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Supplementary information

## Bi-functional Ru/Ca<sub>3</sub>Al<sub>2</sub>O<sub>6</sub>-CaO catalyst-CO<sub>2</sub> sorbent for the production of high purity hydrogen via the sorption-enhanced steam methane reforming

Sung Min Kim,<sup>a</sup> Paula M. Abdala,<sup>a</sup> Davood Hosseini,<sup>a</sup> Andac Armutlulu,<sup>a</sup> Tigran Margossian,<sup>b</sup> Christophe Copéret,<sup>b</sup> and Christoph Müller<sup>\*a</sup>

<sup>a</sup> Department of Mechanical and Process Engineering, ETH Zurich, Leonhardstrasse 21, 8092 Zurich, Switzerland <sup>b</sup> Department of Chemistry and Applied Sciences, ETH Zurich, Vladimir Prelog Weg 1-5, 8093 Zurich, Switzerland

> \*Corresponding author. Tel.: +41 44 632 3440. E-mail address: muelchri@ethz.ch (Prof. Christoph Müller)

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Materials	Coordination	Coordination	R [Å]	$\sigma^2$ [Å <sup>2</sup> ]	ΔE [eV]	R-factor
	shell	number	[]	- []	[]	
	Ru-O	2	$1.94 \pm 0.02$	$0.0030 \pm 0.0003$		0.027
	Ru-O	4	$1.98 \pm 0.02$	$0.0030 \pm 0.0003$	$-3.73 \pm 1.48$	
RuO <sub>2</sub>	Ru-Ru	2	$3.13 \pm 0.02$	$0.0029 \pm 0.0003$		
	Ru-O	4	$3.22 \pm 0.19$	$0.0029 \pm 0.0003$		
	Ru-Ru	8	$3.54\pm0.01$	$0.0029 \pm 0.0003$		
	Ru-O	2	$1.94\pm0.03$	$0.0030 \pm 0.0003$		
	Ru-O	4	$1.98\pm0.02$	$0.0030 \pm 0.0003$		
$Ru/Al_2O_3$	Ru-Ru	2	$3.11\pm 0.01$	$0.0035 \pm 0.0003$	$\textbf{-3.61} \pm 1.39$	0.025
	Ru-O	4	$3.17\pm0.23$	$0.0035 \pm 0.0003$		
	Ru-Ru	8	$3.54\pm0.01$	$0.0035 \pm 0.0003$		
	Ru-O	6	$2.00\pm0.01$	$0.0034 \pm 0.0004$		
	Ru-Ca	2	$3.14 \pm 0.02$	$0.0040 \pm 0.0023$		
	Ru-Ca	2	$3.26\pm0.02$	$0.0040 \pm 0.0023$	1 51 1 1 10	0.000
CaRuO <sub>3</sub>	Ru-Ca	2	$3.37\pm0.02$	$0.0040 \pm 0.0023$	$-1.71 \pm 1.42$	0.028
	Ru-Ca	2	$3.61\pm0.02$	$0.0040 \pm 0.0023$		
	Ru-Ru	5	$3.84\pm0.01$	$0.0037 \pm 0.0011$		
	Ru-O	6	$1.96 \pm 0.03$	$0.0070 \pm 0.0004$		
	Ru-Ca	2	$3.12 \pm 0.01$	$0.0075 \pm 0.0034$		
	Ru-Ca	2	$3.31 \pm 0.07$	$0.0075 \pm 0.0034$		0.021
Ru/lime	Ru-Ca	2	$3.31 \pm 0.07$	$0.0075 \pm 0.0034$	$-3.13 \pm 1.27$	
	Ru-Ca	2	$3.47 \pm 0.14$	$0.0075 \pm 0.0034$		
	Ru-Ru	5	$3.86 \pm 0.01$	$0.0131 \pm 0.0025$		
	110 110	C				
	Ru-O	6	$1.95 \pm 0.04$	$0.0067 \pm 0.0004$		
	Ru-Ca	2	$3.10 \pm 0.02$	$0.0086 \pm 0.0061$		0.020
	Ru-Ca	2	3.10 = 0.02 $3.23 \pm 0.01$	$0.0086 \pm 0.0061$		
Ru/CaO	Ru-Ca	2	$3.23 \pm 0.01$ $3.31 \pm 0.06$	$0.0086 \pm 0.0061$	$-3.60 \pm 1.28$	
	Ru-Ca	2	$3.31 \pm 0.00$ $3.42 \pm 0.19$	$0.0080 \pm 0.0001$ $0.0086 \pm 0.0061$		
		5	$3.42 \pm 0.17$ $3.87 \pm 0.03$	$0.0030 \pm 0.0001$ $0.0175 \pm 0.0049$		
	Ku-Ku	5	$5.07 \pm 0.05$	$0.0173 \pm 0.0049$		
	Ru O	6	$1.97 \pm 0.02$	$0.0001 \pm 0.0006$		
	Ru-O	0	$1.97 \pm 0.02$	$0.0091 \pm 0.0000$		
	Ru-Ca	2	$3.12 \pm 0.01$	$0.0088 \pm 0.0042$		
Ru/Ca3Al2O6-CaC	) Ru-Ca	2	$3.32 \pm 0.08$	$0.0000 \pm 0.0042$	$\textbf{-3.47} \pm 1.53$	0.027
	Ku-Ca	2	$3.32 \pm 0.03$	$0.0088 \pm 0.0042$		
	Ku-Ca	2	$3.42 \pm 0.18$	$0.0088 \pm 0.0042$		
	ки-ки	3	$3.70 \pm 0.08$	$0.0091 \pm 0.0006$		

