

SUPPLEMENTARY INFORMATION

Nano ferrite (AFe_2O_4 , A = Zn, Co, Mn, Cu) as efficient catalysts for catalytic ozonation of toluene

Hongbin Jiang, Xiaochen Xu*, Rao Zhang, Yun Zhang*, Jie Chen, Fenglin Yang

Key Laboratory of Industrial Ecology and Environmental Engineering, Ministry of Education,

School of Environmental Science and Technology, Dalian University of Technology, Linggong

road 2#, Dalian 116024, China.

Corresponding author:

Dr. Xiaochen Xu, Dalian University of Technology, Linggong road 2#, Dalian 116024, China.

Email: xxcep@dlut.edu.cn

Dr. Yun Zhang, Dalian University of Technology, Linggong road 2#, Dalian 116024, China.

Email: zhangyun@dlut.edu.cn

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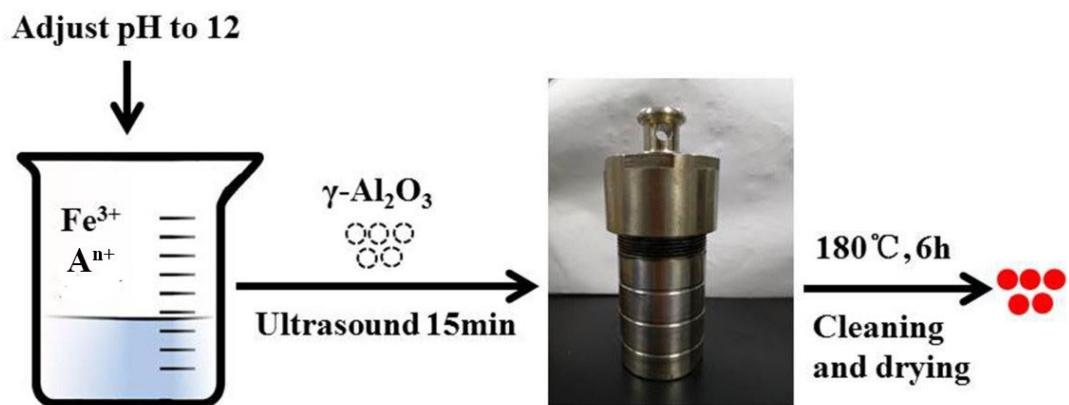


Fig. S1. Schematic illustration of the synthesis of $\text{AFe}_2\text{O}_4/\gamma\text{-Al}_2\text{O}_3$ catalysts.

