

***Electronic Supplementary Information***

**An effective amino acid-assisted growth of ultrafine palladium nanocatalysts  
toward superior synergistic catalysis for hydrogen generation from formic acid**

Cheng-Bin Hong,<sup>a,b</sup> De-Jie Zhu,<sup>a,b</sup> Dong-Dong Ma,<sup>a</sup> Xin-Tao Wu,<sup>a</sup> and Qi-Long

Zhu<sup>a,\*</sup>

<sup>a</sup> State Key Laboratory of Structure Chemistry, Fujian Institute of Research on the  
Structure of Matter, Chinese Academy of Science, Fuzhou 350002, China

<sup>b</sup> University of Chinese Academy of Sciences, Beijing 100049, China

\*Corresponding Author: [qlzhu@fjirsm.ac.cn](mailto:qlzhu@fjirsm.ac.cn)

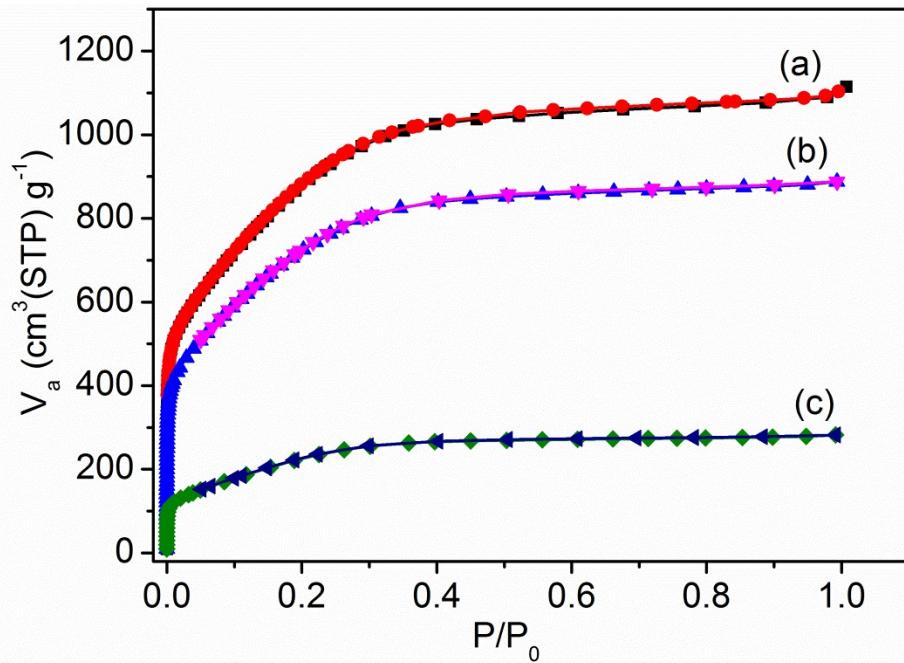
**Table S1.** Catalytic activities for hydrogen generation from formic acid catalyzed by various heterogeneous catalysts

Catalyst	Additive	Temp. (°C)	CO evolution	TOF (h <sup>-1</sup> )	Ref.
<b>Arg-Pd/MSC-30</b>	HCOONa	<b>60</b>	No	<b>5723</b>	This work
	None	<b>50</b>	No	<b>1365</b>	This work
<b>Pd/MSC-30</b>	HCOONa	50	No	2623	S1
<b>Au/ZrO<sub>2</sub> NCs</b>	NEt <sub>3</sub>	50	No	1593 <sup>a</sup>	S2
<b>Ag@Pd/C</b>	Aqueous	20	No	192	S3
<b>Pd-S-SiO<sub>2</sub></b>	Aqueous	85	No	719	S4
<b>AuPd@ED-MIL-101</b>	HCOONa	90	Yes	106	S5
<b>PdAu/C-CeO<sub>2</sub></b>	HCOONa	92	145 ppm	113.5	S6
<b>Ag<sub>42</sub>Pd<sub>58</sub></b>	Aqueous	50	No	328 <sup>a</sup>	S7
<b>Pd-B/C</b>	HCOONa	30	No	1184	S8
<b>PdAu@Au/C</b>	HCOONa	92	30 ppm	21.4	S9
<b>Co<sub>0.30</sub>Au<sub>0.35</sub>Pd<sub>0.35</sub></b>	Aqueous	25	No	80 <sup>a</sup>	S10
<b>Pd/APC</b>	HCOONa	55	No	2999	S11
<b>Pd/N-MSC-30-two-175</b>	HCOONa	60	No	8414	S12
<b>Pd<sub>0.6</sub>Ag<sub>0.4</sub>@ZrO<sub>2</sub>/C/rGO</b>	HCOONa	60	No	4500	S13

