## Electronic Supplementary Information (ESI ${ }^{\dagger}$ )

## Selective catalytic oxidation of benzene to phenol by a vanadium oxide $\left(\mathrm{V}_{\mathrm{nr}}\right)$ nanorod catalyst in $\mathrm{CH}_{3} \mathrm{CN}$ using $\mathrm{H}_{2} \mathrm{O}_{2(\mathrm{aq})}$ and pyrazine-2carboxylic acid (PCA)

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[^0]Table S1. Oxidation of benzene to $p$-benzoquinone ( $p$ - BQ ) and phenol ( PhOH ) catalyzed by the various vanadium catalysts. ${ }^{[a]}$

| Catalyst | TON ${ }^{[b]}$ |  | Total TON ${ }^{[c]}$ | $\begin{gathered} \mathrm{Y}_{\mathrm{S}} \\ {[\%]^{[\mathrm{d}]}} \end{gathered}$ | $\begin{gathered} \mathrm{Y}_{\mathrm{O}} \\ {[\%]^{[\mathrm{e}]}} \end{gathered}$ | $\begin{aligned} & \hline \mathrm{OCE} \\ & {[\%]^{[f]}} \end{aligned}$ | $\begin{aligned} & \mathrm{PhOH} \\ & {[\%]^{[g]}} \\ & \hline \end{aligned}$ | $\mathrm{H}_{2} \mathrm{O}_{2}(\%)$ remained |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $p$-BQ | PhOH |  |  |  |  |  |  |
| $\mathrm{V}_{\mathrm{nr}}$ | 1.75 | 11.74 | 13.49 | 4.21 | 7.03 | 12.10 | 87.03 | 25 |
| $\begin{gathered} \mathrm{V}_{\mathrm{nr}} \\ (\mathrm{PCA}) \end{gathered}$ | 1.30 | 25.54 | 26.83 | 8.37 | 13.99 | 63.93 | 95.17 | 77 |
| $\mathrm{V}_{2} \mathrm{O}_{5}$ | 0.18 | 5.19 | 5.37 | 1.68 | 2.80 | 4.91 | 96.62 | 41 |
| $\begin{gathered} \mathrm{V}_{2} \mathrm{O}_{5} \\ \text { (PCA) } \end{gathered}$ | 0.55 | 9.58 | 10.13 | 3.16 | 5.28 | 8.97 | 94.59 | 38 |
| $\mathrm{VOSO}_{4}$ | 0.78 | 8.38 | 9.16 | 2.86 | 4.78 | 6.50 | 91.46 | 20 |
| $\mathrm{VOSO}_{4}$ <br> (PCA) | 0.58 | 9.11 | 9.70 | 3.03 | 5.06 | 7.56 | 94.00 | 29 |
| $\mathrm{VCl}_{3}$ | 0.68 | 6.12 | 6.80 | 2.12 | 3.55 | 13.13 | 89.98 | 70 |
| $\begin{gathered} \mathrm{VCl}_{3} \\ (\mathrm{PCA}) \\ \hline \end{gathered}$ | 0.48 | 6.93 | 7.41 | 2.31 | 3.86 | 12.14 | 93.50 | 66 |

${ }^{[a]}$ Conditions: Total volume of the reaction solution was 3 mL ; Solvent: acetonitrile; Catalyst: $\mathrm{V}_{\mathrm{nr}} / \mathrm{V}_{2} \mathrm{O}_{5} / \mathrm{VOSO}_{4} / \mathrm{VCl}_{3}(0.014 \mathrm{mmol})$; Substrate: benzene ( 4.486 mmol ); Oxidant: $35 \% \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{aq})(2.685 \mathrm{mmol})$; PCA ( 0.04 mmol ); Temperature: $25^{\circ} \mathrm{C}$; Time: 5 h . Product quantification was conducted by GC analysis with nitrobenzene as the internal standard. ${ }^{[b]}$ Turnover number (TON) for each of the oxygenated products, $p$ BQ and $\mathrm{PhOH}(\mathrm{mmol})$, respectively, was determined by calculating the number of millimoles of product per millimole of catalyst (based on V content). ${ }^{[c]}$ The total TON of the products $(p-\mathrm{BQ}+\mathrm{PhOH})$. ${ }^{[d]} \mathrm{Ys}[\%]_{\mathrm{c}}=\left[\right.$ substrate $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{~mol})\right] \times 100$. ${ }^{[\mathrm{e}]} \mathrm{Y}_{\mathrm{O}}$ $[\%]_{\mathrm{c}}=\left[\right.$ products $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{~mol})\right] \times 100$. ${ }^{[f]}$ Overall catalytic efficiency $(\mathrm{OCE})=(2 \times p-$ $\mathrm{BQ}+\mathrm{PhOH})[\mathrm{TON}] /\left[\mathrm{H}_{2} \mathrm{O}_{2}\right.$ consumed (equiv.)]. ${ }^{[\mathrm{g}]}$ Selectivity of $\mathrm{PhOH}=[(\mathrm{PhOH})$ $(\mathrm{mol}) /[p-\mathrm{BQ}+\mathrm{PhOH}](\mathrm{mol})] \times 100$.