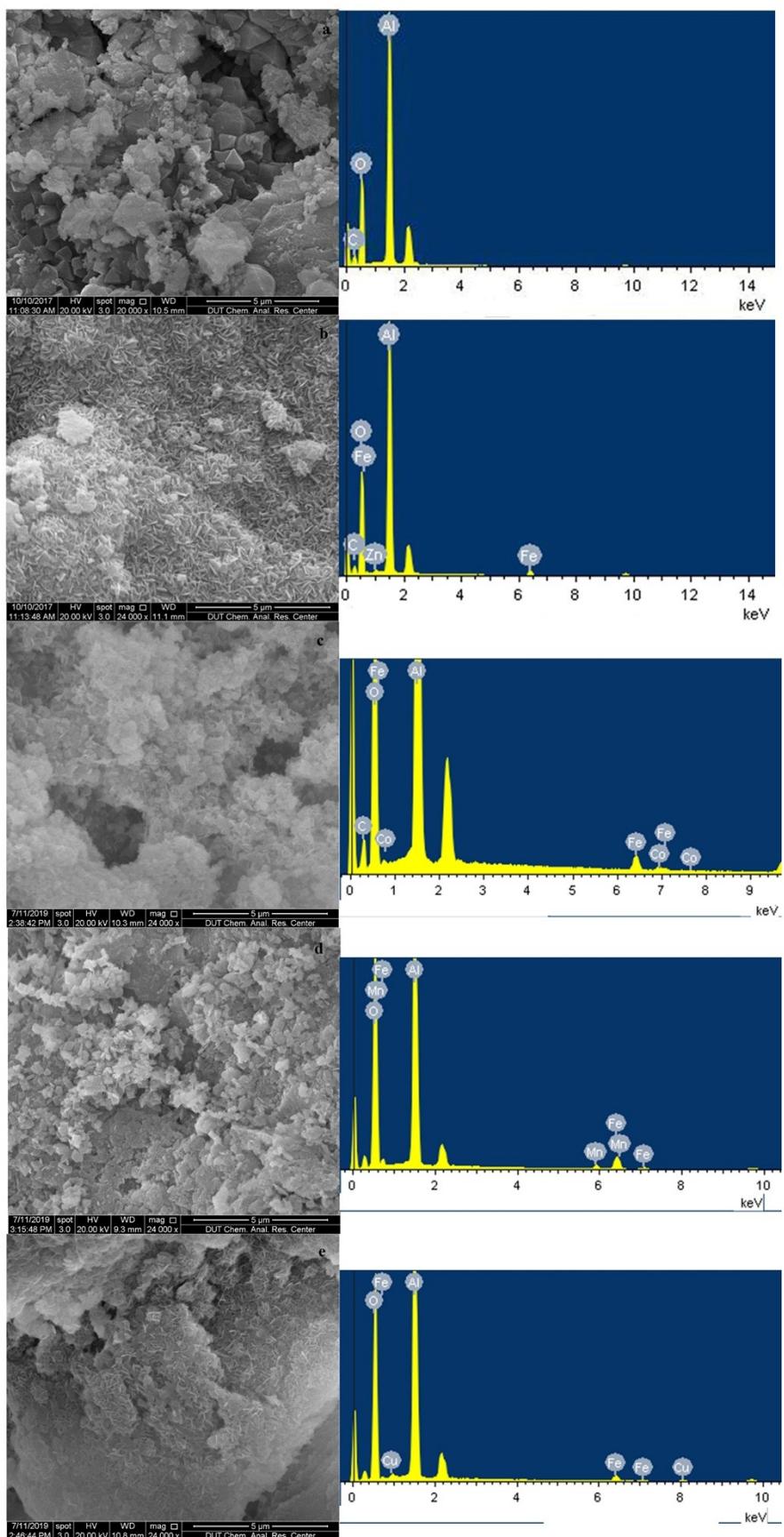


Fig. S2. SEM image and the corresponding EDS pattern of as-synthesized γ -Al₂O₃ supports and AFe₂O₄/ γ -Al₂O₃ catalysts.

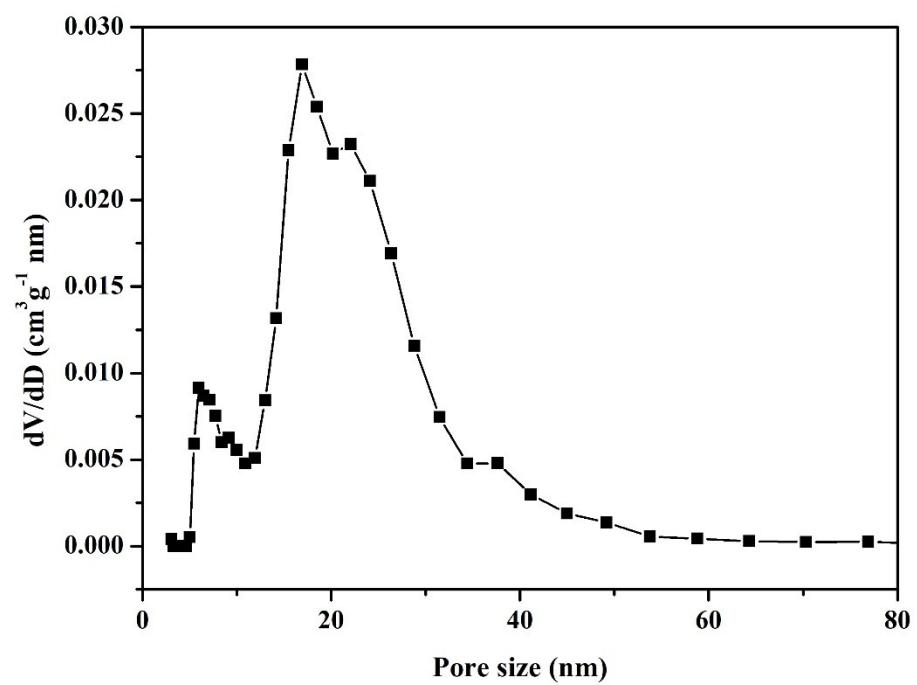


Fig. S3. Corresponding pore size distribution of γ -Al₂O₃ supports.

