

Supplementary Information for

Hierarchically Structured Rugae-Like RuP₃-CoP Arrays
as Robust Catalyst Synergistically Promoting Hydrogen
Generation

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EXPERIMENTAL SECTION

1.1. Materials

Sodium hydroxide (NaOH), sodium borohydride (NaBH_4), cobalt nitrate hexahydrate ($(\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O})$), ruthenium(III) 2,4-pentanedionate ($\text{C}_{15}\text{H}_{21}\text{O}_6\text{Ru}$), ruthenium(III) chloride (RuCl_3), sodium hypophosphite ($\text{NaH}_2\text{PO}_2 \cdot \text{H}_2\text{O}$), dimethylformamide (DMF), hydrochloric acid (HCl) and ethanol ($\text{C}_2\text{H}_5\text{OH}$) are all analytical grade and used without further purification. Nickle foam with thickness of ~ 1.6 mm was purchased from commercial company.

1.2. Synthesis of Ru nanoparticles (NPs)

Ru NPs was prepared through a typical hydrothermal method, where 20.7 mg of RuCl_3 and 500 mg of PVP were successively dissolved into 50 ml ethylene glycol, and ultrasonicated for 10 min to obtain a homogeneous solution. Subsequently, the mixture was transferred into a three-necked flask, and refluxed in an oil bath at 180°C for 10 min. After cooling to room temperature, the product was precipitated by adding acetone, washed several times by acetone, and then dispersed in methanol to keep the mass concentration for 1.0 mg mL^{-1} .

1.3. Different methods for preparing CoRu-species/NF composites

(1) Immersion method: Electrodeposition prepared Co-species@NF-60 samples were put into different concentrations of ruthenium(III) 2,4-pentanedionate in DMF solution (5, 10, 20, 30, 40 and 50 mg mL^{-1}) for 24 h. The resulted samples were labeled as Immersion-CoRu-species/NF-X (X=5, 10, 20, 30, 40 and 50).

(2) Ru NPs method: The above-prepared mixture of Ru NPs in methanol solution was pipetted dropwise onto Co-species@NF-60 surface to prepare CoRu-species@NF hybrid material. The resulted sample was labeled as Ru NPs-CoRu-species@NF.

(3) RuCl_3 method: A certain amount of RuCl_3 aqueous solution was pipetted onto the surface of Co-species@NF-60. The resulted sample was labeled as $\text{RuCl}_3\text{-CoRu-species@NF}$.

1.4. Synthesis of Co-Ru-P@NF by vapor phase phosphidation

The phosphidation process was performed in a tube furnace, where the NaH_2PO_2 in a porcelain boat was put in the upstream side and a series of CoRu-species/NF samples were placed next to the NaH_2PO_2 at a downstream side. The furnace was heated to $350\text{ }^\circ\text{C}$ with $2\text{ }^\circ\text{C min}^{-1}$ in Ar atmosphere (20 sccm), and kept at $350\text{ }^\circ\text{C}$ for 2 h. After the phosphidation, the samples were cooled down to ambient temperature in flowing Ar gas. As a comparison, the CoP/NF and $\text{Ru}_2\text{P}/\text{NF}$ were prepared by a similar phosphidation process.

1.5. Calculations

(1) The electrodeposited Co on the NF surface is calculated by using the Faraday's laws as follows:

$$Q = I \times t = n \times z \times F$$

Where Q (C) is the total charge provided by electrochemical workstation, I (A) is the current set in electrodeposition process, t (s) is the time of electrodeposition, n (mol) is the amount of electrodeposited metal, z is the valence change of electrodeposited metal, and F (96485 C mol^{-1}) is faraday constant.

(2) The effect of temperatures on reaction rates of the synthesized samples are analyzed by using the Arrhenius equation as follows:

$$\ln \kappa = \ln A - E_a/RT$$

Where κ ($\text{L min}^{-1} \text{ g}^{-1}$) is the rate coefficient, A ($\text{L min}^{-1} \text{ g}^{-1}$) is a constant, E_a (kJ mol^{-1}) is the activation energy, R ($8.314 \text{ J mol}^{-1} \text{ K}^{-1}$) is the universal gas constant, and T (K) is the temperature.

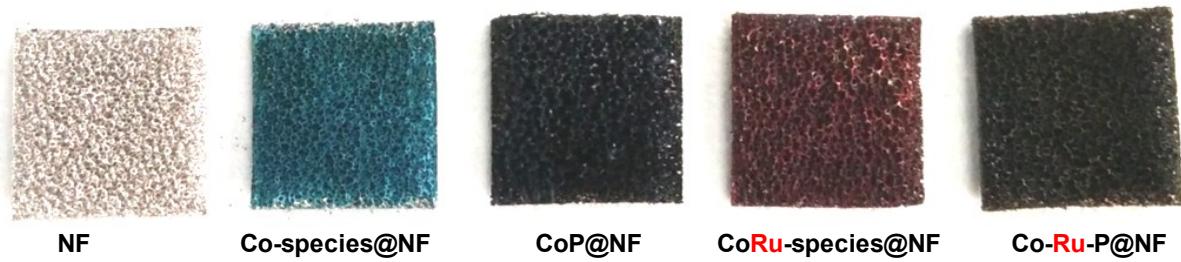


Fig. S1. The photographs of fresh NF, Co-species@NF-60, CoP@NF-60, CoRu-species@NF-60 and Co-Ru-P@NF-60 materials.

