

## Supporting information

### Flexible Two-Dimensional Layered Metal-Organic Framework Functionalized with (Trifluoromethyl)trifluoroborate: Synthesis, Crystal Structure, and Adsorption/Separation Properties

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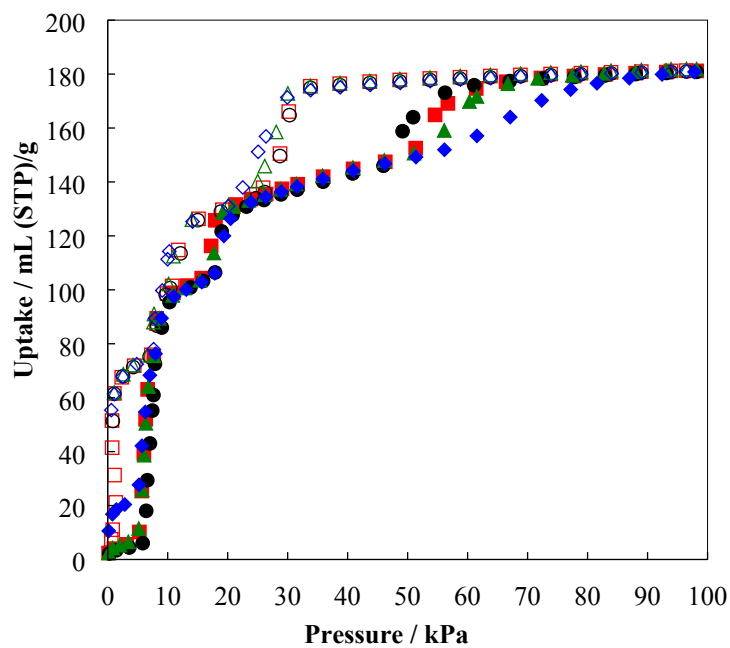
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### Repetitive adsorption property

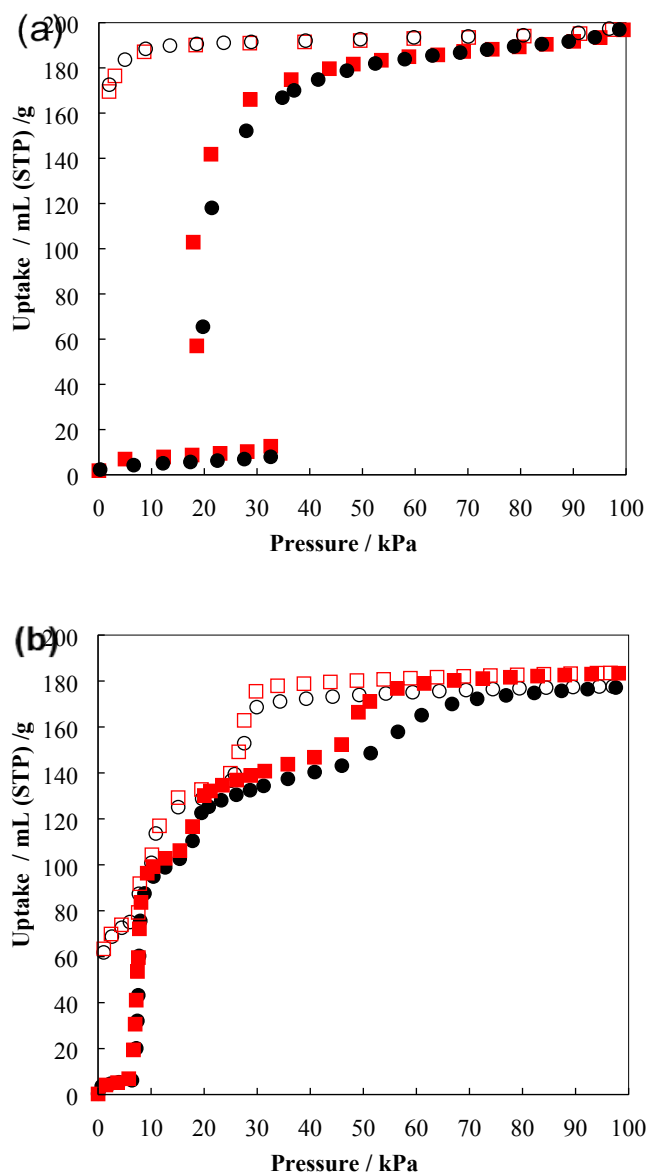
Carbon dioxide repetitive adsorption characteristics of ELM-13 were evaluated. Pre-treatment under reduced pressure at 110 °C was carried out only before the first, second, and 24th measurement. Other measurements (3rd to 23th) were carried out without pretreatment.



