

## Supporting Information

### Atmospheric pressure synthesis of nano-scaled SAPO-34 catalysts for effective conversion of methanol to light olefins

Meng Lyu,<sup>a,b</sup> Chengguang Yang,<sup>\*b</sup> Ziyu Liu,<sup>b</sup> Ting Wang,<sup>b</sup> Hongjiang Liu,<sup>a</sup> Xinqing Chen,<sup>\*b,d</sup> and Yuhan Sun<sup>b,c,d</sup>

<sup>a</sup>Department of Chemistry, School of Science, Shanghai University, Shanghai 200444, PR China

<sup>b</sup>CAS Key Laboratory of Low-Carbon Conversion Science and Engineering, Shanghai Advanced Research Institute, Chinese Academy of Sciences, Shanghai 201210, PR China.

<sup>c</sup>School of Physical Science and Technology, ShanghaiTech University, Shanghai 201210, PR China.

<sup>d</sup>University of Chinese Academy of Science, Beijing, 100049, China

### **Synthesis of $\text{Al}_2\text{MgO}_8\text{Si}_2$**

$\text{Al}_2\text{MgO}_8\text{Si}_2$  was pre-synthesized by the following method.  $\text{Al}_2(\text{SO}_4)_3 \cdot 18\text{H}_2\text{O}$  was dispersed in stirring to the solution of  $\text{Na}_2\text{SiO}_3$  under  $85^\circ\text{C}$ . After cooling down to room temperature,  $\text{MgO}$ ,  $\text{NaAlO}_2$  and  $\text{NaOH}$  solution were added into the above solution in turn. The mixture was filtered after 1 hour of the reaction, washed three times with deionized water to remove sodium ions and dried overnight to obtain  $\text{Al}_2\text{MgO}_8\text{Si}_2$ .

### **Synthesis of SAPO-34 zeolite without MgO**

SAPO-34 zeolite without  $\text{MgO}$  was prepared also under atmospheric pressure. A certain amount of silica resource and aluminum resource was added to TEAOH solution and stirred at room temperature for 2 h. Subsequently, the desired amount of  $\text{H}_3\text{PO}_4$ , SAPO-34 seeds and deionized water were added in turn and stirred for 6 h. The synthesis gel with a molar composition of  $1.0 \text{ Al}_2\text{O}_3 : 0.5 \text{ SiO}_2 : 1.0 \text{ P}_2\text{O}_5 : 1.0 \text{ TEAOH} : 50 \text{ H}_2\text{O}$  was heated to  $90^\circ\text{C}$  and kept for 12 h to remove the solvent before it was crushed and sifed to 20-40 mesh. The obtained particles were transferred into a quartz tube and crystallized at  $200^\circ\text{C}$  for 24 h in presence of steam under atmospheric pressure. After calcination at  $600^\circ\text{C}$  for 5 h, the aimed sample was obtained.

### **Synthesis of SAPO-34 zeolite with MgO**

For comparasion, SAPO-34 zeolite with  $\text{MgO}$  was prepared also under atmospheric pressure. A certain amount of silica resource, aluminum resource and  $\text{MgO}$  was added to TEAOH solution and stirred at room temperature for 2 h. Then desired amount of  $\text{H}_3\text{PO}_4$ , SAPO-34 seeds and deionized water were added in turn and stirred for 6 h. The synthesis gel with a molar composition of  $1.0 \text{ Al}_2\text{O}_3 : 0.5 \text{ SiO}_2 : 1.0 \text{ P}_2\text{O}_5 : 1.0 \text{ TEAOH} : 50 \text{ H}_2\text{O}$  was heated to  $90^\circ\text{C}$  and kept for 12 h to remove the solvent before it was crushed and sifed to 20-40 mesh. The obtained particles were transferred into a quartz tube and crystallized at  $200^\circ\text{C}$  for 24 h in presence of steam under atmospheric pressure. After calcination at  $600^\circ\text{C}$  for 5 h, SAPO-34 containing  $\text{MgO}$  was obtained.