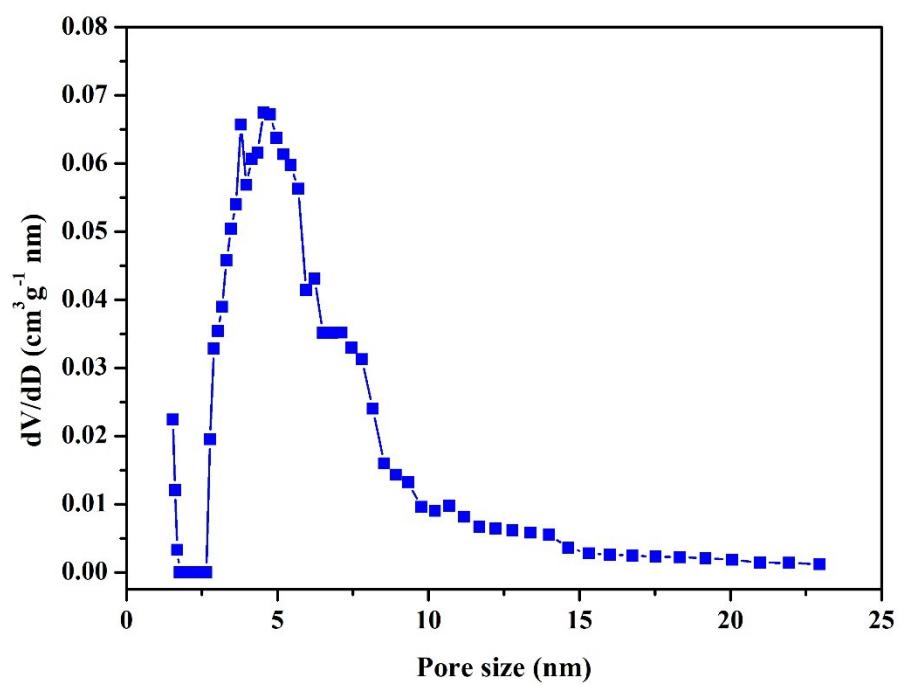


Fig. S4. Corresponding pore size distribution of ZnFe₂O₄/γ-Al₂O₃ catalysts.

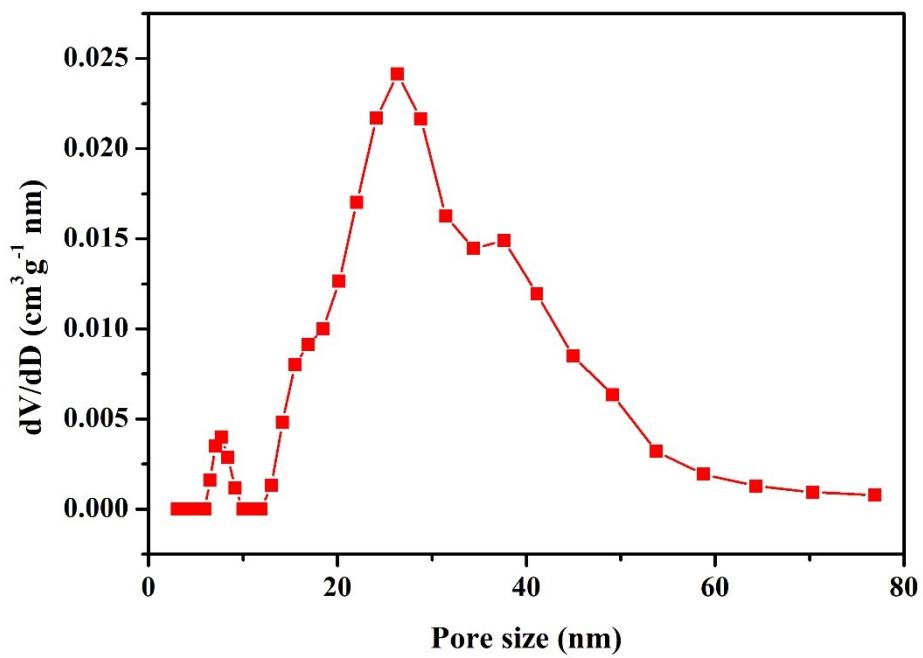


Fig. S5. Corresponding pore size distribution of CoFe₂O₄/γ-Al₂O₃ catalysts.