Table S2. Oxidation of benzene to $p$-benzoquinone ( $p$ - BQ ) and phenol ( PhOH ) catalyzed by the vanadium oxide nanorod catalyst ( $\mathbf{V}_{\mathbf{n r}}$ ) using various $\mathrm{H}_{2} \mathrm{O}_{2(\mathrm{aq})}$ concentrations. ${ }^{[a]}$

| $\begin{aligned} & 35 \%_{H_{2} \mathrm{O}_{2}} \\ & (\mathrm{mmol}) \end{aligned}$ | TON ${ }^{[b]}$ |  | $\begin{aligned} & \text { Total } \\ & \text { TON } \end{aligned}$ | $\underset{[\%]^{[d]}}{\mathrm{Y}_{\mathrm{S}}}$ | $\begin{gathered} \mathrm{Y}_{\mathrm{O}} \\ {[\%]^{[\mathrm{ec}}} \end{gathered}$ | $\begin{aligned} & \text { OCE } \\ & {[\%]^{[f]}} \end{aligned}$ | $\begin{aligned} & \mathrm{PhOH} \\ & {[\%]^{[s]}} \end{aligned}$ | $\mathrm{H}_{2} \mathrm{O}_{2}(\%)$ remained |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $p$-BQ | PhOH |  |  |  |  |  |  |
| 0.31 | 0.06 | 2.34 | 2.40 | 0.75 | 10.85 | 13.69 | 97.42 | 18 |
| 0.67 | 0.08 | 13.14 | 13.22 | 4.12 | 27.62 | 37.98 | 99.43 | 27 |
| 1.34 | 0.09 | 16.99 | 17.09 | 5.33 | 17.85 | 31.23 | 99.46 | 42 |
| 2.68 | 1.30 | 25.54 | 26.83 | 8.37 | 13.99 | 63.93 | 95.17 | 77 |
| 4.64 | 0.21 | 6.71 | 6.92 | 2.16 | 2.09 | 10.35 | 96.90 | 79 |
| 9.28 | 0.13 | 8.26 | 8.38 | 2.62 | 1.26 | 10.77 | 98.47 | 88 |

${ }^{[a]}$ Conditions: Total volume of the reaction solution was 3 mL , Solvent: acetonitrile; Catalyst: $\mathrm{V}_{\mathrm{nr}}$ (V content: 0.014 mmol ), Substrate: benzene ( 4.486 mmol ); PCA ( 0.04 mmol ), Temperature: $25^{\circ} \mathrm{C}$; Time: 5 h . Product quantification was conducted by GC analysis with nitrobenzene as the internal standard; ${ }^{[b]}$ Turnover number (TON) for each of the oxygenated products, $p-\mathrm{BQ}$ and PhOH ( mmol ), respectively, was determined by calculating the number of millimoles of product per millimole of catalyst (based on V content). ${ }^{[\mathrm{c}]}$ The total TON of the products $(p-\mathrm{BQ}+\mathrm{PhOH}) .{ }^{[\mathrm{d}]} \mathrm{Ys}[\%]_{\mathrm{c}}=[$ substrate $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{~mol})\right] \times 100 \cdot{ }^{[\mathrm{ef}]} \mathrm{Y}_{\mathrm{O}}[\%]_{\mathrm{c}}=\left[\right.$ products $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{~mol})\right] \times 100$. ${ }^{[f]}$ Overall catalytic efficiency $(\mathrm{OCE})=(2 \times p-\mathrm{BQ}+\mathrm{PhOH})[\mathrm{TON}] /\left[\mathrm{H}_{2} \mathrm{O}_{2}\right.$ consumed. ${ }^{[g]}$ Selectivity of $\mathrm{PhOH}=[(\mathrm{PhOH})(\mathrm{mol}) /[p-\mathrm{BQ}+\mathrm{PhOH}](\mathrm{mol})] \times 100$. (equiv.) $]$

