

Supporting information

3D Hierarchical Porous Indium Catalyst for Highly Efficient Electroreduction of CO₂

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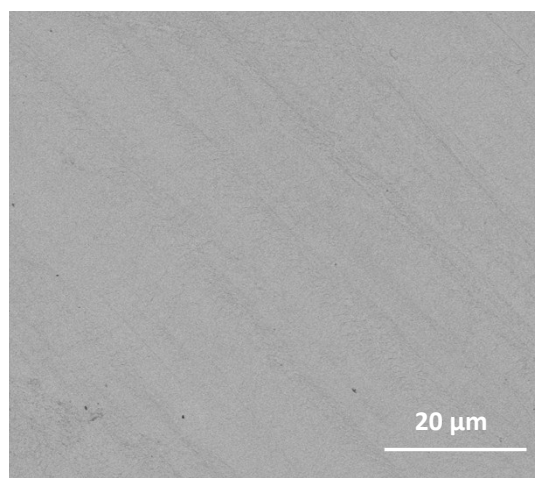


Figure S1 SEM image of the cleaned In foil sample

Table S1 Mass loading of *hp*-In, Pd-In and porous Pd samples measured by ICP-OES.

| Sample | <i>hp</i> -In | Pd-In-0.1 | Pd-In-0.5 | Pd-In-1.0 | Pd-In-2.0 | Porous Pd |
|----------------------------------|---------------|-----------|-----------|-----------|-----------|-----------|
| Mass of In (mg/cm ²) | 13.3 | 13.1 | 13.0 | 13.4 | 13.5 | - |
| Mass of Pd (mg/cm ²) | - | 1.4 E-2 | 3.1 E-2 | 5.2 E-2 | 9.9 E-2 | 1.7 E-1 |

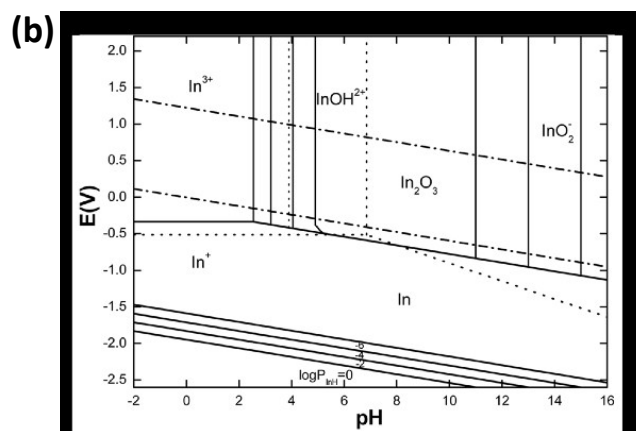
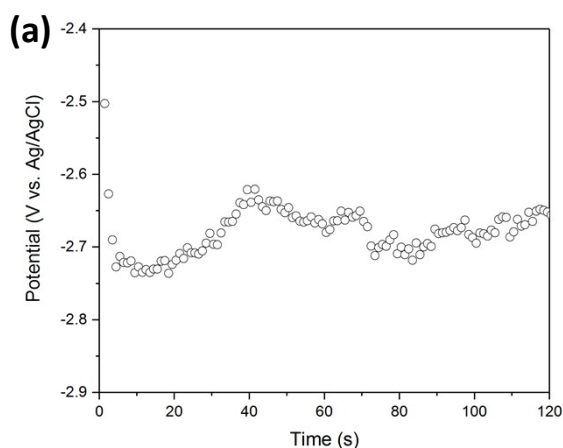


Figure S2 (a) Potential as a function of time for electrodeposition of *hp*-In. (b) Pourbaix diagram (E vs. pH diagram) for indium in water at 25 °C.^{1,2} Figure S2 a shows that during the electrodeposition, the applied voltage was extremely low (around -2.7 V vs. Ag/AgCl, which is about -2.5 V vs. SHE). Compared with the Pourbaix diagram shown in Figure S2 b, under our deposition condition, no indium oxide or hydroxide can form.