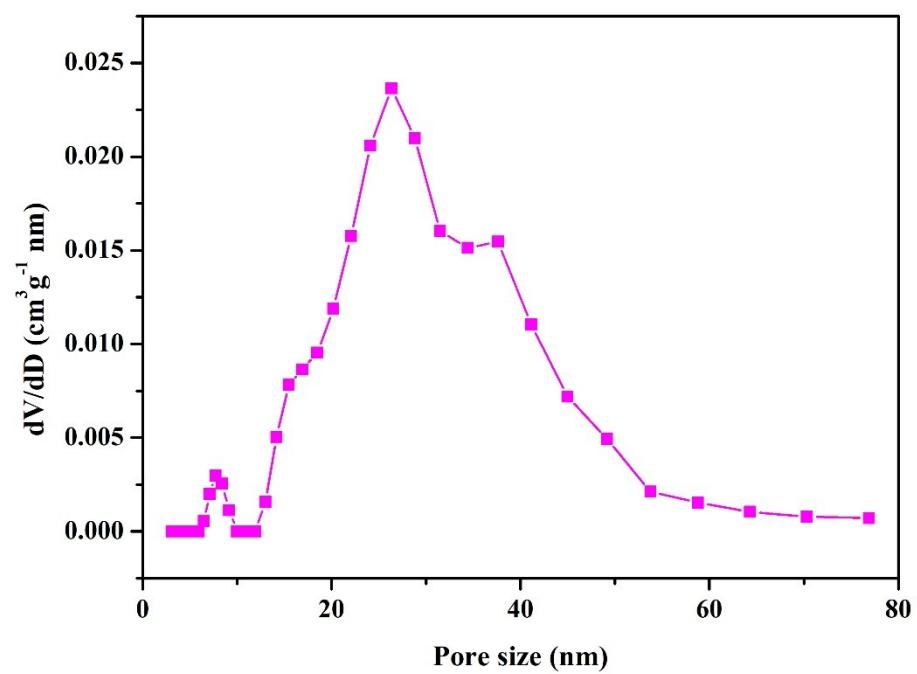


Fig. S6. Corresponding pore size distribution of MnFe₂O₄/γ-Al₂O₃ catalysts.

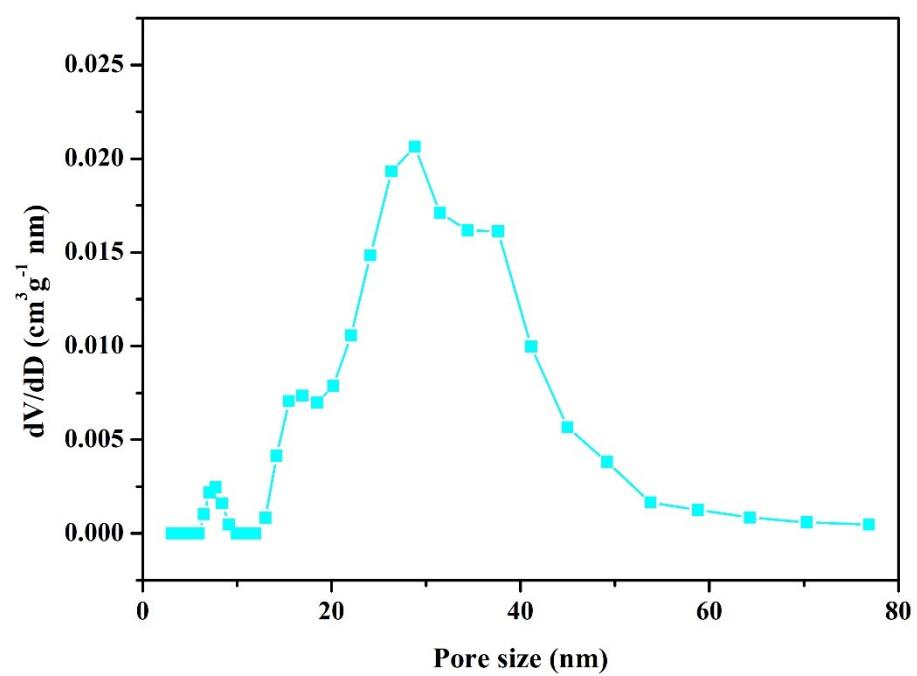


Fig. S7. Corresponding pore size distribution of CuFe₂O₄/γ-Al₂O₃ catalysts.

