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Supporting Information

Enhanced removal of antibiotics in hospital wastewater by Fe-ZnO

activated persulfate-based oxidation

Gnougon Nina COULIBALY^{1,2}, Sungjun BAE², Joohyun KIM², Aymen Amin ASSADI¹,

Khalil HANNA^{1*}

¹Univ. Rennes, Ecole Nationale Supérieure de Chimie de Rennes, CNRS, ISCR-UMR 6226,

F-35000 Rennes, France

²Department of Civil and Environmental Engineering, Konkuk University, 120 Neungdong-ro,

Gwangjin-gu, Seoul 05029, Republic of Korea

*Corresponding author: khalil.hanna@ensc-rennes.fr

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| Chemical elements | Nanowire ZnO | Nanoparticles |
|-------------------|--------------|---------------|
| | (wt %) | Fe-doped ZnO |
| Zn | 80 | 79.04 |
| Ο | 20 | 18.05 |
| Fe | 0 | 2.91 |
| | | |

Table S1. EDX analysis results for different samples

| | SWW | RHW | |
|---|---------|---------|--|
| pH | 8.0±0.5 | 6.8±0.2 | |
| Turbidity (NTU) | 2±1 | 196±5 | |
| Conductivity (μ S cm ⁻¹) | 1250±5 | 1340±5 | |
| TOC (mg L^{-1}) | 80±5 | 50±10 | |
| Suspended solid (mg L ⁻¹) | 0 | 20±2 | |
| Chloride (mg L ⁻¹) | 450±20 | 620±10 | |
| Nitrate mg L ⁻¹) | 35±2 | 7±2 | |
| Sulfate (mg L ⁻¹) | 20±2 | 60±10 | |
| Phosphate (mg L ⁻¹) | 150±10 | 60±10 | |
| | | | |

Table S2. Inorganic species and physico-chemical characteristics of SWW and RHW

Synthetic wastewater (SWW) were prepared by adding 400 mg L⁻¹ of NaCl, 50 mg L⁻¹ of citric acid, 30 mg L⁻¹ of ascorbic acid, 100 mg L⁻¹ of sucrose and 230 mg L⁻¹ Na₂HPO₄ to tap water (conductivity 408 μ S cm⁻¹).



Fig. S1. Schematic diagram of recirculation glass reactor system



Fig. S2. EDX analysis of (a) ZnO and (b) Fe-ZnO particles. Abbreviations: energy dispersive X-ray (EDX)



Fig. S3. FLU removal kinetics in presence of oxidants. Experimental conditions: [FLU] $_0 = 5$ μ M, [PS] $_0 = 0.5$ mM, [H₂O₂] $_0 = 0.2$ mM, UV-A reaction time = 24 h. pH $_0 = 7.0 \pm 0.2$, V = 1 L, recirculation flow rate = 222 mL min⁻¹. The correlation coefficients for kinetic models were more than 0.98). Abbreviations: FLU = flumequine, PS = Persulfate, H₂O₂ = hydrogen peroxide.



Fig. S4. Removal kinetics of FLU with 0.7 wt% Fe-ZnO/CA membrane catalyst at different concentration. Experimental conditions: [FLU] $_0 = 5 \mu$ M, UV-A reaction time = 24 h UV-A reaction time = 24 h. pH $_0 = 7.0 \pm 0.2$, recirculation flow rate = 222 mL min⁻¹. The correlation coefficients for kinetic models were more than 0.99.



Fig. S5. Removal of (a): FLU and (b): CIP in single system in different water matrices. Experimental conditions: [FLU] $_0$ = [CIP] $_0$ =5 μ M, [PS] $_0$ = 0.5 mM, [0.7 wt % Fe-ZnO] = 7.77 g m⁻² CA membrane, UV-A reaction time = 24 h , pH $_0$ =7.0 ± 0.2, V = 1 L, recirculation flow rate = 222 mL min⁻¹. The correlation coefficients for kinetic models were more than 0.99. Abbreviations: FLU = flumequine, CIP = ciprofloxacin, PS = Persulfate: UPW = Ultrapure water, SWW = Synthetic wastewater, RHW = Real hospital wastewater.



Fig. S6. Effect of water matrices in (a): FLU and (b): CIP degradation in binary system. Experimental conditions: $[FLU] = [CIP]_0 = 5 \ \mu\text{M}$, $[PS]_0 = 0.5 \ \text{mM}$, $[0.7 \ \text{wt \% Fe-ZnO}] = 7.77 \ \text{g} \ \text{m}^{-2} \ \text{CA}$ membrane, UV-A reaction time = 24 h, pH₀=7.0 ± 0.2, V = 1 L, recirculation flow rate = 222 mL min⁻¹. The correlation coefficients for kinetic models were more than 0.95. Abbreviations: FLU = flumequine, CIP = ciprofloxacin, PS = persulfate, UPW = Ultrapure water, SWW = Synthetic wastewater, RHW = Real hospital wastewater.



Fig. S7. Adsorption of inorganic ligands and LHA on TiO₂ and 0.7 wt % Fe-ZnO/CA membrane surface in dark, without FLU and PS. Experimental conditions: catalyst mass = 0.025 g, [Phosphate] $_0 = 150$ mg L⁻¹, [Nitrate] $_0 = 10$ mg L⁻¹, [Sulfate] $_0 = 120$ mg L⁻¹, [Chloride] $_0 = 250$ mg L⁻¹ and [LHA] $_0 = 40$ mgC L⁻¹, reaction time = 12 h, pH $_0 = 7.0 \pm 0.2$, V = 1 L, recirculation flow rate = 222 mL min⁻¹. Abbreviation: FLU = flumequine, PS = Persulfate, LHA = Leonardite Humic Acid.