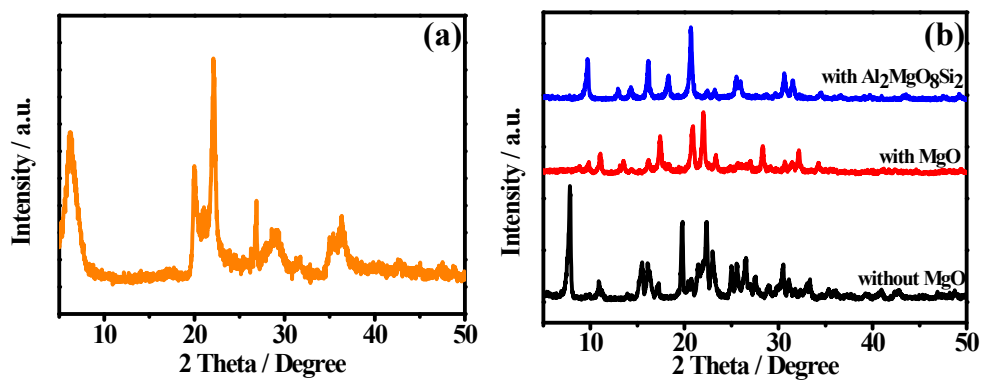


Fig. S1 XRD patterns of  $\text{Al}_2\text{MgO}_8\text{Si}_2$  (a), and SAPO-34 synthesized without MgO, with MgO and with  $\text{Al}_2\text{MgO}_8\text{Si}_2$  (b).

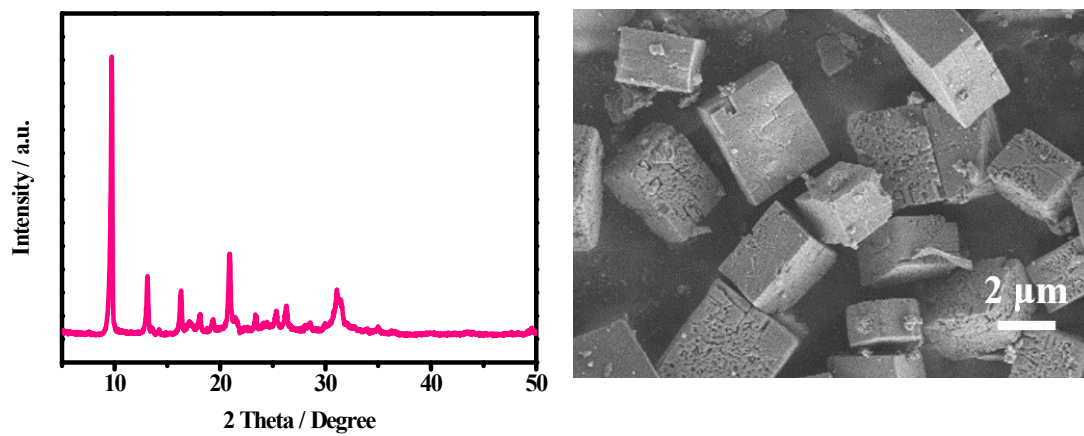


Fig. S2 XRD pattern and SEM image of SP34-CS.

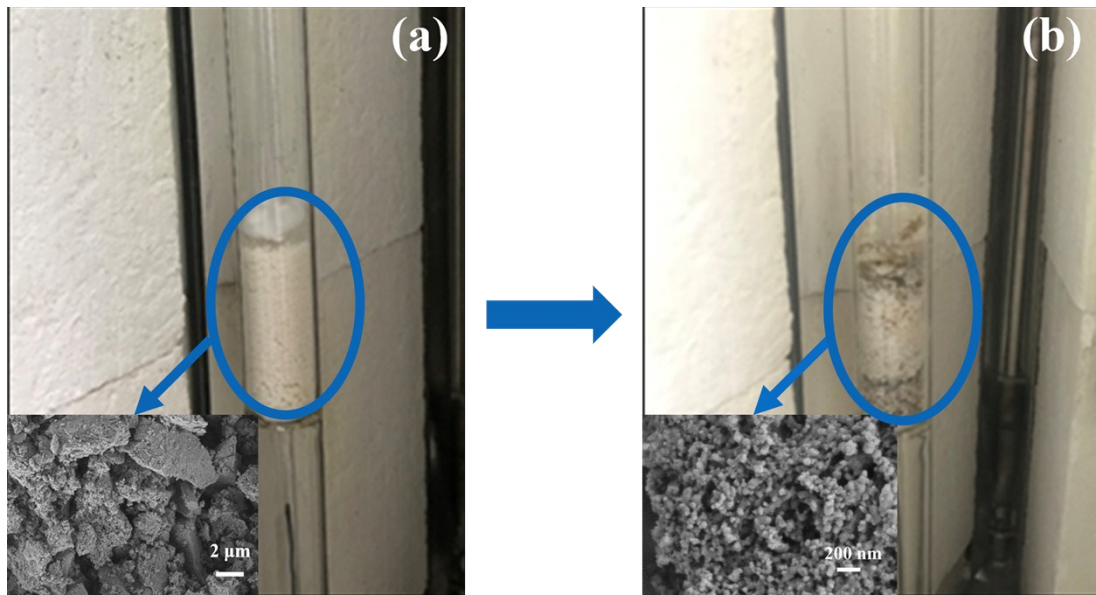


Fig. S3 Photographs and SEM images of dried gels before (a) and after (b) crystallization.