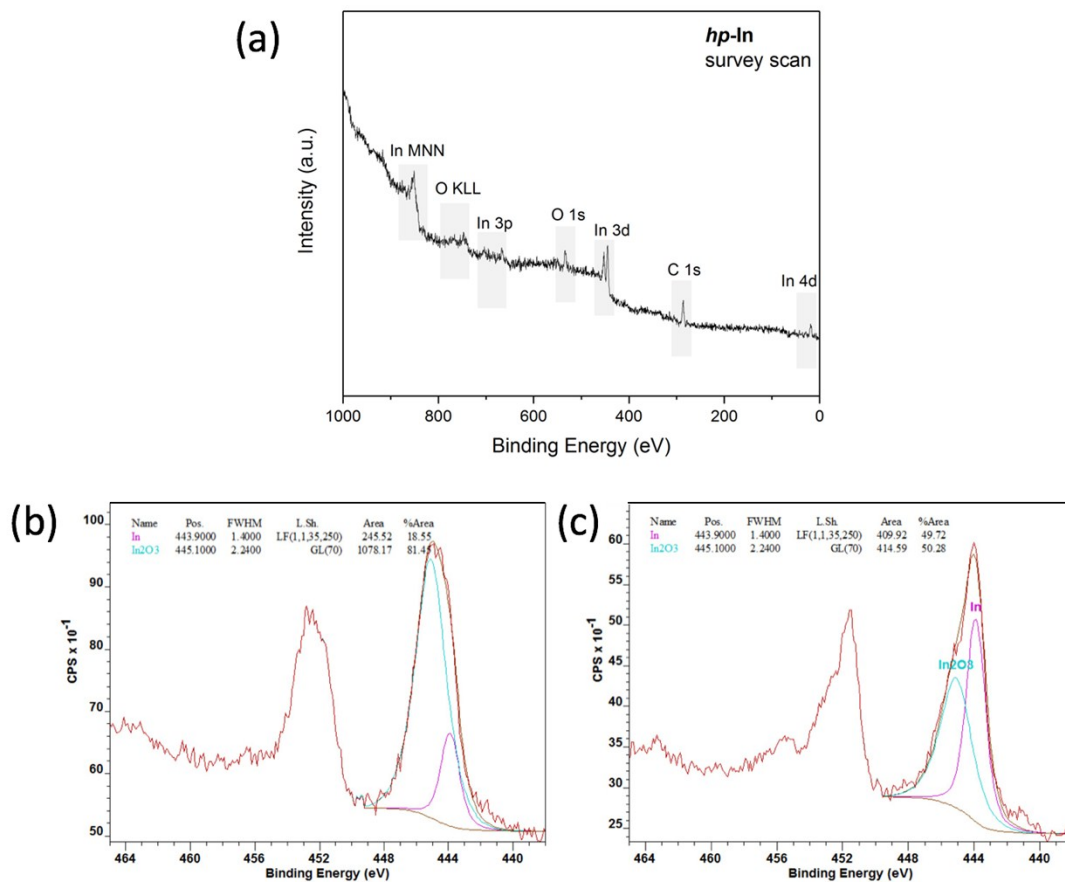


Figure S3 (a) XPS survey scan of as-prepared *hp*-In, and XPS deconvolution parameters of (b) In foil and (c) *hp*-In.

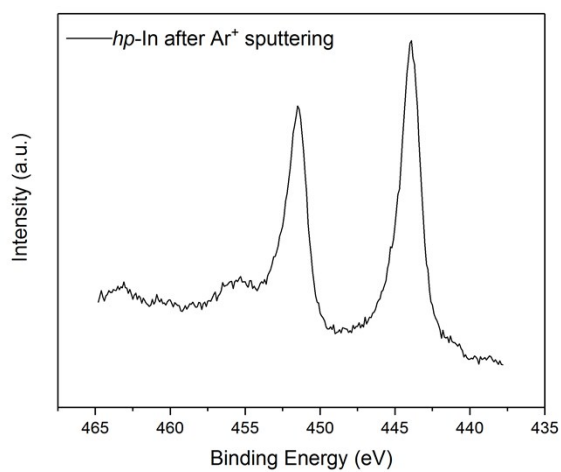


Figure S4 In 3d XP spectrum of *hp*-In after Ar⁺ sputtering.

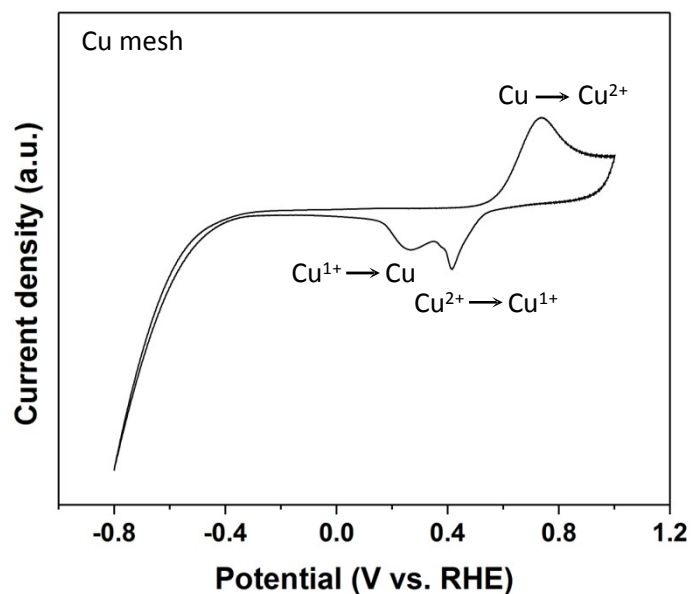


Figure S5 CV of Cu mesh performed in CO₂ saturated 0.1 M KHCO₃ (scan rate 50 mV/s). The redox peaks of Cu appear at higher potential range compared with those of In.