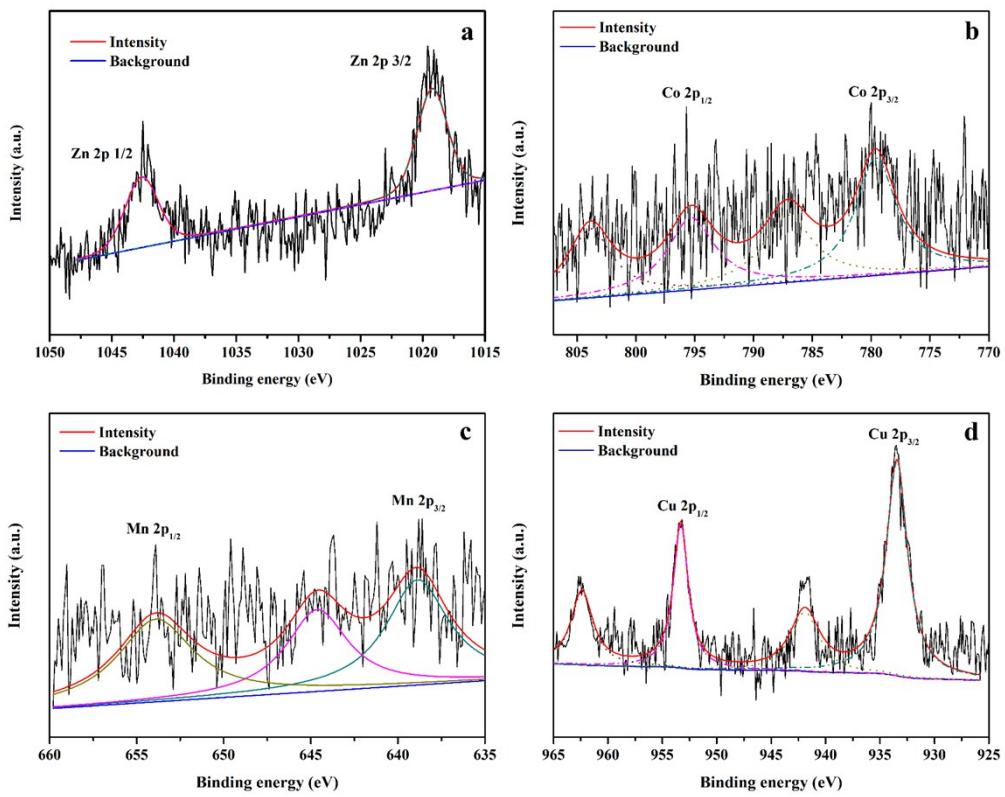


Fig. S8. XPS spectra of AFe₂O₄/γ-Al₂O₃ catalysts, **a)** Zn 2P; **b)** Co 2p; **c)** Mn 2P, **and d)** Cu 2p.

