

CO₂ reactivity with Mg₂NiH₄ synthesized by *in situ* monitoring mechanical milling

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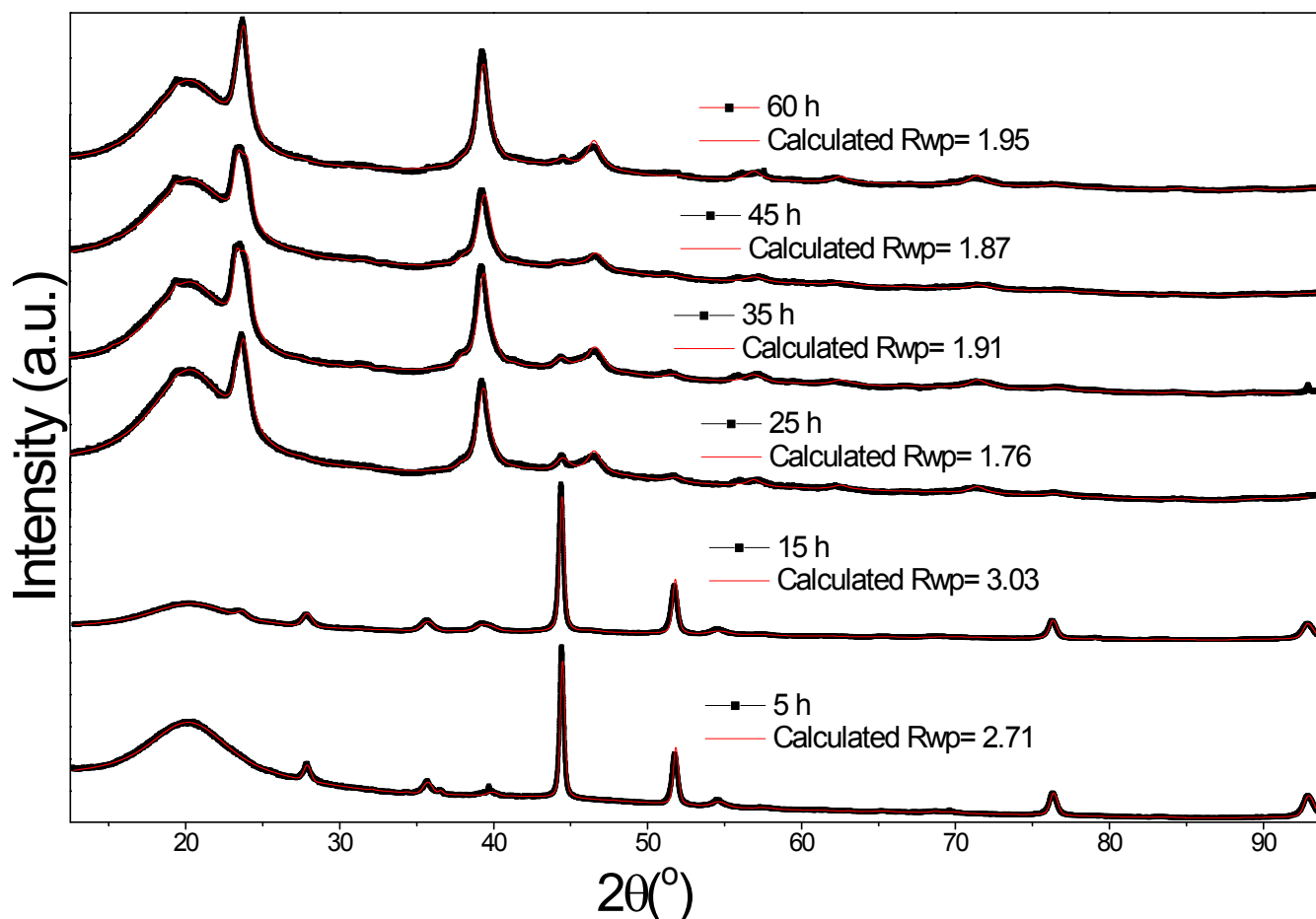


Figure S1 – Diffractograms taken at different milling times and Rietveld fitting for quantitative analyses.

Milling time (h)	Ni	Mg	MgH ₂	LT - Mg ₂ NiH ₄ (C2/c1)	HT - Mg ₂ NiH ₄ (Fm3-m)	Mg ₂ NiH ₄	Rwp (%)
5	66.4±0.6	3.2±0.10	30.4±0	-	-	0	2.71
15	64.1±0.5	-	26.8±0	-	9.1±0.1	9.1 ±0.1	3.03
25	8.6±0.5	-	-	7.5±0.2	83.9±0.9	91.4 ±1.0	1.76
35	5.6±0	-	-	20.2±0.6	74.2±1	94.4 ±2.0	1.91
45	3.3±0	-	-	29.1±1	67.6±2	96.7 ±3.0	1.87
60	3.5±0	-	-	5.7±0.2	90.8±2	96.5 ±2.0	1.95

Table S1 – Amounts of phases during the milling process expressed in wt.%. Results coming from Rietveld analyses of samples taken at different milling times (Diffractograms and fittings shown in Figure S2). HT-Mg₂NiH₄ (Cubic, S.G. *Fm-3m*) and LT-Mg₂NiH₄ (LT1, Monoclinic, S.G. *C12/c1*).

