## Supporting information

for

## Sequences controlled copolymerization of lactide and functional cyclic carbonate using stereoselective aluminum catalysts <br> Xiufang Hua, ${ }^{\text {a,b }}$ Xinli Liu *a and Dongmei Cui *a <br> Contents

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## Supplemental Figures:



Figure S1. GPC profiles of representative samples, entries 1-4, Table 1.

Complex 1, $90^{\circ} \mathrm{C}$


Complex 1, $70{ }^{\circ} \mathrm{C}$


Figure S2. Inverse gated decoupled ${ }^{13} \mathrm{C}$ NMR spectrum for the homopolymerization of rac-LA by complex $1\left(500 \mathrm{MHz}, \mathrm{CDCl}_{3}\right)$.


Figure S3. Semilogarithmic kinetic plot in each monomer catalyzed by complex $1\left(k_{\text {app }}\right.$ (MAC) $=$ $176.1 \times 10^{-4}, k_{\text {app }}(r a c-L A)=37.6 \times 10^{-4}, k_{\text {app }}($ L-LA $\left.)=9.2 \times 10^{-4}\right)$, Polymerization conditions:

Complex $\mathbf{1}=10 \mu \mathrm{~mol} ; \mathrm{T}=90^{\circ} \mathrm{C} ;$ Tol. $=2 \mathrm{~mL} ;$ ratio $=[$ monomer $]:[1]=100: 1$.
a)

b)


Figure S4. Plots of conversion vs time for the copolymerization with complex $\mathbf{1}$ of a) LLA/MAC and b) $r a c-L A / M A C$.



Figure S5. Inverse gated decoupled ${ }^{13} \mathrm{C}$ NMR spectrum for the homopolymerization of rac-LA by complex $2\left(500 \mathrm{MHz}, \mathrm{CDCl}_{3}\right)$.


Figure S6. Semilogarithmic kinetic plot in each monomer catalyzed by complex $2\left(k_{\text {app }}(\mathrm{MAC})=\right.$ $\left.87.6 \times 10^{-3}, k_{\text {app }}(\mathrm{L}-\mathrm{LA})=24.8 \times 10^{-3}\right), k_{\text {app }}(\mathrm{rac}$-LA $)=9.7 \times 10^{-3}$, Polymerization conditions: complex $\mathbf{2}=10 \mu \mathrm{~mol} ; \mathrm{T}=90^{\circ} \mathrm{C} ;$ Tol. $=2 \mathrm{~mL} ;$ ratio $=[$ monomer $]:[2]=100: 1$.


Figure S7. Plots of composition vs time for the copolymerization with complex $\mathbf{2}$ of a) LLA/MAC and b) $r a c-L A / M A C$.


Figure S8. (a) ${ }^{1} \mathrm{H}$ NMR and (b) ${ }^{13} \mathrm{C}$ NMR spectroscopy in $\mathrm{CDCl}_{3}$ :
(1) poly(MAC- $r$-L-LA), $L_{\mathrm{L}-\mathrm{LA}}=3.40 / L_{\mathrm{MAC}}=3.08$, (table 1 , entry 9);
(2) poly(MAC-grad-rac-LA), $L_{\text {rac-LA }}=4.45 / L_{\mathrm{MAC}}=3.76$, (table 1, entry 13);
(3) poly(rac-LA-tapered-MAC), $L_{\text {rac-LA }}=6.83 / L_{\mathrm{MAC}}=2.29$, (table 2, entry 9);
(4) quasi-diblock poly(L-LA-b-MAC), $L_{\mathrm{L}-\mathrm{LA}}=7.43 / L_{\mathrm{MAC}}=3.68$, (table 2, entry 4).


Figure S9. DSC thermograms of quasi-diblock Poly(L-LA-b-MAC) (table 2, entry 4) ( $T_{\mathrm{g}}$ value was calculated by STAR ${ }^{\mathrm{e}}$ method with heating/cooling rate of $10^{\circ} \mathrm{C} / \mathrm{min}$ and using second cycle from $-10^{\circ} \mathrm{C}$ to $200^{\circ} \mathrm{C}$ ): (1) first heating cycle; (2) after eliminating thermal history; (3) after isothermal crystallization.

Table S1. Homopolymerization of rac-LA or MAC with complex 1 and 2.

| entry $^{a}$ | Cat. | M | $[\mathrm{Cat} .]_{0}:[\mathrm{CTA}]_{0}:[\mathrm{M}]_{0}$ | $\operatorname{conv} .^{b}(\%)$ | $M_{\mathrm{n}, \mathrm{calcd}}{ }^{c}(\mathrm{KDa})$ | $M_{\mathrm{n}, \mathrm{SEC}}{ }^{d}(\mathrm{KDa})$ | $M_{\mathrm{w}} / M_{\mathrm{n}}{ }^{d}$ | $T_{\mathrm{g}} / T_{\mathrm{m}}{ }^{e}\left({ }^{\circ} \mathrm{C}\right)$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathbf{1}$ | $\mathbf{1}$ | rac -LA | $1: 3: 100$ | 94 | 4.70 | 6.06 | 1.04 | $40.0 /-$ |
| $\mathbf{2}$ | $\mathbf{2}$ | rac-LA | $1: 3: 100$ | 91 | 4.55 | 7.75 | 1.28 | $49.8 / 188.5$ |
| $\mathbf{3}$ | $\mathbf{1}$ | MAC | $1: 3: 100$ | 95 | 6.52 | 7.24 | 1.20 | $-10.5 /-$ |

