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Supporting Information

## Enhanced removal of antibiotics in hospital wastewater by Fe-ZnO

## activated persulfate-based oxidation

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Chemical elements	Nanowire ZnO	Nanoparticles
	(wt %)	Fe-doped ZnO
Zn	80	79.04
Ο	20	18.05
Fe	0	2.91

Table S1. EDX analysis results for different samples

	SWW	RHW	
pH	8.0±0.5	6.8±0.2	
Turbidity (NTU)	2±1	196±5	
Conductivity ( $\mu$ S cm <sup>-1</sup> )	1250±5	1340±5	
TOC (mg $L^{-1}$ )	80±5	50±10	
Suspended solid (mg L <sup>-1</sup> )	0	20±2	
Chloride (mg L <sup>-1</sup> )	450±20	620±10	
Nitrate mg L <sup>-1</sup> )	35±2	7±2	
Sulfate (mg L <sup>-1</sup> )	20±2	60±10	
Phosphate (mg L <sup>-1</sup> )	150±10	60±10	

Table S2. Inorganic species and physico-chemical characteristics of SWW and RHW

Synthetic wastewater (SWW) were prepared by adding 400 mg L<sup>-1</sup> of NaCl, 50 mg L<sup>-1</sup> of citric acid, 30 mg L<sup>-1</sup> of ascorbic acid, 100 mg L<sup>-1</sup> of sucrose and 230 mg L<sup>-1</sup> Na<sub>2</sub>HPO<sub>4</sub> to tap water (conductivity 408  $\mu$ S cm<sup>-1</sup>).



Fig. S1. Schematic diagram of recirculation glass reactor system



**Fig. S2.** EDX analysis of (a) ZnO and (b) Fe-ZnO particles. Abbreviations: energy dispersive X-ray (EDX)



**Fig. S3.** FLU removal kinetics in presence of oxidants. Experimental conditions: [FLU]  $_0 = 5$   $\mu$ M, [PS]  $_0 = 0.5$  mM, [H<sub>2</sub>O<sub>2</sub>]  $_0 = 0.2$  mM, UV-A reaction time = 24 h. pH  $_0 = 7.0 \pm 0.2$ , V = 1 L, recirculation flow rate = 222 mL min<sup>-1</sup>. The correlation coefficients for kinetic models were more than 0.98). Abbreviations: FLU = flumequine, PS = Persulfate, H<sub>2</sub>O<sub>2</sub> = hydrogen peroxide.



**Fig. S4.** Removal kinetics of FLU with 0.7 wt% Fe-ZnO/CA membrane catalyst at different concentration. Experimental conditions: [FLU]  $_0 = 5 \mu$ M, UV-A reaction time = 24 h UV-A reaction time = 24 h. pH  $_0 = 7.0 \pm 0.2$ , recirculation flow rate = 222 mL min<sup>-1</sup>. The correlation coefficients for kinetic models were more than 0.99.



**Fig. S5.** Removal of (a): FLU and (b): CIP in single system in different water matrices. Experimental conditions: [FLU]  $_0$  = [CIP]  $_0$  =5  $\mu$ M, [PS]  $_0$  = 0.5 mM, [0.7 wt % Fe-ZnO] = 7.77 g m<sup>-2</sup> CA membrane, UV-A reaction time = 24 h , pH  $_0$  =7.0 ± 0.2, V = 1 L, recirculation flow rate = 222 mL min<sup>-1</sup>. The correlation coefficients for kinetic models were more than 0.99. Abbreviations: FLU = flumequine, CIP = ciprofloxacin, PS = Persulfate: UPW = Ultrapure water, SWW = Synthetic wastewater, RHW = Real hospital wastewater.



**Fig. S6.** Effect of water matrices in (a): FLU and (b): CIP degradation in binary system. Experimental conditions:  $[FLU] = [CIP]_0 = 5 \ \mu\text{M}$ ,  $[PS]_0 = 0.5 \ \text{mM}$ ,  $[0.7 \ \text{wt \% Fe-ZnO}] = 7.77 \ \text{g} \ \text{m}^{-2} \ \text{CA}$  membrane, UV-A reaction time = 24 h, pH<sub>0</sub>=7.0 ± 0.2, V = 1 L, recirculation flow rate = 222 mL min<sup>-1</sup>. The correlation coefficients for kinetic models were more than 0.95. Abbreviations: FLU = flumequine, CIP = ciprofloxacin, PS = persulfate, UPW = Ultrapure water, SWW = Synthetic wastewater, RHW = Real hospital wastewater.



**Fig. S7.** Adsorption of inorganic ligands and LHA on TiO<sub>2</sub> and 0.7 wt % Fe-ZnO/CA membrane surface in dark, without FLU and PS. Experimental conditions: catalyst mass = 0.025 g, [Phosphate]  $_0$  = 150 mg L<sup>-1</sup>, [Nitrate]  $_0$  = 10 mg L<sup>-1</sup>, [Sulfate]  $_0$  = 120 mg L<sup>-1</sup>, [Chloride]  $_0$  = 250 mg L<sup>-1</sup> and [LHA]  $_0$  = 40 mgC L<sup>-1</sup>, reaction time = 12 h, pH  $_0$  = 7.0 ± 0.2, V = 1 L, recirculation flow rate = 222 mL min<sup>-1</sup>. Abbreviation: FLU = flumequine, PS = Persulfate, LHA = Leonardite Humic Acid.