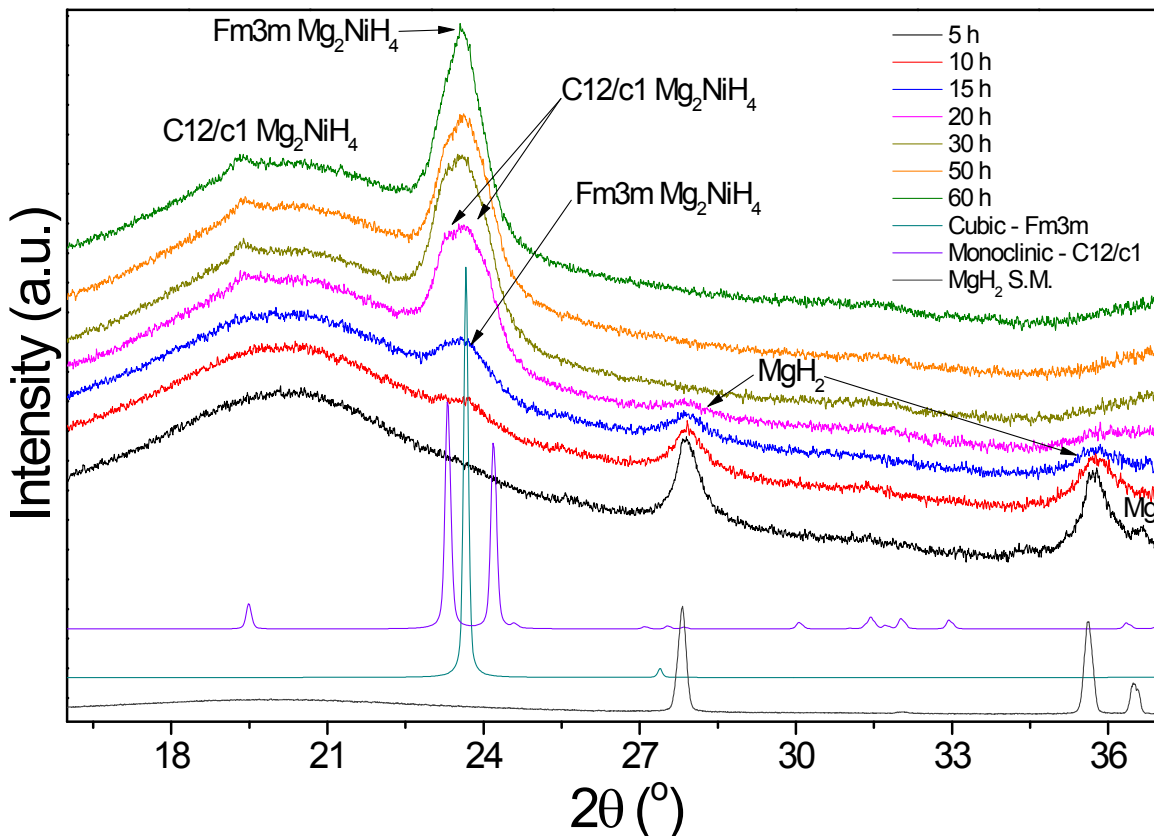


Figure S2 – Diffractograms taken at different milling times from 15° to 40°.

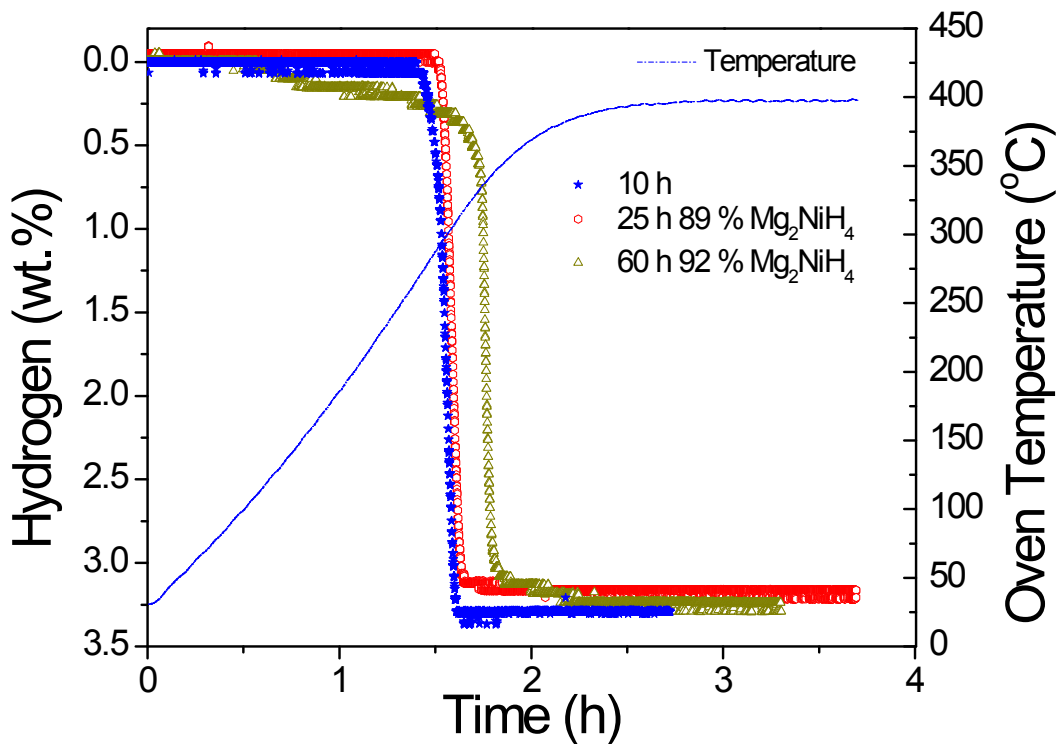


Figure S3 - Non-isothermal dehydrogenation curves for $2\text{MgH}_2\text{-Ni}$ at 10 h, 25 h and 60 h of mechanical milling. Heating ramp of about $3^\circ\text{C}/\text{min}$ from 25°C to 400°C under 1 bar H_2 .

