm	3.97 (methanol)	97% for MO (327.3 g mol <sup>-1</sup> )
Chong al. <sup>S3</sup>	et	GO hollow fiber membrane	150 nm	2.8 (water); 7.54 (acetone)	90% for methyl red (269.3 g $mol^{-1}$ ) in water
Hua et al	S4	TPP/GO/HPE I	62 nm	14.9 (ethanol)	95% for Alcian blue (1299 g $mol^{-1}$ )
		TPP/GO/HPE I/PSS		3.1 (ethanol)	97% for Rose Bengal (1017 g mol <sup>-1</sup> )
Li et al. <sup>se</sup>	5	GO/PI	70 nm	1 (ethanol)	95.34% for vitamin B12 (1355.4 g mol <sup>-1</sup> )
This wor	k	GO/BA	60 nm	3.5 (methanol)	95% for AF (585.54 g mol <sup>-1</sup> ); 99.0% for VB12

Table S1. Performances of GO-based membranes for molecular separations in organic solvents

## **References:**

- S1. Q. Yang, Y. Su, C. Chi, C. T. Cherian, K. Huang, V. G. Kravets, F. C. Wang, J. C. Zhang, A. Pratt, A. N. Grigorenko, F. Guinea, A. K. Geim and R. R. Nair, *Nat. Mater.*, 2017, 16, 1198.
- S2. N. F. D. Aba, J. Y. Chong, B. Wang, C. Mattevi and K. Li, J. Membr. Sci., 2015, 484, 87.
- S3. J. Y. Chong, N. F. Aba, B. Wang, C. Mattevi and K. Li, *Sci. Rep.*, 2015, 5, 15799.
- S4. D. Hua and T.-S. Chung, *Carbon*, 2017, **122**, 604.
- S5. B. Li, Y. Cui, S. Japip, Z. Thong and T.-S. Chung, *Carbon*, 2018, **130**, 503.



**Fig. S1** Chemical structures of BA polymer (a), vitamin B12 (b), acid fuchsin (c), methyl orange (d) and Evans blue (e).



**Fig. S2** (a) One pot preparation of BA polymer via the combination of the Biginelli reaction and radical polymerization. (b) <sup>1</sup>H and <sup>11</sup>B NMR spectra (DMSO- $d_6$  + D<sub>2</sub>O, 400 MHz) of BA polymer.

In a 100 mL Schlenk tube, AEMA (2.14 g, 10.0 mmol), 4formylphenylboronic acid (1.50 g, 10.0 mmol), thiourea (1.14 g, 15.0 mmol), MgCl<sub>2</sub> (0.19 g, 2.0 mmol), polyethylene glycol maleate (PEGMA, M<sub>n</sub>: 950 g mol<sup>-1</sup>; 9.50 g, 10 mmol) and 2,2'-Azobis(2,4-dimethyl)valeronitrile (ABVN, 0.05 g, 0.2 mmol) were mixed in 20.0 mL of acetic acid. The tube was sealed with a rubber septum and purged by nitrogen flow for 20 min, then kept in a 70 °C oil bath for 12 h. The polymerization was quenched using an ice-water bath. Then the mixture was precipitated in diethyl ether for 3 times and dried under vacuum to obtain the pure BA polymer for further characterization and use.



**Fig. S3** A typical process of stabilizing a 44-GO-0.5BA-T membrane by filtrating methanol to achieve a steady flux.



Fig. S4 (a, b) SEM images of GO sheets in different resolutions.



**Fig. S5** (a) C1s XPS spectra of GO, GO-0.5BA-M, GO-T and GO-0.5BA-T membranes. (b) XPS survey spectra of GO, GO-0.5BA-M and GO-0.5BA-T membranes. (c) S 2p XPS spectra of a GO-0.5BA-T membrane.



**Fig. S6** (a) The digital photos of GO (left) and GO-0.5BA-T (right) dispersions. (b) The digital photos of 44-GO (left) and 44-GO-0.5BA-T (right) membranes on the nylon microfiltration membrane.



**Fig. S7** (a) FTIR spectra and (b, c) magnified FTIR spectra of a GO membrane, BA polymer and a GO-0.5BA-T membrane. (d) Thermogravimetric (TGA) analyses of GO and GO-0.5BA-T membranes. (e) Schematic illustration of the covalent and noncovalent interactions between BA polymer and GO. (f) Reaction scheme between boronic moiety of BA polymer and the GO sheet.



**Fig. S8** AFM images and the corresponding height profiles of a 44-GO membrane (a, b) and a 44-GO-0.5BA-M membrane (c, d).



**Fig. S9** (a) The differences of 2 Theta in XRD patterns between dried membranes and membranes in methanol. (b-d) The XRD patterns of GO, GO-0.5BA-M (b), GO-0.5BA-T (c) and GO-1BA-T (d) membranes in methanol.



**Fig. S10** The methanol permeances of m-GO (a) and m-GO-0.5BA-T (b) membranes with different GO loadings.



Fig. S11 MWCO curves of the 44-GO and 44-GO-0.5BA-T membranes in methanol.



**Fig. S12** UV-vis adsorption spectra of Evans Blue (a, c, e) and acid fuchsin (b, d, f) methanol solution before and after filtration through a 44-GO membrane (a, b), a 44-GO-0.5BA-M membrane (c, d) and a 44-GO-0.5BA-T membrane (e, f).



**Fig. S13** UV-vis adsorption spectra of Evans Blue (a, c) and acid fuchsin (b, d) methanol solution before and after filtration through a 44-GO-0.1BA-T membrane (a, b) and a 44-GO-1BA-T membrane (c, d).



**Fig. S14** (a) The variations of DMF flux with transmembrane pressure at the range of 4~10 bar. (b) The rejections for EB and AF in DMF solutions of the 44-GO-0.5BA-T membrane under different pressures and temperatures as indicated.



**Fig. S15** UV-vis adsorption spectra of EB methanol solution (a), EB aqueous solution (b), AF aqueous solution (c) and MO aqueous solution (d) before and after filtration through a 44-GO-0.5BA-T membrane which was soaked in water for one month.



**Fig. S16** (a) The UV-vis adsorption spectra of AF in methanol before and after filtration through a 44-GO-0.5BA-T membrane after soaking in water for one month. (b, c) The UV-vis adsorption spectra of mixed EB-MO solution (b) and VB12 (c) in methanol before and after filtration through a 44-GO-0.5BA-T membrane. Insert images were photos of feed solution (left) and permeate solution (right) of VB12 methanol solution.



**Fig. S17** The digital photos of 44-GO-0.5BA-T membranes on the nylon microfiltration membrane after soaking in 0.1 M HCl (left) and 0.1 M NaOH (right) under vigorous shaking for one and a half month.