

Supplementary Information

Kinetics and reactor modeling of the conversion of n-pentane using HZSM-5 catalysts with different Si/Al ratio

Tomás Cordero-Lanzac^{a,*}, Andrés T. Aguayo^a, Pedro Castaño^{a,b}, Javier Bilbao^a

^a*Department of Chemical Engineering, University of the Basque Country (UPV/EHU),
PO Box 644, 48080, Bilbao, Spain*

^b*Multiscale Reaction Engineering, KAUST Catalysis Center (KCC), King Abdullah
University of Science and Technology (KAUST), Thuwal, 23955-6900, Saudi Arabia*

Corresponding author: tomas.cordero@ehu.eus

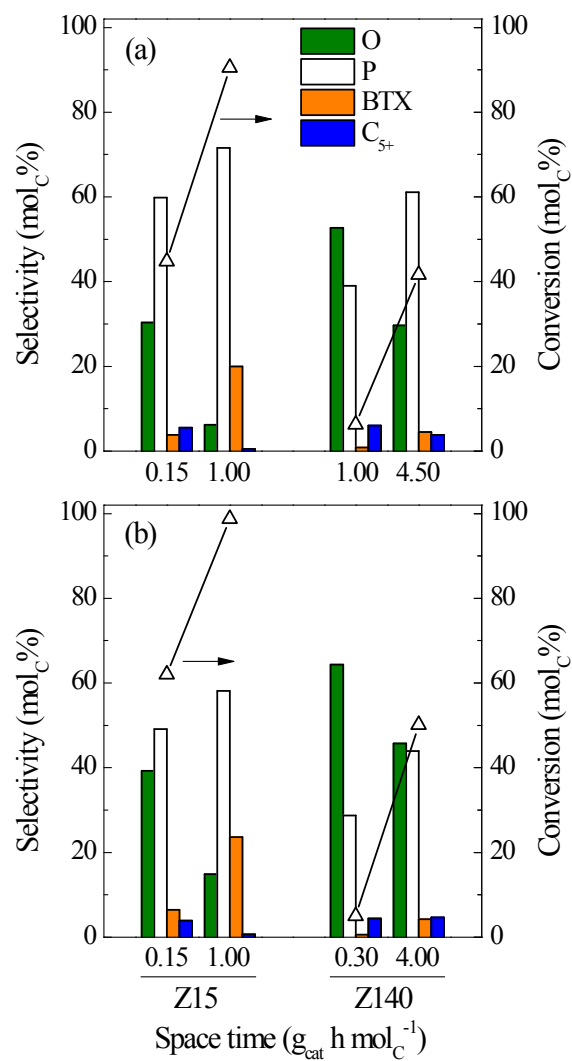


Fig. S1. Conversion and selectivity with Z15 and Z140 catalysts using different values of space time at (a) 500 °C and (b) 550 °C.