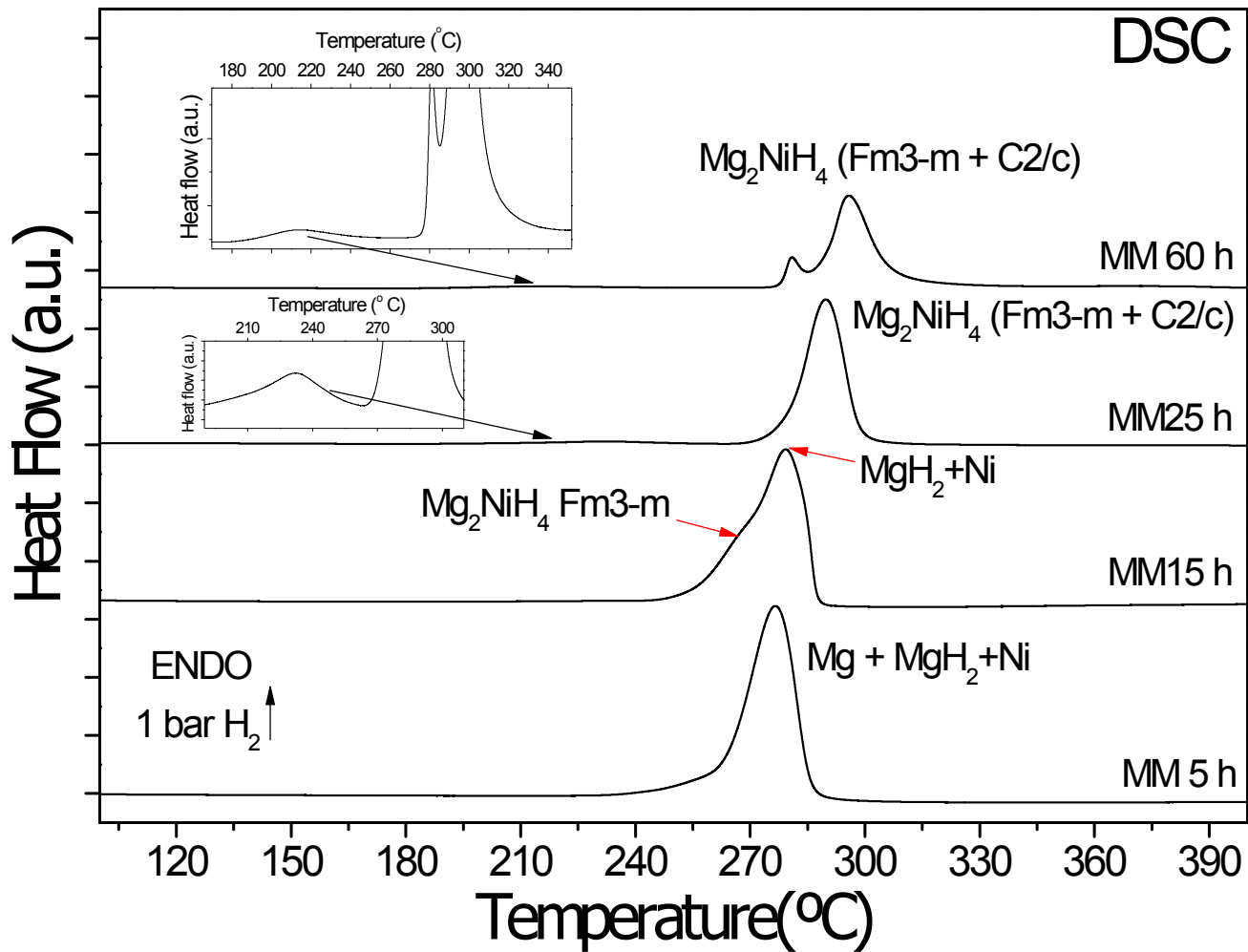
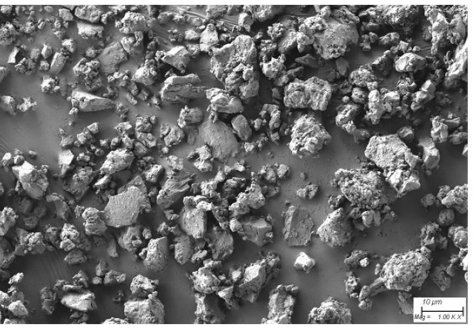
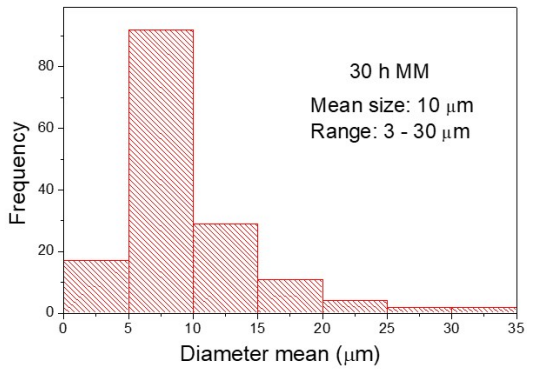
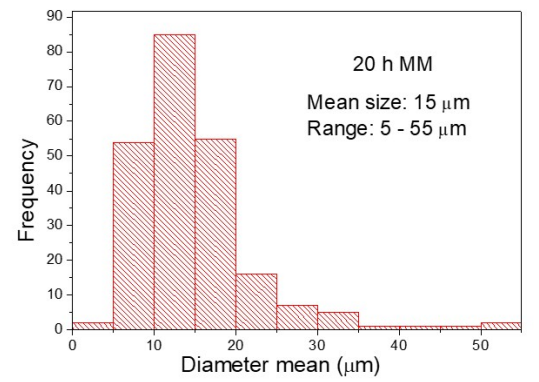
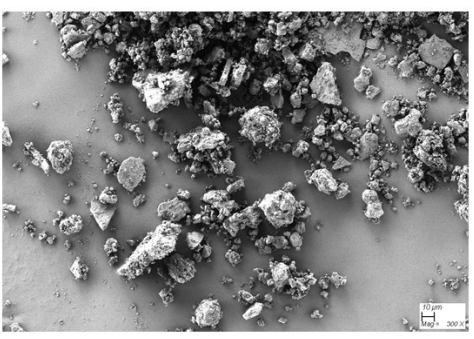