Table S3. Oxidation of benzene to $p$-benzoquinone ( $p-\mathrm{BQ}$ ) and phenol ( PhOH ) catalyzed by the vanadium oxide nanorod catalyst ( $\mathbf{V}_{\mathrm{nr}}$ ) using various $\mathrm{H}_{2} \mathrm{O}_{2(\mathrm{aq})}$ percentages. ${ }^{[a]}$

|  | $\mathrm{TON}^{[b]}$ |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\%^{[b]} \mathrm{H}_{2}$ | $p$-BQ | PhOH | Total <br> $\mathrm{TON}^{[c]}$ | $\mathrm{Y}_{\mathrm{S}}$ <br> $[\%]^{[d]}$ | $\mathrm{Y}_{\mathrm{O}}$ <br> $[\%]^{[e]}$ | OCE <br> $[\%]^{[f]}$ | PhOH <br> $\left.[\%]^{[g] ~}\right]$ | $\mathrm{H}_{2} \mathrm{O}_{2}(\%)$ <br> remained |
| 5 | 0.09 | 3.32 | 3.42 | 1.07 | 12.45 | 25.07 | 97.26 | 49 |
| 10 | 0.16 | 7.03 | 7.19 | 2.24 | 13.13 | 28.29 | 97.73 | 52 |
| 20 | 0.23 | 10.81 | 11.04 | 3.45 | 10.08 | 28.92 | 97.88 | 64 |
| 35 | 1.30 | 25.54 | 26.83 | 8.37 | 13.99 | 63.93 | 95.17 | 77 |

${ }^{[a]}$ Conditions: Total volume of the reaction solution was 3 mL ; Solvent: acetonitrile; Catalyst: $\mathrm{V}_{\mathrm{nr}}(\mathrm{V}$ content: 0.014 mmol$)$, Substrate: benzene ( 4.486 mmol ); $\mathrm{H}_{2} \mathrm{O}_{2(\text { (aq) }}(260$ $\mu \mathrm{L}$ ); PCA ( 0.04 mmol ); Temperature: $25^{\circ} \mathrm{C}$; Time: 5 h . The products were determined using GC analysis with nitrobenzene as the internal standard. ${ }^{[b]}$ Turnover number (TON) for each of the oxygenated products, $p-\mathrm{BQ}$ and PhOH (mmol), respectively, was determined by calculating the number of millimoles of product per millimole of catalyst (based on V content). ${ }^{[\mathrm{c}]}$ The total TON of the products $(p-\mathrm{BQ}+\mathrm{PhOH}) .{ }^{[\mathrm{d}]} \mathrm{Ys}[\%]_{\mathrm{c}}=$ [substrate $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{~mol})\right] \times 100 \cdot{ }^{[\mathrm{e}]} \mathrm{Y}_{\mathrm{O}}[\%]_{\mathrm{c}}=\left[\right.$ products $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{~mol})\right] \times 100$. ${ }^{[f]}$ Overall catalytic efficiency $(\mathrm{OCE})=(2 \times p-\mathrm{BQ}+\mathrm{PhOH})[\mathrm{TON}] /\left[\mathrm{H}_{2} \mathrm{O}_{2}\right.$ consumed (equiv.)]. ${ }^{[g]}$ Selectivity of $\mathrm{PhOH}=[(\mathrm{PhOH})(\mathrm{mol}) /[p-\mathrm{BQ}+\mathrm{PhOH}](\mathrm{mol})] \times 100$.

Table S4. Oxidation of benzene to $p$-benzoquinone ( $p-\mathrm{BQ}$ ) and phenol ( PhOH ) catalyzed by the vanadium oxide nanorod catalyst $\left(\mathrm{V}_{\mathrm{nr}}\right)$ in presence of PCA. ${ }^{[a]}$

