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## **Supporting Information**

## Molybdenum Carbide Chemical Sensor with Ultrahigh Signal-to-Noise Ratio and Ambient Stability

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**Figure S1**. Schematic illustration of molybdenum carbide synthesis. x-axis represents reaction time and y-axis shows reaction temperature.



**Figure S2. (a)** Barrett-Joyner-Halenda (BJH) pore size distributions of synthesized molybdenum carbides (represented as differential pore volume against log scale of pore diameter). **(b)** Nitrogen adsorption isotherm linear plot by Brunauer-Emmett\_Teller (BET) model for two phases of molybdenum carbides

Material	BET Surface Area (m²/g)	Pore Volume (cm <sup>3</sup> /g)	Average Pore Diameter (nm)
Commercial MoC <sub>x</sub>	0.6031	0.002324	46.2534
α-MoC <sub>1-x</sub>	66.0359	0.138961	6.5202
β-Mo <sub>2</sub> C	44.0782	0.171089	11.7959

**Table S1**. The BET surface area, pore volume and average pore diameter information of molybdenum carbides.

## HR-TEM lattice fringe analysis

1. Cubic structure (MoC<sub>1-x</sub>, JCPDS 01-077-7176)  

$$a = b = c = 4.244973 \quad \mathring{A}, \qquad \alpha = \beta = \gamma = 90^{\circ}$$

$$|\vec{a}^*| = |\vec{b}^*| = |\vec{c}^*| = \frac{1}{a}$$

$$d_{hkl} = \frac{a}{\sqrt{h^2 + k^2 + l^2}}$$

$$d_{111} = \frac{4.244973 \quad \mathring{A}}{\sqrt{3}} = 2.45 \quad \mathring{A} \quad , \qquad d_{220} = \frac{4.244973 \quad \mathring{A}}{\sqrt{8}} = 1.501 \quad \mathring{A}$$

$$\cos \phi = \frac{h_1 h_2 + k_1 k_2 + l_1 l_2}{\sqrt{h_1^2 + k_1^2 + l_1^2} \sqrt{h_2^2 + k_2^2 + l_2^2}}$$

$$\cos \phi = \frac{4}{\sqrt{3}\sqrt{8}} = 0.8165$$

$$\therefore \phi = 35.26^{\circ}$$
2. Orthorhombic structure (\beta-Mo\_2C, JCPDS 01-077-0720)  

$$a \neq b \neq c, \qquad a = 6.041758 \quad \mathring{A}, \qquad b = 4.745728 \quad \mathring{A}, \qquad c = 5.214426 \quad \mathring{A}$$

$$\alpha = \beta = \gamma = 90^{\circ}$$

$$|\vec{a}^*| = \frac{1}{a} \quad , |\vec{b}^*| = \frac{1}{b} \quad , |\vec{c}^*| = \frac{1}{c}$$

$$d_{hkl} = \frac{1}{\sqrt{(\frac{h}{a})^2 + (\frac{k}{b})^2 + (\frac{l}{c})^2}}$$

$$d_{020} = \frac{1}{\sqrt{\frac{4}{4.745728^2}}} \mathring{A} = 2.37 \mathring{A}$$

$$d_{211} = \frac{1}{\sqrt{\frac{4}{6.041758^2} + \frac{1}{4.745728^2} + \frac{1}{5.214426^2}}} \mathring{A} = 2.29 \mathring{A}$$

$$\cos \emptyset = \frac{\frac{h_1 h_2}{a^2} + \frac{k_1 k_2}{b^2} + \frac{l_1 l_2}{c^2}}{\sqrt{\frac{h_1^2}{a^2} + \frac{k_1^2}{b^2} + \frac{l_1^2}{c^2}} \sqrt{\frac{h_2^2}{a^2} + \frac{k_2^2}{b^2} + \frac{l_2^2}{c^2}}}$$
$$\cos \emptyset = \frac{\frac{2}{b^2}}{\sqrt{\frac{4}{b^2}} \sqrt{\frac{4}{a^2} + \frac{1}{b^2} + \frac{1}{c^2}}} = 0.48245$$
$$\therefore \emptyset = 61.15^0$$



**Figure S3**. Schematic of the overall gas delivery system. Various analytes and  $N_2$  was introduced in a controlled manner into the reaction chamber by using the MFC, tubing system, and multi-position valve. The serial dilution system was also used to obtain 2.5–30000 ppm concentrations of the analyzed gas.



**Figure S4**. Response time of the  $\alpha$ -MoC<sub>1-x</sub> and  $\beta$ -Mo<sub>2</sub>C sensors onto wide concentration range of (a) ethanol, (b) NH<sub>3</sub> and (c) NO<sub>2</sub>.



**Figure S5**. The real-time NO<sub>2</sub> (5 ppm), NH<sub>3</sub> (5 ppm), C<sub>2</sub>H<sub>5</sub>OH (1000 ppm) response behavior of the one-year old  $\alpha$ -MoC<sub>1-x</sub> and  $\beta$ -Mo<sub>2</sub>C sensors under the air condition.



**Figure S6**. (a) Photo-image of the powder resistivity measurement setup (HPRM-M2, HANTECH<sup>TM</sup>). (b) Pellet form of the  $\alpha$ -MoC<sub>1-x</sub> and  $\beta$ -Mo<sub>2</sub>C after measurement with pressing. (c) Resistivity and (d) conductivity of the  $\alpha$ -MoC<sub>1-x</sub> and  $\beta$ -Mo<sub>2</sub>C with varied pressure.