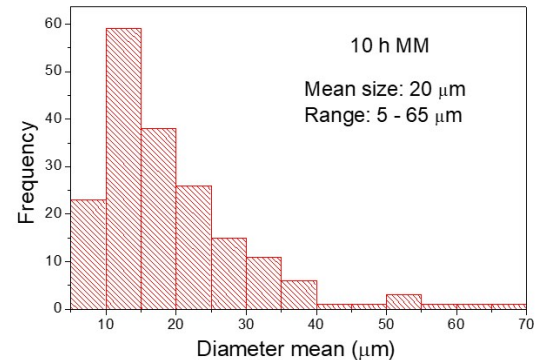
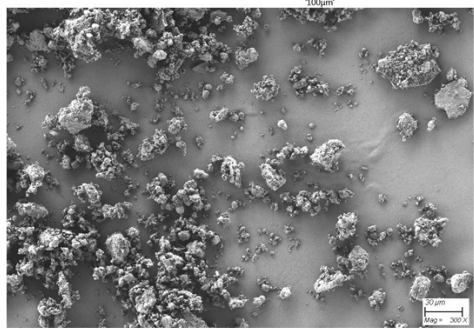
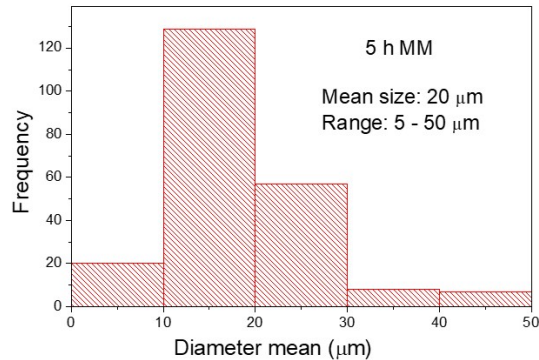
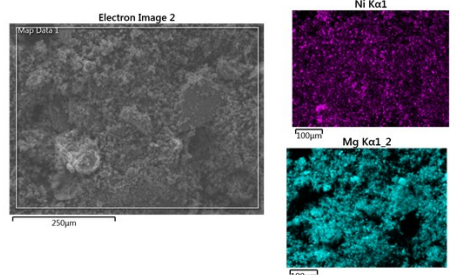