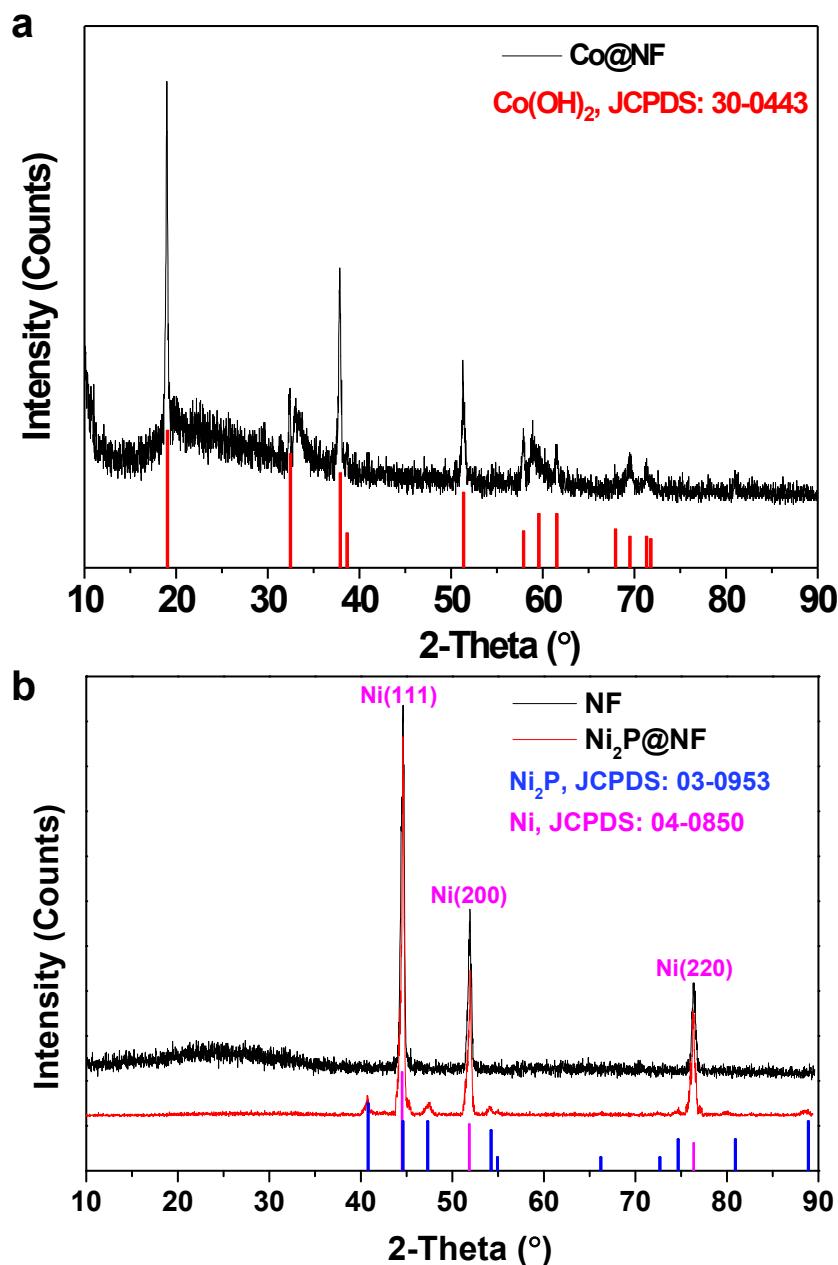


Fig. S2. (a) XRD pattern of the electrodeposited Co-species@NF-60. (b) XRD patterns of the NF and Ni₂P@NF. Note: The Ni₂P@NF was obtained by direct phosphating NF.

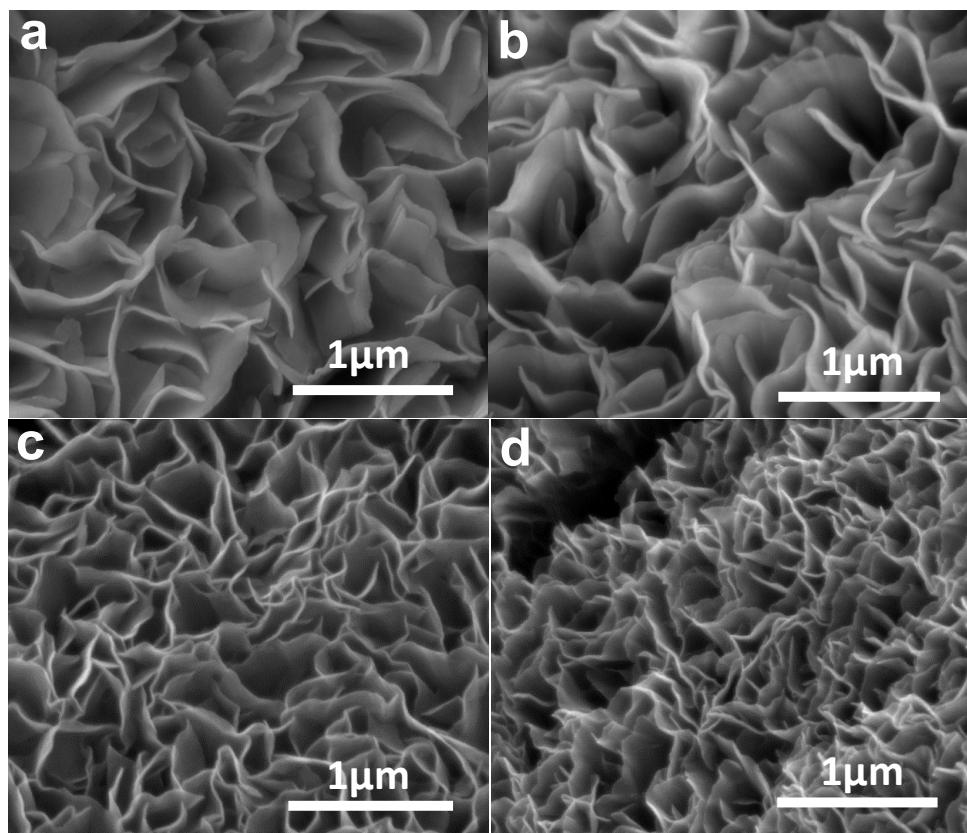


Fig. S3. SEM images of Co-species@NF with different electrodeposition times of (a) 20 min, (b) 30 min, (c) 40 min and (d) 50 min.