| Time <br> (h) | TON ${ }^{[b]}$ |  | $\begin{gathered} \text { Total } \\ \text { TON }^{[c]} \end{gathered}$ | $\underset{[\%]^{[d]}}{\mathrm{Y}_{\mathrm{S}}}$ | $\begin{gathered} \mathrm{Y}_{\mathrm{O}} \\ {[\%]^{[\mathrm{ce}]}} \end{gathered}$ | $\begin{gathered} \mathrm{OCE} \\ {[\%]^{[\mathrm{f]}]}} \end{gathered}$ | $\begin{aligned} & \mathrm{PhOH} \\ & {[\%]^{[g]}} \end{aligned}$ | $\begin{gathered} \mathrm{H}_{2} \mathrm{O}_{2}(\%) \\ \text { remained } \end{gathered}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $p-\mathrm{BQ}$ | PhOH |  |  |  |  |  |  |
| 1 min | 0.21 | 0.45 | 0.67 | 0.21 | 0.35 | 21.95 | 68.26 | 98 |
| 10 min | 0.30 | 2.33 | 2.63 | 0.82 | 1.37 | 22.51 | 88.65 | 93 |
| 20 min | 0.34 | 2.64 | 2.99 | 0.93 | 1.56 | 19.60 | 88.45 | 91 |
| 30 min | 0.44 | 2.74 | 3.18 | 0.99 | 1.66 | 17.22 | 86.21 | 89 |
| 45 min | 0.53 | 3.21 | 3.74 | 1.17 | 1.95 | 17.79 | 85.78 | 87 |
| 1 | 0.69 | 9.83 | 10.52 | 3.28 | 5.48 | 41.49 | 93.45 | 86 |
| 2 | 1.09 | 21.39 | 22.48 | 7.01 | 11.72 | 69.31 | 95.16 | 82 |
| 3 | 1.36 | 23.03 | 24.39 | 7.61 | 12.72 | 71.53 | 94.43 | 81 |
| 5 | 1.30 | 25.54 | 26.83 | 8.37 | 13.99 | 63.93 | 95.17 | 77 |
| 10 | 1.26 | 27.23 | 28.49 | 8.89 | 14.85 | 39.65 | 95.59 | 61 |
| 18 | 0.82 | 27.23 | 28.05 | 8.75 | 14.62 | 26.48 | 97.08 | 43 |
| 24 | 0.57 | 27.48 | 28.04 | 8.75 | 14.62 | 24.88 | 97.97 | 40 |
| 48 | 0.37 | 28.36 | 28.73 | 8.97 | 14.98 | 21.39 | 98.72 | 29 |

${ }^{[a]}$ Conditions: Total volume of the reaction solution was 3 mL ; Solvent: acetonitrile; Catalyst: $\mathrm{V}_{\mathrm{nr}}$ (V content: 0.014 mmol ); Substrate: benzene ( 4.486 mmol ); Oxidant: $35 \%$ $\mathrm{H}_{2} \mathrm{O}_{2 \text { (aq) }}(2.685 \mathrm{mmol})$; PCA ( 0.04 mmol ); Temperature: $25^{\circ} \mathrm{C}$. The products were determined using GC analysis with nitrobenzene as the internal standard. ${ }^{[b]}$ Turnover number (TON) for each of the oxygenated products, $p$ - BQ and PhOH (mmol), respectively, was determined by calculating the number of millimoles of product per millimole of catalyst (based on V content). ${ }^{[\mathrm{c}]}$ The total TON of the products ( $p-\mathrm{BQ}+$ $\mathrm{PhOH}) .{ }^{[d]} \mathrm{Y}_{\mathrm{s}}[\%]_{\mathrm{c}}=\left[\right.$ substrate $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{~mol})\right] \times 100 .{ }^{[\mathrm{e}]} \mathrm{Y}_{\mathrm{O}}[\%]_{\mathrm{c}}=$ [products $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2} \quad(\mathrm{~mol})\right] \times 100$. ${ }^{[f]}$ Overall catalytic efficiency $(\mathrm{OCE})=(2 \times p-\mathrm{BQ}+$ $\mathrm{PhOH})[\mathrm{TON}] /\left[\mathrm{H}_{2} \mathrm{O}_{2}\right.$ consumed (equiv.)]. ${ }^{[\mathrm{g}\}}$ Selectivity of $\mathrm{PhOH}=[(\mathrm{PhOH})(\mathrm{mol}) /[p-$ $\mathrm{BQ}+\mathrm{PhOH}](\mathrm{mol})] \times 100$.