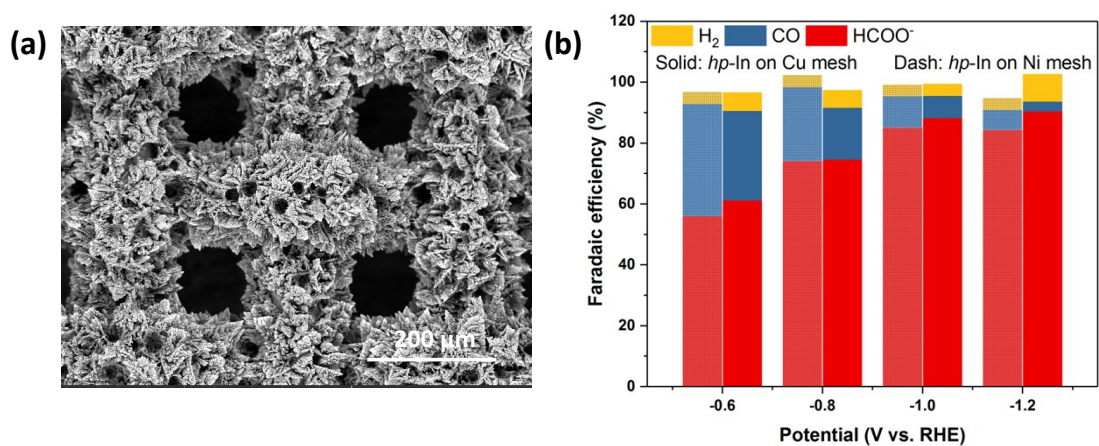


Figure S6 (a) SEM image of porous In deposited on Ni mesh. (b) Potential dependent faradaic efficiencies for *hp*-In on Cu mesh and porous In on Ni mesh.

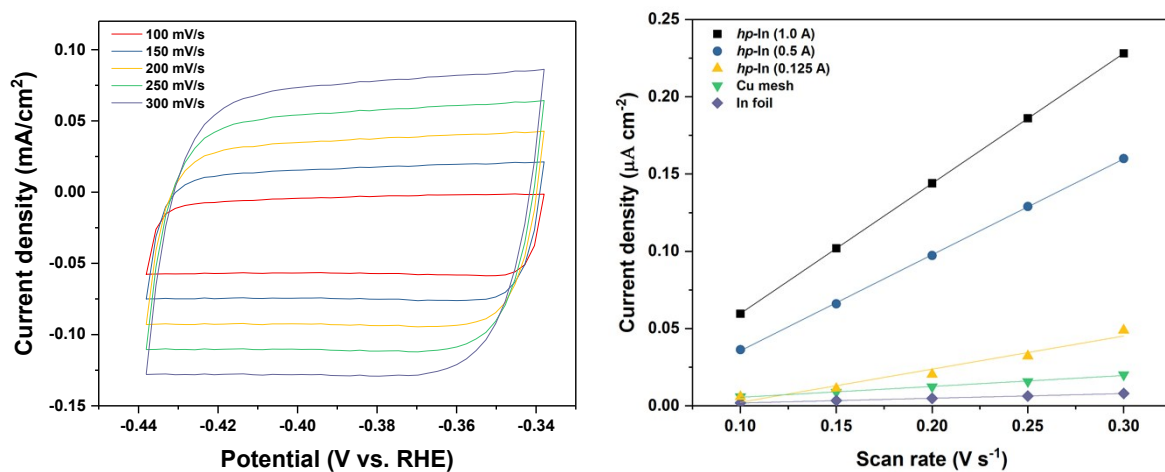


Figure S7 CVs for the *hp*-In at various scan rates (left). The linear regression of the double layer capacitance of each material obtained from the electrochemical studies (right).

