

## Support Information

### **Amine-functionalized mesoporous silica-supported PdIr catalyst: boosting room-temperature hydrogen generation from formic acid**

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**Table S1** Catalytic activities of different heterogeneous catalysts.

### Reference

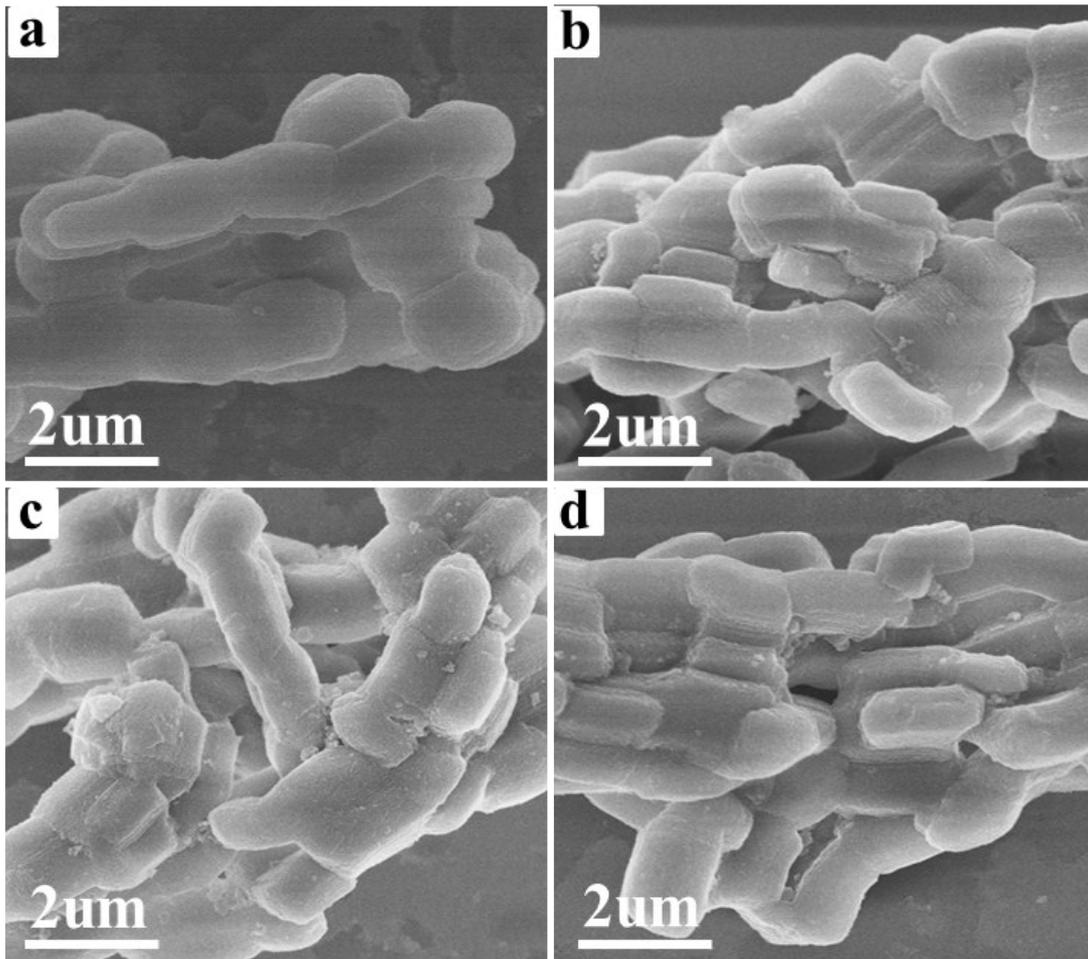
## **Experimental Section**

### **Synthesis of SBA-15**

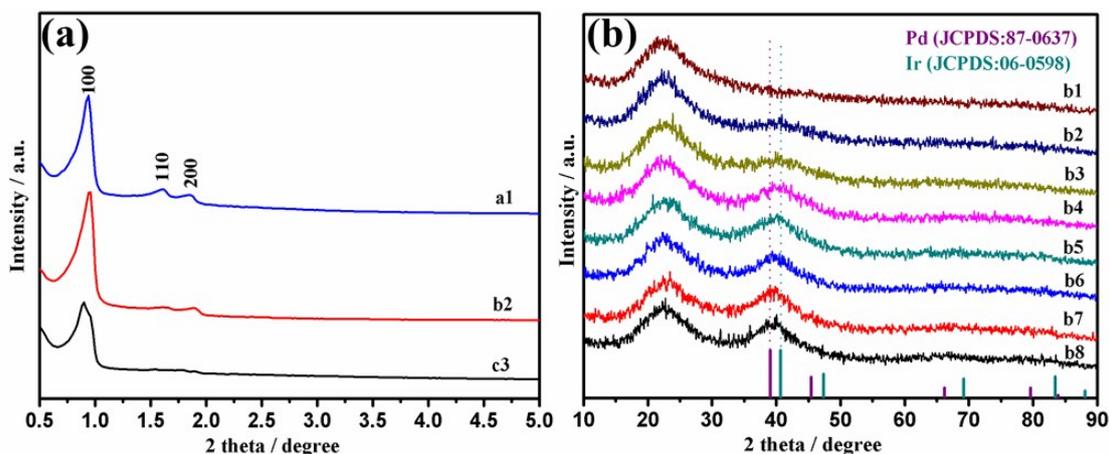
According to previous work,<sup>S1</sup> SBA-15 was prepared via a supramolecular self-assembly method. Typically, Pluronic® 123 (4.0 g) was dissolved in 94 mL deionized water, and stirred for 2 h at 313 K. Subsequently, HCl (20 mL) and TEOS (8.8 g) were added into above mixture, which was stirred continuously for 24 h at 313 K. The mixture was put into an autoclave and hydrothermally treated at 373 K for 24 h. Then white precipitate was collected by filtration, washed with copious amount of deionized water until neutral pH and dried at 333 K overnight. The organic template was removed by calcination at 823 K for 6 h to obtain the SBA-15 support.

### **Synthesis of SBA-15-NH<sub>2</sub>**

Functionalization of SBA-15 with amine groups was referring to a reported procedure.<sup>S2</sup> 1.0 g of SBA-15 was mixed with 6 mL of APTES in 60 mL of anhydrous toluene after treated at 378 K for 12 h. The resulting slurry was allowed to stir and reflux for 24 h at 353 K under the nitrogen atmosphere. The SBA-15-NH<sub>2</sub> was obtained as a white precipitate after washed with ethanol and dried at 313 K under vacuum overnight. In addition, to obtain varying -NH<sub>2</sub> groups loading on SBA-15, varying dosage of APTES (1.5 mL, 3 mL, 6 mL, 9 mL, and 12 mL) was added.