 Table S1.
 EXAFS fitting results of calcined materials at Ru K-edge

		N <sub>2</sub> physisorption				
Catalyst	Cycles	$S_{BET}$ [m <sup>2</sup> /g]	V <sub>Pore</sub> [cm <sup>3</sup> /g]	D <sub>pore</sub> [nm]		
	2	6	0.07	19		
Ru/lime	10	1	0.01	1.8		
Dec/C=O	2	8	0.10	1.9		
Ru/CaO	10	2	0.05	1.9		
Ru/Ca <sub>3</sub> Al <sub>2</sub> O <sub>6</sub> -CaO	10	18	0.23	2.0		

Table S2.	Textural	properties	of	bifunctional	Ru-CaO	after	repeated	carbonation	and
	regenerat	ion (in calci	ined	form).					

**Table S3.**Physicochemical properties of bifunctional Ru-CaO after 10 cycles of SE-SMR and<br/>regeneration.

	]	N <sub>2</sub> physisorption	1	Dorticle size <sup>[a]</sup>	H. chamisorntion <sup>[b]</sup>		
Catalyst	$S_{BET}$ [m <sup>2</sup> /g]	V <sub>Pore</sub> [cm <sup>3</sup> /g]	D <sub>pore</sub> [nm]	[nm]	II2 chem [μmo	[µmol <sub>Ru</sub> /g <sub>cat</sub> ]	
Ru/lime	5	0.06	1.8	$34\pm4$	2.1	(0.7%)	
Ru/CaO	6	0.07	1.9	$23 \pm 4$	7.2	(2.4%)	
Ru/Ca <sub>3</sub> Al <sub>2</sub> O <sub>6</sub> -CaO	18	0.21	1.8	$8\pm 2$	31.5	(10.6%)	

[a] average Ru particle size as determined by TEM, and [b] the quantity of surface Ru was calculated via  $H_2$  chemisorption using a stoichiometry factor of 1.0 for H/Ru,<sup>30-32</sup> the parenthesis give the Ru dispersion



Figure S1. (a) N<sub>2</sub> physisorption isotherm and (b) BJH pore size distribution of Ru/lime, Ru/CaO and Ru/Ca<sub>3</sub>Al<sub>2</sub>O<sub>6</sub>-CaO calcined at 850 °C.



Figure S2. STEM EDX mapping of calcined Ru/Ca<sub>3</sub>Al<sub>2</sub>O<sub>6</sub>-CaO, and calcined and reduced CaRuO<sub>3</sub>.



**Figure S3.** XRD of the reference RuO<sub>2</sub> (Sigma-aldrich), calcined Ru/Al<sub>2</sub>O<sub>3</sub>, calcined CaRuO<sub>3</sub> and reduced CaRuO<sub>3</sub>: ( $\Box$ ) RuO<sub>2</sub>, ( $\triangle$ )  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>, ( $\blacklozenge$ ) Ru, and ( $\blacksquare$ ) CaO.



Figure S4. synthetic bifunctional materials.



Figure S5. CaO conversion in the kinetically-controlled carbonation regime as a function of pore volume: (■) 1<sup>st</sup>, (●) 2<sup>nd</sup>, (▲) 5<sup>th</sup> and (◆) 10<sup>th</sup> cycle.



Figure S6. (a) Off-gas composition during the  $1^{st}$  cycle for Ca-Ni-ex-Htlc and (b) the breakthrough curves for H<sub>2</sub> and CH<sub>4</sub> in the  $1^{st}$ ,  $5^{th}$  and  $10^{th}$  cycle.



Figure S7. CO<sub>2</sub> uptake under SE-SMR-mimicking conditions (carbonation: 550 °C using 50 ml/min of 20 % CO<sub>2</sub>/N<sub>2</sub>, 2 h, and regeneration:750 °C, 50 ml/min of N<sub>2</sub>, 15 min) as a function of number of carbonation-regeneration cycles. The solid line gives the theoretical CO<sub>2</sub> uptake of pure CaO, i.e., 0.78  $g_{CO_2}/g$ .



regeneration.