Table S2 Summary of the roughness factors of the four In electrodes and the Cu mesh substrate used in this work.

| Electrode | Capacitance | Electrochemical surface area (cm ²) |
|-------------------------|-------------|---|
| In foil | 30.5 μF | 1 |
| Cu mesh | 71.0 μF | 2 |
| <i>hp</i> -In (0.125 A) | 0.22 mF | 7.1 |
| <i>hp</i> -In (0.5 A) | 0.62 mF | 20.3 |
| <i>hp</i> -In (1.0 A) | 0.84 mF | 27.6 |

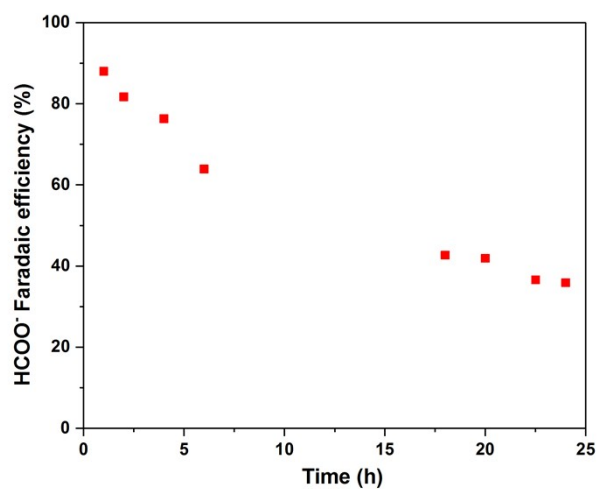


Figure S8 Stability of *hp*-In, tested without exchanging the electrolyte.

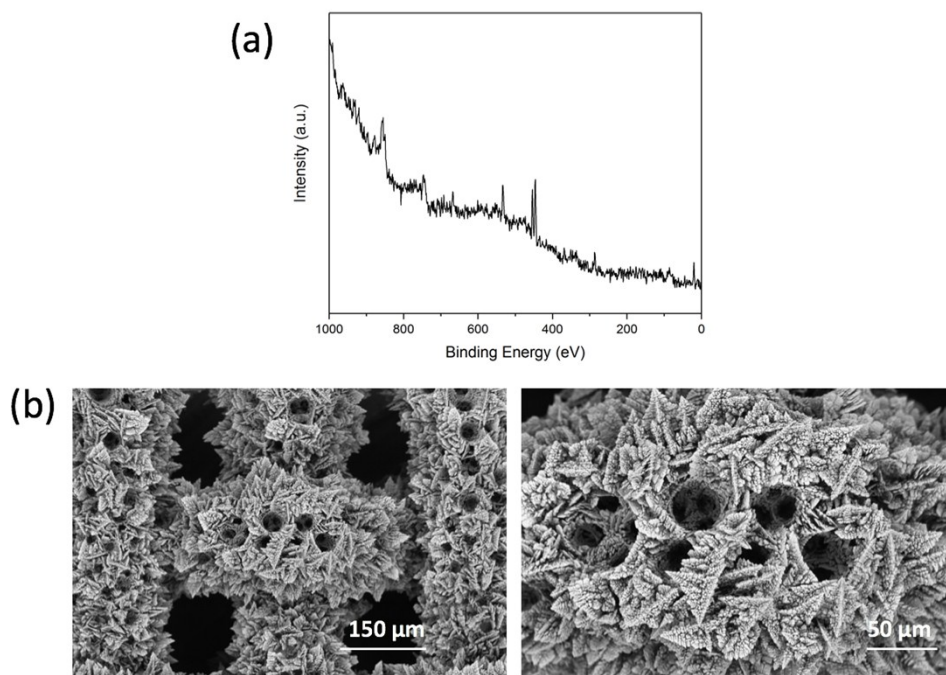


Figure S9 (a) XPS survey scan (b) SEM images of *hp*-In after 24 h stability test. No Cu from Cu mesh can be detected by XPS. SEM images show similar 3D structure as that of the fresh *hp*-In sample.