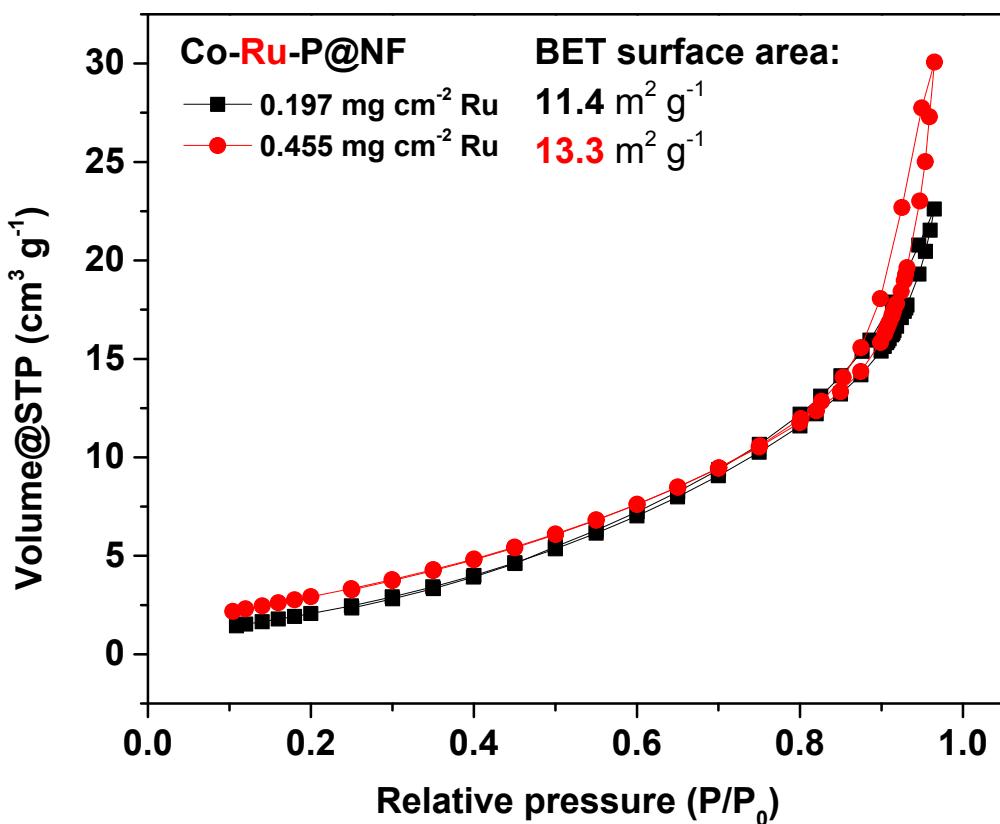


Fig. S4. Nitrogen adsorption–desorption isotherms curves of Co-Ru-P@NF composite with different loadings of Ru species.

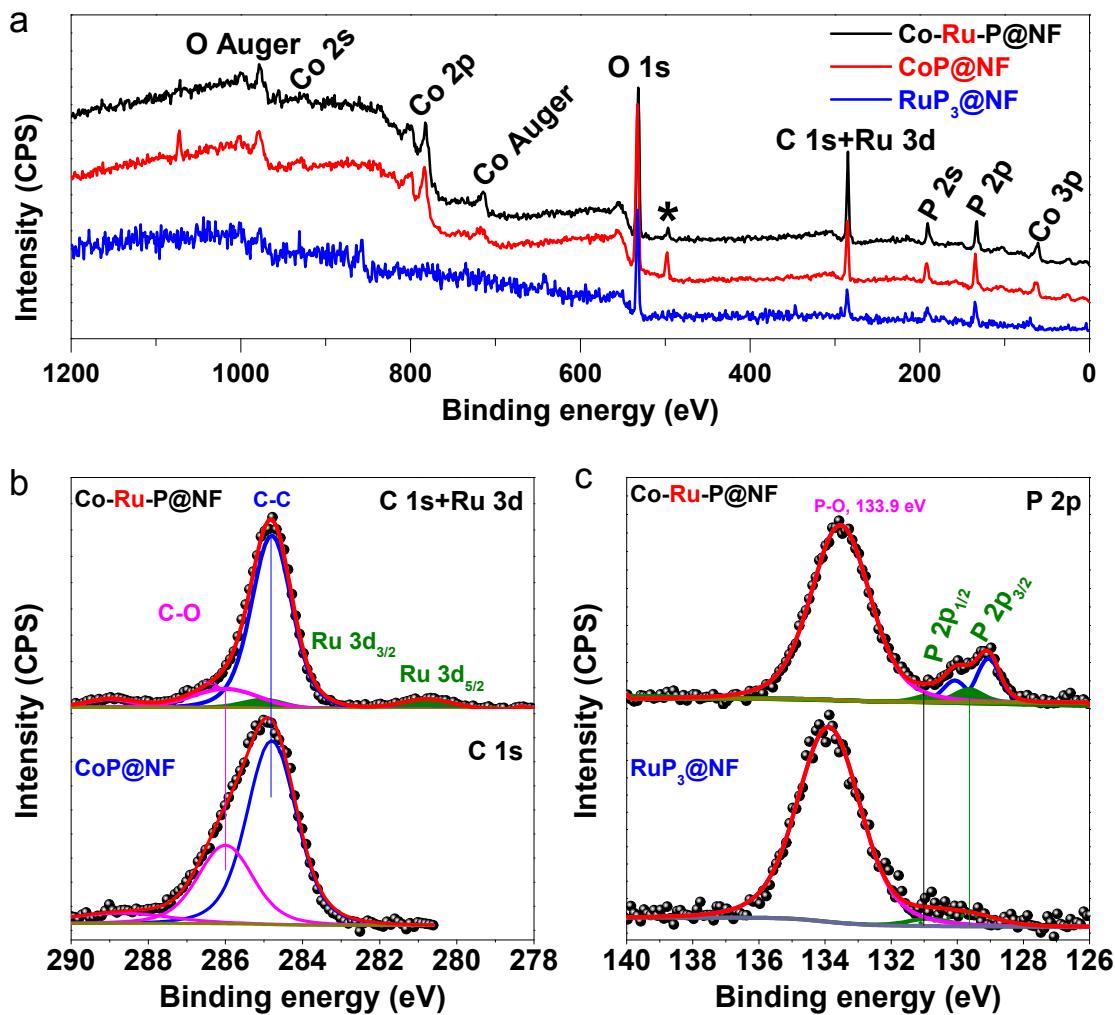


Fig. S5. (a) XPS survey spectrum of Co-Ru-P@NF, CoP@NF and RuP₃@NF. High-resolution XPS spectra of (b) C 1s+Ru 3d and (c) P 2p regions from Co-Ru-P@NF and RuP₃@NF, respectively.