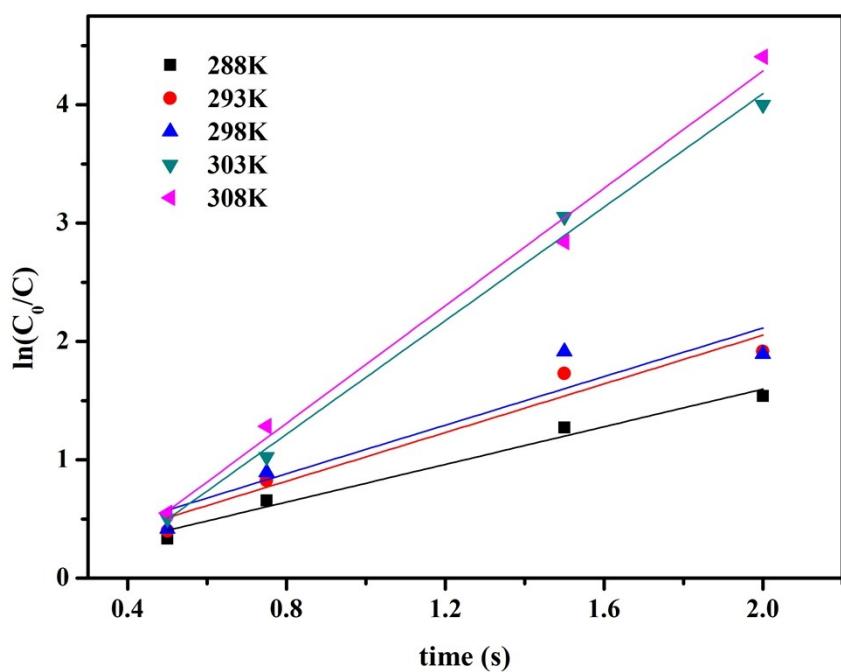


Fig. S9. Pseudo-first-order kinetics fitting at various temperatures.

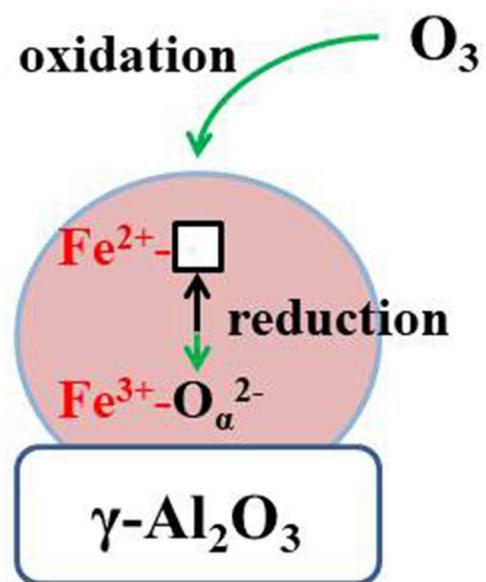


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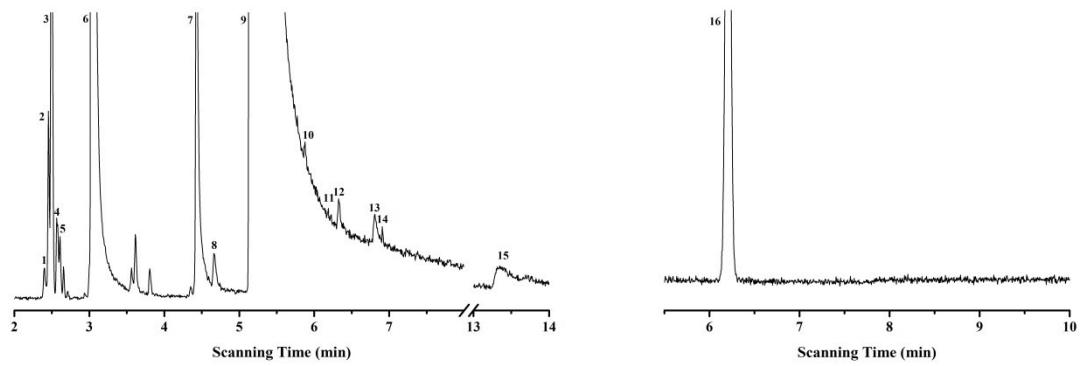


Fig. S11. a) GC/MS analysis of catalyst surface residues; **b)** GC/MS analysis of produced gas.

