

Electronic Supporting Information

Selective synthesis of 1,3-propanediol from glycidol over carbon film encapsulated Co catalyst

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Table S1 Loading amount and particle size of active metals.

Entry	Catalyst	Active metal loading (wt. %) ^a	Particle size (nm)	
			XRD ^b	TEM ^c
1	Co@NC	58.90	23.1	25.6
2	Co/AC	15.85	10.2	11.0
3	Co@NG-ZIF	41.40	12.1	13.3
4	Co/H-BEA	14.74	—	—
5	Co/MCM-41	13.71	—	—
6	Co/ZnO	14.88	—	—
7	Co/MgO	13.29	—	—
8	Co/Al ₂ O ₃	13.49	—	—
9	Co/MWCNTs	14.90	—	—
10	Ni/MWCNTs	14.92	—	—
11	Cu/MWCNTs	14.89	—	—
12	Pt/ MWCNTs	3.57	—	—
13	Pd/MWCNTs	3.78	—	—
14	Ru/MWCNTs	3.80	—	—

^a Metal contents were estimated by ICP-AES.

^b Calculated according to the Scherrer formula.

^c Derived from the TEM images.

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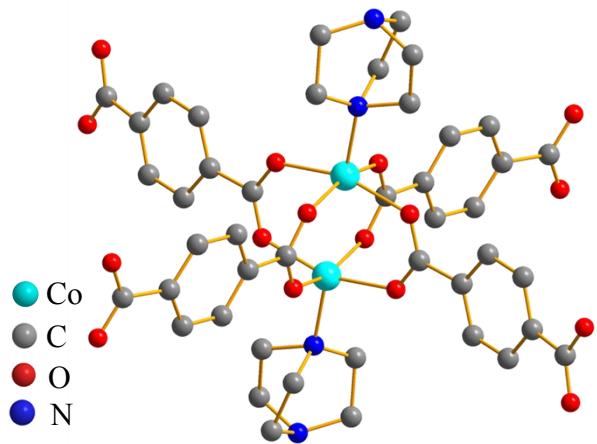


Fig. S1 Coordination environment of $\text{Co}_2(\text{bdc})_2(\text{ted})$ ^[1].

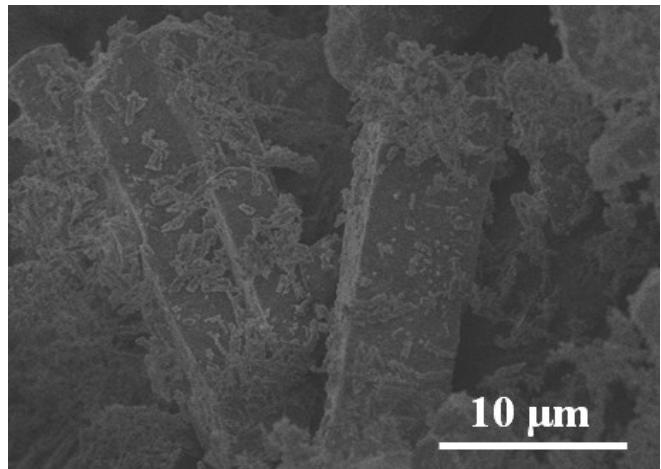


Fig. S2 SEM image of $\text{Co}_2(\text{bdc})_2(\text{ted})$.

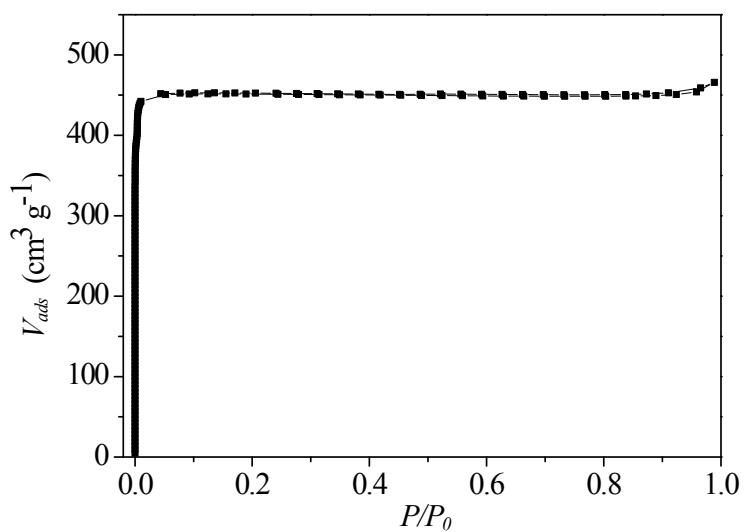


Fig. S3 N_2 adsorption-desorption isotherm of $\text{Co}_2(\text{bdc})_2(\text{ted})$.