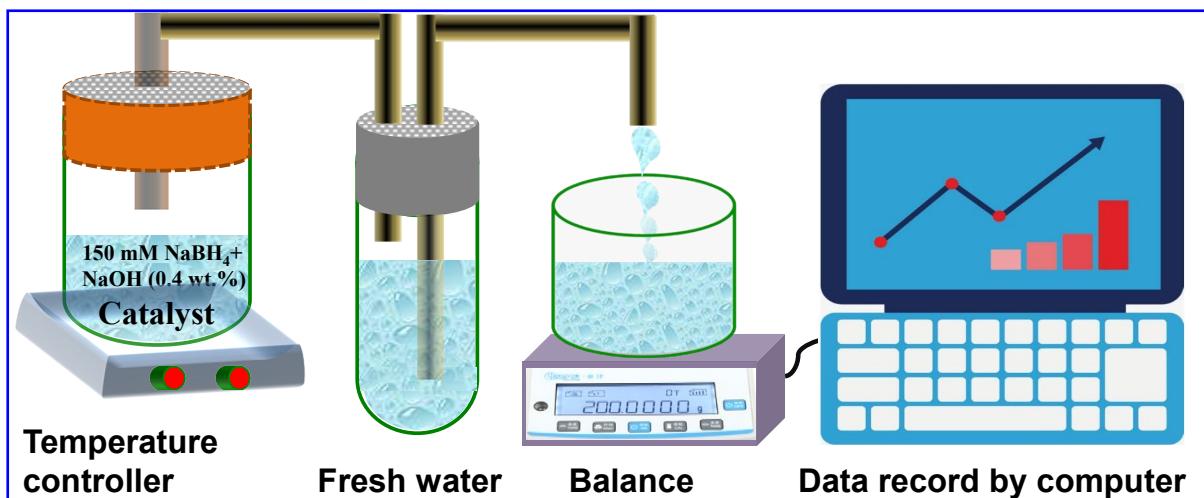


Fig. S5. Schematic illustration of the setup for H_2 production by hydrolysis of 150 mM $NaBH_4$ + 0.4 wt % $NaOH$ solution.

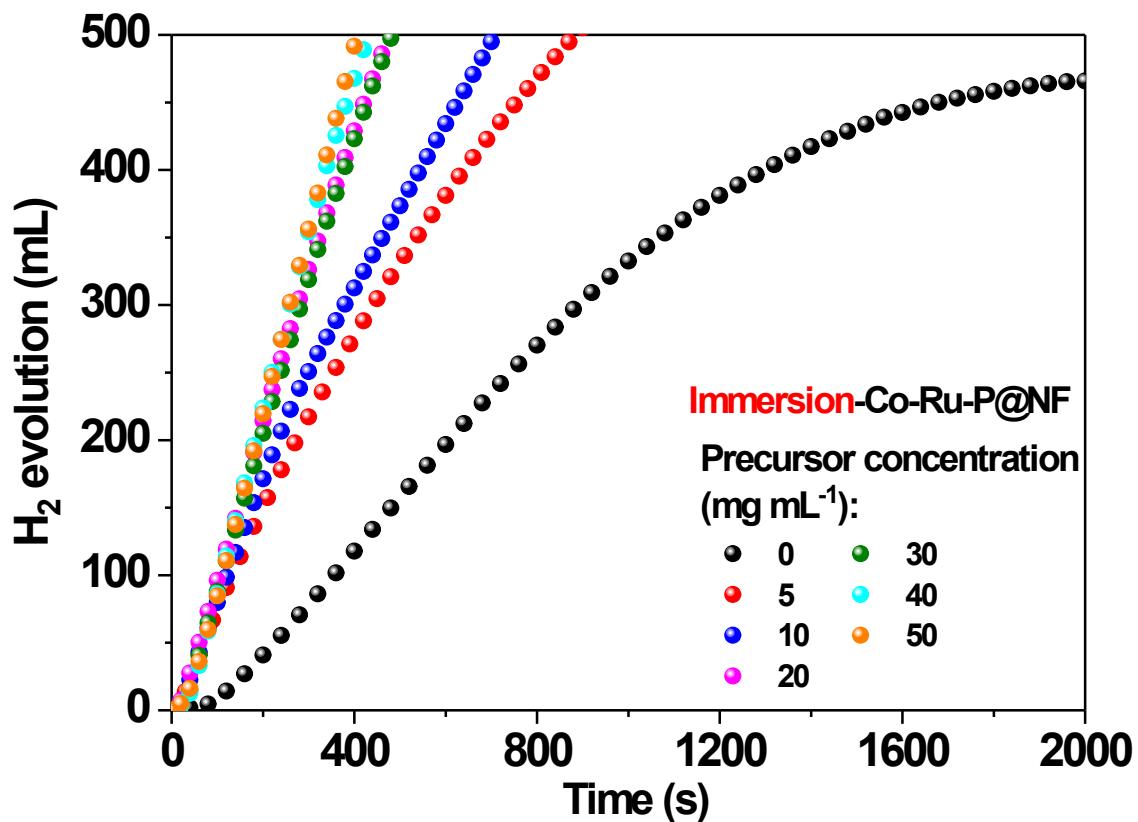


Fig. S7. The H_2 generation rate (25 °C) of series of Co-Ru-P@NF catalysts prepared by immersing in different concentrations of $C_{15}H_{21}O_6Ru$ in DMF solution. The hydrolysis solution is 150 mM NaBH_4 + 0.4 wt % NaOH solution.