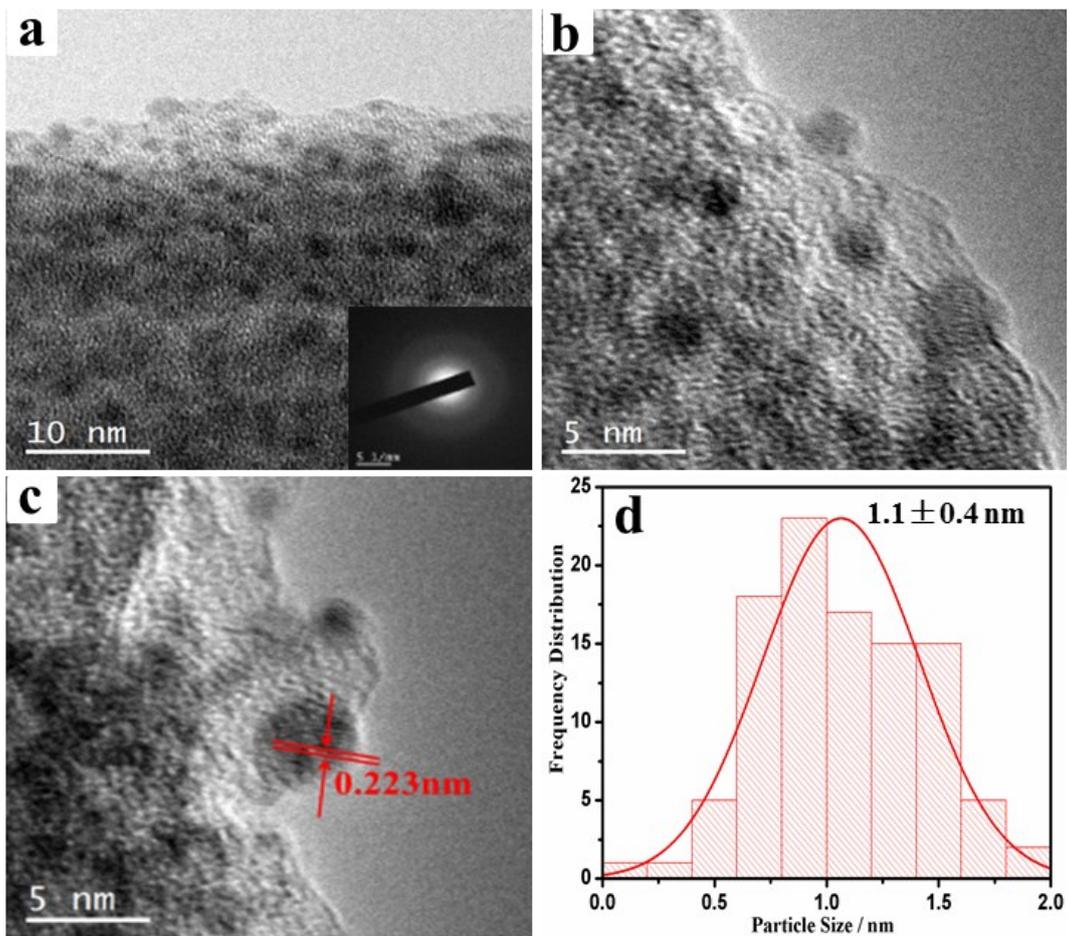


**Figure S1.** SEM images of the (a) SBA-15, (b) SBA-15-NH<sub>2</sub>, (c) fresh-prepared Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs, and (d) Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs after reusability test.

