

## Supporting information

### **Quantitative determination of the Cu species, acid sites and NH<sub>3</sub>-SCR mechanism on Cu-SSZ-13 and H-SSZ-13 at low temperatures**

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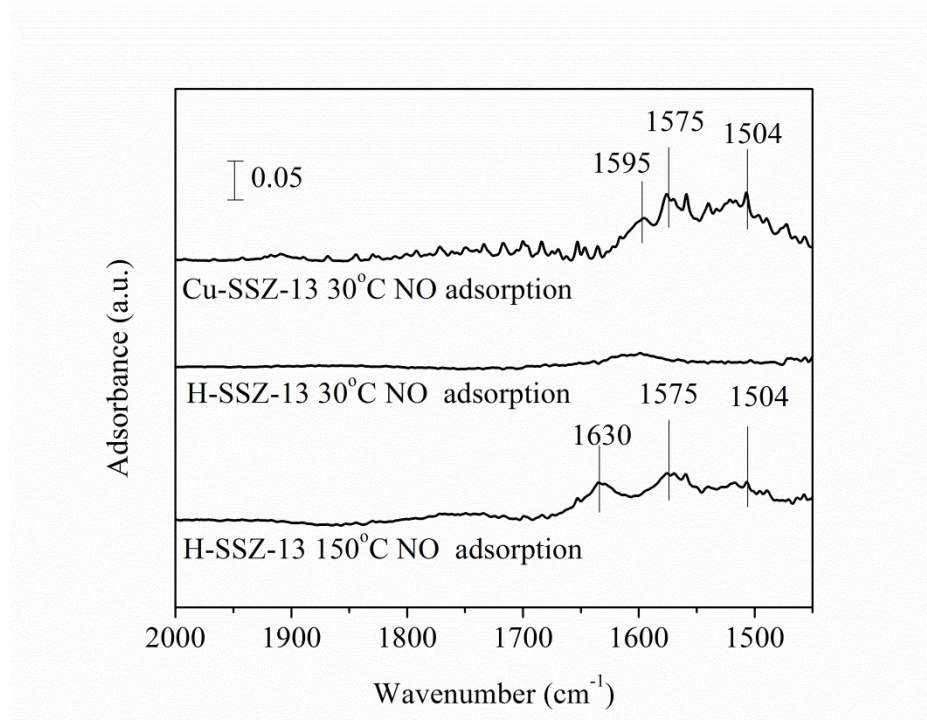
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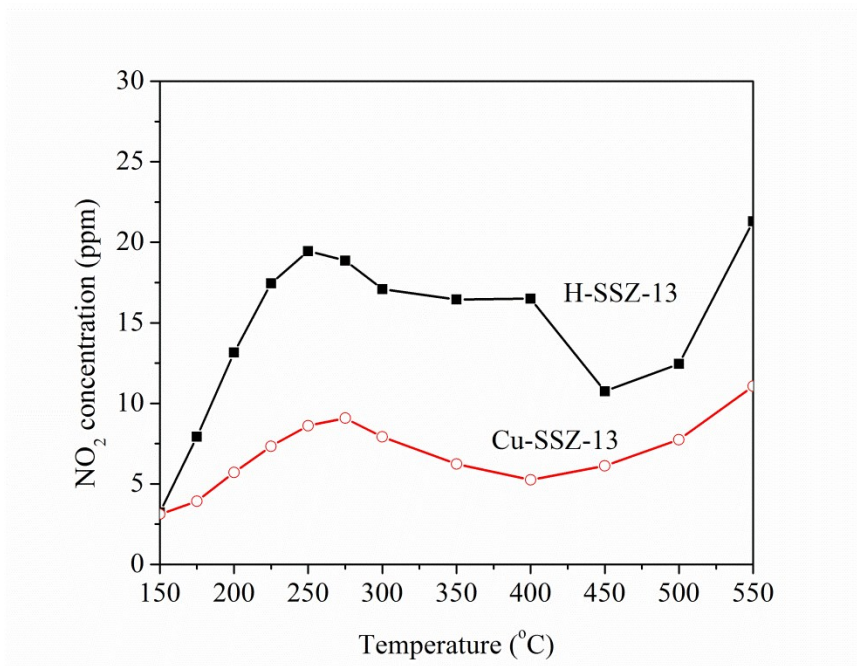
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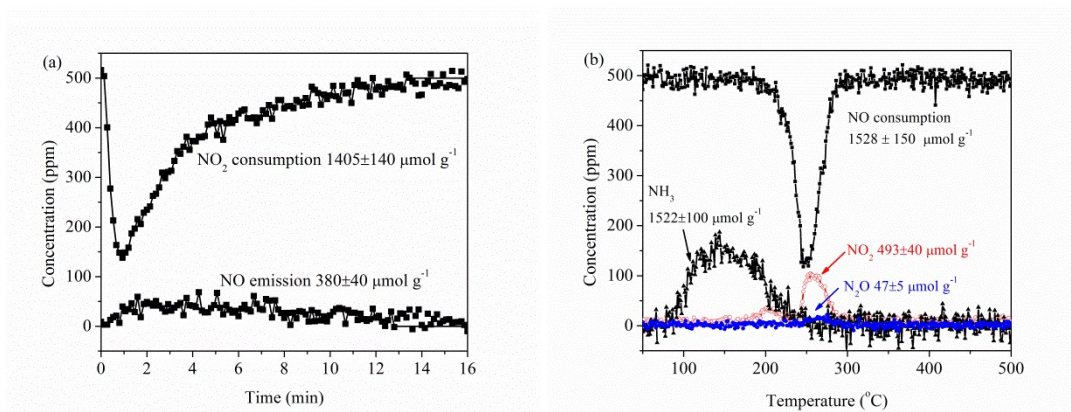
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**Figure S1** In situ DRIFT spectra of species on Cu-SSZ-13 and H-SSZ-13 after NO adsorption.