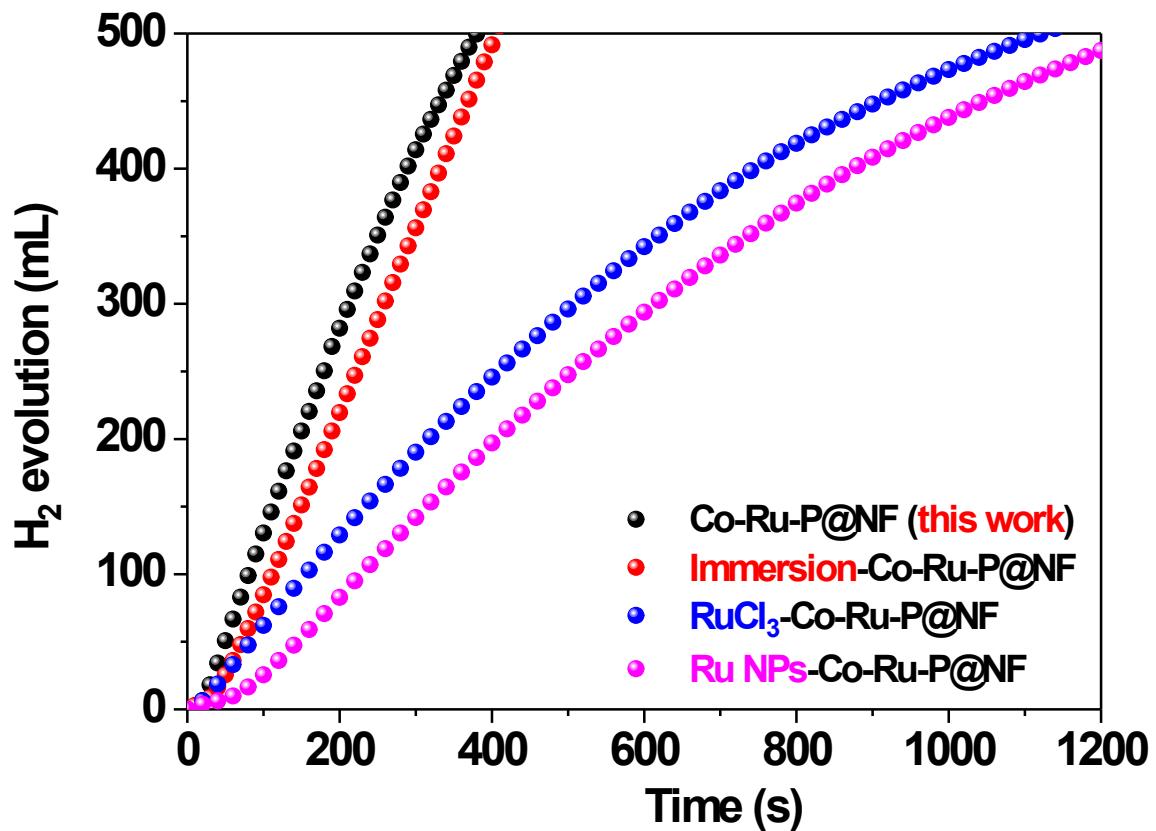


Fig. S8. Comparison of H₂ evolution capacity on Co-Ru-P@NF catalysts synthesized by different methods in 150 mM NaBH₄ + 0.4 wt % NaOH solution at 25 °C.

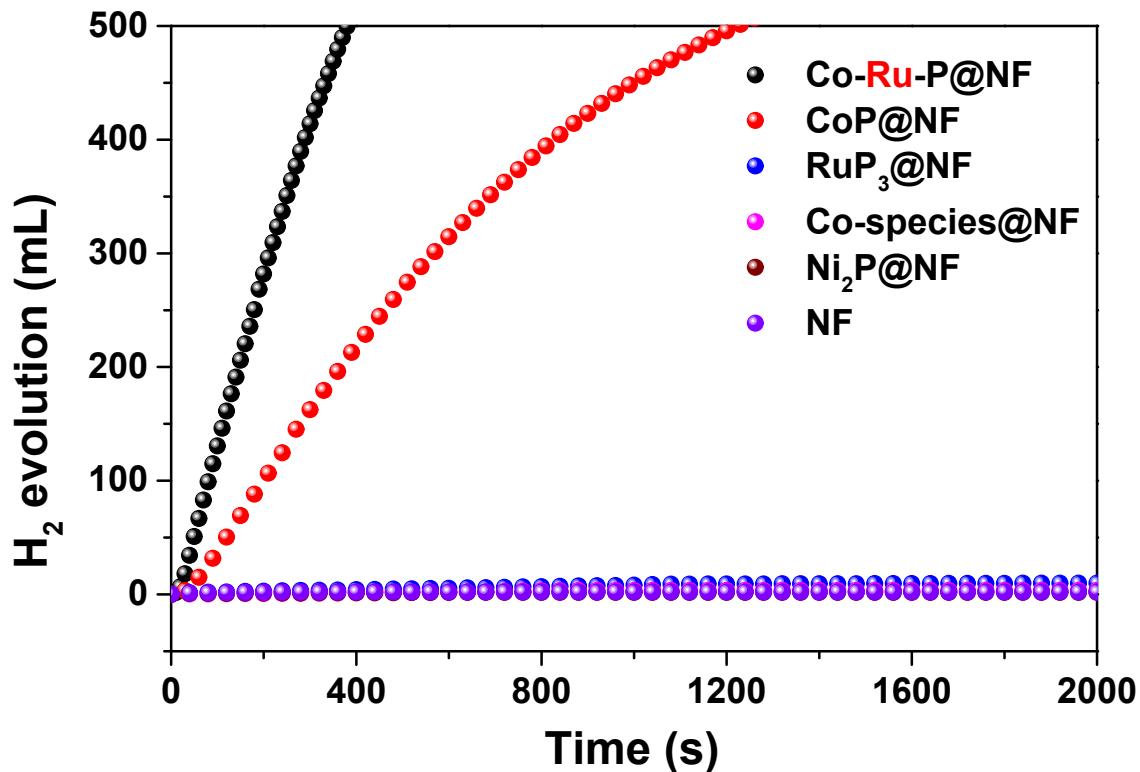


Fig. S9. Stoichiometric hydrogen evolution in 150 mM NaBH₄ + 0.4 wt % NaOH solution by different catalysts at 25 °C.