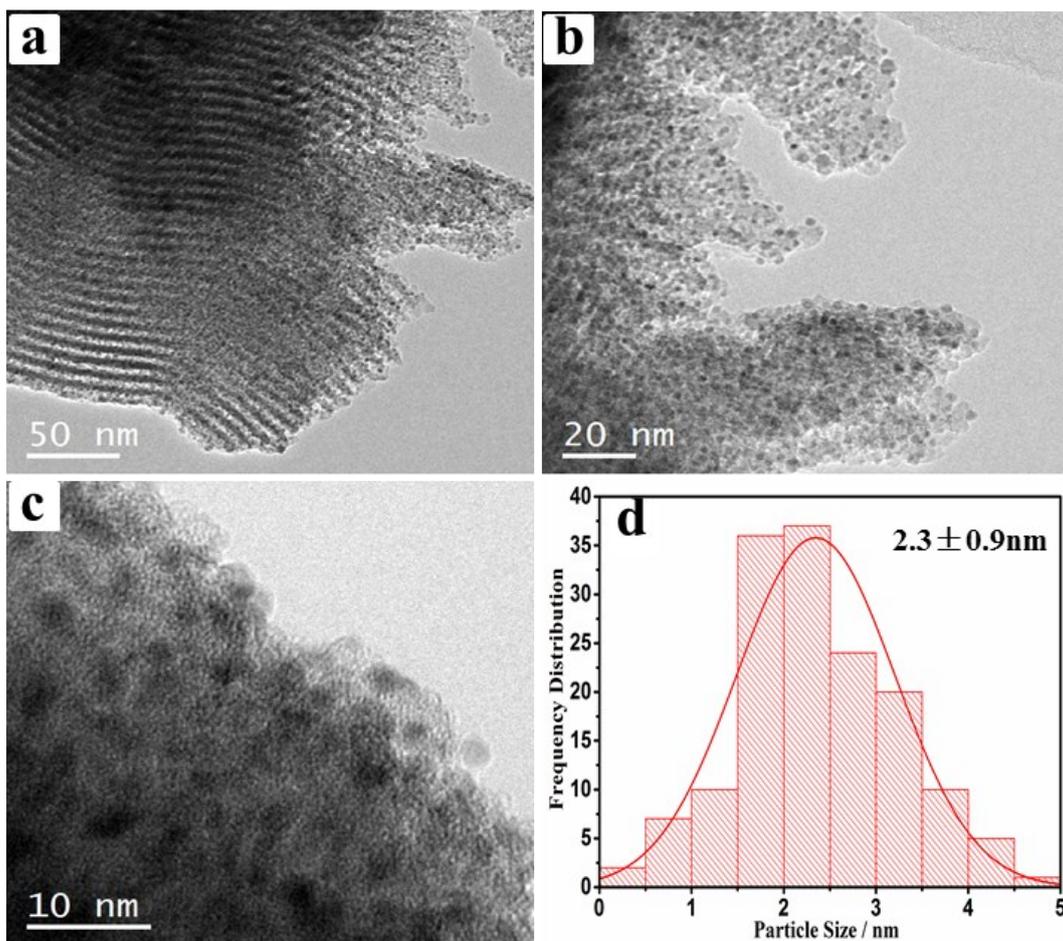


**Figure S2.** (a) Small-angle XRD patterns of (a1) SBA-15, (a2) SBA-15-NH<sub>2</sub>, and (a3) Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs; (b) Wide-angle XRD patterns of (b1) Ir/SBA-15-NH<sub>2</sub>, (b2) Pd<sub>0.2</sub>Ir<sub>0.8</sub>/SBA-15-NH<sub>2</sub>, (b3) Pd<sub>0.4</sub>Ir<sub>0.6</sub>/SBA-15-NH<sub>2</sub>, (b4) Pd<sub>0.6</sub>Ir<sub>0.4</sub>/SBA-15-NH<sub>2</sub>, (b5) Pd<sub>0.8</sub>Ir<sub>0.2</sub>/SBA-15-NH<sub>2</sub>, (b6) Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub>, (b7) Pd<sub>0.9</sub>Ir<sub>0.1</sub>/SBA-15-NH<sub>2</sub>, and (b8) Pd/SBA-15-NH<sub>2</sub> NCs.

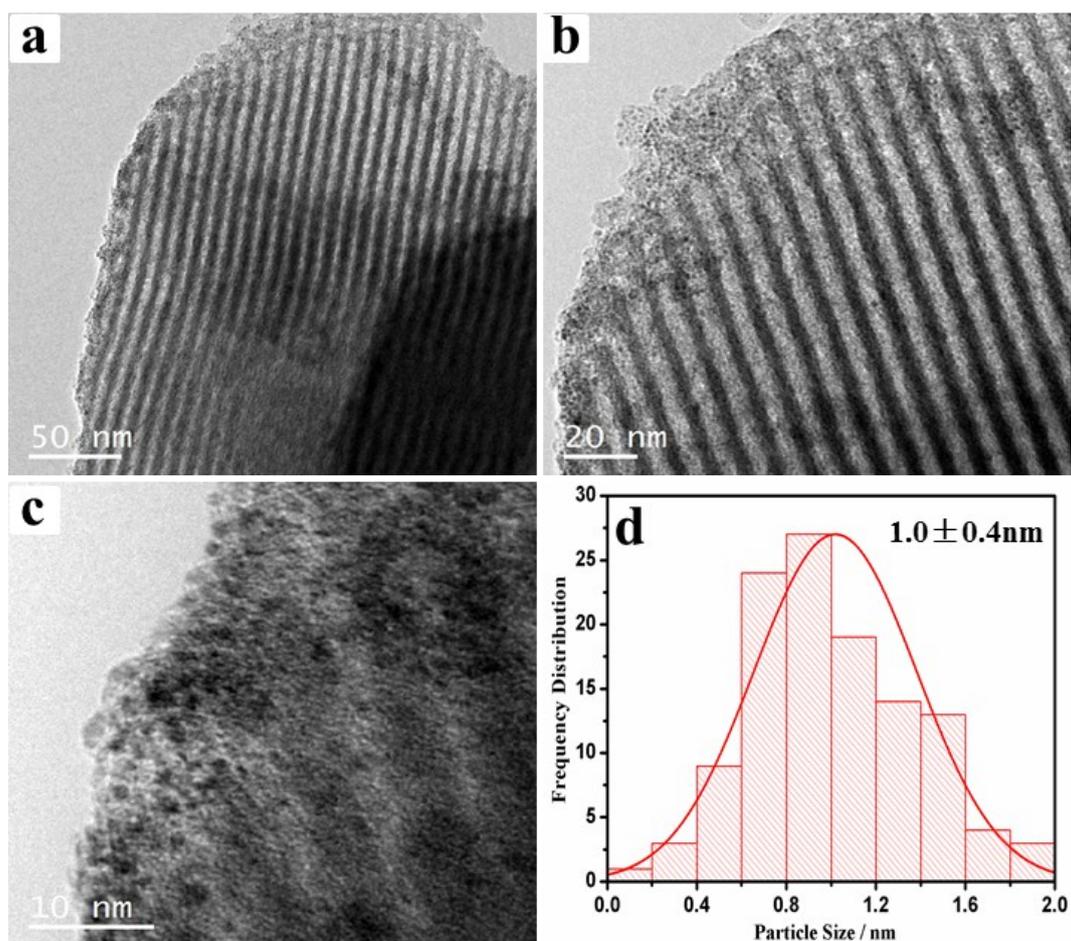
X-ray diffraction (XRD) was applied to investigate the detailed crystal structure of the as-prepared specimens. Figure S2a shows the small-angle XRD patterns of the SBA-15, SBA-15-NH<sub>2</sub>, and Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs. It can be seen that the three peaks at  $2\theta = 0.90^\circ$ ,  $1.59^\circ$ , and  $1.89^\circ$  are observed for all catalyst samples, which can be attributed to the (100), (110), and (200) planes of the ordered two-dimensional hexagonal mesoporous structure. Moreover, the framework of SBA-15 is maintained after the APTES functionalization and the loading of PdIr NPs, which agrees very well with the results measured by nitrogen adsorption-desorption isotherms (Figure 1) and FT-IR spectra (Figure 3a). The wide-angle XRD patterns (Figure S2b) shows that the strong and broad diffraction patterns at  $2\theta = 15\text{--}35^\circ$  can be attributed to the amorphous silica. Besides the diffraction of amorphous silica, the peaks between those of metallic Pd (111) (JCPDS: 87-0637) and Ir (111) (JCPDS: 06-0598) are also observed for the specimens, suggesting the formation of PdIr alloy structure.