Table S5. Oxidation of benzene to $p$-benzoquinone ( $p-\mathrm{BQ}$ ) and phenol ( PhOH ) catalyzed by the recycled vanadium oxide nanorod catalyst $\left(\mathbf{V}_{\mathbf{n r}}\right) .{ }^{[a]}$

| Catalyst | TON ${ }^{[b]}$ |  | $\begin{gathered} \hline \text { Total } \\ \text { TON }^{[c]} \end{gathered}$ | $\begin{gathered} \mathrm{Y}_{\mathrm{S}} \\ {[\%]^{[\mathrm{d}}} \\ ] \end{gathered}$ | $\begin{gathered} \mathrm{Y}_{\mathrm{o}} \\ {[\%]^{[\mathrm{ec}}} \end{gathered}$ | $\begin{aligned} & \hline \mathrm{OCE} \\ & {[\%]^{[f]}} \end{aligned}$ | $\begin{aligned} & \mathrm{PhOH} \\ & {[\%]^{[g]}} \end{aligned}$ | $\mathrm{H}_{2} \mathrm{O}_{2}(\%)$remained |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $\begin{aligned} & p- \\ & \mathrm{BQ} \\ & \hline \end{aligned}$ | $\begin{gathered} \mathrm{PhO} \\ \mathrm{H} \end{gathered}$ |  |  |  |  |  |  |
| $\mathbf{V}_{\mathrm{nr}}$ (w/o PCA) | 1.75 | 11.74 | 13.49 | 4.21 | 7.03 | 12.10 | 87.03 | 25 |
| $\mathbf{V}_{\mathrm{nr}}+$ (PCA) | 1.30 | 25.54 | 26.83 | 8.37 | 13.99 | 63.93 | 95.17 | 77 |
| $\begin{aligned} & 1^{\text {st }} \text { recycled } \mathbf{V}_{\mathrm{nr}} \\ & \text { (w/o PCA) } \end{aligned}$ | 1.65 | 15.73 | 17.38 | 5.42 | 9.06 | 12.49 | 90.50 | 32 |
| $\begin{aligned} & 1^{\text {st }} \begin{array}{c} \text { recycled } \\ \mathbf{V}_{\mathrm{nr}} \end{array}+ \\ & (\mathrm{PCA}) \end{aligned}$ | 2.04 | 20.34 | 22.38 | 6.99 | 11.67 | 31.15 | 90.88 | 65 |
| $\begin{gathered} 2^{\text {nd }} \text { recycled } \mathbf{V}_{\mathrm{nr}} \\ (\text { w/o PCA) } \end{gathered}$ | 1.89 | 16.85 | 18.74 | 5.85 | 9.77 | 13.42 | 90.00 | 37 |
| $\begin{gathered} 2^{\text {nd }} \text { recycled } \mathbf{V}_{\mathrm{nr}}+ \\ \text { (PCA) } \end{gathered}$ | 2.14 | 20.75 | 22.90 | 7.15 | 11.94 | 22.30 | 92.72 | 54 |
| $\mathbf{V}_{\mathrm{nr}}$ leaching | - | 1.75 | 1.75 | 0.03 | 0.05 | 2.32 | 100 | 57 |

${ }^{[a]}$ Conditions: Total volume of the reaction solution was 3 mL ; Solvent: acetonitrile; $\mathbf{V}_{\mathbf{n r}}$ ( V content: 0.014 mmol ), $1^{\text {st }}$ recycled $\mathbf{V}_{\mathbf{n r}}$ (V content: 0.012 mmol ) ; 2 ${ }^{\text {nd }}$ recycled $\mathbf{V}_{\mathbf{n r}}$ ( V content: 0.011 mmol ), the leached $\mathbf{V}_{\mathbf{n r}}$ ( V content: $8.4 \times 10^{-4} \mathrm{mmol}$ ), Substrate: benzene ( 4.486 mmol ); Oxidant: $35 \% \mathrm{H}_{2} \mathrm{O}_{2 \text { (aq) }}$ ( 2.685 mmol ); PCA ( 0.04 mmol ); Temperature: $25^{\circ} \mathrm{C}$; Time: 5 h . The products were determined using GC analysis with nitrobenzene as the internal standard. ${ }^{[b]}$ Turnover number (TON) for each of the oxygenated products, $p-\mathrm{BQ}$ and PhOH ( mmol ), respectively, was determined by calculating the number of millimoles of product per millimole of catalyst (based on V content). ${ }^{[c]}$ The total TON of the products $(p-\mathrm{BQ}+\mathrm{PhOH}) .{ }^{[d]} \mathrm{Y}_{\mathrm{s}}[\%]_{\mathrm{c}}=[$ substrate $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{~mol})\right] \times 100 .{ }^{[\mathrm{el}]} \mathrm{Y}_{\mathrm{O}}[\%]_{\mathrm{c}}=\left[\right.$ products $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{~mol})\right] \times 100$. ${ }^{[f]}$ Overall catalytic efficiency $(\mathrm{OCE})=(2 \times p-\mathrm{BQ}+\mathrm{PhOH})[\mathrm{TON}] /\left[\mathrm{H}_{2} \mathrm{O}_{2}\right.$ consumed (equiv.) $]$. ${ }^{[g]}$ Selectivity of $\mathrm{PhOH}=[(\mathrm{PhOH})(\mathrm{mol}) /[p-\mathrm{BQ}+\mathrm{PhOH}](\mathrm{mol})] \times 100$.