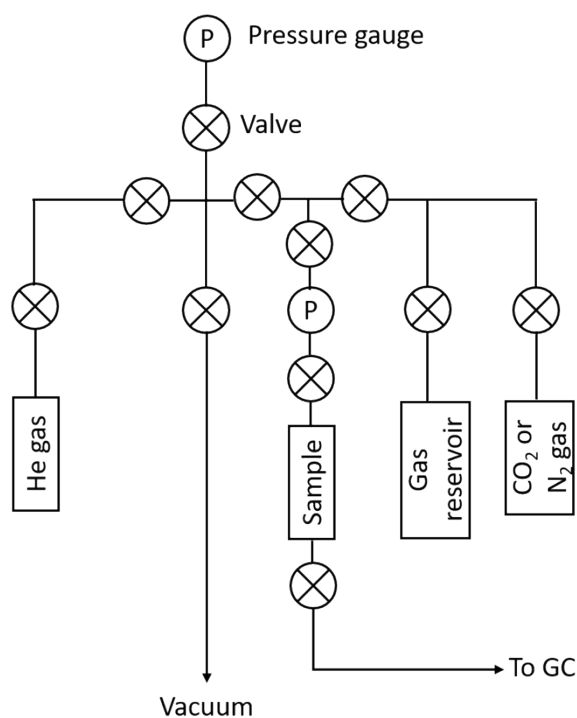
**Figure 1S.** Adsorption isotherms of CO<sub>2</sub> at 195 K: the first (black, circle), 2nd (red, square), 3rd (green, triangle), and 24th (diamond, blue). Open and solid symbol denotes adsorption and desorption, respectively.

### Long-term preservability in synthetic mother liquid

The crystal of ELM-13 was kept in the synthetic mother liquor at room temperature. The crystal was filtered after 9 years, washed with water, air-dried and gas adsorption property was compared to freshly prepared ELM-13.



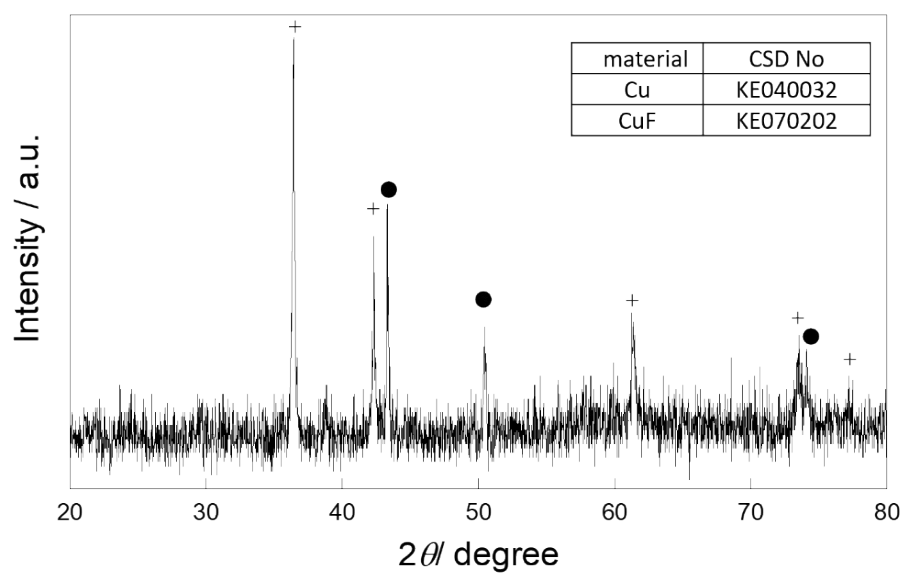
**Figure 2S.** Gas adsorptivity of freshly prepared ELM-13 (black, circle) and ELM-13 aged in mother liquid for 9 years (red, square). Open and solid symbol denotes adsorption and desorption, respectively: (a) N<sub>2</sub> at 77 K, (b) CO<sub>2</sub> at 195 K.



