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## **Electronic Supplementary Information (ESI)**

## Lower methane combustion temperature on palladium nanoparticles anchored on TiO<sub>x</sub> subnano-islets in stellate mesoporous silica nanospheres

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**Scheme S1.** Different synthesis routes followed to generate Pd<sub>1</sub>TiMSNsc, Pd<sub>1</sub>TiMSNs and Pd<sub>1</sub>TiMSN catalysts.



Fig. S1: Thermogravimetric analysis (TG) of (a) MSN, (b) MSN<sub>S</sub> and (c) MSN<sub>S'</sub>.

The first mass loss occurring at 130 °C was attributed to physically adsorbed water. The weight loss centered at 350 °C was attributed to  $CTA^+$  adsorbed onto its tosylate counterion and the peak located at 250 °C was associated to  $CTA^+$  interacting directly with silanolate groups (SiO<sup>-</sup>). The last mass loss at 600 °C was assigned to water evolution from silanol condensation. Fig. S1b shows TGA profiles of silylated MSN particles (MSN<sub>s</sub>) which displays weight loss at 100 °C due to the adsorbed water of the external surface of MSN and it was approximately less than 0.5% which confirm the hydrophobicity enhancement obtained by the replacement of the surface silanol groups by trimethylsilyl groups. A small

weight loss was observed at 300 °C probably due to the remaining surfactant. The decomposition of TMS groups occurs at higher temperature, between 450° and 600 °C. The TGA decomposition curve of silylated MSN particles (MSN<sub>s</sub>) after calcination at 450°C (MSN<sub>s'</sub>) shows the appearance of a small weight loss about 550 °C attributed to the decomposition of methyl groups to form siloxane bridge.



Fig. S2: FT-IR spectra of (a) as-made MSN, (b) MSNs and (c)TiMSNs'.



**Fig. S3:** N<sub>2</sub> adsorption-desorption isotherms at 77K of calcined materials (a) Pd<sub>1</sub>MSN, (b) Pd<sub>0.2</sub>MSN, (c) Pd<sub>0.2</sub>TiMSN, (d) Pd<sub>1</sub>TiMSN, (e) Pd<sub>1</sub>TiMSN<sub>s</sub>, and (f) Pd<sub>1</sub>TiMSNsc.



Fig. S4: TEM images of (a)  $Pd_{0.2}TiMSN$  and (b)  $Pd_1TiMSN$  catalysts.



**Fig. S5:** Stability test at 500°C of catalysts (A) Pd<sub>1</sub>TiMSN, Pd<sub>0.2</sub>TiMSN, Pd<sub>1</sub>MSN and Pd<sub>0.2</sub>MSN and (B) Pd<sub>1</sub>TiMSN, Pd<sub>1</sub>TiMSN<sub>s</sub> and Pd<sub>1</sub>TiMSN<sub>sc</sub>.

**Table S1:** H/Pd molar ratio of hydrogen consumed by reduction or by formation of hydride between 25 and 80 °C from Temperature programmed reduction (TPR) and tentative distribution of PdH<sub>2</sub>, Si-H and Ti<sup>3+</sup>.

catalysts	$Pd^a$ (mmol $g^{-1}$ )	$H_2 \text{ consumption}^{b}$ (mmol g <sup>-1</sup> )	H/Pd <sup>c</sup>	molar distribution per Pd of H spill over / PdH <sub>2</sub> / Ti <sup>3+ d</sup>
Pd <sub>0.2</sub> MSN	0.019	0.042	4.4	2.4 / 1 / 0
Pd <sub>0.2</sub> TiMSN	0.019	0.055	5.8	2.4 / 1 / 2.4
Pd <sub>1</sub> MSN	0.103	0.383	7.4	5.4 / 1 / 0
Pd <sub>1</sub> TiMSN	0.103	0.307	5.6	2.4 / 1 / 2.2
Pd <sub>1</sub> TiMSN <sub>S</sub>	0.094	0.239	5.1	2.4 / 1 / 1.7

a) Pd content from chemical analysis

b)  $H_2$  consumption from the area integration of TCD signal mesured between 50 to 75°C;

c) molar ratio of hydrogen atoms consumed per palladium atoms

d) molar ratio of Si-H,  $Ti^{3+}$  ions species calculated assuming that, i) at 25°C PdO particles are totally reduced into metallic Pd<sup>0</sup> particles, ii) yielding first hydride PdH<sub>2</sub> above 25°C followed by reduction of the support consumption of the hydride forming Si-H from surface silanol groups, Si-OH and Ti<sup>3+</sup> ions in the presence of TiO<sub>x</sub> anchoring subnano islands.