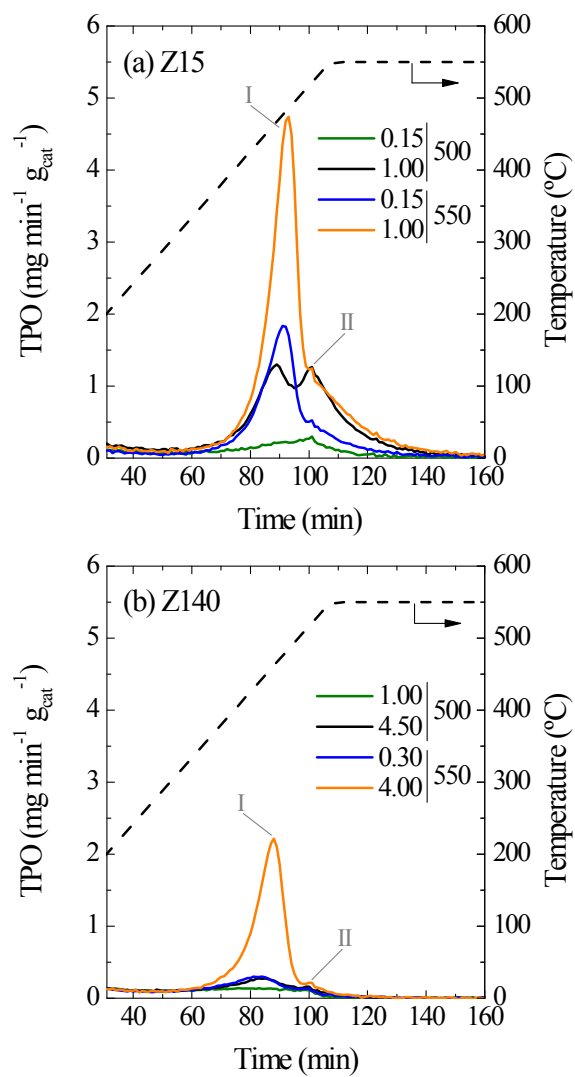


Fig. S2. TPO profile of (a) Z15 and (b) Z140 catalysts used at 500 and 550 °C

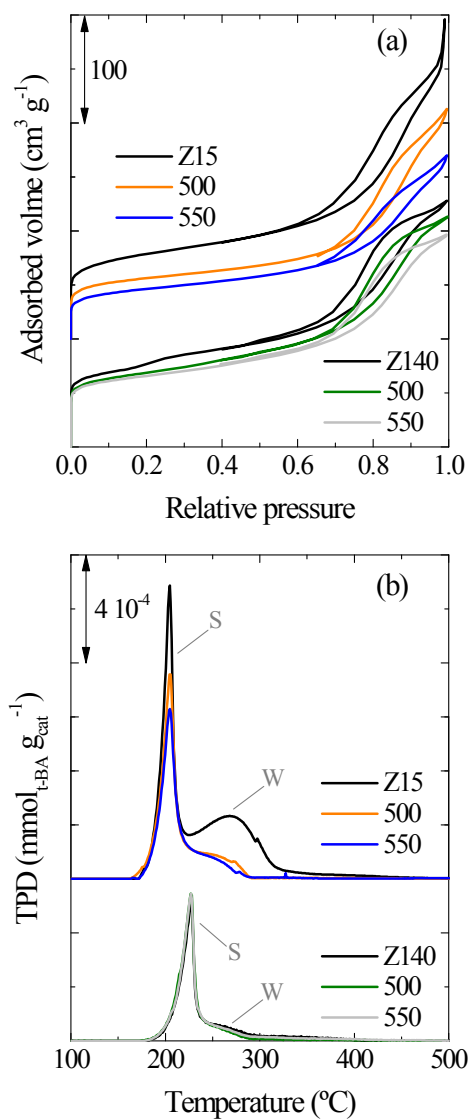


Fig. S3. (a) N₂ adsorption-desorption isotherms and (b) t-BA TPD of the fresh and used Z15 and Z140 catalysts at 500 and 550 °C (Space time, 1.00 g_{cat} h mol_C⁻¹)

Table S1. Kinetic constant at 500 °C and activation energy values for the catalytic cracking of n-pentane over Z15 and Z140 catalysts

	Z15		Z140	
	k^*	E (kJ mol ⁻¹)	k^*	E (kJ mol ⁻¹)
<i>Kinetic rates</i>				
k_1 (mol _C g _{cat} ⁻¹ h ⁻¹ atm ⁻¹)	(8.54 ± 0.07) 10 ⁻¹	(6.15 ± 0.15) 10 ¹	(2.50 ± 1.66) 10 ⁻²	(6.74 ± 1.89) 10 ¹
k_2 (mol _C g _{cat} ⁻¹ h ⁻¹ atm ⁻¹)	(8.57 ± 0.27) 10 ⁻¹	(3.84 ± 1.13) 10 ¹	(6.46 ± 4.15) 10 ⁻²	(3.91 ± 1.66) 10 ¹
k_3 (mol _C g _{cat} ⁻¹ h ⁻¹ atm ⁻¹)	(2.45 ± 0.89) 10 ⁻¹	(7.07 ± 1.65) 10 ¹	(1.42 ± 0.81) 10 ⁻²	(7.24 ± 0.45) 10 ¹
k_4 (mol _C g _{cat} ⁻¹ h ⁻¹ atm ⁻²)	(4.13 ± 1.15) 10 ⁰	(3.77 ± 1.11) 10 ¹	(2.45 ± 0.12) 10 ⁻¹	(3.76 ± 0.69) 10 ¹
k_5 (mol _C g _{cat} ⁻¹ h ⁻¹ atm ⁻²)	(4.14 ± 1.29) 10 ⁰	(3.74 ± 1.15) 10 ¹	(4.19 ± 1.52) 10 ⁻¹	(3.81 ± 1.51) 10 ¹
k_6 (mol _C g _{cat} ⁻¹ h ⁻¹ atm ⁻²)	(1.34 ± 0.47) 10 ⁰	(2.62 ± 0.48) 10 ¹	(1.27 ± 0.13) 10 ⁻¹	(2.72 ± 0.54) 10 ¹
k_7 (mol _C g _{cat} ⁻¹ h ⁻¹ atm ⁻¹)	(6.56 ± 0.62) 10 ⁻¹	(2.66 ± 0.12) 10 ¹	(2.63 ± 0.16) 10 ⁻²	(2.78 ± 0.92) 10 ¹
k_8 (mol _C g _{cat} ⁻¹ h ⁻¹ atm ⁻¹)	(3.40 ± 0.08) 10 ⁰	(1.01 ± 0.10) 10 ¹	(1.64 ± 0.86) 10 ⁻¹	(1.04 ± 0.15) 10 ¹
k_9 (mol _C g _{cat} ⁻¹ h ⁻¹ atm ⁻¹)	(5.72 ± 0.13) 10 ⁻¹	(1.54 ± 0.26) 10 ¹	(1.77 ± 0.22) 10 ⁻²	(1.59 ± 0.75) 10 ¹
k_{10} (mol _C g _{cat} ⁻¹ h ⁻¹ atm ⁻¹)	(1.05 ± 0.41) 10 ⁻³	(2.36 ± 0.31) 10 ¹	(1.07 ± 0.95) 10 ⁻³	(2.29 ± 1.07) 10 ¹
<i>Deactivation rate</i>				
k_d (atm ⁻¹ h ⁻¹)	(3.14 ± 0.06) 10 ⁻¹	(3.00 ± 0.15) 10 ¹	(1.05 ± 0.29) 10 ⁻¹	(3.21 ± 0.78) 10 ¹
d	(1.01 ± 0.12) 10 ⁰		(1.13 ± 0.20) 10 ⁰	