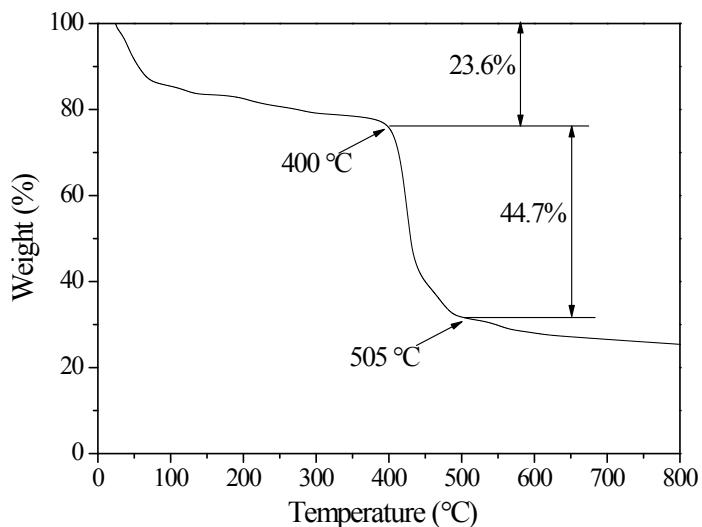


Fig. S4 TG curve of $\text{Co}_2(\text{bdc})_2(\text{ted})$.

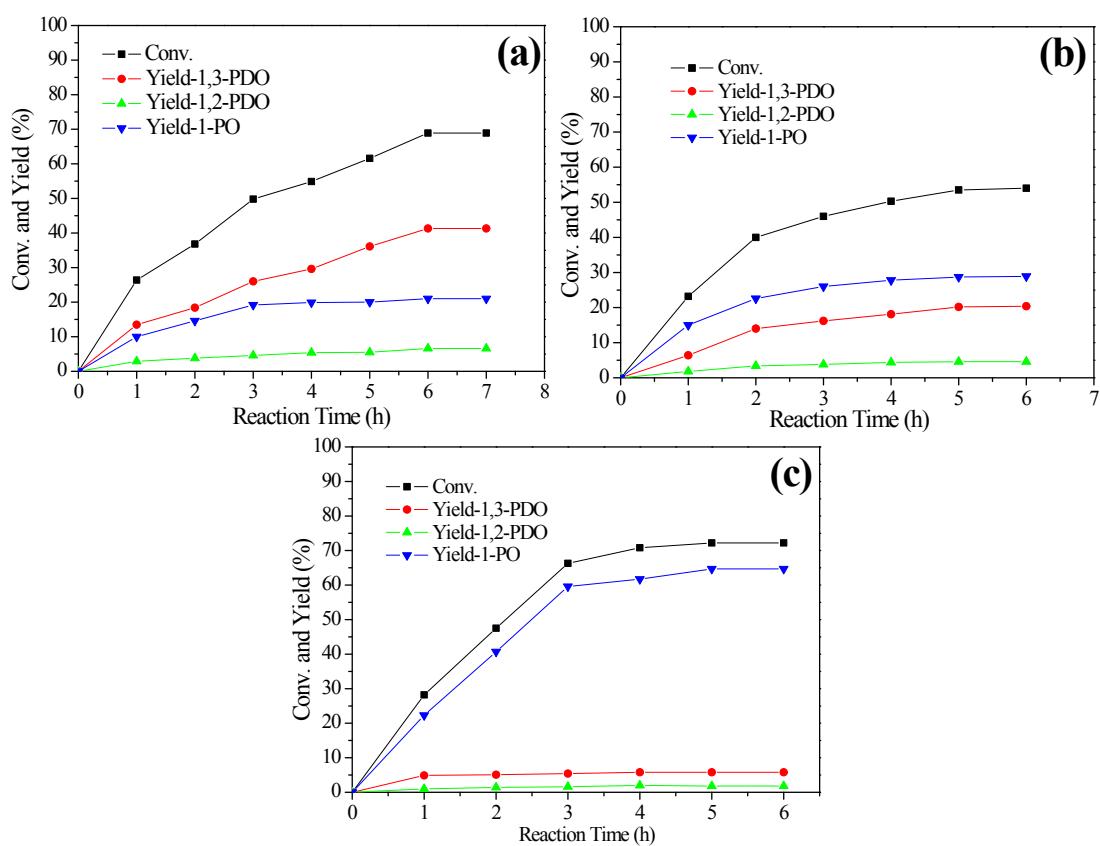


Fig. S5 Time courses of glycidol hydrogenation over (a) $\text{Co}@\text{NC}$, (b) Co/AC at 120 °C, and (c) $\text{Co}@\text{NG-ZIF}$ at 100 °C.