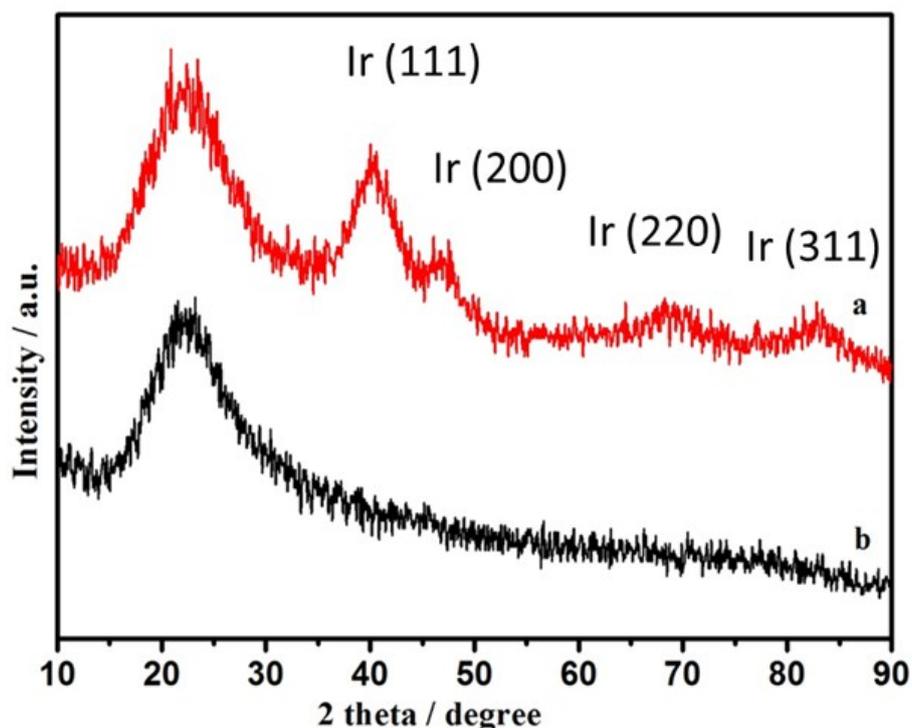
**Figure S3.** (a-c) High-resolution TEM images (inset of a) corresponding SAED pattern, and (d) particle distribution of the Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs.



**Figure S4.** (a-c) TEM images and (d) particle distribution of Pd/SBA-15-NH<sub>2</sub> NCs.

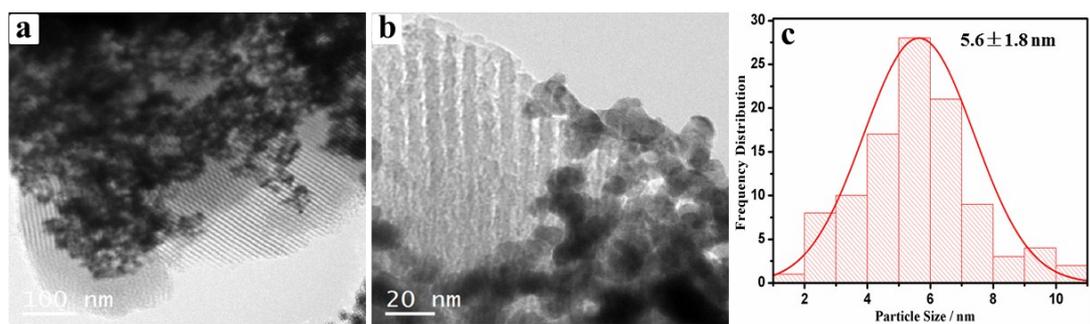


**Figure S5.** (a-c) TEM images and (d) particle distribution of Ir/SBA-15-NH<sub>2</sub> NCs.

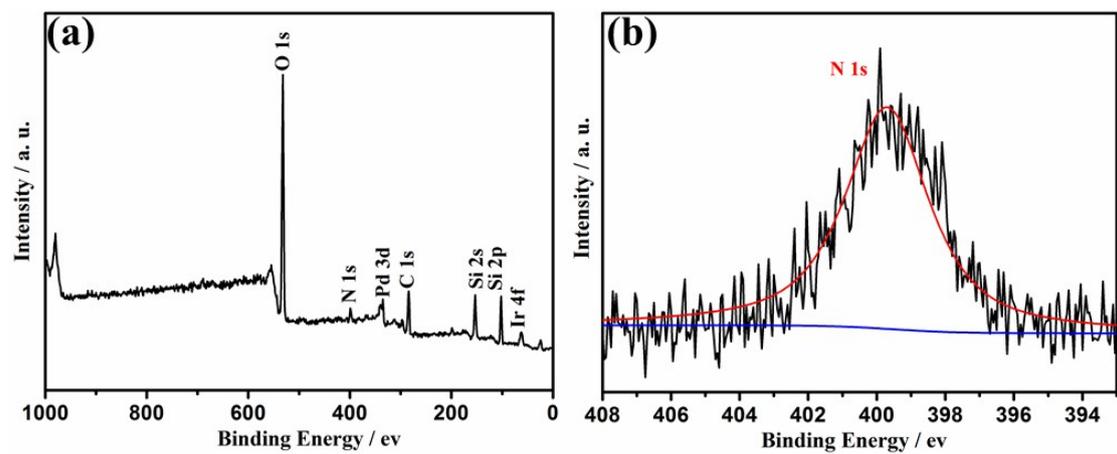


**Figure S6.** Wide-angle XRD patterns for the Ir/SBA-15-NH<sub>2</sub> NCs (a) after and (b) before treated at 823 K for 4 h in Ar atmosphere.

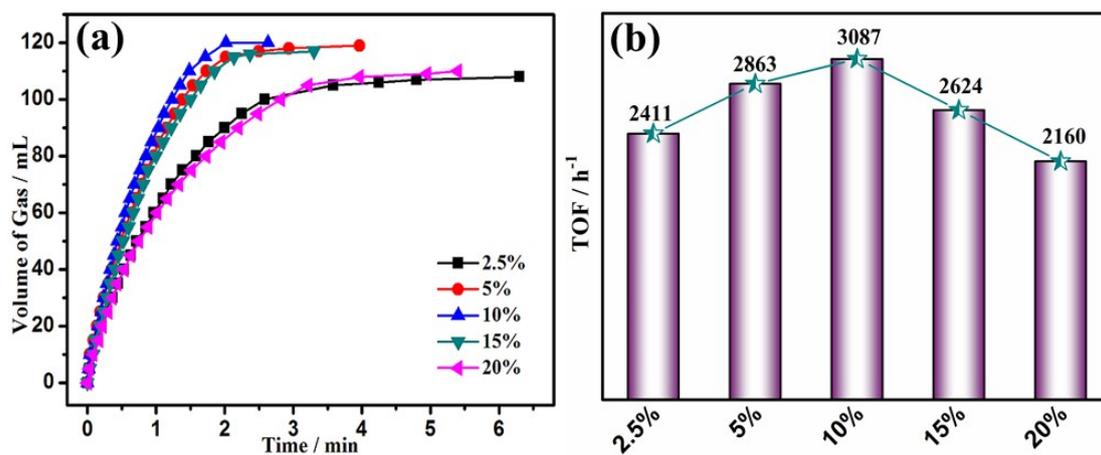
As shown in Figure S6, the diffraction peaks of metallic Ir was absent in the Ir/SBA-15-NH<sub>2</sub> NCs. It can be attributed to the high dispersion of Ir NPs on SBA-15-NH<sub>2</sub> with very small particle size and low crystallinity. The TEM images (Figure S5) confirmed that the Ir NPs are well dispersed on SBA-15-NH<sub>2</sub>. After Ir/SBA-15-NH<sub>2</sub> NCs was treated at 823 K for 4 h in Ar atmosphere, the typically diffraction peaks of metallic Ir at  $2\theta = 40.6^\circ$ ,  $47.3^\circ$ ,  $69.14^\circ$ , and  $83.4^\circ$  were appeared, and the peaks are indexed as (111), (200), (220), and (311) plans of metallic Ir (JCPDS: 06-0598), respectively.