Figure S4 – HP – DSC for $2\text{MgH}_2\text{-Ni}$ material upon milling: 5 h, 15 h, 25 h and 60 h. Heating ramp $5^\circ\text{C}/\text{min}$ and under 1 bar H_2 .



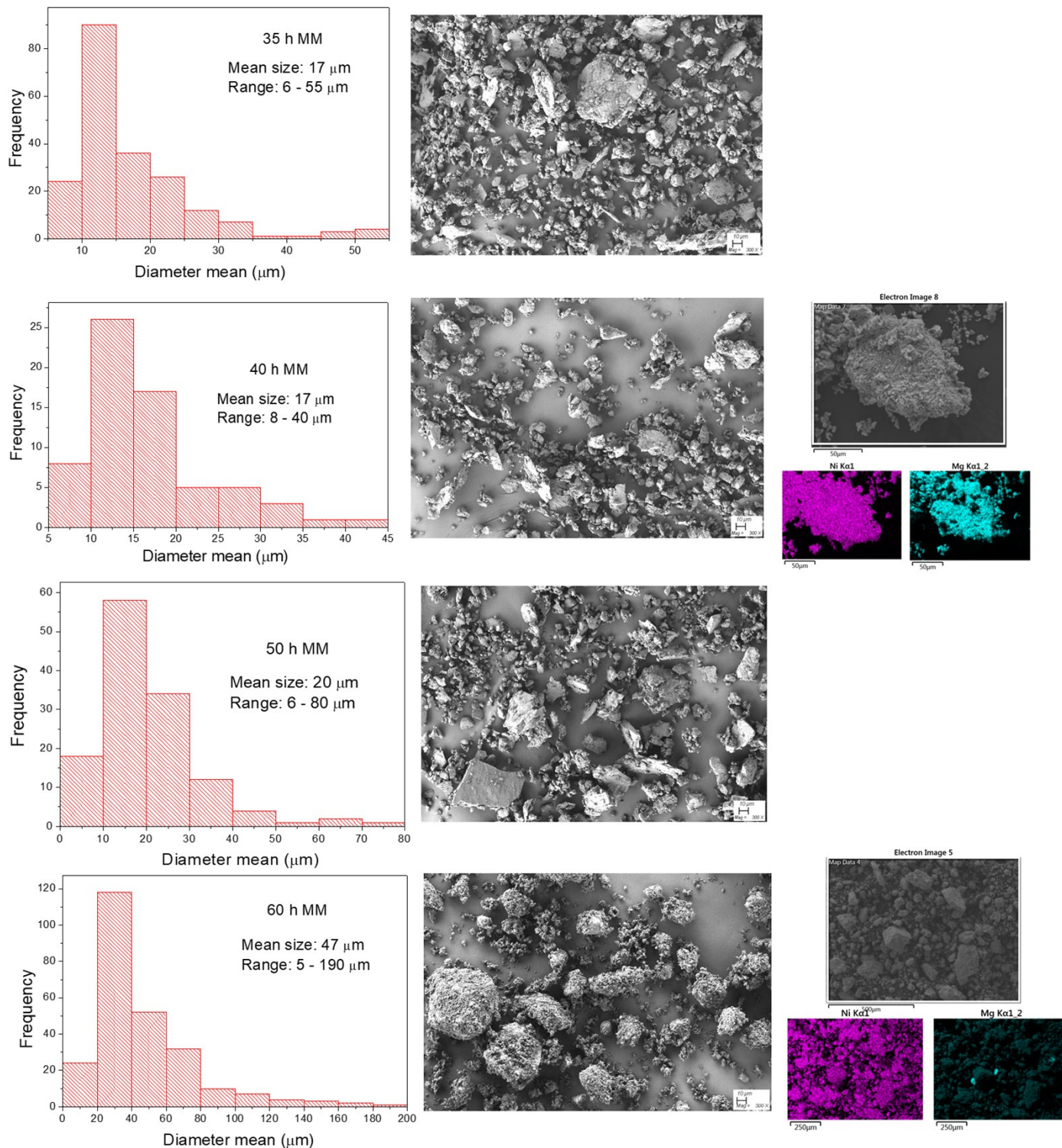


Figure S5 – Particle size distributions (PSDs), Scanning electron microscopy (SEM) observations and mapping.

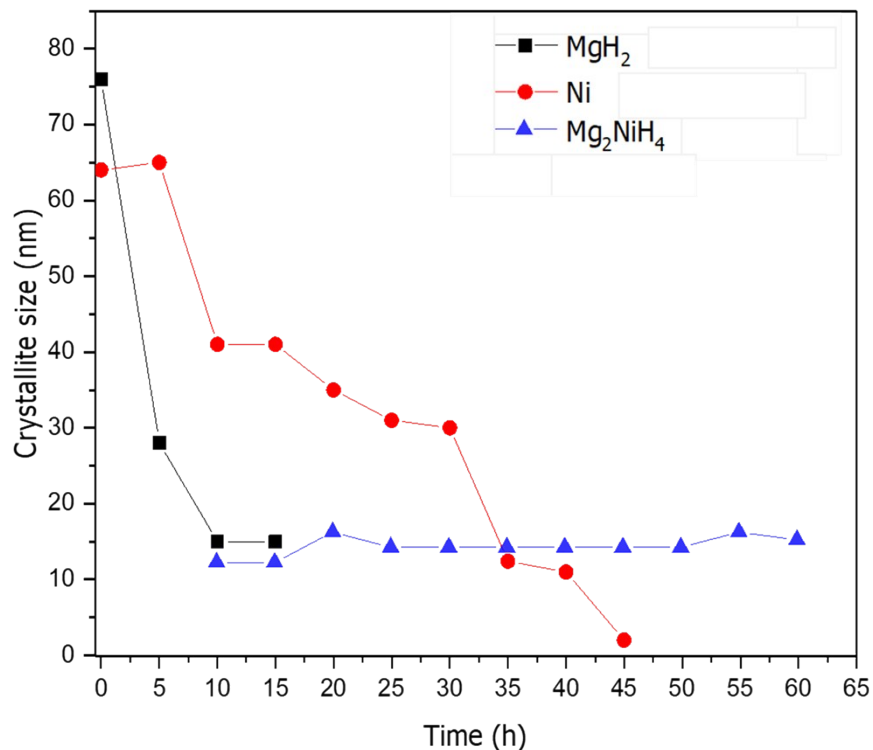


Figure S6 – Crystallite size evolution during milling for MgH₂, Ni and Mg₂NiH₄.