Table S6. Oxidation of toluene to benzaldehyde (a), methyl p-benzoquinone (b) benzyl alcohol (c), o-cresol (d), and p-cresol (e) catalyzed by the vanadium oxide nanorod catalyst $\left(\mathrm{V}_{\mathrm{nr}}\right) .{ }^{[\mathrm{a}]}$

| Catalyst | $\mathrm{TON}^{[b]}$ |  |  |  |  | $\begin{gathered} \text { Total } \\ \text { TON }^{[c]} \end{gathered}$ | $\begin{gathered} \mathrm{Y}_{\mathrm{S}} \\ {[\%]^{[\mathrm{d}]}} \end{gathered}$ | $\begin{gathered} \mathrm{Y}_{0} \\ {[\%]^{[\mathrm{e}]}} \end{gathered}$ | $\begin{gathered} \text { OCE } \\ {[\%]^{[f]}} \end{gathered}$ | $\begin{gathered} s p^{2} / s p^{3} \\ {[\%]^{[g]}} \end{gathered}$ | $\mathrm{H}_{2} \mathrm{O}_{2}$ <br> (\%) remained |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | a | b | c | d | e |  |  |  |  |  |  |
| $\mathrm{V}_{\mathrm{nr}}$ | 3.33 | 0.74 | 0.36 | 1.01 | 1.13 | 6.57 | 2.06 | 3.43 | 8.06 | 44/56 | 33 |
| $\begin{gathered} \mathrm{V}_{\mathrm{nr}} \\ (\mathrm{PCA}) \end{gathered}$ | 6.9 | 4.6 | 1.64 | 4.02 | 3.41 | 20.57 | 6.44 | 10.73 | 25.05 | 58/42 | 31 |
| $\begin{gathered} \mathrm{V}_{\mathrm{nr}} \\ \left(\mathrm{PCA}, \mathrm{PPh}_{3}\right)^{[\mathrm{h}]} \end{gathered}$ | 4.5 | - | 3.67 | 3.82 | 3.64 | 15.62 | 4.89 | 8.14 | 12.05 | 48/52 | 13 |

${ }^{[a]}$ Conditions: Total volume of the reaction solution was 3 mL ; Solvent: acetonitrile; $\mathrm{V}_{\mathrm{nr}}$ (V content: 0.014 mmol$)$; Substrate: toluene ( 4.47 mmol ); Oxidant: $35 \% \mathrm{H}_{2} \mathrm{O}_{2(\mathrm{aq})}(2.685$ $\mathrm{mmol})$; PCA ( 0.04 mmol ); Temperature: $25{ }^{\circ} \mathrm{C}$; Time: 5 h . The products were determined using GC analysis with nitrobenzene as the internal standard. ${ }^{[b]}$ Turnover number (TON) for each of the oxygenated products, a-e (mmol), respectively, was determined by calculating the number of millimoles of product per millimole of catalyst (based on V content). ${ }^{[\mathrm{cl}]}$ The total TON of the products $(\mathbf{a}+\mathbf{b}+\mathbf{c}+\mathbf{d}+\mathbf{e}) .{ }^{[d]} \mathrm{Y}_{\mathrm{s}}[\%]_{\mathrm{c}}=$ [substrate $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{~mol})\right] \times 100$. ${ }^{[\mathrm{el}]} \mathrm{Y}_{\mathrm{O}}[\%]_{\mathrm{c}}=\left[\right.$ products $\left.(\mathrm{mol}) / \mathrm{H}_{2} \mathrm{O}_{2}(\mathrm{~mol})\right] \times 100$. ${ }^{[f]}$ Overall catalytic efficiency $(\mathrm{OCE})=(2 \times \mathbf{a}+2 \times \mathbf{b}+\mathbf{c}+\mathbf{d}+\mathbf{e})[\mathrm{TON}] /\left[\mathrm{H}_{2} \mathrm{O}_{2}\right.$ consumed (equiv.)]. ${ }^{[\mathrm{g}]}$ Selectivity for products, $o-, p$-cresols and methyl $p-\mathrm{BQ}=[(\mathrm{c}+\mathrm{d}+\mathrm{e})(\mathrm{mol}) /$ all oxidation products $(\mathrm{mol})] \times 100$. ${ }^{[\mathrm{h}]} \mathrm{PPh}_{3}$ was added after 5 h of reaction time and continued stirring for additional 30 min .