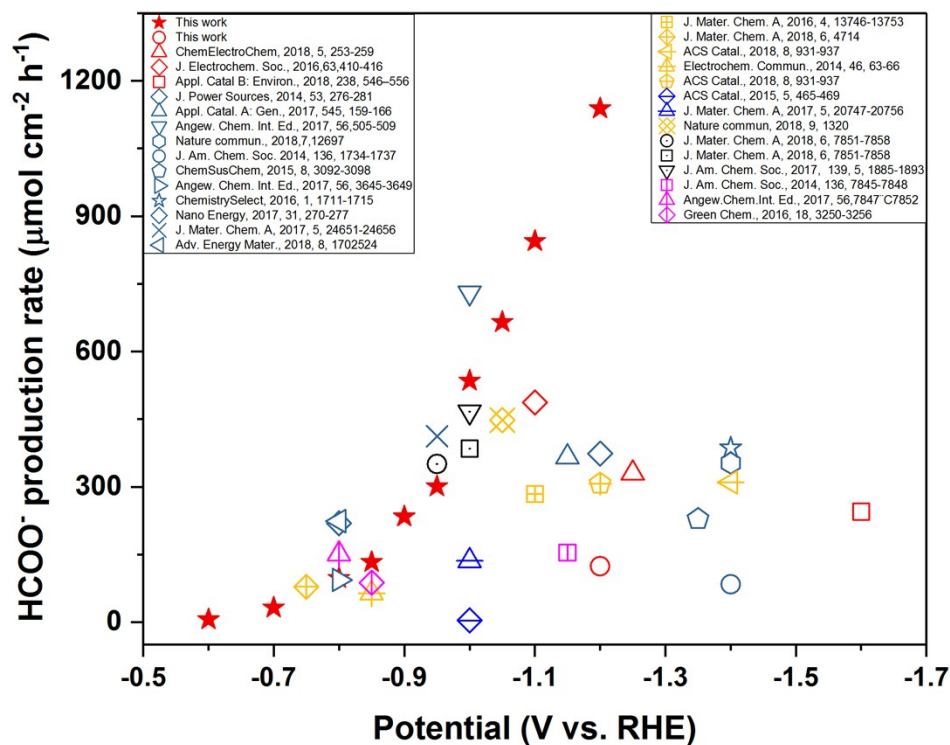


Figure S10 Formate production rate at various applied potentials on the *hp*-In electrode, along with an overview of the formate production rate on the state-of-the-art CO₂-to-formate catalysts.

Table S3 Comparison of CO₂ reduction performance on different In-based catalysts.

| Electrode | Electrolyte | Operating potential (vs. RHE) | Current density (mA/cm ²) | Faradaic efficiency for formate | Reference |
|------------------------|--|--------------------------------|---------------------------------------|---------------------------------|------------------|
| <i>hp</i>-In | 0.1 M KHCO₃ | -1.0 V -1.2 V | 32.5 67.5 | 89.1% 90.4% | This work |
| In/C GDE | 0.1 M Na ₂ SO ₄ | -1.05 V | 6.3 | 45% | 3 |
| In/Graphite | 0.05 M NaHCO ₃ | -1.6 V | ~ 18.5 ^[a] | 94.5% | 4 |
| Dendritic In | 0.5 M KHCO ₃ | -0.86 V | 5.8 | 86% | 5 |
| Anodized In | 0.5 M Na ₂ SO ₄ | -1.2 V | - | ~ 88% ^[a] | 6 |
| In(OH) ₃ /C | 0.5 M K ₂ SO ₄ | -1.1 V | ~5.4 ^[a] | 70% -77% | 7 |
| In nanoparticle | 0.5 M K ₂ SO ₄ | -0.85 V | ~2 ^[a] | ~100% | 8 |
| In nanocrystal | Ion liquid (AN-BMIMPF ₆ solution) | -1.9 V (SCE) | ~15 | ~99% (CO) | 9 |

^[a] This value is derived from the graphical results in the article.

Table S4 Optimized adsorption configurations of *H, *COOH and *OCHO on three facets of In.