Reaction conditions: 0.3 g glycidol in 10.0 mL ethanol, Co 9.8 wt.%, 2.0 MPa H_2 .

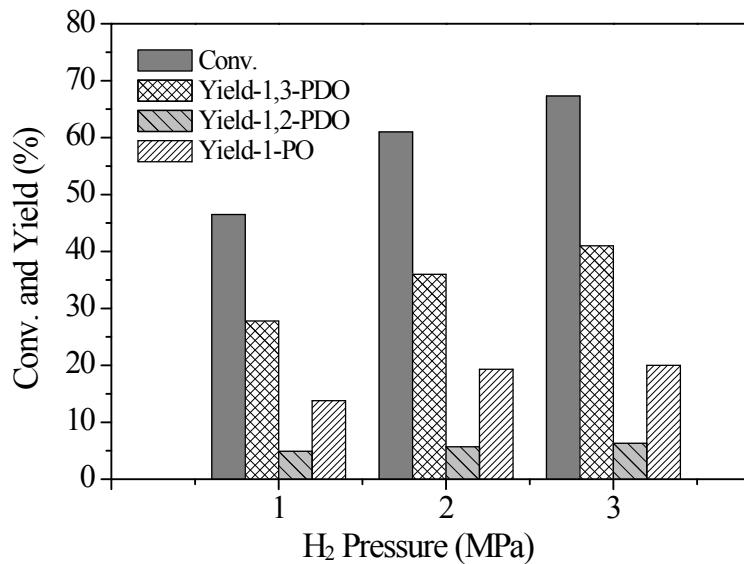


Fig. S6 Hydrogenation of glycidol under varied H₂ pressure.

Reaction conditions: 0.3 g glycidol in 10.0 mL ethanol with 9.8 wt.% of Co (Co@NC catalyst), 120 °C, 5 h.

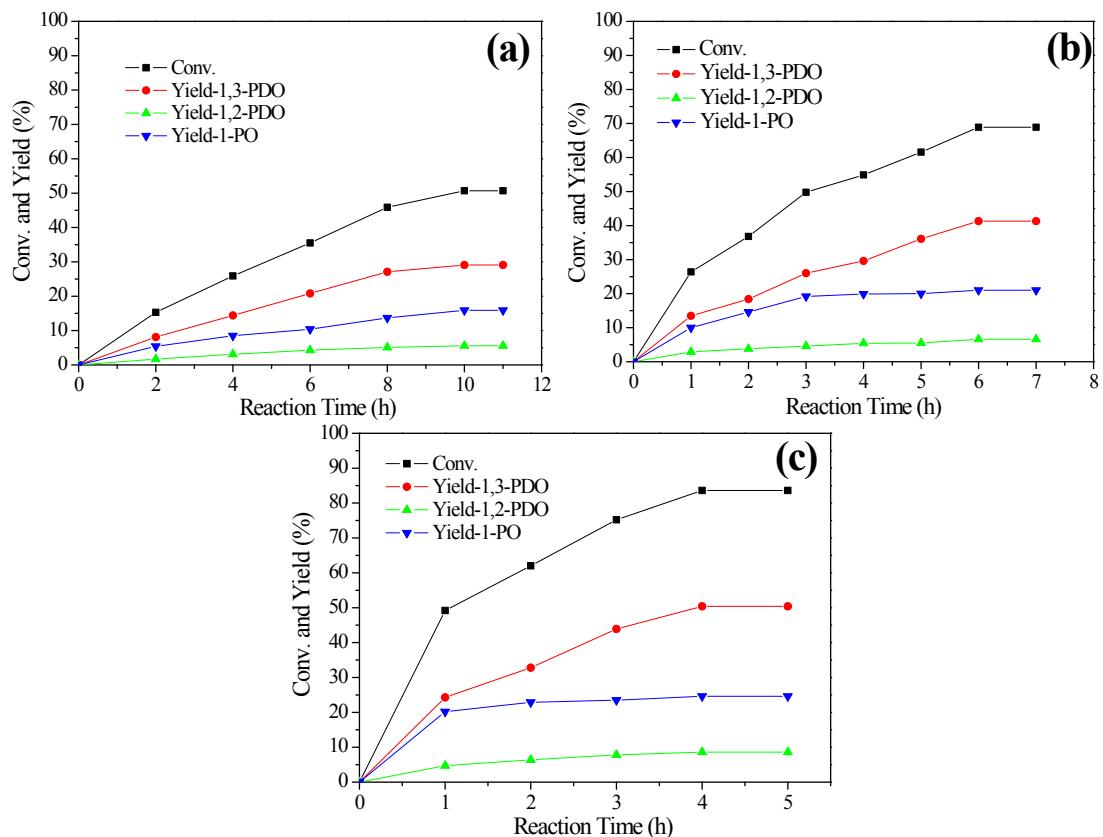


Fig. S7 Hydrogenation of glycidol over Co@NC at (a) 100 °C, (b) 120 °C and (c) 140 °C.