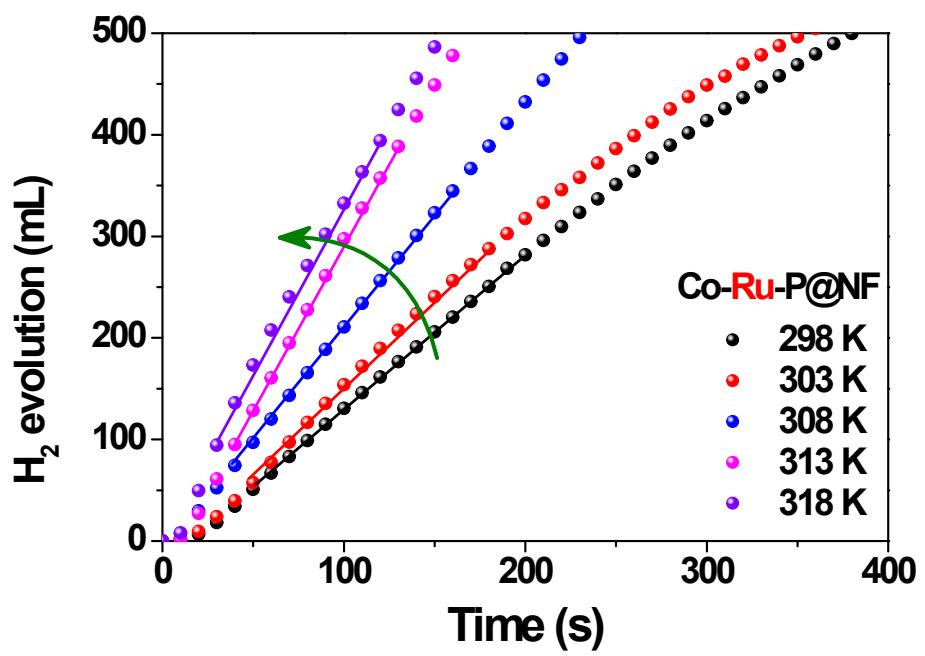


Fig. S10. The relationship between the H_2 generation rate and the reaction temperatures of Co-Ru-P@NF by hydrolysis of 150 mM $NaBH_4$ + 0.4 wt % $NaOH$ solution.

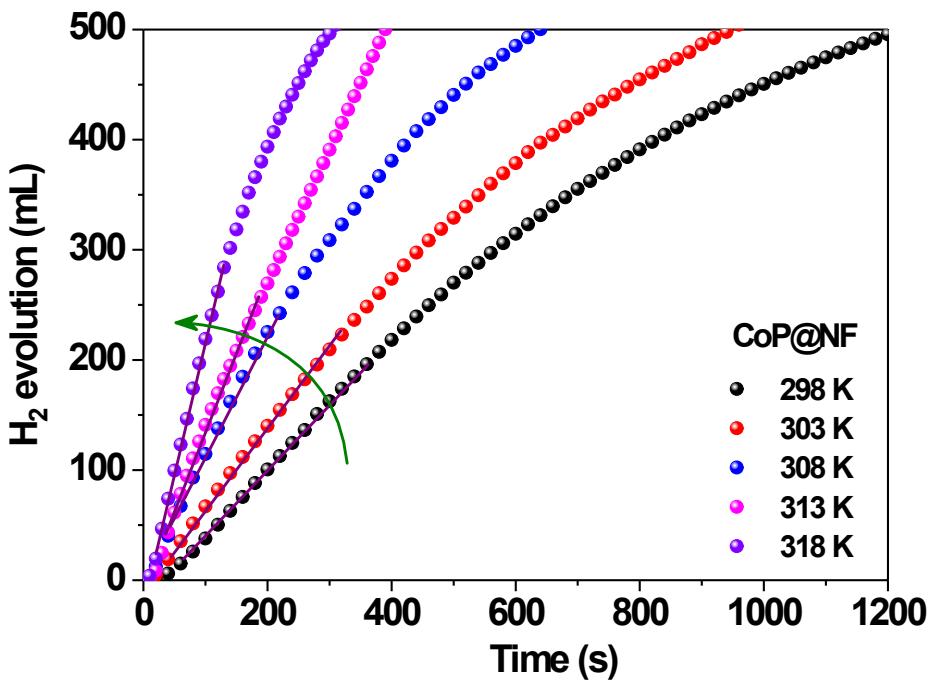


Fig. S11. The effect of hydrolysis temperatures for H₂ production on the CoP@NF catalyst by hydrolysis of 150 mM NaBH₄ + 0.4 wt % NaOH solution.