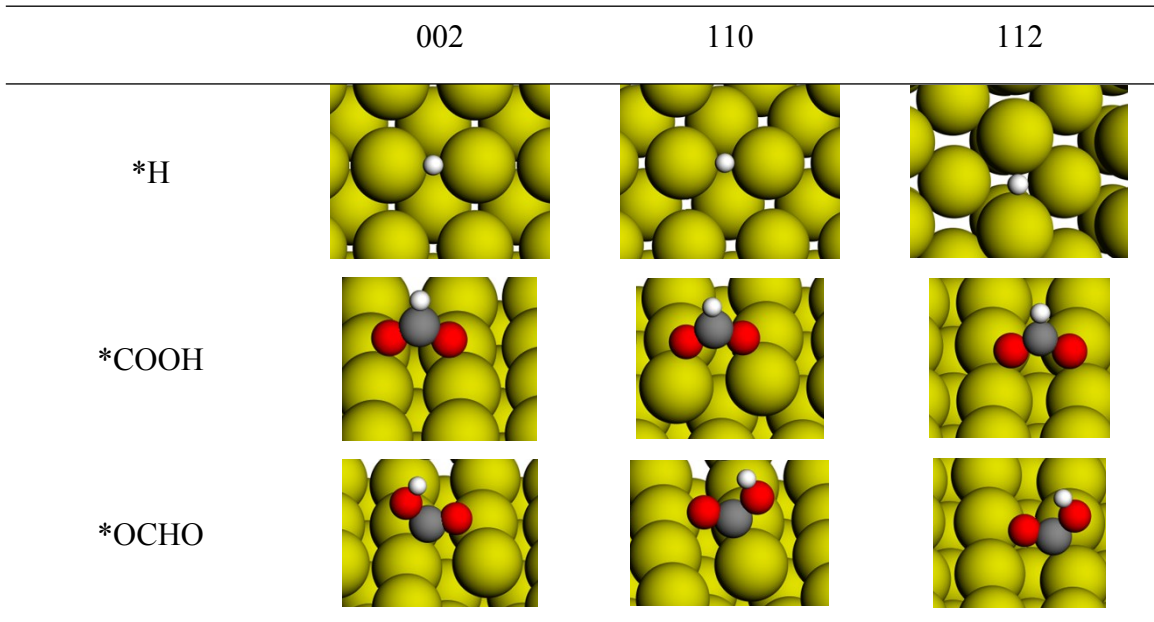


Table S5 The zero-point energy correction (E_{ZPE}), enthalpy correction ($\int C_v dT$), and entropy correction ($-TS$) for adsorbates on three different structures. All values are given in eV.

| Structure | Adsorbates | E_{ZPE} | $\int C_v dT$ | $-TS$ |
|-----------|------------|-----------|---------------|-------|
| In(101) | *COOH | 0.60 | 0.24 | -0.89 |
| | *OCHO | 0.59 | 0.23 | -0.94 |
| In(002) | *COOH | 0.59 | 0.24 | -0.88 |
| | *OCHO | 0.60 | 0.23 | -0.88 |
| In(110) | *COOH | 0.59 | 0.24 | -0.89 |
| | *OCHO | 0.59 | 0.21 | -0.83 |
| In(112) | *COOH | 0.59 | 0.24 | -0.89 |
| | *OCHO | 0.60 | 0.23 | -0.89 |

Table S6 The zero-point energy correction (E_{ZPE}), enthalpy correction ($\int C_v dT$), and entropy correction ($-TS$) for free gaseous molecules with their partial pressure of 101325 Pa except for H_2O and HCOOH . In the case of H_2O , 3534 Pa was used and 2 Pa was used for HCOOH . Gas phase corrections were applied to CO_2 , CO and HCOOH with the value of 0.13, -0.54 and -0.1 eV, respectively.¹⁰ All values are given in eV.

| Species | E_{ZPE} | $\int C_v dT$ | $-TS$ | $G - E_{\text{DFT}}$ |
|----------------------|------------------|---------------|-------|----------------------|
| CO_2 | 0.31 | 0.14 | -0.64 | -0.19 |
| CO | 0.14 | 0.12 | -0.60 | -0.34 |
| H_2O | 0.58 | 0.11 | -0.53 | 0.17 |
| H_2 | 0.28 | 0.11 | -0.45 | -0.06 |
| HCOOH | 0.90 | 0.18 | -0.69 | 0.39 |

Table S7 Calculated DFT energies for HER.^a

| Species | E_{DFT} |
|------------------|------------------|
| H_2 (g) | -6.81 |
| In(101) H* | -65.92 -68.64 |
| In(002) H* | -29.13 -31.89 |
| In(110) H* | -28.78 -31.54 |
| In(112) H* | -27.67 -30.51 |

^a The HER free energy G_{H^*} is determined as $G_{\text{H}^*} = E[\text{surf} + \text{H}] - E[\text{surf}] - E[\text{H}_2]/2 + \Delta E_{\text{ZPE}} - TS$. Where $E[\text{surf} + \text{H}]$ and $E[\text{surf}]$ are the total energies of the surface with and without the H adsorbate, respectively. $E[\text{H}_2]$ is the total energy of a hydrogen molecule. ΔE_{ZPE} is the difference in the zero-point energy between the adsorbed H atom and the gaseous phase H_2 . S is the difference in entropy. At $T = 298$ K, G_{H^*} can be calculated by $G_{\text{H}^*} = E[\text{surf} + \text{H}] - E[\text{surf}] - E[\text{H}_2]/2 + 0.24$ eV.^{10,11}

