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Supporting Information

Surface Acidity Enhancement of CeO₂ Catalysts via Modification with a Heteropoly Acid for the Selective Catalytic Reduction of NO with Ammonia

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Table S1Textual properties of the x% HSiW/Ce catalysts

Samples	Grain size (nm)	Surface area (m²/g)	Pore volume (cc g ⁻¹)
CeO ₂	10.7	44.05	0.21
1%HSiW/Ce	13.1	46.12	0.19
5%HSiW/Ce	12.8	34.25	0.18
10%HSiW/Ce	14.3	40.15	0.20
20%HSiW/Ce	12.3	31.28	0.17

Table S2

XPS parameters of the series catalysts investigated

Samples	Surface composition (at.%)			Ce ³⁺ /Ce ⁴⁺	O _{ads} /O _{lat}
	Ce	W	O		
CeO ₂	18.36	/	53.84	0.22	0.58
HSiW	/	12.04	51.36	/	0.35
10%HSiW/Ce (fresh)	13.58	3.54	56.30	0.19	0.52
10%HSiW/Ce (used)	14.10	3.60	57.64	0.18	0.51

Table S3 Spectrophotometry of HSiW/Ce after SCR reaction at 150 °C for 10 h.

Ions	Methods	Concentrations mg/L
NO ₃ -	Disulfonic acid phenol spectrophotometry	0.8650
NO_2^-	Diazo coupling spectrophotometry	0.8180
NH ⁴⁺	Nessler reagent spectrophotometry	241

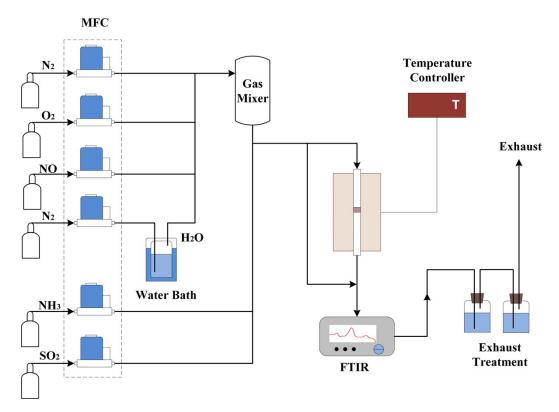


Fig. S1. Schematic diagram for SCR evaluation fixed-bed reaction system

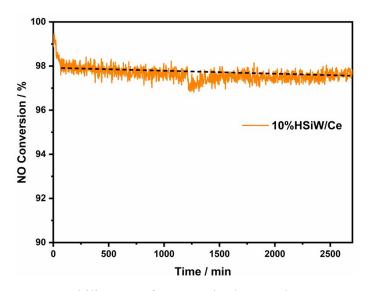


Fig. S2. Stability test of 10% HSiW/Ce catalyst at 250 °C

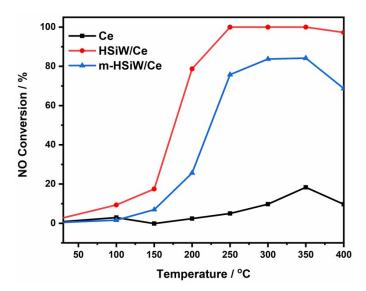


Fig. S3. SCR performance of m-HSiW/Ce (mechanical mixing CeO_2 and HSiW) and HSiW/Ce

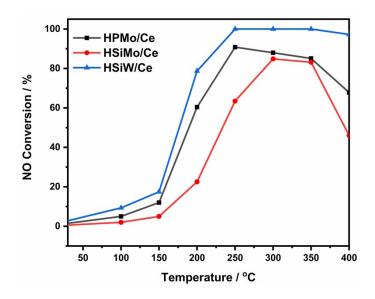


Fig. S4. SCR performance of different Keggin-type HPAs

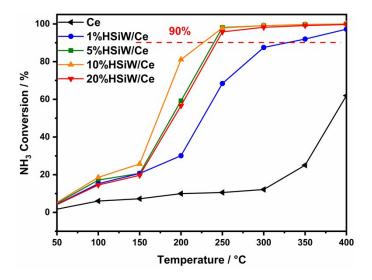


Fig. S5. NH₃ conversion of the various catalysts. Conditions: $[NH_3] = [NO] = 500$ ppm, $[O_2] = 3$ vol.%, N_2 as balance gas, $GHSV = 127000 \ h^{-1}$

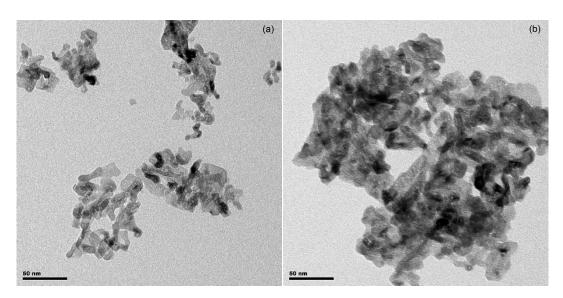


Fig. S6. TEM images of (a) CeO₂ and (b) HSiW/Ce

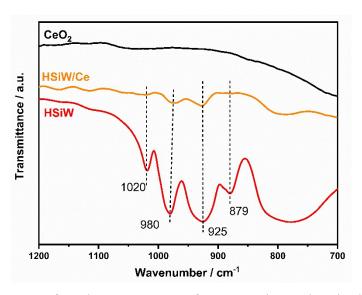
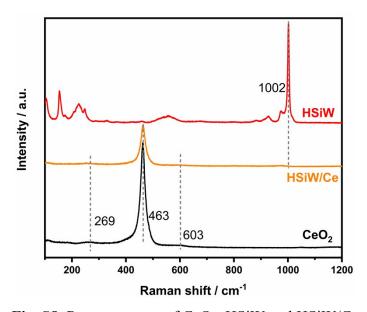


Fig. S7. Infrared Spectroscopy of CeO_2 , HSiW and HSiW/Ce



 $\textbf{Fig. S8}. \ Raman \ spectra \ of \ CeO_2, \ HSiW \ and \ HSiW/Ce$