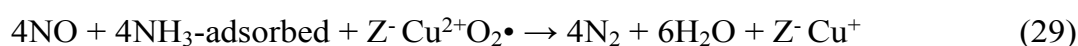
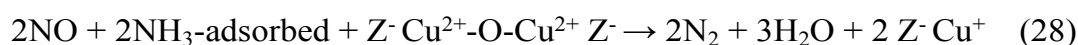
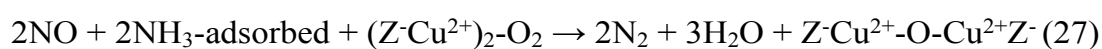
**Figure S2** NO<sub>2</sub> formation during NO oxidation on Cu-SSZ-13 and H-SSZ-13. Reaction conditions: 500 ppm NO and 5% O<sub>2</sub>, with N<sub>2</sub> balance; 500 mL/min gas flow rate.

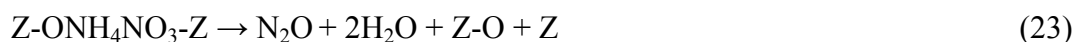
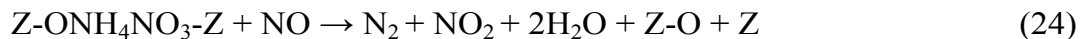


**Figure S3** (a) Adsorption of  $\text{NO}_2$  on Cu-SSZ-13 pretreated by  $\text{NH}_3$  at  $30^\circ\text{C}$  and (b) TPSR in  $\text{NO}/\text{N}_2$  of Cu-SSZ-13 pretreated by 500 ppm  $\text{NH}_3$  and then 500 ppm  $\text{NO}_2$  at  $30^\circ\text{C}$ .

Following experiment was conducted to study if the reaction mechanism changes with the change of the adsorption:  $\text{NH}_3$  was adsorbed on Cu-SSZ-13 firstly, and then  $\text{NO}_2$  was introduced into the reactor. Afterwards, TPSR in  $\text{NO}/\text{N}_2$  was conducted, and the results are shown in **Figure S3**.

The amount of  $\text{NH}_3$  adsorbed on fresh Cu-SSZ-13 was  $3829 \mu\text{mol g}^{-1}$  (**Figure 6a**), and the subsequent  $\text{NO}_2$  adsorption resulted in  $1405 \mu\text{mol g}^{-1}$   $\text{NO}_2$  consumption and  $380 \mu\text{mol g}^{-1}$   $\text{NO}$  evolution. Thus, the nitrate adsorbed on Cu-SSZ-13 was  $1405 - 380 = 1025 \mu\text{mol g}^{-1}$ . Since the amounts of weakly adsorbed  $\text{NH}_3$  and nitrates were  $721$  and  $456 \mu\text{mol g}^{-1}$ , respectively, the remaining amounts of  $\text{NH}_3$  and nitrates on Cu-SSZ-13 could be calculated to be  $3829 - 721 = 3108 \mu\text{mol g}^{-1}$  and  $1025 - 456 = 569 \mu\text{mol g}^{-1}$ , respectively. During TPSR, the amounts of  $\text{NO}$  consumption,  $\text{NO}_2$ ,  $\text{N}_2\text{O}$  and  $\text{NH}_3$  evolution were  $1528$ ,  $493$ ,  $47$  and  $1522 \mu\text{mol g}^{-1}$ , respectively. Therefore, it can be concluded that  $3108 - 1522 = 1586 \mu\text{mol g}^{-1}$   $\text{NH}_3$  and  $569 \mu\text{mol g}^{-1}$  nitrates could reacted with  $1528 \mu\text{mol g}^{-1}$   $\text{NO}$  at the ratios of  $\text{NO}/\text{NH}_3$  1/1 ( $1035/1035$ ),  $\text{NO}/\text{NH}_4\text{NO}_3/(\text{NO}_2 \text{ emission})$  1/1/1 ( $493/493/493$ ), and  $\text{NH}_4\text{NO}_3/(\text{N}_2\text{O emission})$  1/1 ( $47/47$ ), and following reactions took place:





The mechanism was the same as that concluded from **Figure 10a**, i.e., the results of TPSR of Cu-SSZ-13 in NO pretreated by NO<sub>2</sub> and then NH<sub>3</sub>, indicating that the reaction mechanism was not affected by the adsorption order. It should be noted that more NH<sub>3</sub> adsorbed on the fresh Cu-SSZ-13 catalyst than on NO<sub>2</sub>-pretreated Cu-SSZ-13 (**Figure S3a**), and thus, the amount of NH<sub>3</sub> desorption in **Figure S3b** was higher than that in **Figure 10a**. The amount of NO<sub>2</sub> adsorbed on NH<sub>3</sub>-pretreated Cu-SSZ-13 was smaller than that on fresh Cu-SSZ-13 (**Figure 6a**), leading to lower amounts of NO<sub>2</sub> and N<sub>2</sub>O emission.