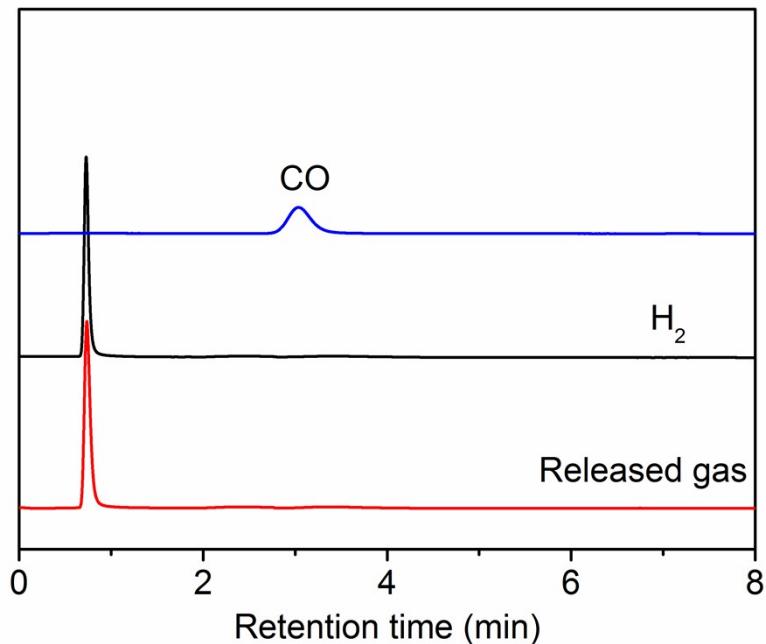
<sup>a</sup> Initial TOF values calculated at the initial stages of the catalytic reactions.

**Table S2.** ICP results of Pd content for Pd/MSC-30 and Arg-Pd/MSC-30

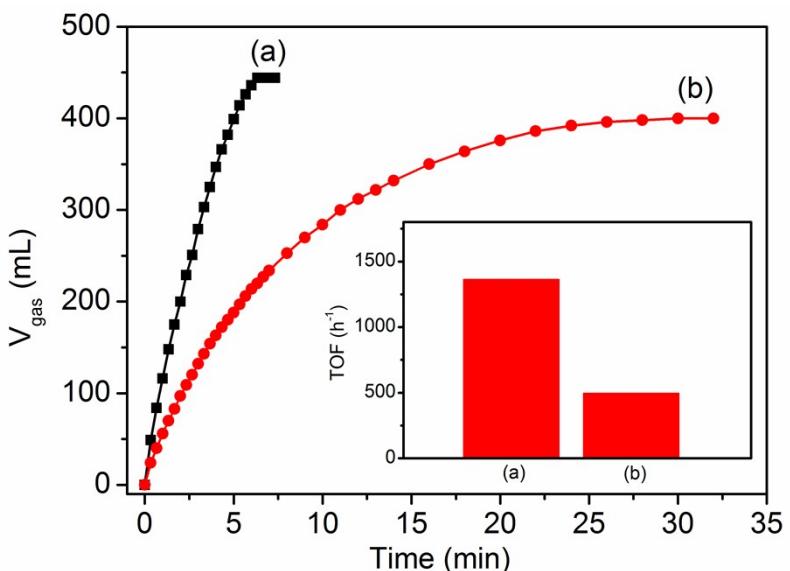
Sample	Pd content (wt%)
<b>Pd/MSC-30</b>	7.92
<b>Arg-Pd/MSC-30</b>	3.81
<b>Recycled Arg-Pd/MSC-30</b>	3.75



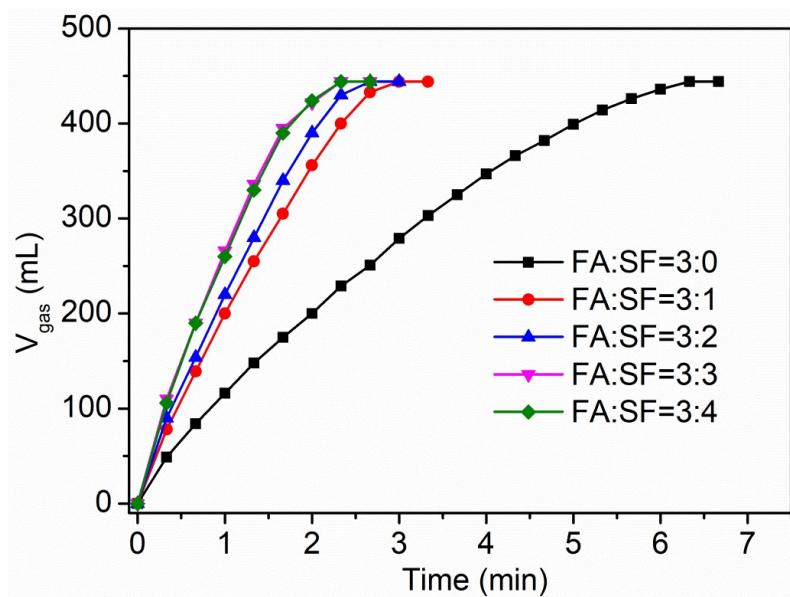
**Figure S1.**  $\text{N}_2$  sorption isotherms of (a) MSC-30, (b) Pd/MSC-30, and (c) Arg-Pd/MSC-30 at 77K.