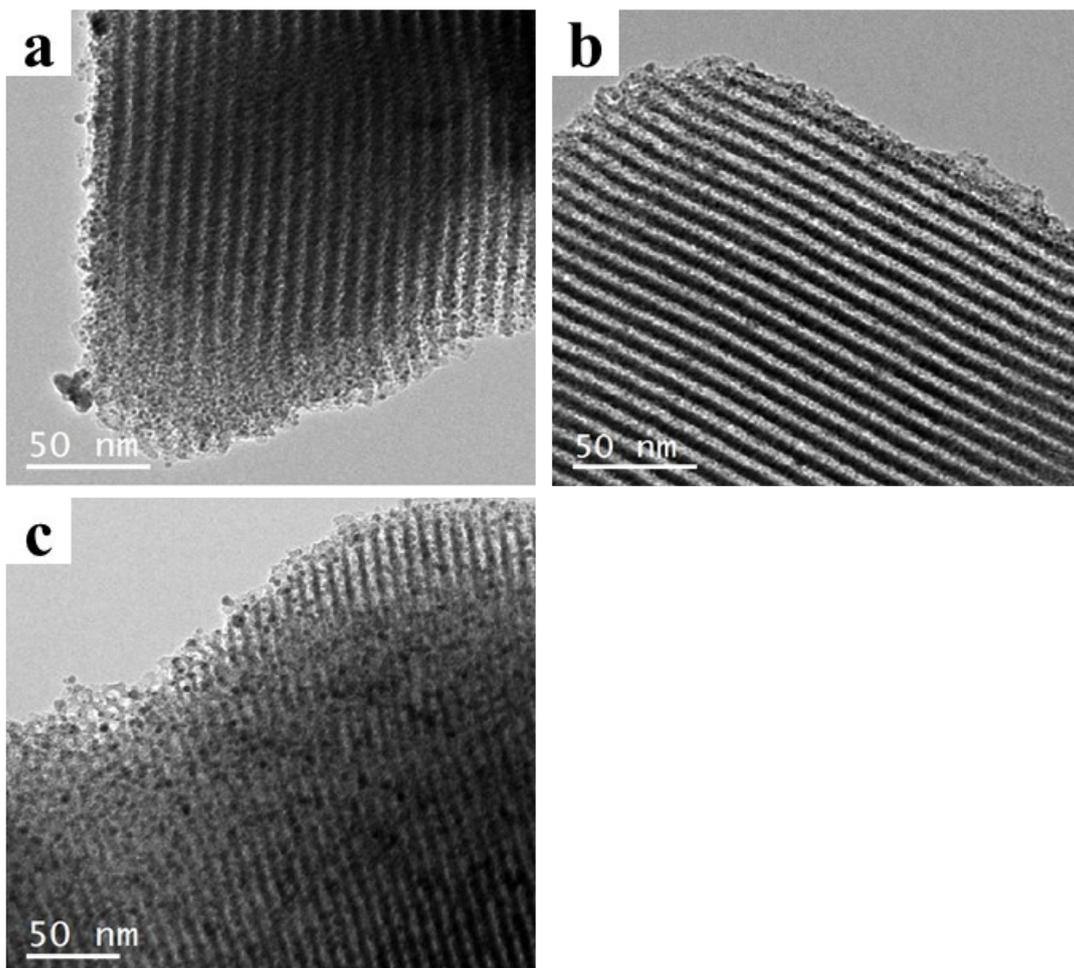
**Figure S7.** (a-b) TEM images and (c) particle distribution of Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15 NCs.



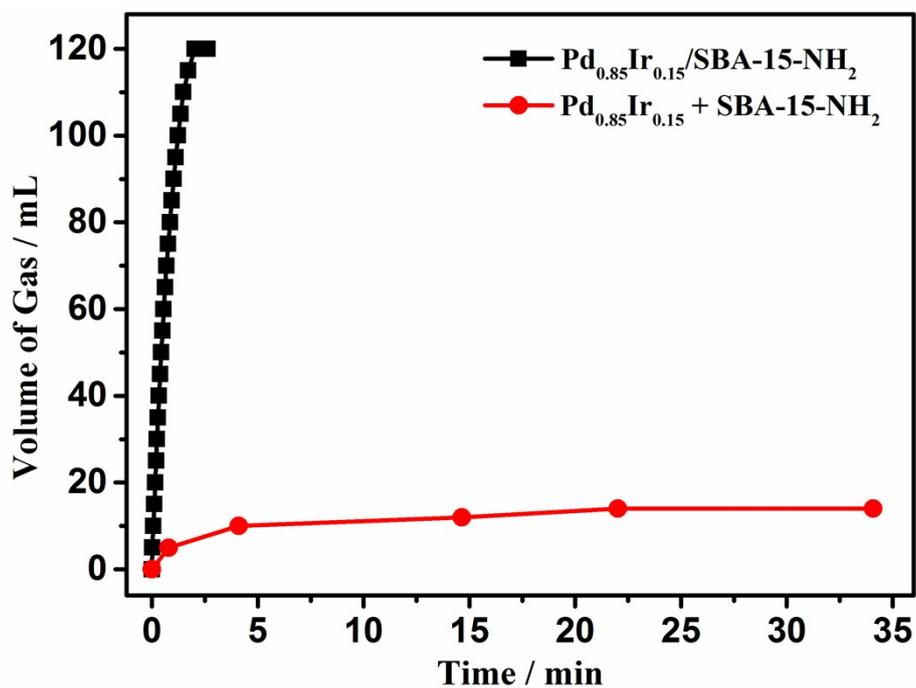
**Figure S8.** (a) The survey XPS spectrum of Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs and XPS spectra of N 1s in the Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs.