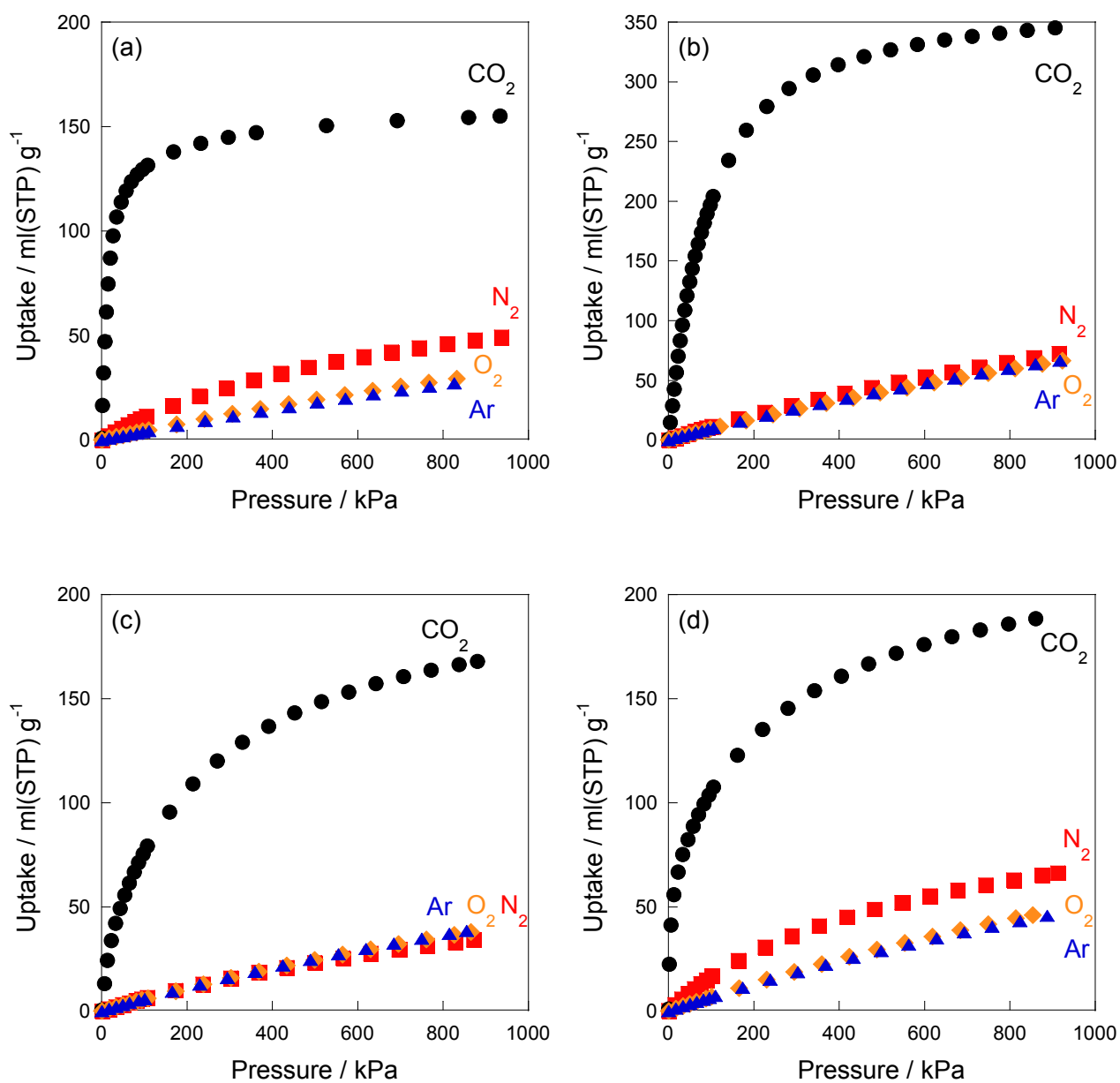
**Figure 3S.** Schematic representation of a hand-made vacuum/gas loading line for high-pressure mixed-gas separation experiments.