${ }^{a}$ Polymerization conditions: $[\mathrm{M}]_{0}=0.5 \mathrm{M} ; \mathrm{CTA}=\mathrm{Ph}_{2} \mathrm{CHOH} ; T=90^{\circ} \mathrm{C}$; time $=24 \mathrm{~h}$; toluene $=2 \mathrm{~mL}$ ${ }^{b}$ Measured by ${ }^{1} \mathrm{H}$ NMR. ${ }^{c} M_{\mathrm{n}, \text { calcd }}=$ molar mass of $\mathrm{M} \times[\mathrm{M}]_{0} /[\mathrm{CTA}]_{0} \times$ conversion $\%+$ the molar mass of CTA. ${ }^{d}$ Molecular weight $\left(M_{\mathrm{n}}\right)$ and dispersity values $\left(M_{\mathrm{w}} / M_{\mathrm{n}}\right)$ determined by SEC in THF at $40{ }^{\circ} \mathrm{C}$ using polystyrene standards. ${ }^{e}$ Calculated by DSC measurement (Figure 4)

## Reactivity Ratio Calculation:

Table S2. Reactivity ratio calculation for copolymerization of L-LA and MAC catalyzed by

| entry | $\begin{aligned} & \text { L-LA } \\ & \left(f_{1}\right)^{a} \end{aligned}$ | $\begin{gathered} \text { MAC } \\ \left(f_{2}\right)^{a} \end{gathered}$ | $f_{1} / f_{2}$ | conversion |  | LA $\left(\mathrm{F}_{1}\right)^{b}$ | $\operatorname{MAC}\left(\mathrm{F}_{2}\right)^{b}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  |  | LA (\%) | MAC(\%) |  |  |
| 1 | 0.8 | 0.2 | 4 | 5.67 | 13.76 | 0.622 | 0.378 |
| 2 | 0.7 | 0.3 | 2.333 | 4.67 | 9.32 | 0.539 | 0.461 |
| 3 | 0.6 | 0.4 | 1.5 | 8.67 | 13.70 | 0.487 | 0.513 |
| 4 | 0.5 | 0.5 | 1 | 6.00 | 7.69 | 0.438 | 0.562 |
| 5 | 0.4 | 0.6 | 0.667 | 10.67 | 11.63 | 0.380 | 0.620 |
| 6 | 0.3 | 0.7 | 0.429 | 10.67 | 9.34 | 0.329 | 0.671 |

## complex 1.

${ }^{a} f_{1}$ and $f_{2}$ are defined as mole fractions of monomers LA and MAC in the feed and $f_{1}=1-f_{2}$.
${ }^{b} \mathrm{~F}_{1}$ and $\mathrm{F}_{2}$ represents the mole fraction of each monomer in the copolymer and $\mathrm{F}_{1}=1-\mathrm{F}_{2}$

$H=\frac{f_{1}^{2}\left(1-F_{1}\right)}{\left(1-f_{1}\right)^{2} F_{1}} \quad, \quad G=\frac{f_{1}\left(2 F_{1}-1\right)}{\left(1-f_{1}\right) F_{1}}$
Where $G=H r_{1}-r_{2}$, a plot of H versus G yields a straight line with slope $r_{1}$ and intercept $-r_{2}$.
$r_{\mathrm{L}-\mathrm{LA}}=0.217, r_{\mathrm{MAC}}=0.578$.

| entry | rac-LA | MAC <br> $\left(f_{1}\right)^{a}$ | $f_{1} / f_{2}$ | conversion |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  |  | LA (\%) | MAC $(\%)$ | LA $\left(\mathrm{F}_{1}\right)^{b}$ | MAC $\left(\mathrm{F}_{2}\right)^{b}$ |
| 1 | 0.7 | 0.3 | 2.333 | 4.81 | 9.80 | 0.534 | 0.466 |
| 2 | 0.6 | 0.4 | 1.5 | 4.75 | 10.07 | 0.414 | 0.586 |
| 3 | 0.5 | 0.5 | 1 | 3.52 | 7.70 | 0.314 | 0.686 |
| 4 | 0.45 | 0.55 | 0.818 | 5.67 | 12.71 | 0.267 | 0.733 |
| 5 | 0.4 | 0.6 | 0.667 | 3.53 | 7.98 | 0.228 | 0.772 |