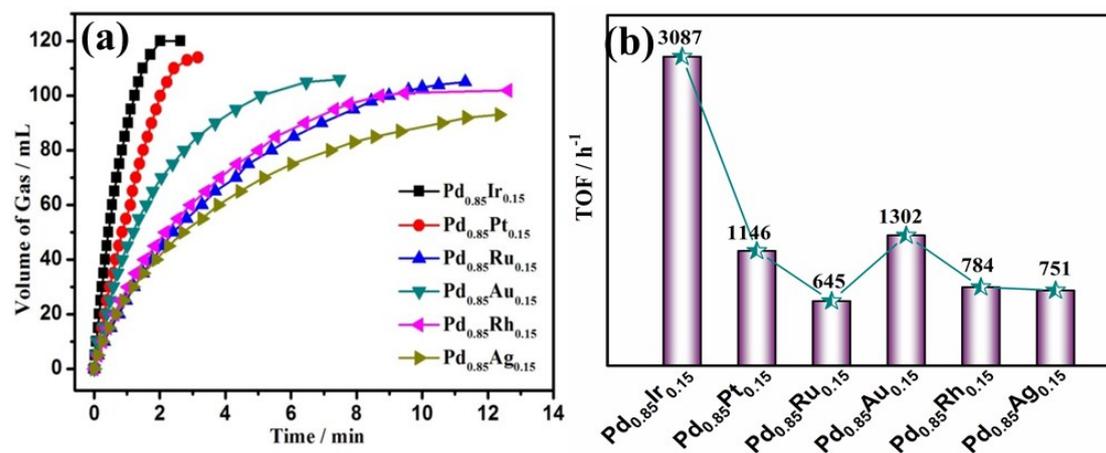
**Figure S9.** Volume of the generated gas (CO<sub>2</sub> + H<sub>2</sub>) versus time for the dehydrogenation of FA in FA-SF aqueous solution over Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs (a) with different metal loadings at 298 K and (b) the corresponding initial TOF values ( $n_{\text{PdIr}}/n_{\text{FA}} = 0.02$ , FA/SF=1/3).



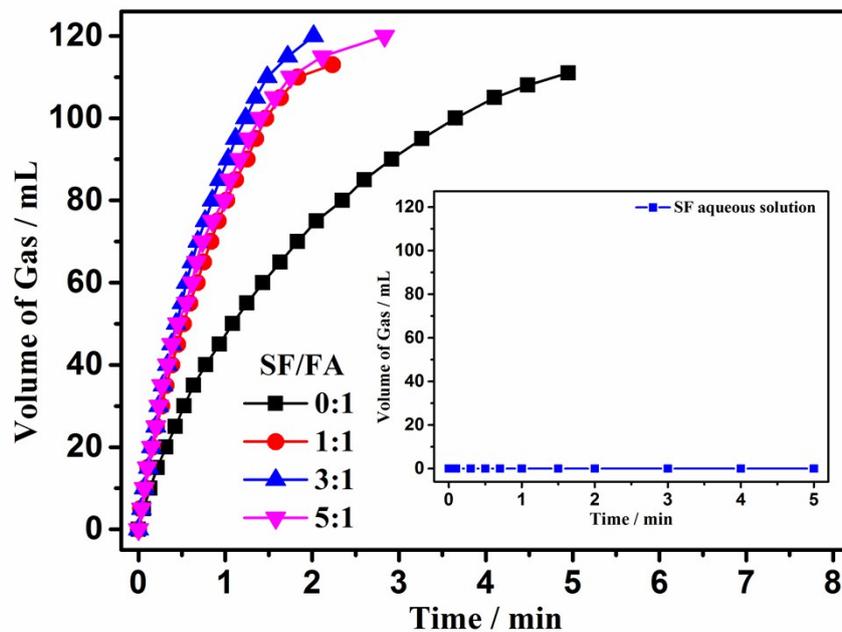
**Figure S10.** TEM images of Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15 NCs with different PdIr loading (a) 5 wt%, (b) 10 wt% and (c) 20wt %.



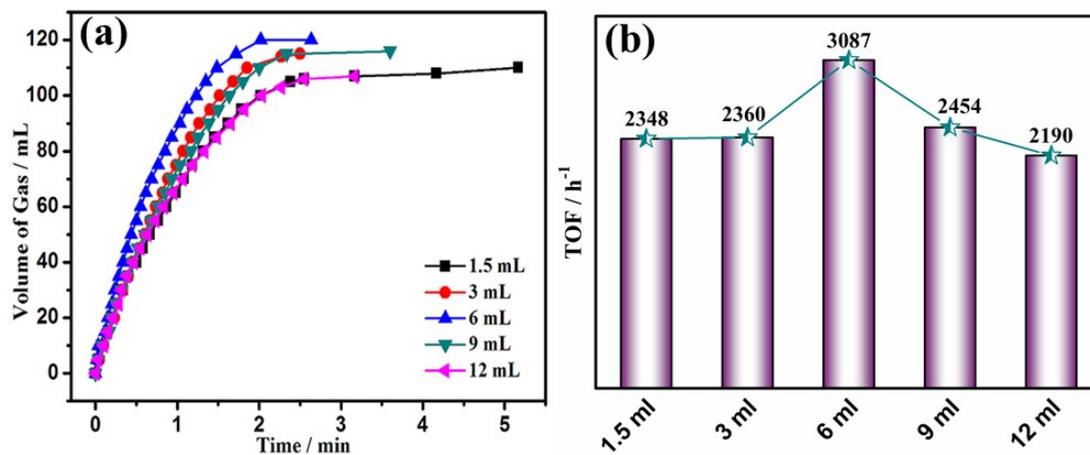
**Figure S11.** Volume of the generated gas (CO<sub>2</sub> + H<sub>2</sub>) versus time for the dehydrogenation of FA in FA-SF aqueous solution over physical mixture of Pd<sub>0.85</sub>Ir<sub>0.15</sub> and SBA-15-NH<sub>2</sub> and Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs at 298 K ( $n_{\text{PdIr}}/n_{\text{FA}} = 0.02$ , FA/SF=1/3, 10 wt% ).