### Experimental procedure of high-pressure CO<sub>2</sub>/N<sub>2</sub> mixed-gas separation

High-pressure CO<sub>2</sub>/N<sub>2</sub> mixed-gas separation experiments were performed with a hand-made line shown in Figure 3S. Several grams (ca. 2 g) of powder sample were placed in a stainless steel column with an inner diameter of 3.1 mm and connected to the line. Before the experiment, the column was heated at 373 K for 2 h under vacuum ( $P < 1$  mPa) to activate the sample. Equimolar CO<sub>2</sub>/N<sub>2</sub> mixed gas with a total pressure of 1.0 MPa was introduced into the column containing the sample at 273 K in an ice-water bath. After 30 min to reach adsorption equilibrium, the sample was heated at 353-333 K to desorb the adsorbed gases, and then the desorbed gases were collected in a gas bag with He gas loading. The ratio of CO<sub>2</sub>/N<sub>2</sub> obtained from a GC-9A gas chromatograph with a thermal conductivity detector (Shimadzu Co.) was used to calculate the ratio of the adsorbed gases on the sample.



**Figure 4S.** XRD pattern (CuK $\alpha$  radiation,  $\lambda = 1.5418 \text{ \AA}$ ) of the residue after TG measurement. Cross and circle symbol indicates diffraction peaks assigned to CuF (CSD No. KE070202) and Cu (CSD No. KE040032), respectively.



**Figure 5S.** High pressure adsorption isotherms on (a) zeolite 13X, (b) HKUST-1, (c) UiO-66, and (d) Mg-MOF-74 at 273 K. (CO<sub>2</sub>, black; N<sub>2</sub>, red; O<sub>2</sub>, orange; Ar, blue).

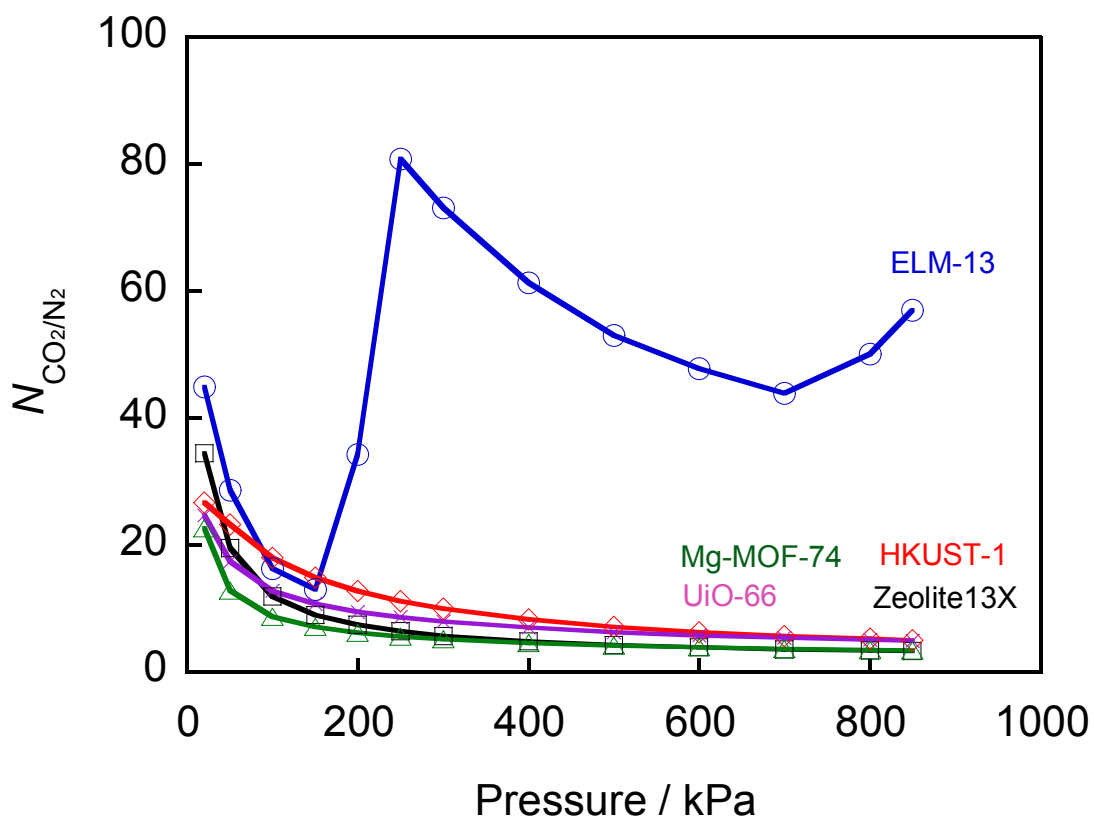
### Estimation of CO<sub>2</sub> selectivity