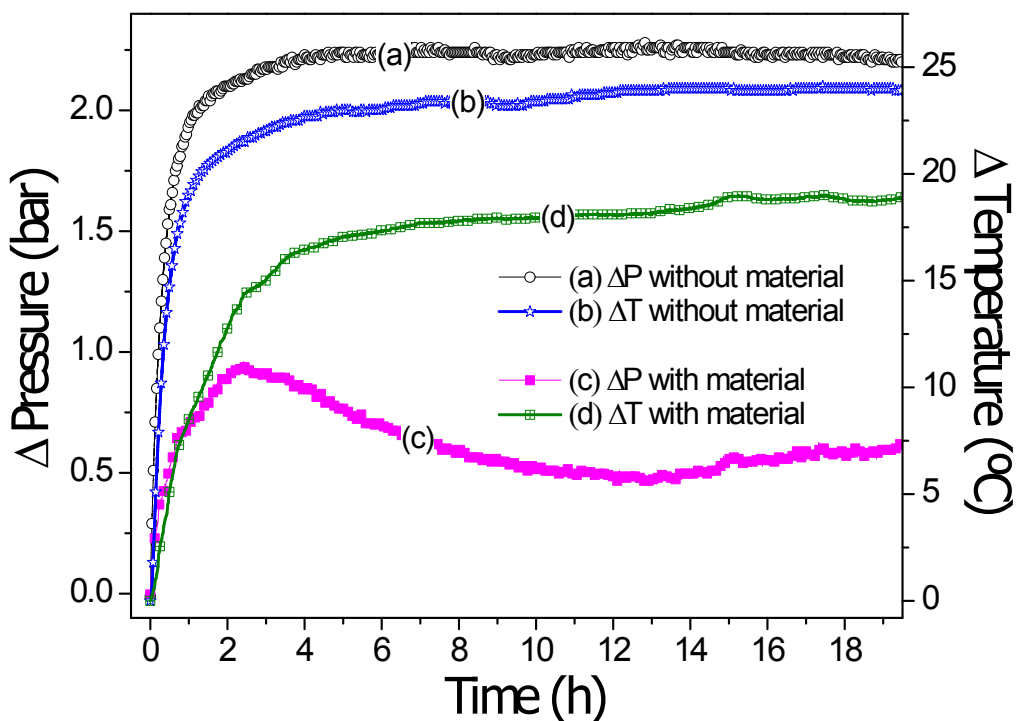
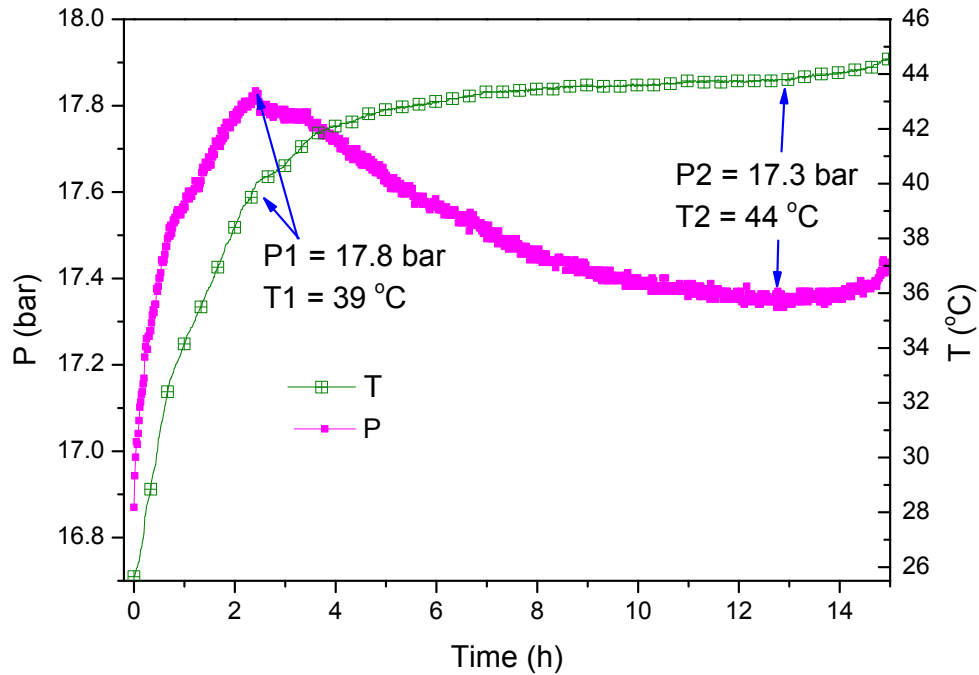


Figure S7 – Comparison between temperature and pressure evolution during the first 20 h of milling with and without material.

Hydrogen consumption at the beginning of the milling process

From Fig.S7 – Curves (c) and (d) expressed as were measured (not in delta). From these curves the data of the gas phase is subtracted:



Volume of the milling chamber = 0.2 L

$R = 0.082 \text{ L.atm/K mol}$

Ideal gas equation $P.V = n.R.T$

State 1

$$n1 = P1.V/R.T1$$

$$n1 = (17.5 \text{ atm} \cdot 0.2 \text{ L}) / (0.082 \text{ L.atm/K mol} \cdot 312 \text{ K})$$

$$n1 = 0.1368 \text{ mol}$$

State 2

$$n2 = P2.V/R.T2$$

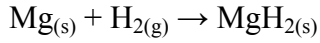
$$n2 = (17.0 \text{ atm} \cdot 0.2 \text{ L}) / (0.082 \text{ L.atm/K mol} \cdot 317 \text{ K})$$

$$n2 = 0.1307 \text{ mol}$$

Consumed moles $\Delta n = (0.1368 - 0.1307) \text{ mol}$

$\Delta n = 0.0060 \text{ mol}$

It is assumed that the free Mg reacts with H_2 to form MgH_2



Amount of Mg = $0.0060 \text{ mol} * 24.31 \text{ g/mol}$

Amount of Mg = 0.146 g

wt.% of free Mg = $(0.146 \text{ g}/5 \text{ g sample}) * 100$

wt.% of free Mg = 2.92

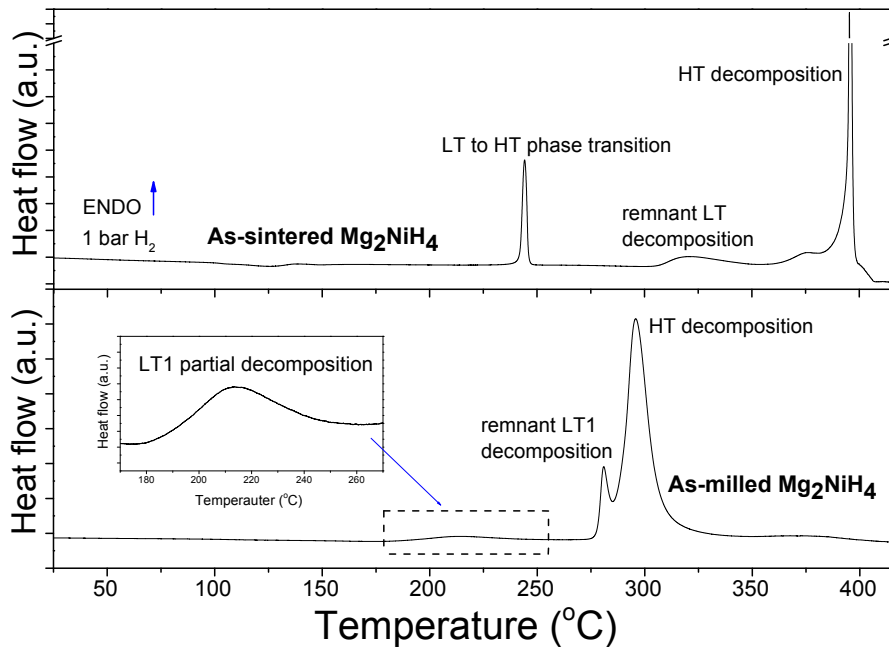
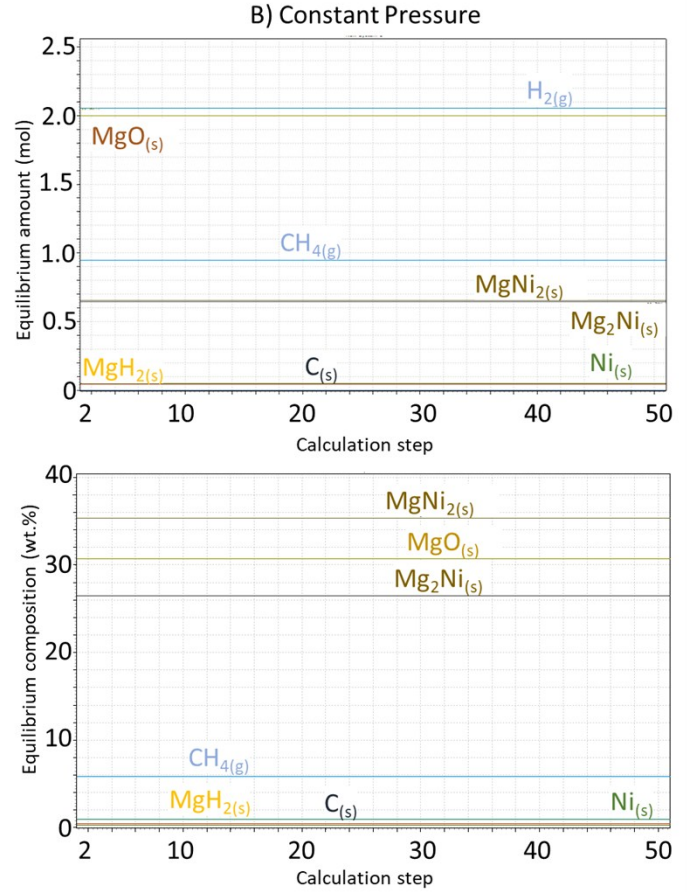
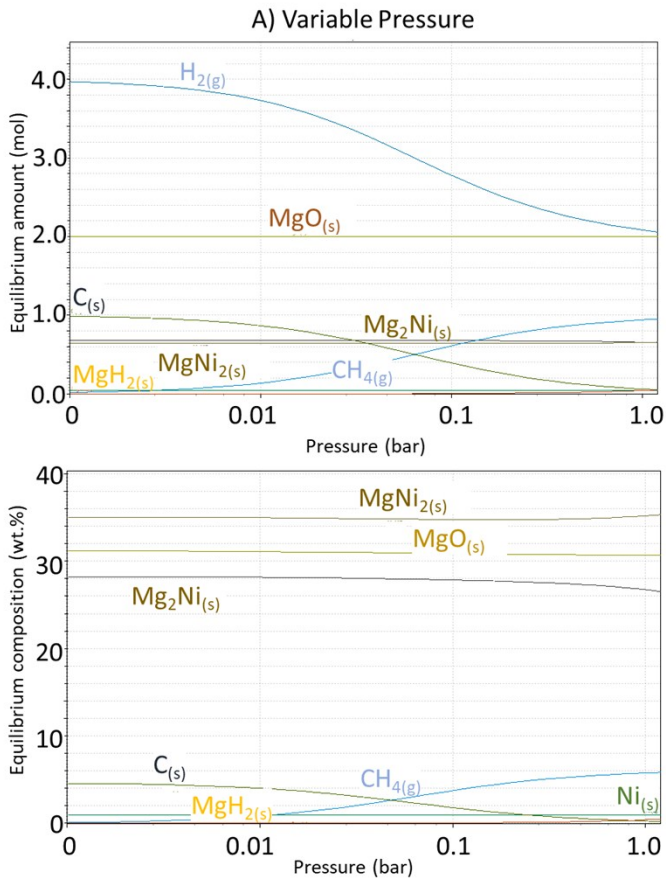