Reaction conditions: 0.3 g glycidol in 10.0 mL ethanol with 9.8 wt.% of Co, 2.0 MPa H₂.

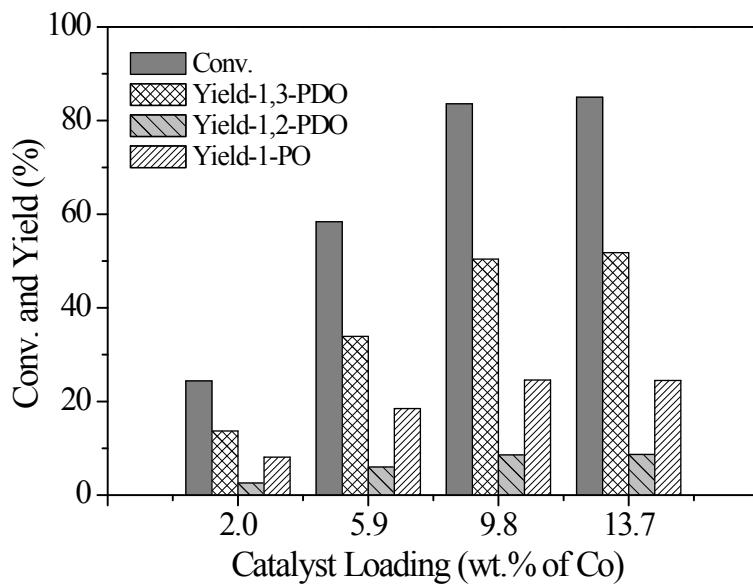


Fig. S8 Hydrogenation of glycidol with varied dosage of catalyst.
Reaction conditions: 0.3 g glycidol in 10.0 mL ethanol with different amount of Co@NC catalyst, 2.0 MPa H₂, 140 °C, 4 h.

Table S2 Results of glycidol hydrogenation in those pioneering works and this work.

Catalyst	Conv. (%)	Selectivity (%)				1,3-PDO Yield (%)	Ref.
		1,3-PDO	1,2-PDO	1-PO	Others ^a		
Pd/C	96.1	<1	93.1	-	6.7	<0.96	[2]
Pd/C+A15	100±8	-	>99	-	-	>99	[3]
Ni(40)/Sap	100	26	53	-	21	26	[4]
NiRe(7)/MS	98	47	38	7	6	46.1	[5]
Co@NC	83.6	60.3	10.3	29.4	-	50.4	This work ^b

^aOligomers of glycidol.

^bData was obtained at 140 °C and 4 h (Fig. S7 (c)).

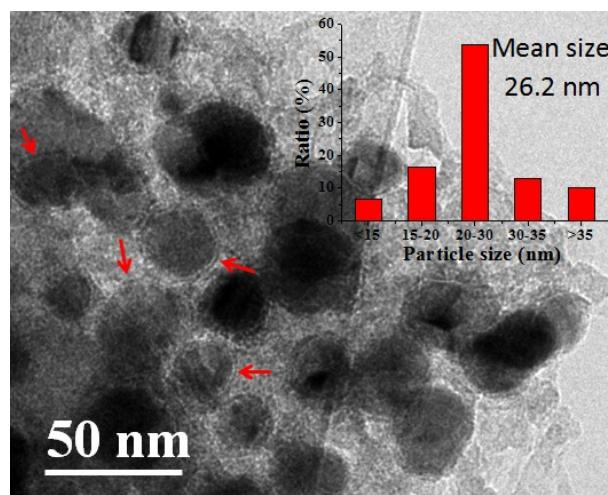


Fig. S9 TEM image of recycled Co@NC.