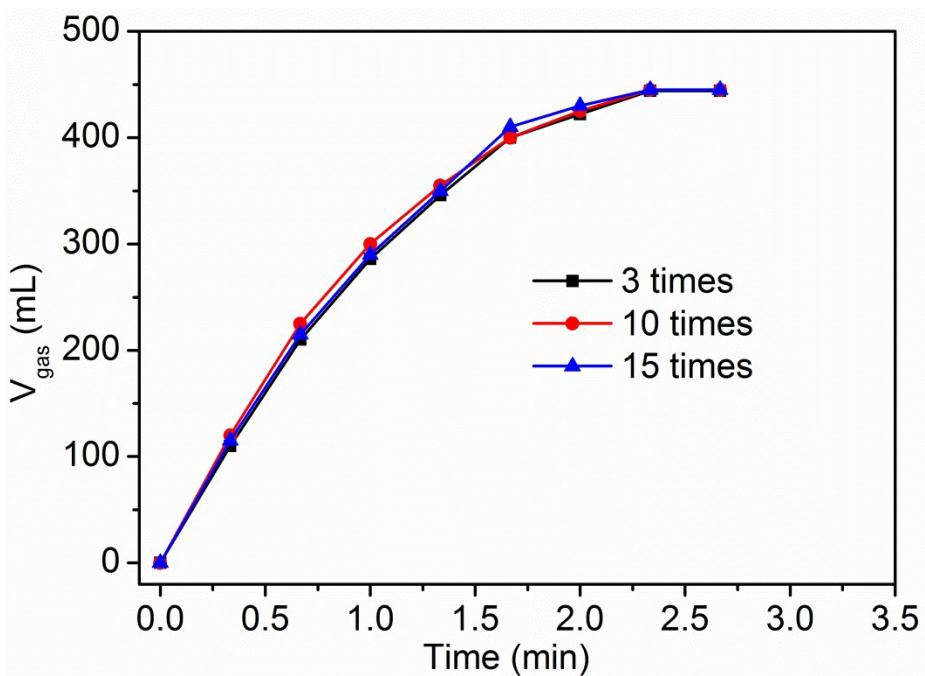
**Figure S2.** Gas chromatograms of CO and  $\text{H}_2$  as reference gases and the released gas from the dehydrogenation of FA over Arg-Pd/MSC-30 ( $n_{\text{Pd}}/n_{\text{FA}} = 0.01$ ,  $\text{FA/SF} = 1:1$ , 323 K).



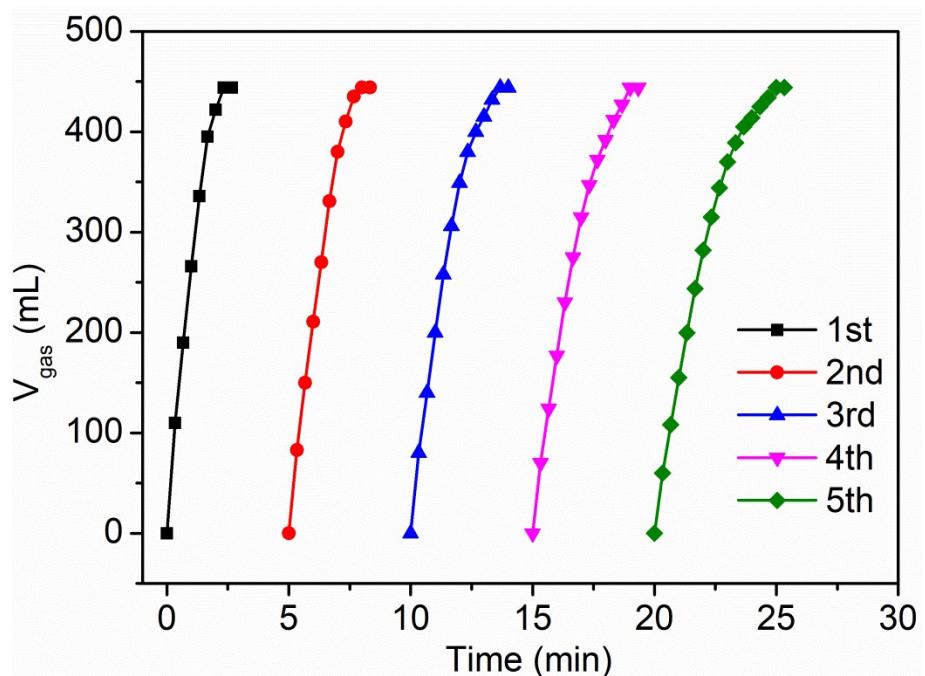
**Figure S3.** Volume of the generated gas ( $\text{CO}_2 + \text{H}_2$ ) versus time for the dehydrogenation of pure FA over the as-prepared (a) Arg-Pd/MSC-30 and (b) Pd/MSC-30 ( $n_{\text{Pd}}/n_{\text{FA}} = 0.01$ , 323 K,  $n_{\text{FA}} = 9.0$  mmol). Insert: corresponding TOF values for dehydrogenation of pure FA over the Arg-Pd/MSC-30 and Pd/MSC-30 catalysts.