Figure S8 – High-pressure differential scanning calorimetry (HP-DSC) for as-sintered Mg_2NiH_4 ¹⁶ and as-milled Mg_2NiH_4 . Heating ramp 5 °C/min and under 1 bar H_2 .



Equilibrium Amount at variable pressure Final temperature and pressure conditions		
Species	Mol	Mol %
CO _{2(g)}	0.0	0.0
H _{2(g)}	2.05	32.0
Mg ₂ Ni _(s)	0.65	10.0
MgNi _{2(s)}	0.65	10.0
O _{2(g)}	0.000	0.0
CO _(g)	0.000	0.0
H ₂ O _(g)	0.000	0.0
CH _{4(g)}	0.95	15.0
C ₂ H _{4(g)}	0.000	0.0
Ni _(s)	0.04	0.60
CH ₃ OH _(g)	0.000	0.0
C _(s)	0.05	0.70
MgO _(s)	2.000	31.0
MgCO _{3(s)}	0.000	0.0
NiCO _{3(s)}	0.000	0.0
H ₂ O _(l)	0.000	0.0
C ₂ H _{6(g)}	0.000	0.0
MgH _{2(s)}	0.05	0.70

Equilibrium Amount at constant pressure Last step of the calculation		
Species	Mol	Mol %
CO _{2(g)}	0.0	0.0
H _{2(g)}	2.05	32.0
Mg ₂ Ni _(s)	0.649	10.0
MgNi _{2(s)}	0.654	10.0
O _{2(g)}	0.000	0.0
CO _(g)	0.000	0.0
H ₂ O _(g)	0.000	0.0
CH _{4(g)}	0.949	15.0
C ₂ H _{4(g)}	0.000	0.0
Ni _(s)	0.042	0.60
CH ₃ OH _(g)	0.000	0.0
C _(s)	0.051	0.70
MgO _(s)	2.000	31.0
MgCO _{3(s)}	0.000	0.0
NiCO _{3(s)}	0.000	0.0
H ₂ O _(l)	0.000	0.0
C ₂ H _{6(g)}	0.000	0.0
MgH _{2(s)}	0.05	0.70

Figure S9 – Equilibrium amounts of phases calculated at 400 °C, 4H₂:1CO₂ stoichiometric ratio and volume of 10 cm³: A – under variable pressure up to 1.2 bar and B – constant pressure of 1.2 bar.

Reaction Equation					
$2\text{Mg}_2\text{NiH}_4(\text{s}) + \text{CO}_2(\text{g}) = 0.75\text{Mg}_2\text{Ni}(\text{s}) + 2\text{MgO}(\text{s}) + 0.25\text{Ni}(\text{s}) + 0.5\text{MgNi}_2(\text{s}) + \text{C}(\text{s}) + 4\text{H}_2(\text{g})$					
Reaction Data					
T °C	ΔH kJ	ΔS J/K	ΔG kJ	K	Log K
25.000	-535.517	314.791	-629.371	1.873E+110	110.273
50.000	-535.494	314.862	-637.242	1.032E+103	103.014
75.000	-535.395	315.155	-645.116	6.282E+096	96.798
100.000	-535.228	315.617	-653.001	2.610E+091	91.417
125.000	-535.001	316.205	-660.898	5.162E+086	86.713
150.000	-534.719	316.892	-668.812	3.687E+082	82.567
175.000	-534.386	317.657	-676.744	7.678E+078	78.885
200.000	-534.003	318.487	-684.695	3.936E+075	75.595
225.000	-533.574	319.370	-692.668	4.339E+072	72.637
250.000	-533.104	320.290	-700.664	9.219E+069	69.965
275.000	-532.596	321.238	-708.683	3.451E+067	67.538
300.000	-532.049	322.214	-716.726	2.114E+065	65.325
325.000	-531.460	323.219	-724.794	1.993E+063	63.299
350.000	-530.825	324.260	-732.887	2.744E+061	61.438
375.000	-530.146	325.328	-741.007	5.285E+059	59.723
400.000	-529.456	326.373	-749.154	1.372E+058	58.137

Table S2 – Thermodynamic data for the reaction between $2\text{Mg}_2\text{NiH}_4(\text{s}) + \text{CO}_2(\text{g})$ (4).