Table S3. Reactivity ratio calculation for copolymerization of rac -LA and MAC catalyzed by complex 1.
${ }^{a} f_{1}$ and $f_{2}$ are defined as mole fractions of monomers LA and MAC in the feed and $f_{1}=1-f_{2}$.
${ }^{b} \mathrm{~F}_{1}$ and $\mathrm{F}_{2}$ represents the mole fraction of each monomer in the copolymer and $\mathrm{F}_{1}=1-\mathrm{F}_{2}$.


| entry | L-LA | MAC <br> $\left(f_{1}\right)^{a}$ | $f_{1} / f_{2}$ | conversion |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $\left(f_{2}\right)^{a}$ |  | LA (\%) | MAC $(\%)$ | LA $\left(\mathrm{F}_{1}\right)^{b}$ | MAC ( $\left.\mathrm{F}_{2}\right)^{b}$ |  |
| 1 | 0.55 | 0.45 | 1.222 | 11.37 | 4.30 | 0.764 | 0.236 |
| 2 | 0.5 | 0.5 | 1 | 11.67 | 4.33 | 0.729 | 0.271 |
| 3 | 0.45 | 0.55 | 0.818 | 11.55 | 4.11 | 0.697 | 0.303 |
| 4 | 0.4 | 0.6 | 0.667 | 14.09 | 4.54 | 0.674 | 0.326 |
| 5 | 0.3 | 0.7 | 0.429 | 16.00 | 4.62 | 0.597 | 0.403 |

$H=\frac{f_{1}^{2}\left(1-F_{1}\right)}{\left(1-f_{1}\right)^{2} F_{1}} \quad G=\frac{f_{1}\left(2 F_{1}-1\right)}{\left(1-f_{1}\right) F_{1}}$

Where $G=H r_{1}-r_{2}$, a plot of H versus G yields a straight line with slope $r_{1}$ and intercept $-r_{2}$. $r_{r a c-\mathrm{LA}}=0.584, r_{\mathrm{MAC}}=2.478$.

Table S4. Reactivity ratio calculation for copolymerization of L-LA and MAC catalyzed by complex 2.
${ }^{a} f_{1}$ and $f_{2}$ are defined as mole fractions of monomers LA and MAC in the feed and $f_{1}=1-f_{2}$.
${ }^{b} \mathrm{~F}_{1}$ and $\mathrm{F}_{2}$ represents the mole fraction of each monomer in the copolymer and $\mathrm{F}_{1}=1-\mathrm{F}_{2}$.

$H=\frac{f_{1}^{2}\left(1-F_{1}\right)}{\left(1-f_{1}\right)^{2} F_{1}} \quad, \quad G=\frac{f_{1}\left(2 F_{1}-1\right)}{\left(1-f_{1}\right) F_{1}}$

Where $G=H r_{1}-r_{2}$, a plot of H versus G yields a straight line with slope $r_{1}$ and intercept $-r_{2}$. $r_{\mathrm{L}-\mathrm{LA}}=2.035, r_{\mathrm{MAC}}=0.112$.

Table S5. Reactivity ratio calculation for copolymerization of rac -LA and MAC catalyzed by complex 2.
${ }^{a} f_{1}$ and $f_{2}$ are defined as mole fractions of monomers LA and MAC in the feed and $f_{1}=1-f_{2}$.
${ }^{b} \mathrm{~F}_{1}$ and $\mathrm{F}_{2}$ represents the mole fraction of each monomer in the copolymer and $\mathrm{F}_{1}=1-\mathrm{F}_{2}$.

| entry | rac-LA | MAC | $f_{1} / f_{2}$ | conversion |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $\left(f_{1}\right)^{a}$ | $\left(f_{2}\right)^{a}$ |  | LA (\%) | MAC $(\%)$ | LA $\left(\mathrm{F}_{1}\right)^{b}$ | MAC $\left(\mathrm{F}_{2}\right)^{b}$ |
| 1 | 0.8 | 0.2 | 4 | 13.58 | 7.89 | 0.873 | 0.127 |
| 2 | 0.7 | 0.3 | 2.333 | 11.82 | 6.22 | 0.816 | 0.184 |
| 3 | 0.6 | 0.4 | 1.5 | 11.67 | 5.59 | 0.758 | 0.242 |
| 4 | 0.5 | 0.5 | 1 | 10.11 | 5.53 | 0.646 | 0.354 |
| 5 | 0.4 | 0.6 | 0.667 | 11.52 | 5.08 | 0.602 | 0.398 |
| 6 | 0.3 | 0.7 | 0.429 | 11.95 | 5.48 | 0.483 | 0.517 |


$H=\frac{f_{1}^{2}\left(1-F_{1}\right)}{\left(1-f_{1}\right)^{2} F_{1}} \quad, \quad G=\frac{f_{1}\left(2 F_{1}-1\right)}{\left(1-f_{1}\right) F_{1}}$

Where $G=H r_{1}-r_{2}$, a plot of H versus G yields a straight line with slope $r_{1}$ and intercept $-r_{2}$.
$r_{r a c-\mathrm{LA}}=1.619, r_{\mathrm{MAC}}=0.283$.