Table S7. The XPS characterization of vanadium oxide catalysts.

| Samples | XPS |  |
| :---: | :---: | :---: |
|  | $\mathrm{V} / \mathrm{O}$ | $\mathrm{V}^{4+} / \mathrm{V}^{5+}$ |
| $\mathbf{V}_{\mathbf{n r}}$ | 0.037 | 0.301 |
| $\mathbf{V}_{\mathbf{n r}(\text { cal }}$ | 0.274 | 0.218 |
| $1^{\text {st }}$ recycled $\mathbf{V}_{\mathbf{n r}}+(\mathrm{PCA})$ | 0.222 | 0.639 |
| $\mathrm{~V}_{2} \mathrm{O}_{5}$ commercial | 0.364 | 0.118 |

## 2. Figures



Fig. S1. The XPS survey spectrum of vanadium oxide nanorod $\left(\mathbf{V}_{\mathbf{n r}}\right)$ catalyst.


Fig. S2. The high-resolution XPS spectra of vanadium oxide nanorod ( $\mathbf{V}_{\mathbf{n r}}$ ) catalyst de-convoluted presented for: (a) O 1s and (b) C 1s. (Si-O signal contribution is from the Si sample holder)


Fig. S3. The high-resolution XPS spectra of vanadium oxide catalysts were deconvoluted presented for V 2 p3/2. (a) $\mathbf{V}_{\mathbf{n r}}$; (b) calcined $\mathbf{V}_{\mathbf{n r}}$; (c) ${ }^{\text {st }}$ recycled $\mathbf{V}_{\mathbf{n r}}$ and (d) $\mathrm{V}_{2} \mathrm{O}_{5}$ commercial catalyst.


Fig. S4. Thermogravimetric analysis (TGA) diagram of vanadium oxide nanorod $\left(\mathbf{V}_{\mathbf{n r}}\right)$ catalyst and commercialized bulk $\mathrm{V}_{2} \mathrm{O}_{5}$ powder.


Fig. S5. X-ray diffraction (XRD) spectra of vanadium oxide nanorods ( $\mathbf{V}_{\mathbf{n r}}$ ) catalyst.


Fig. S6. Scanning Electron Microscopy (SEM) image of the vanadium oxide catalyst: (a) the $\mathbf{V}_{\mathbf{n r}}$ catalyst; (b) the $1^{\text {st }}$ recycled $\mathbf{V}_{\mathbf{n r}}$ from $\mathbf{V}_{\mathbf{n r}}$ catalyzed reaction mixtures in normal reaction condition with the addition of PCA.


Fig. S7. ${ }^{51} \mathrm{~V}$ NMR spectra of solutions of vanadium oxide nanorod in ethanol- $d 1$. (a) $\mathbf{V}_{\mathbf{n r}}$ (V content: 0.014 mmol$)(\mathrm{b}) \mathbf{V}_{\mathbf{n r}}(\mathrm{V}$ content: 0.014 mmol$)+35 \%_{2} \mathrm{O}_{2}(2.685 \mathrm{mmol}) ;$ (c) $\mathbf{V}_{\mathbf{n r}}(\mathrm{V}$ content: 0.014 mmol$)+$ PCA $(0.04 \mathrm{mmol})$; (d) $\mathbf{V}_{\mathbf{n r}}(\mathrm{V}$ content:0.014 mmol) + PCA ( 0.04 $\mathrm{mmol})+35 \% \mathrm{H}_{2} \mathrm{O}_{2}(2.685 \mathrm{mmol})$.