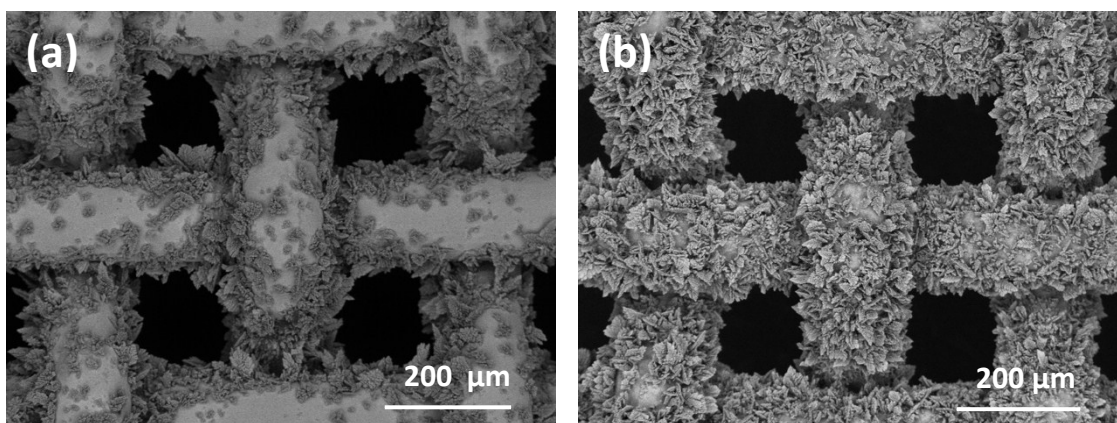


Figure S11 SEM images of as-prepared (a) *hp*-In-0.125 and (b) *hp*-In-0.5.

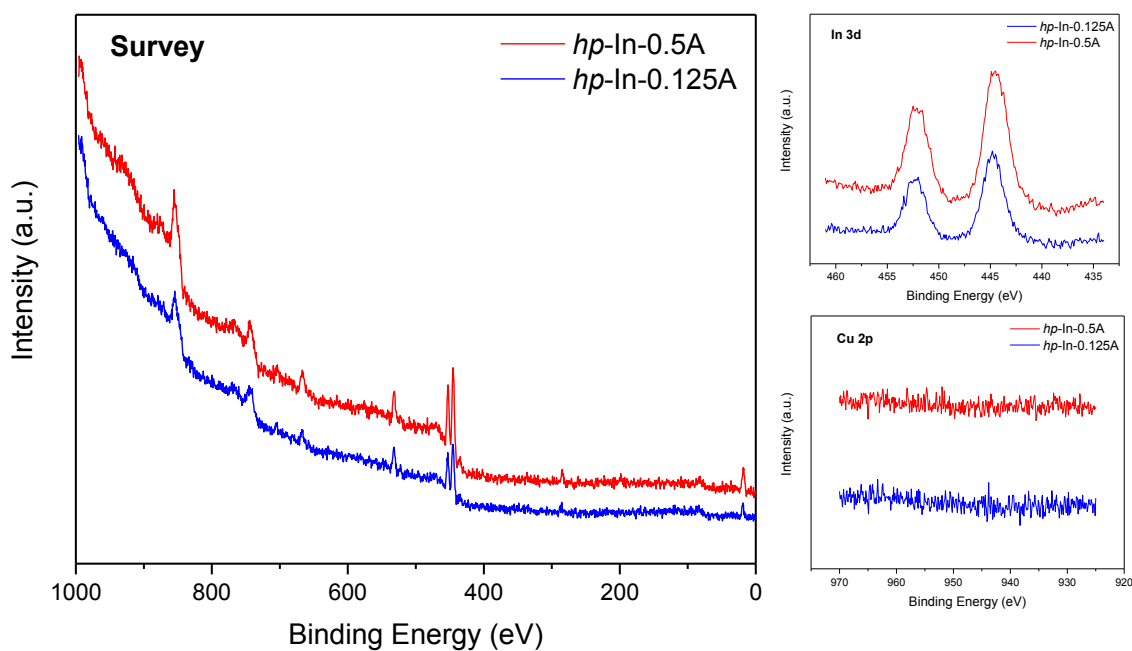


Figure S12 XPS survey, In 3d and Cu 2p spectra of as-prepared *hp*-In-0.125 and *hp*-In-0.5. Although the SEM images show that the porous In was not homogeneous deposited on these two samples at low current densities (Figure S10), XPS spectra indicate that the Cu mesh was fully covered by a layer of In.

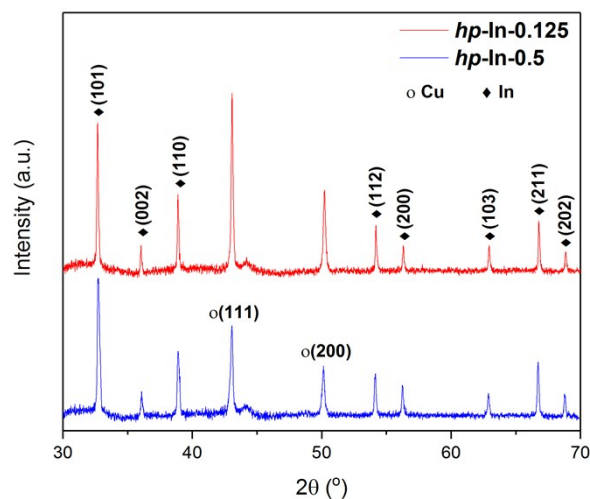


Figure S13 XRD patterns of as-prepared *hp*-In-0.125 and *hp*-In-0.5.