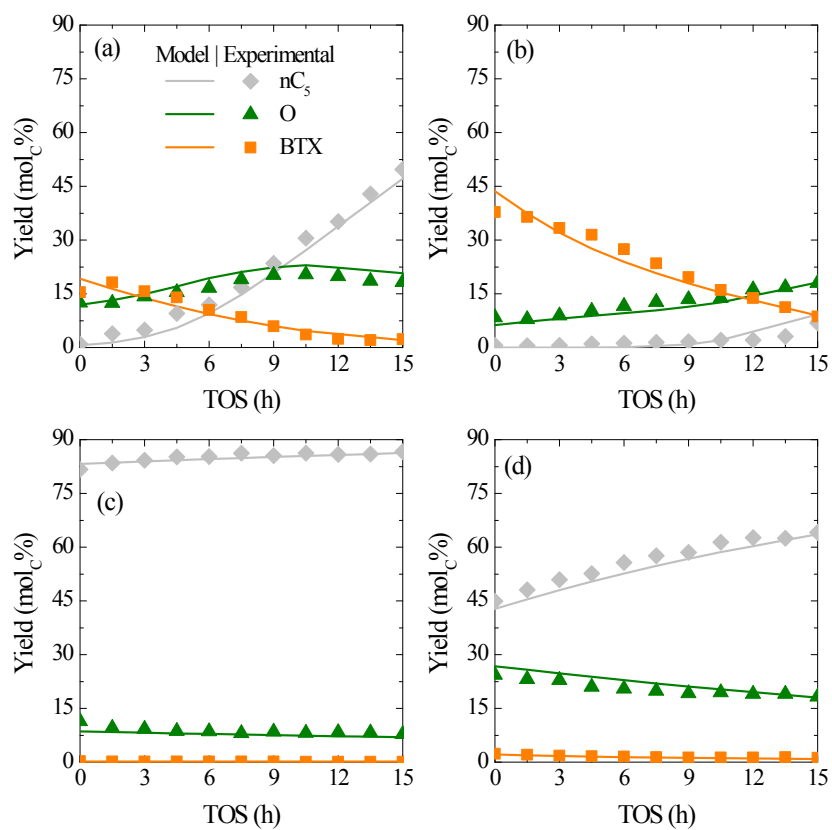


Fig. S5. Comparison of the predicted results with the model (lines) and additional experimental runs (dots) for the evolution with time on stream of yields using the Z15 catalyst and space time values of (a) 1.0 and (b) 3.5 g_{cat} h mol_C⁻¹ and using Z140 catalyst and space time values of (c) 1.0 and (d) 3.5 g_{cat} h mol_C⁻¹, at 550 °C.

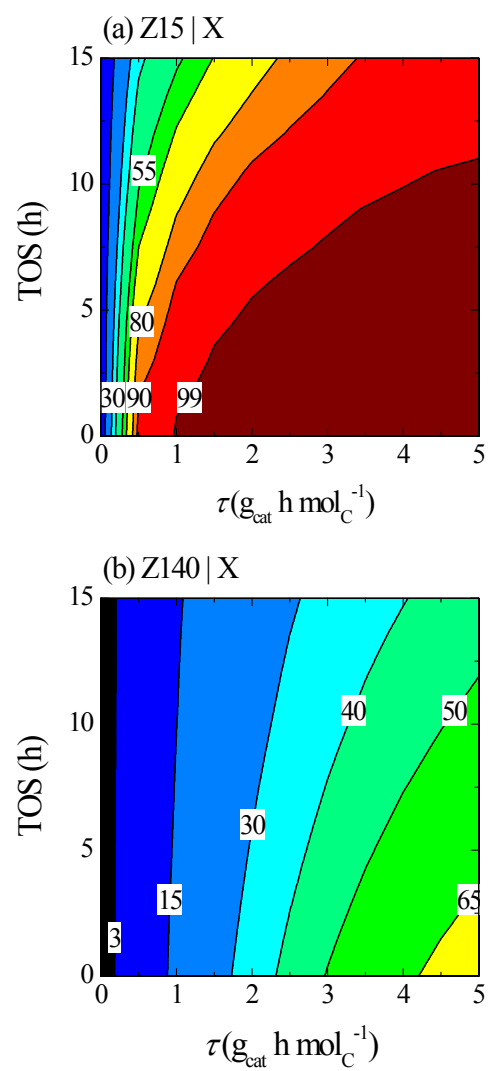


Fig. S6. Simulated contour maps for (a) Z15 and (b) Z140 catalysts of the evolution with the time on stream and space time of the n-pentane conversion at 550 °C