Fig. S8. ${ }^{51}$ V-MAS-NMR experimental spectra of vanadium oxide nanorod $\left(\mathbf{V}_{\mathbf{n r}}\right)$ catalyst.
3. Mechanistic study of catalytic oxidation of benzene to phenol using ${ }^{18} \mathrm{O}_{2}$ or $\mathrm{H}_{2}{ }^{18} \mathrm{O}_{2}$.


Fig. S9. The oxygen-isotopic distribution of PhOH under the reaction mixtures of vanadium catalyst, $\mathbf{V}_{\mathbf{n r}}$ containing (a) $35 \% \mathrm{H}_{2}{ }^{16} \mathrm{O}_{2 \text { (aq) }}$ enriched at 1 atm of ${ }^{18} \mathrm{O}_{2}$ and (b) $35 \% \mathrm{H}_{2}{ }^{18} \mathrm{O}_{2}$ in $\mathrm{H}_{2} \mathrm{O}$ at $1 \mathrm{~atm} \mathrm{~N}_{2}$ in $\mathrm{CH}_{3} \mathrm{CN}$. The reactions were proceeded for 3 h . The ratios of $\mathrm{PhOH}:{ }^{18} \mathrm{O}-\mathrm{PhOH}$ derived from the deconvolution of the mass spec of ${ }^{16} \mathrm{O}$ enriched PhOH were 98:2 and 32:68, respectively; the mass spec of the parent ${ }^{16} \mathrm{O}$ enriched PhOH is represented in (c).

## 4. Determination of NIH-shift ratios of $4-\left[{ }^{2} \mathbf{H}_{0,1}\right]$ toluene catalyzed by vanadium oxide catalyst in $\mathrm{CH}_{3} \mathrm{CN}$ by the addition of $\mathrm{H}_{2} \mathrm{O}_{2(\text { aq })}$ using GC-MS

## Synthesis of $\mathbf{4}-\left[{ }^{2} \mathbf{H}_{\mathbf{0}, 1}\right]$ toluenes:

4- $\left.{ }^{2} \mathrm{H}_{0,1}\right]$ toluenes were synthesized by carrying out a hydrolysis of (4methylphenyl)magnesium bromide, which was prepared by the reaction of 4bromotoluene with magnesium in anhydrous tetrahydrofuran and with $\mathrm{D}_{2} \mathrm{O}$ according to the reported procedure. ${ }^{1}$


Scheme S1. Preparation of $4-\left[{ }^{2} \mathrm{H}_{0,1}\right]$ toluenes.


Fig. S10 (a) toluene


Fig. S10 (b) 4-[ $\left.{ }^{2} \mathrm{H}_{0,1}\right]$ toluene


Fig. S10 (c) toluene: $4-\left[{ }^{2} \mathrm{H}_{1}\right]$ toluene $=22 \%: 78 \%$


Scheme S2. Total volume of the reaction solution was 3 mL ; Solvent: acetonitrile; Catalyst: Vanadium oxide nanorod (V content: 0.014 mmol); Substrate: 4[ ${ }^{2} \mathrm{H}_{0,1}$ ]toluenes (with a deuterium enrichment of $78 \%$ ) ( 4.47 mmol ); Oxidant: $35 \%$ $\mathrm{H}_{2} \mathrm{O}_{2 \text { (aq) }}(2.685 \mathrm{mmol})$; Reaction time: 3 h ; Temperature: $25^{\circ} \mathrm{C}$.


Fig. S11. The mass spectra of the oxygenated product, $4-\left[{ }^{2} \mathrm{H}_{0,1}\right]$-o-cresols.


$M W=108$
38\%

$M W=109$ 62\%

Fig. S12. The mass spectra of the oxygenated product, $3-\left[{ }^{2} \mathrm{H}_{0,1}\right]-p$-cresol. (Deuterium enrichment (78\%) for the reactant, $4-\left[{ }^{2} \mathrm{H}_{0,1}\right]$ toluenes).

NIH-shift ratio of the deuterium ( $62 \%$ ) remaining in the oxidation product 3$\left[{ }^{2} \mathbf{H}_{0,1}\right]-p$-cresols of 4-[ $\left.{ }^{2} \mathbf{H}_{0,1}\right]$ toluenes $\mathbf{( 7 8 \%}$ deuterium enrichment) $=\mathbf{6 2 \%} / 78 \%=$ 80\%

## Reference

1 Y. Morimoto, S. Bunno, N. Fujieda, H. Sugimoto and S. Itoh, J. Am. Chem. Soc., 2015, 137, 5867-5870.


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