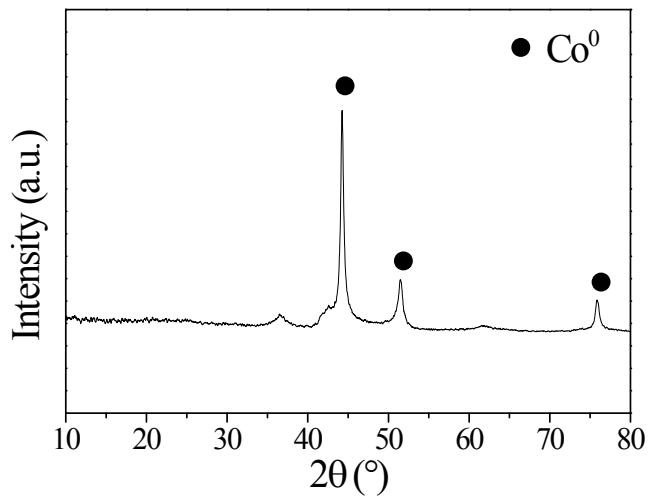


Fig. S10 XRD pattern of recycled Co@NC.

Table S3 Hydrogenation of PDOs and propylene oxide over three Co catalysts ^a.

Entry	Substrate	Catalyst	Conversion (%)	Product selectivity	
				Compound	(%)
1	<chem>OCCCO</chem>	Co@NC	NR ^b	—	—
2		Co/AC	NR	—	—
3		Co@NG-ZIF	NR	—	—
4	<chem>OCC(C)CO</chem>	Co@NC	NR	—	—
5		Co/AC	NR	—	—
6		Co@NG-ZIF	NR	—	—
7	<chem>C1CCOC1</chem>	Co@NC	93.8	1-propanol propane	86.8 13.2
8		Co@NG-ZIF	95.0	1-propanol propane	13.0 87.0

^a Reaction conditions: 0.3 g substrate in 10.0 mL ethanol with 9.8 wt.% of Co, 2.0 MPa H₂, 140 °C, 4 h. ^b NR: no reaction.

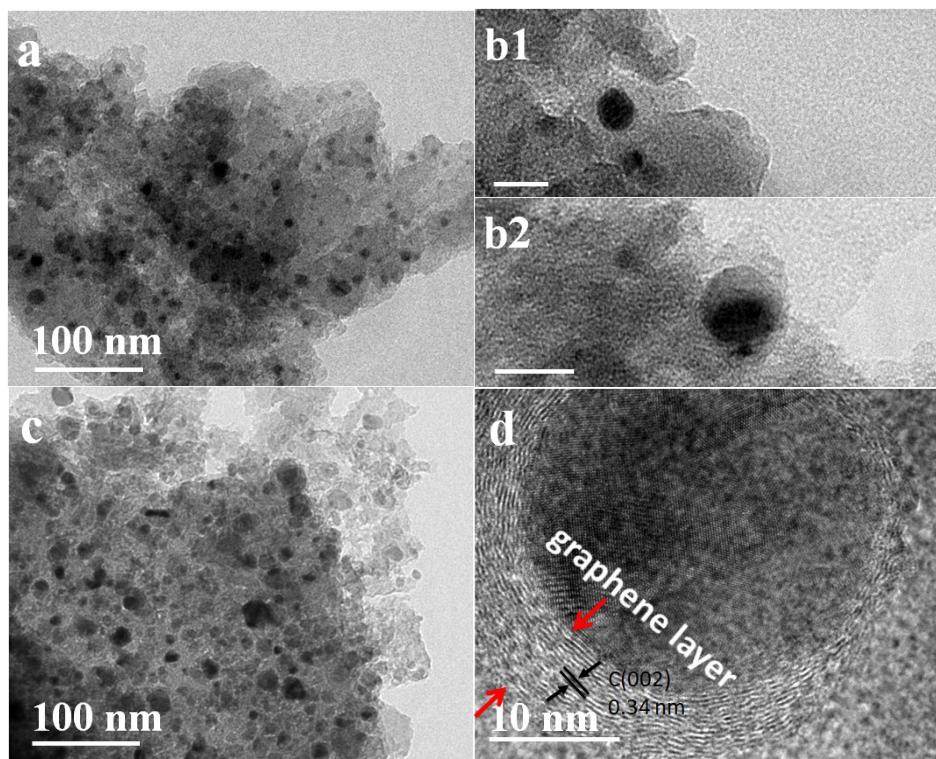


Fig. S11 TEM images of (a, b) Co/AC, and (c, d) Co@NG-ZIF (the scale bar in Fig. b was 20 nm).

Table S4 Surface elemental composition of different Co-based catalysts.

Entry	Catalyst	Surface atom composition (%) ^a			
		C	O	N	Co
1	Co@NC	80.2	14.1	1.1	4.6
2	Co@NG-ZIF	79.6	12.4	5.8	2.2

^a Surface composition determined from XPS.

References

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