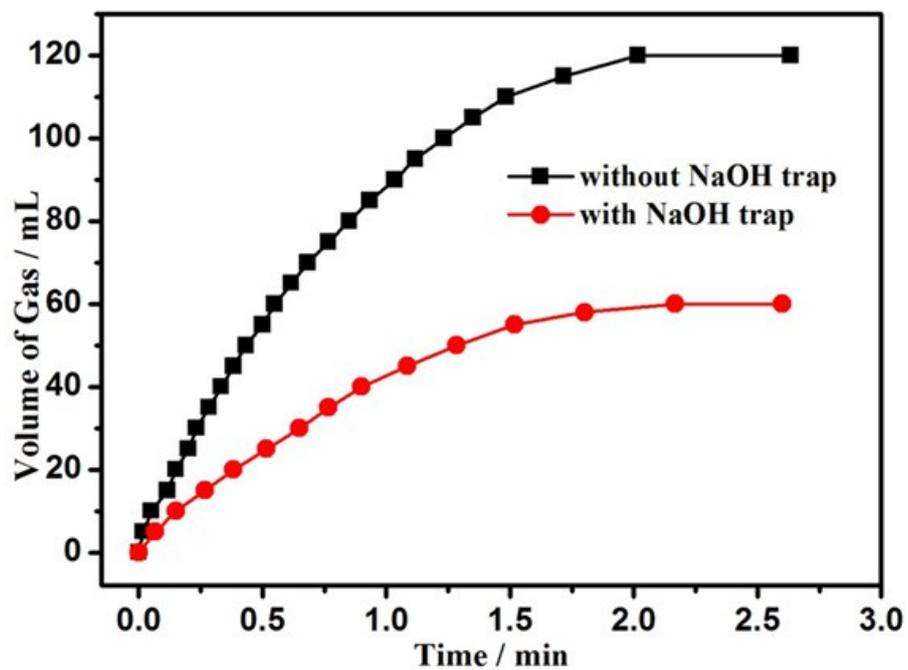
**Figure S12.** Volume of the generated gas (CO<sub>2</sub> + H<sub>2</sub>) versus time for the dehydrogenation of FA in FA-SF aqueous solution over Pd<sub>0.85</sub>M<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs (M = Ir, Pt, Ru, Au, Rh, and Ag) at 298 K and (b) the corresponding initial TOF value ( $n_{\text{PdIr}}/n_{\text{FA}} = 0.02$ , FA/SF=1/3, 10 wt% ).



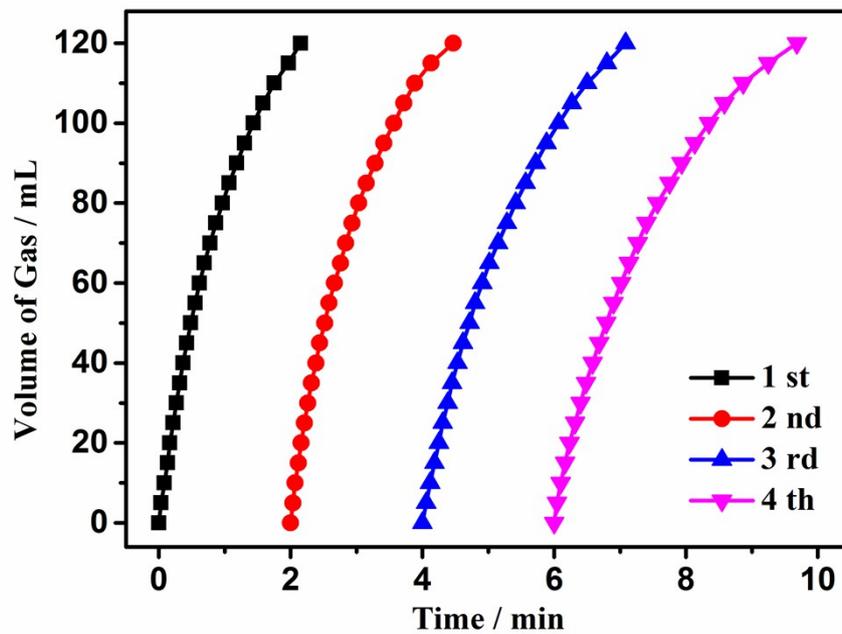
**Figure S13.** Volume of the generated gas ( $\text{CO}_2 + \text{H}_2$ ) versus time for the dehydrogenation of FA in the presence of different SF/FA molar ratios and (inset) pure SF aqueous solution over  $\text{Pd}_{0.85}\text{Ir}_{0.15}/\text{SBA-15-NH}_2$  NCs at 298 K ( $n_{\text{PdIr}}/n_{\text{FA}} = 0.02$ , 10 wt%).



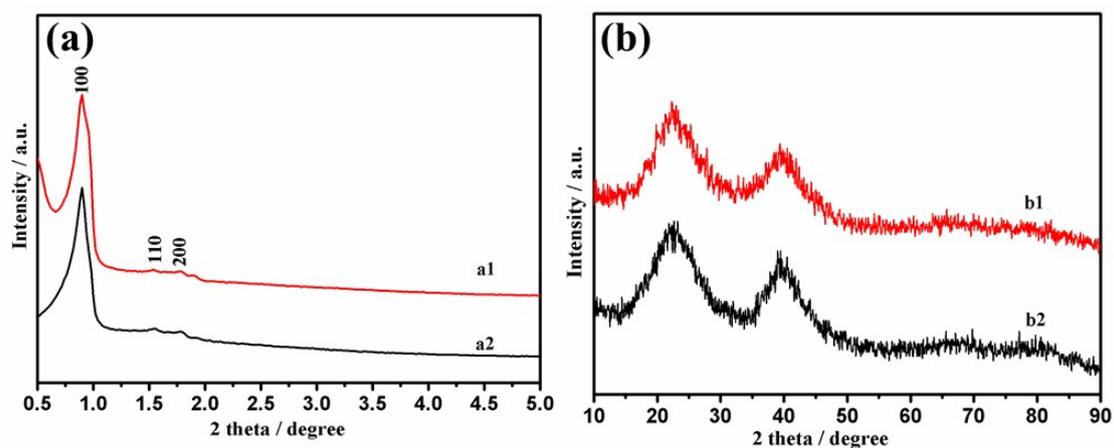
**Figure S14.** Volume of the generated gas (CO<sub>2</sub>+H<sub>2</sub>) versus time for the dehydrogenation of FA in FA-SF aqueous solution over Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs (a) with different volume of APTES at 298 K and (b) the corresponding initial TOF values ( $n_{\text{PdIr}}/n_{\text{FA}} = 0.02$ , FA/SF=1/3, 10 wt%).