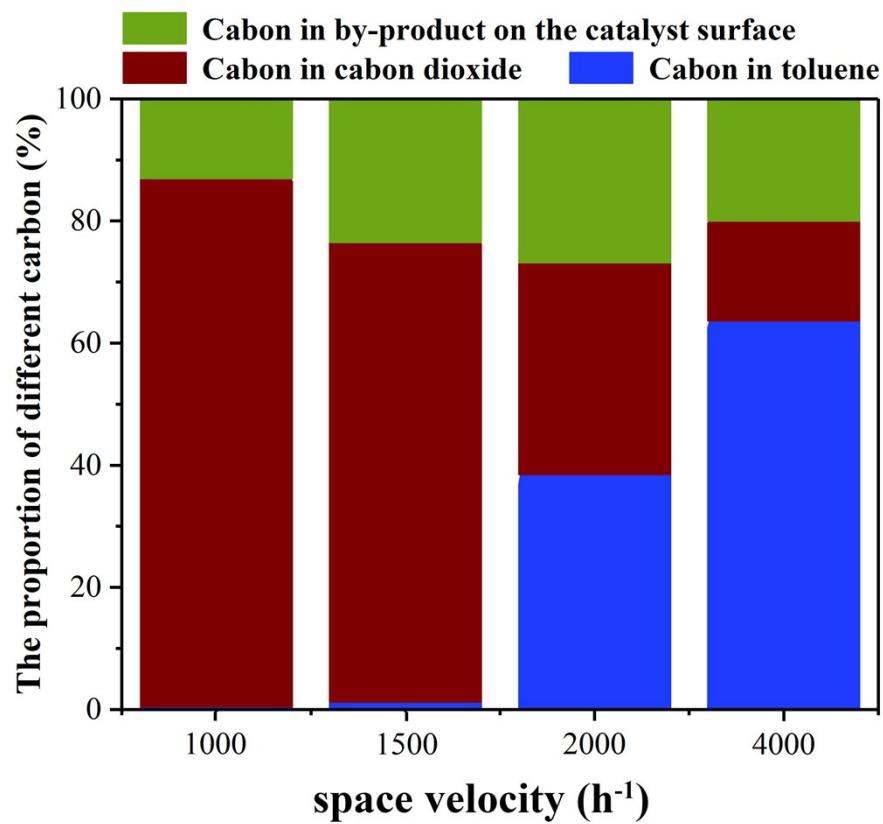


Fig. S12. Impact of space velocity on carbon balance.

Table S1. The comparison of BET surface area, pore structure for γ -Al₂O₃ and the AFe₂O₄/ γ -Al₂O₃ catalysts.

Sample	S _{BET} (m ² /g)	Pore volume (cm ³ /g)	Average pore diameter (nm)
γ -Al ₂ O ₃	320	0.617	30.66
ZnFe ₂ O ₄ / γ -Al ₂ O ₃ catalysts	300	0.615	32.66
CoFe ₂ O ₄ / γ -Al ₂ O ₃ catalysts	286	0.589	32.96
MnFe ₂ O ₄ / γ -Al ₂ O ₃ catalysts	245	0.513	32.99
CuFe ₂ O ₄ / γ -Al ₂ O ₃ catalysts	154	0.294	34.56

Table S2. Amounts and proportional relationship of BAS and LAS.

Samples	150 °C, μmol/g			Total
	LAS	BAS	B/L	
γ-Al ₂ O ₃	61.8	1.2	0.019	63.0
ZnFe ₂ O ₄ /γ-Al ₂ O ₃ catalyst	71.9	1.5	0.021	73.4
CoFe ₂ O ₄ /γ-Al ₂ O ₃ catalyst	68.3	1.1	0.017	69.4
MnFe ₂ O ₄ /γ-Al ₂ O ₃ catalyst	32.6	0.4	0.011	33.0
CuFe ₂ O ₄ /γ-Al ₂ O ₃ catalyst	60.7	0.9	0.14	61.6

Table S3. Comparison of parameters of reaction kinetic equations for toluene-catalyzed ozonation in different systems under the same reaction conditions.

Kinetics equation	Zero order		pseudo-first order	
	Rate Constant/K	R ²	Rate Constant/K	R ²
Sole O ₃	1584	0.2978	0.1171	0.9073
γ -Al ₂ O ₃ +O ₃	9070	0.8917	0.3430	0.9875
ZnFe ₂ O ₄ / γ -Al ₂ O ₃ +O ₃	27708	0.9171	0.6419	0.9184
CoFe ₂ O ₄ / γ -Al ₂ O ₃ +O ₃	22574	0.9073	0.5951	0.9241
MnFe ₂ O ₄ / γ -Al ₂ O ₃ +O ₃	8864	0.7152	0.3574	0.7736
CuFe ₂ O ₄ / γ -Al ₂ O ₃ +O ₃	9483	0.8874	0.3748	0.8876