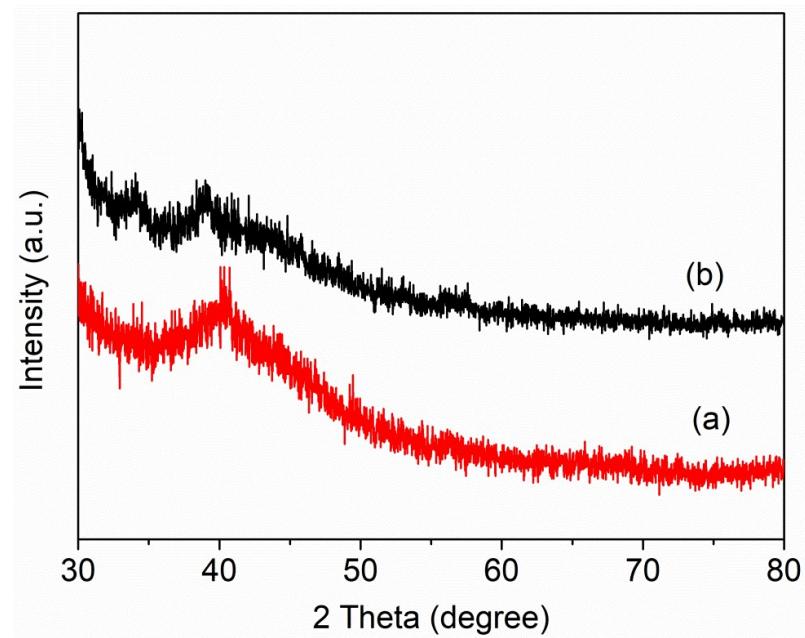
**Figure S4.** Volume of the generated gas ( $\text{CO}_2 + \text{H}_2$ ) versus time for the dehydrogenation of FA with different FA/SF molar ratios over the as-prepared Arg-Pd/MSC-30 catalyst ( $n_{\text{Pd}}/n_{\text{FA}} = 0.01$ , 323 K).



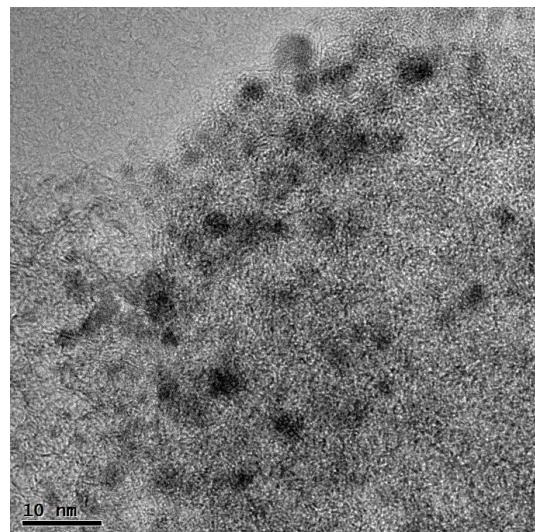
**Figure S5.** Volume of the generated gas ( $\text{CO}_2 + \text{H}_2$ ) versus time for the dehydrogenation of FA with over the as-prepared Arg-Pd/MSC-30 catalyst washed with different times after reduction ( $n_{\text{Pd}}/n_{\text{FA}} = 0.01$ , 323 K).



**Figure S6.** Durability test for the dehydrogenation of FA over Arg-Pd/MSC-30 ( $n_{\text{Pd}}/n_{\text{FA}} = 0.01$ , FA/SF = 1:1, 323 K).



**Figure S7.** PXRD patterns of Arg-Pd/MSC-30 (a) before and (b) after catalysis.



**Figure S8.** TEM image of Arg-Pd/MSC-30 after catalysis

## References

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