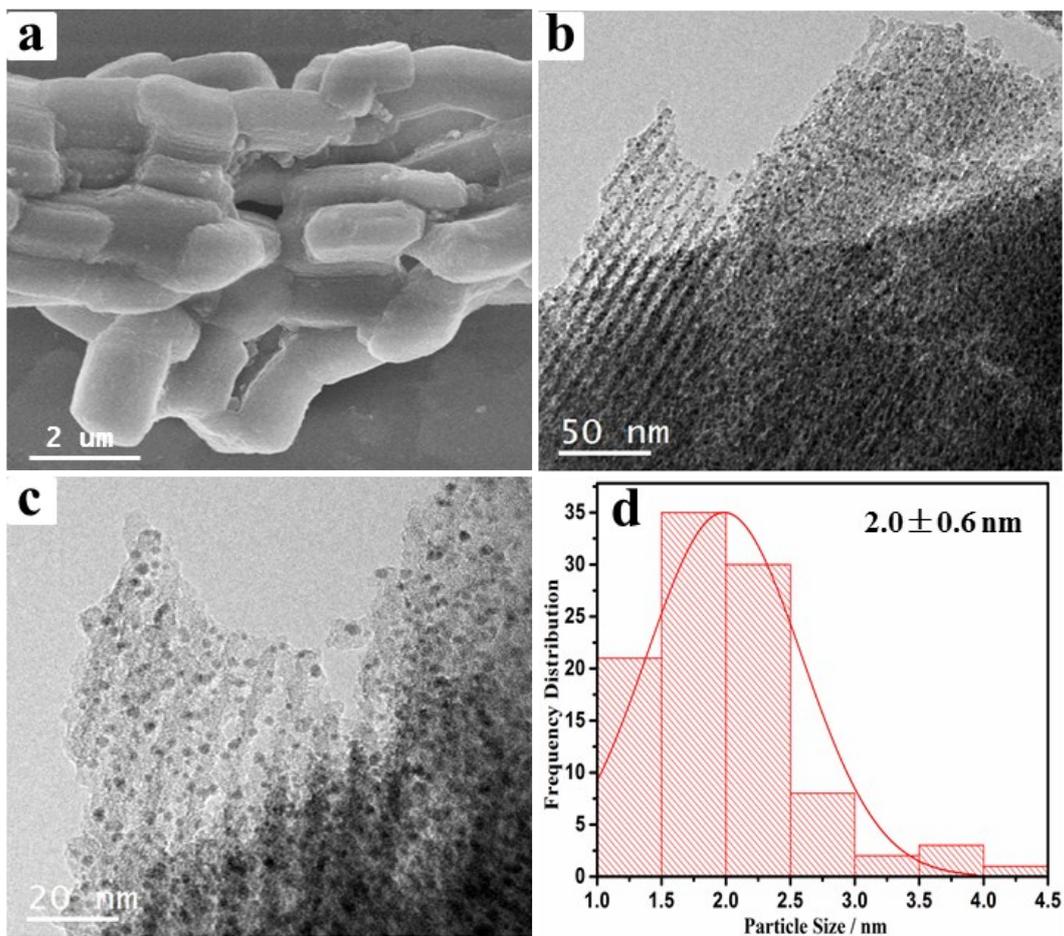
**Figure S15.** Volume of the generated gas ( $\text{CO}_2+\text{H}_2$ ) versus time for the dehydrogenation of FA in FA-SF aqueous solution over  $\text{Pd}_{0.85}\text{Ir}_{0.15}/\text{SBA-15-NH}_2$  NCs with/without NaOH trap at 298 K ( $n_{\text{PdIr}}/n_{\text{FA}} = 0.02$ , FA/SF=1/3, 10 wt%).



**Figure S16.** Reusability test of the optimized Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs for the dehydrogenation of FA in FA-SF aqueous solution at 298 K.



**Figure S17.** (a) Small-angle XRD patterns and (b) wide-angle XRD patterns for (a1, b1) the Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs and (a2, b2) Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs after reusability test.



**Figure S18.** (a) SEM images, (b,c) TEM images, and (d) particle distribution of Pd<sub>0.85</sub>Ir<sub>0.15</sub>/SBA-15-NH<sub>2</sub> NCs after reusability test.

**Table S1** Catalytic activities for the dehydrogenation of formic acid catalyzed by different heterogeneous catalysts.

Catalyst	Temp. (K)	additive	$E_a$ (kJ/mol)	TOF <sup>[a]</sup> (h <sup>-1</sup> )	Ref.
<b>Without Additive</b>					
Au <sub>0.5</sub> Pd <sub>0.5</sub> /NH <sub>2</sub> -N-rGO	298	None	--	4445.6	S3
Ag <sub>0.025</sub> Pd <sub>0.975</sub> /NH <sub>2</sub> -N-rGO	298	None	--	2556.2	S3
Pd <sub>0.85</sub> Ir <sub>0.15</sub> /SBA-15-NH <sub>2</sub>	298	None	26.7	1500	This work
Pd <sub>60</sub> Au <sub>40</sub> /ZrSBA-15-AP	298	None	42.5	1185	S4
PdAu-MnO <sub>x</sub> /N-SiO <sub>2</sub>	298	None	26.2	785	S5
SBA-15-Amine/Pd	299	None		377	S2
CoAuPd/DNA-rGO	298	None		85	S6
AuPd-CeO <sub>2</sub> /N-rGO	298	None		52.9	S7
Pd-MnO <sub>x</sub> /SiO <sub>2</sub> -NH <sub>2</sub>	323	None		1300	S8
<b>With Additive</b>					
Pd <sub>0.85</sub> Ir <sub>0.15</sub> /SBA-15-NH <sub>2</sub>	298	SF	26.7	3087	This work
Pd@CN900K	298	SF	46.9	1963 <sup>[b]</sup>	S9
Au <sub>1</sub> Pd <sub>1.5</sub> /MIL-101-NH <sub>2</sub>	298	SF	32.5	526 <sup>[b]</sup>	S10
Au <sub>0.28</sub> Pd <sub>0.47</sub> Co <sub>0.25</sub> /MIL-101-NH <sub>2</sub>	298	SF	32.5	347 <sup>[b]</sup>	S11
Au <sub>2</sub> Pd <sub>3</sub> @(P)N-C	303	SF	34.8	5400 <sup>[b]</sup>	S12
Pd <sub>1</sub> Au <sub>1</sub> /72-LA	303	SF	34.4	3583 <sup>[b]</sup>	S13
In situ-Pd@MSC	303	SF	31.7	2965	S14
Pd@SS-CNR	303	SF	38.8	1878 <sup>[b]</sup>	S15
(Co <sub>6</sub> )Ag <sub>0.1</sub> Pd <sub>0.9</sub> /RGO	323	SF	43.1	2739 <sup>[b]</sup>	S16
Au <sub>2</sub> Pd <sub>8</sub> /SBA-15-Amine	323	SF	47.6	1786	S17
Pd <sub>0.58</sub> Ni <sub>0.18</sub> Ag <sub>0.24</sub> /C	323	SF	20.5	85	S18
Pd <sub>0.85</sub> Ir <sub>0.15</sub> /SBA-15-NH <sub>2</sub>	328	SF	26.7	8248	This work
Pd <sub>0.6</sub> Ag <sub>0.4</sub> @ZrO <sub>2</sub> /C/rGO	333	SF	50.1	4500	S19
AuPd@ED-MIL-101	363	SF	--	106	S20
PdAu@Au/C	365	SF	--	59.6	S21

[a] Initial TOF values calculated on initial reaction time or initial conversion of FA.

[b] TOF values calculated on the complete time of gas releasing.

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