The ratio of adsorbed amount of CO<sub>2</sub> over that of N<sub>2</sub> ( $N_{\text{CO}_2/\text{N}_2} = N_{\text{CO}_2}/N_{\text{N}_2}$ ) was calculated from single component gas adsorption isotherms by dividing the CO<sub>2</sub> adsorption amount by that of N<sub>2</sub> at each pressure points. The adsorbed amounts of CO<sub>2</sub> and N<sub>2</sub> at 273 K and 0.25 MPa and resultant value  $N_{\text{CO}_2/\text{N}_2}$  on zeolite 13X, HKUST-1, UiO-66, Mg-MOF-74 and ELM-13 are summarized in table 1S. The CO<sub>2</sub> selectivities ( $K_{\text{CO}_2}/K_{\text{N}_2}$ ) were also evaluated by using Henry coefficients estimated from the CO<sub>2</sub> and N<sub>2</sub> adsorption isotherms at low pressures except ELM-13. The value of the selectivity on Mg-MOF-74 was took from reference [1]. Pressure dependence of the ratio  $N_{\text{CO}_2/\text{N}_2}$  on the microporous materials in the wide pressure range up to 850 kPa are also shown in Figure 6S.

**Table 1S.** Adsorption amount of CO<sub>2</sub> and N<sub>2</sub>, ratio of adsorbed CO<sub>2</sub> over N<sub>2</sub> ( $N_{\text{CO}_2/\text{N}_2}$ ) at 273 K and 0.25 MPa, and selectivity ( $S_{\text{Henry}}$ ) evaluated from Henry coefficients on selected microporous materials.

	CO <sub>2</sub> / mmol g <sup>-1</sup>	N <sub>2</sub> / mmol g <sup>-1</sup>	$N_{\text{CO}_2/\text{N}_2}$	$S_{\text{Henry}}$
Zeolite 13X	6.5	0.95	6.8	45
HKUST-1	12.7	1.2	10.6	26
UiO-66	5.1	0.62	8.2	25
Mg-MOF-74	8.1	1.5	5.4	29*
This work	2.8	0.035	81	-

\*The value was used from reference [1]



**Figure 6S.** Pressure dependence of the ratio of adsorbed CO<sub>2</sub> over N<sub>2</sub> at 273 K. (ELM-13, blue; zeolite 13X, black; HKUST-1, red; UiO-66, purple; Mg-MOF-74, green)

References

- [1] A. N. Dickey, A. Ö. Yazaydin, R. R. Willis, R. Q. Snurr, *Can. J. Chem. Eng.*, **2012**, *90*, 825-832.