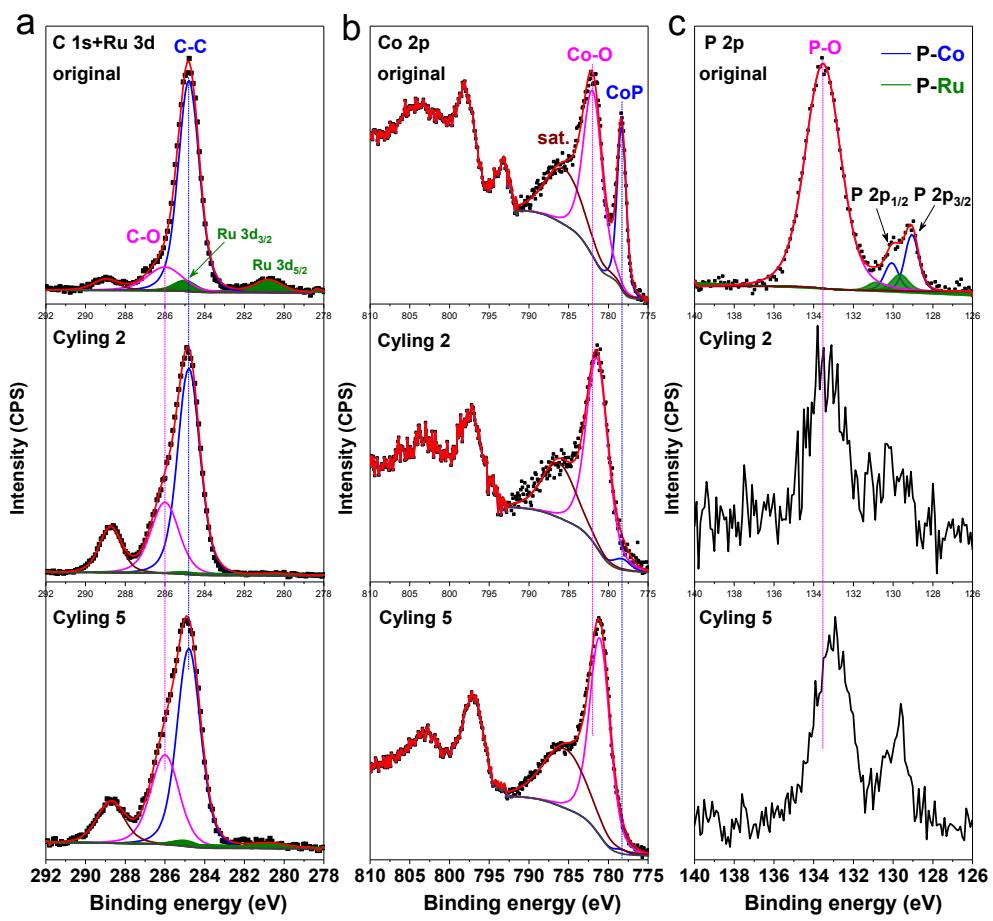


Fig. S12. High-resolution XPS spectra of (a) C 1s+Ru 3d, (b) Co 2p and (c) P 2p regions from original Co-Ru-P@NF, recycle 1 time and recycle 5 times later.

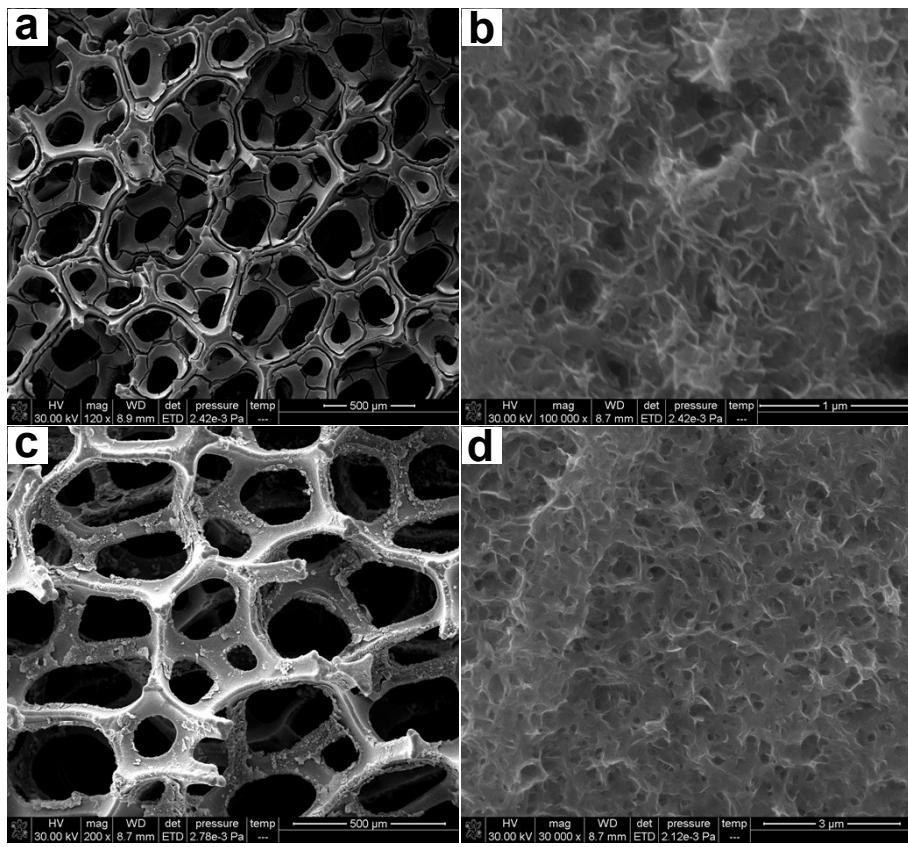


Fig. S13. SEM and high-magnification SEM images (a-b) after recycle 2 times and (c-d) after recycle 5 times of Co-Ru-P@NF catalysts.

Table S1. Inductive coupled plasma atomic emission spectroscopy (ICP-AES) results of different samples.

Sample	Total mass ($\mu\text{g/L}$)	Co ($\mu\text{g/L}$)	Co (wt %)	Ru ($\mu\text{g/L}$)	Ru (wt %)
1	436	222.557	51.0	2.406	0.552
2	400	221.667	55.4	3.472	0.868
3	382	215.303	56.4	4.181	1.095
4	362	191.336	52.9	5.863	1.620
5	376	143.016	38.0	6.534	1.738

Note: In this process, ~2.0 mg samples were dissolved in aqua regia solution, and then diluted into 2.0 mg/L catalyst solution. Before ICP testing, the prepared solution was further diluted into about 400 $\mu\text{g/L}$ catalyst solution. The standard solution of Co and Ru was bought from commercial company and used directly.

Table S2. Summary of Co-Ru-P@NF catalysts with different loadings.

Sample	Fresh NF (mg)	Co-Ru-P@NF (mg)	Loading of Ru (mg cm^{-2})
1	44.4	62.2 ($\Delta = 17.8$)	0.121
2	44.3	62.8 ($\Delta = 18.5$)	0.197
3	40.9	59.6 ($\Delta = 18.7$)	0.251
4	40.2	61.9 ($\Delta = 21.7$)	0.431
5	41.1	62.5 ($\Delta = 21.4$)	0.455

Note: The quality of the materials are obtained by weighing three parallel materials and averaging them.

Table S3. The summarized various parameters of noble metal and non-noble metal catalysts catalyze the production of H₂ by hydrolysis of NaBH₄/NH₃BH₃/N₂H₄·H₂O.