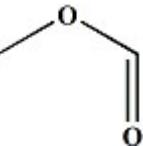
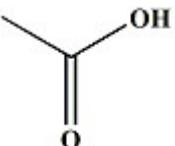
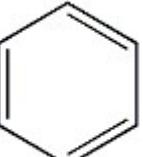
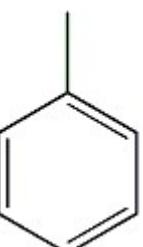
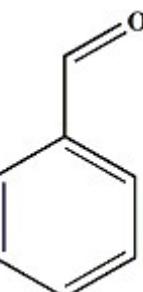
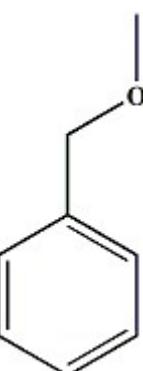
Table S4. Reaction rate constant value (k) at each temperature.

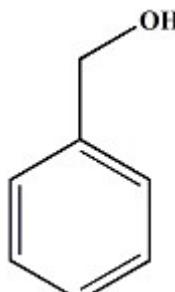
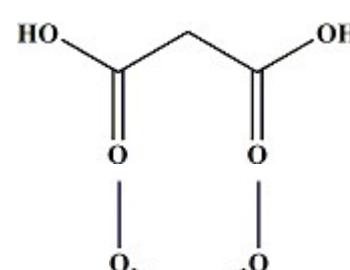
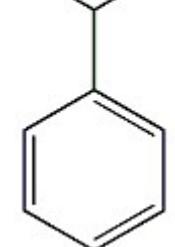
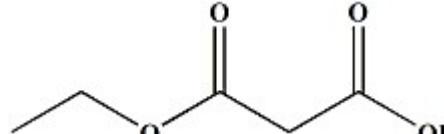
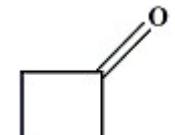
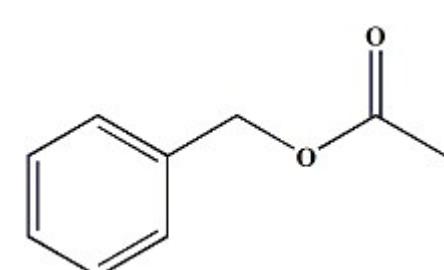
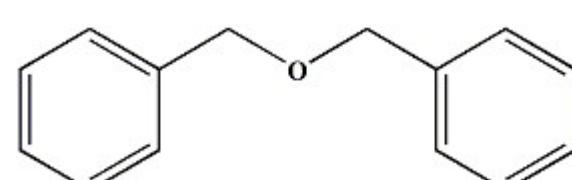
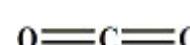
Temperature (K)	288	293	298	303	308
k	0.7961	1.0280	1.0261	2.3989	2.4812

Table S5. $[O_3]_w$ (mg/m³) in sole ozonation and catalytic ozonation process, respectively.

Initial ozone concentration (mg/L)	Sole O ₃	γ -Al ₂ O ₃ +O ₃	ZnFe ₂ O ₄ / γ -Al ₂ O ₃ +O ₃
5	4.12	0	0
10	9.17	5.31	1.57
15	13.96	11.88	4.92
20	18.41	18.38	5.04

Table S6. Summary of GC/MS results.

Label	Molecular formula	Molecular structure	Name of Compound
1	CH ₄ O	CH ₃ OH	Methanol
2	C ₂ H ₄ O ₂		Methyl formate
3	C ₂ H ₆ O		Ethanol
4	C ₂ H ₄ O ₂		Acetic acid
5	C ₆ H ₆		Benzene
6	C ₇ H ₈		Toluene
7	C ₇ H ₆ O		Benzaldehyde
8	C ₈ H ₁₀ O		Benzyl methyl ether

9	C_7H_8O		Benzyl alcohol
10	$C_3H_4O_4$		Propanedioic acid
11	$C_9H_{12}O_2$		Benzaldehyde dimethyl acetal
12	$C_5H_8O_4$		Ethyl hydrogen malonate
13	C_4H_6O		Cyclobutanone
14	$C_9H_{10}O_2$		Acetic acid, phenylmethyl ester
15	$C_{14}H_{14}O$		Benzyl Ether
16	CO_2		Carbon dioxide