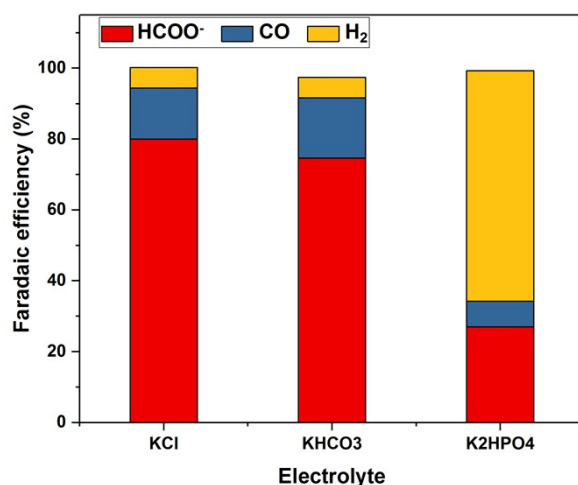


Figure S14 FEs of formate, CO and H₂ for *hp*-In measured in CO₂ saturated 0.1 M KCl, 0.1 M KHCO₃ and 0.1 M K₂HPO₄ at 7 mA/cm².

The local pH effect was further confirmed by performing CO₂RR in three different electrolyte with different buffer abilities (i.e., 0.1 M K₂HPO₄ > 0.1M KHCO₃ > 0.1M KClO₄). Figure S14 shows the FE of H₂ significantly increased when K₂HPO₄, a strong buffer electrolyte, was used instead of KHCO₃. In KCl electrolyte, the H₂ FE is similar as that in KHCO₃. This may be because the local pH in KHCO₃ is already quite high that limits the H₂ FE to only 5.8 %. Thus, the results shown here confirm that the high local pH created near *hp*-In could suppress H₂ evolution and therefore increase the CO₂RR FEs.

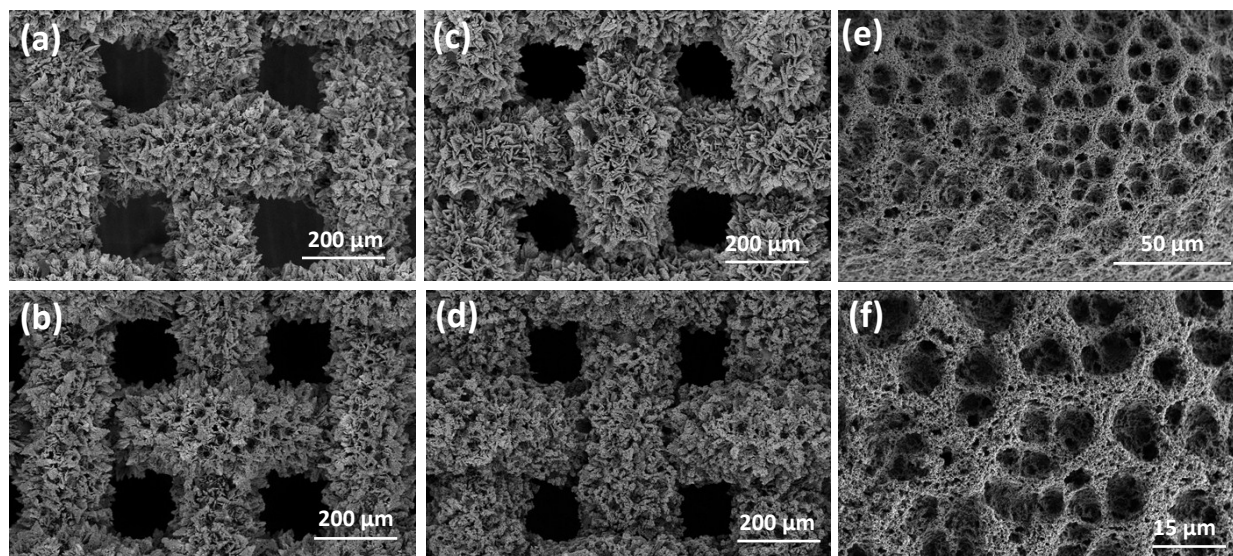


Figure S15 SEM images of Pd-In electrodes treated by different PdCl₂ solutions (a) 0.1 mM, (b) 0.5 mM, (c) 1.0 mM and (d) 2.0 mM, and porous Pd electrode with different magnifications (e) and (f).

References:

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