Noble metal catalysts	TOF (mol _{H2} mol _M ⁻¹ min ⁻¹)	Specific rate (mL min ⁻¹ g ⁻¹)	Activation energy (kJ mol ⁻¹)	solute	Temperatur e (°C)
Co-Ru-P@NF (this work)	2123.6 (mol_{H2} mol_{Ru}⁻¹ min⁻¹)	4839.8 (L min⁻¹ g_{cat}⁻¹)	40.3	150 mM NaBH₄ + 0.4 wt% NaOH	25
Pt/mesoporous silica ¹	187.9 (mol _{H2} mol _{Pt} ⁻¹ min ⁻¹)	19.1 (L min ⁻¹ g _{Pt} ⁻¹)	40.1	12 wt% NaBH ₄ +2 wt% NaOH	80
Pt/3D SiC ²	N.A.	268.75	N.A.	0.12 g/mL NaBH ₄ +2 wt% NaOH	80
Pt/Co ₃ O ₄ ³	N.A.	~1138	N.A.	5 mg/mL NaBH ₄	N.A.
13.1% Pt/C ⁴	N.A.	~1.3	N.A.	10 wt% NaBH ₄ +5 wt% NaOH	25
1 wt% Pt/LiCoO ₂ ⁵	N.A.	2700	70.4	10 wt% NaBH ₄ +5 wt% NaOH	25
Rh/Ni BNPs ⁶	193 (mol _{H2} mol _{Rh} ⁻¹ min ⁻¹)	N.A.	47.2±2.1	KBH ₄ , pH=12	30
Ni-Ru ⁷	N.A.	980	N.A.	10 wt% NaBH ₄ +7 wt% NaOH	25
Co _{0.8} -Ag _{0.2} -B ⁸	N.A.	2990	56.78	5 wt% NaBH ₄ +5 wt% NaOH	20±0.5
Ni/Au/Co ⁹	19.5	N.A.	18.8	30 mM NaBH ₄ , pH=12	30
Ni ₂ Pt@ZIF-8 ¹⁰	2222 (mol _{H2} mol _{Pt} ⁻¹ min ⁻¹)	N.A.	23.3	NH ₃ BH ₃ + 0.3 M NaOH	20±0.5
Ni _{0.9} Pt _{0.1} /Ce ₂ O ₃ ¹¹	28.1 h ⁻¹	N.A.	42.3	0.5 M NH ₃ BH ₃ + 0.5 M NaOH	25
Ru@SiO ₂ ¹²	200 (mol _{H2} mol _{Ru} ⁻¹ min ⁻¹)	N.A.	38.2	200 mM NH ₃ BH ₃	25
Ru(0)/SiO ₂ -CoFe ₂ O ₄ ¹³	172 (mol _{H2} mol _{Ru} ⁻¹ min ⁻¹)	N.A.	45.6	100 mM NH ₃ BH ₃	25.0±0.1
Pd(0)/SiO ₂ -CoFe ₂ O ₄ ¹⁴	254 (mol _{H2} mol _{Pd} ⁻¹ min ⁻¹)	N.A.	52±2	100 mM NH ₃ BH ₃	25.0±0.1
Ag(0)/SiO ₂ -CoFe ₂ O ₄ ¹⁵	264	N.A.	53.4	100 mM NH ₃ BH ₃	25
Rh/VO ₂ ¹⁶	~25.8	N.A.	38.7±2.6	5 mg/mL NH ₃ BH ₃	~50
Pt ₅₈ Ni ₁₃ Al ₉ ¹⁷	496	N.A.	N.A.	0.1 M NH ₃ BH ₃	25
ALD-prepared Pt/CNT ¹⁸	416.5 (mol _{H2} mol _{Pt} ⁻¹ min ⁻¹)	N.A.	48.3±1.2	0.15 mol L ⁻¹ NH ₃ BH ₃	25±0.5
Ru/γ-Al ₂ O ₃ ¹⁹	256.8 (mol _{H2} mol _{Ru} ⁻¹ min ⁻¹)	N.A.	N.A.	10 mg/mL NH ₃ BH ₃	30
Non-noble metal catalysts	TOF (mol _{H2} mol _M ⁻¹ min ⁻¹)	Specific rate (mL min ⁻¹ g ⁻¹)	Activation energy (kJ mol ⁻¹)	solute	Temperatur e (°C)
Fe-CoP/Ti ²⁰	N.A.	6060	43.4	1 wt% NaBH ₄ +1 wt% NaOH	25
Co/elastic foam ²¹	N.A.	33.2 mL/min	40.2	52.87 mM NaBH ₄	20
Co ₃ O ₄ macrocubes ²²	N.A.	1497.55	47.97	2 wt% NaBH ₄	25
Pyridinium polymeric ²³	N.A.	5433±141	20.84 ± 0.76	500 mM NaBH ₄	25
Cell-EPC-DETA-HCl ²⁴	N.A.	3215	30.8	4.8 mg/mL NaBH ₄	25
Co-B-P ²⁵	N.A.	3976	49.11	2.5 wt% NaBH ₄ +5 wt% NaOH	30
Cu-Co-P/γ-Al ₂ O ₃ ²⁶	N.A.	1115	47.8	5 wt% NaBH ₄ +5 wt% NaOH	45
NiCo ₂ O ₄ hollow sphere ²⁷	N.A.	1000	52.211	1 wt% NaBH ₄	25
CoP NA/Ti ²⁸	N.A.	6500	41	1 wt% NaBH ₄ +1 wt% NaOH	20
Co/Fe ₃ O ₄ -CNT ²⁹	N.A.	1200	42.79	NaBH ₄	25
Co-P/Cu sheet ³⁰	N.A.	2275.1	27.9	NaBH ₄	50
Ni-B ³¹	N.A.	4991.8	36.3	5 wt% NaBH ₄	30
Ce _{0.05} -Ni-W-B ³²	N.A.	440	52.87	2.5 wt% NaBH ₄ +5 wt% NaOH	30
CoP nanosheet arrays ³³	N.A.	6100	42.01	1 wt% NaBH ₄ +2 wt% NaOH	25
ZIF-67 (600 °C) ³⁴	12.91	1738	25.8	125 mM NaBH ₄	35
Co _{0.9} Cu _{0.1} ³⁵	N.A.	~4166.7	16.5	0.12 g/mL NaBH ₄ +0.5 M NaOH	40
Ni-copolymer ³⁶	11.6	N.A.	47.82	1.9 mg/mL NaBH ₄	45
Co ₃ O ₄ nanorods ³⁷	N.A.	~1788	49.52	0.6 wt% NaBH ₄	25
Ni/BN sphere ³⁸	1.248	476.6	47.3	0.5 wt% NH ₃ BH ₃	25
CoP NA/Ti ³⁹	42.8	N.A.	34.1	1 wt% NH ₃ BH ₃	25
Co/NPCNW ⁴⁰	N.A.	2638	25.4	0.5 wt% NH ₃ BH ₃	25

Note: the M represents the noble metal in the TOF calculation. The total mass is used when the H₂ evolution rate is calculated. However, the pH of each condition may be slightly different.

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