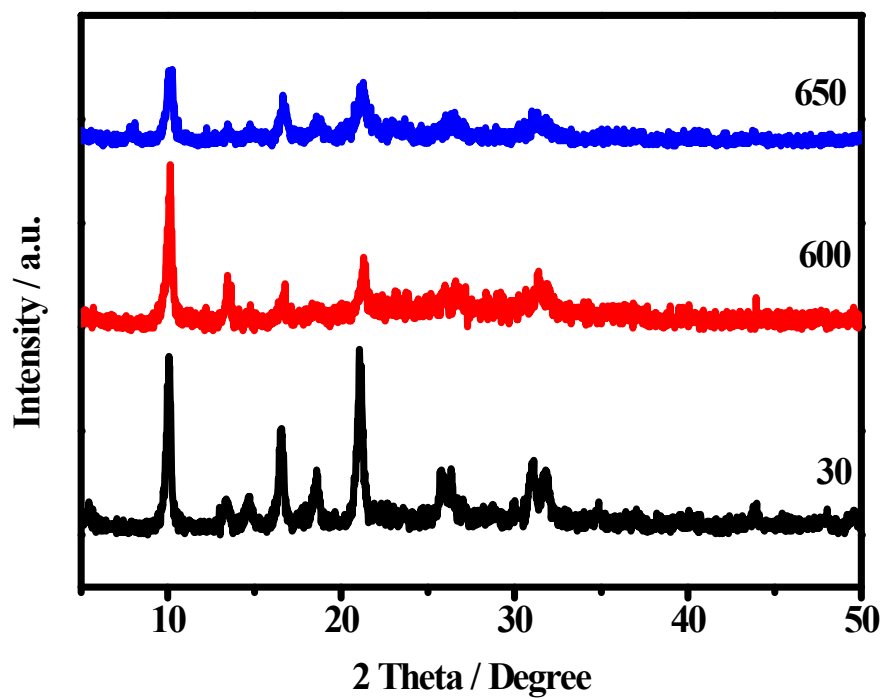


Fig. S4 XRD pattern of SP34-AS-3 before and after hydrothermally treated at 600 and 650 °C for 2 h .

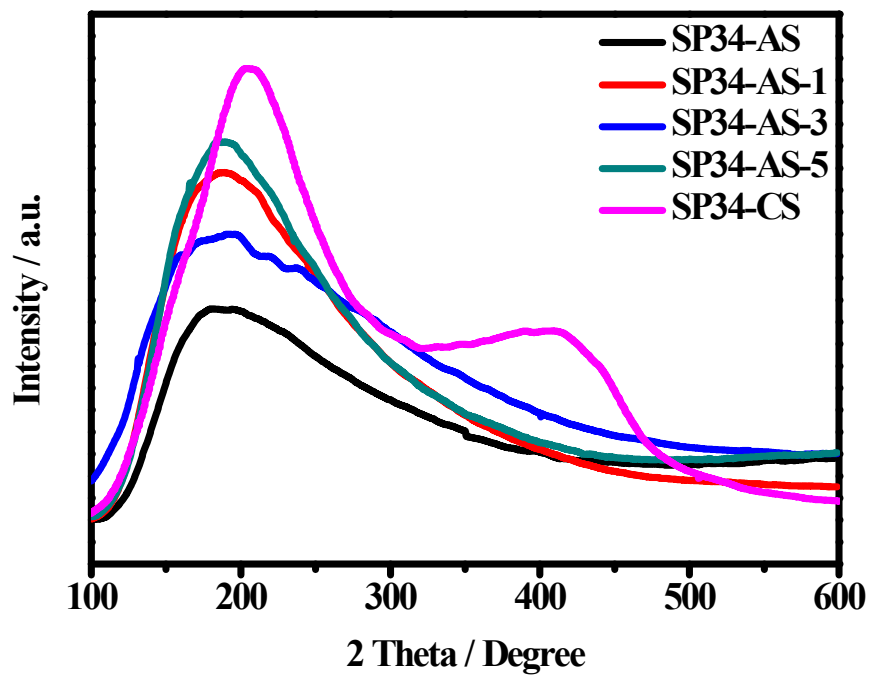


Fig. S5 NH<sub>3</sub>-TPD profiles of SP34-AS, SP34-AS-1, SP34-AS-3, SP34-AS-5 and SP34-CS.

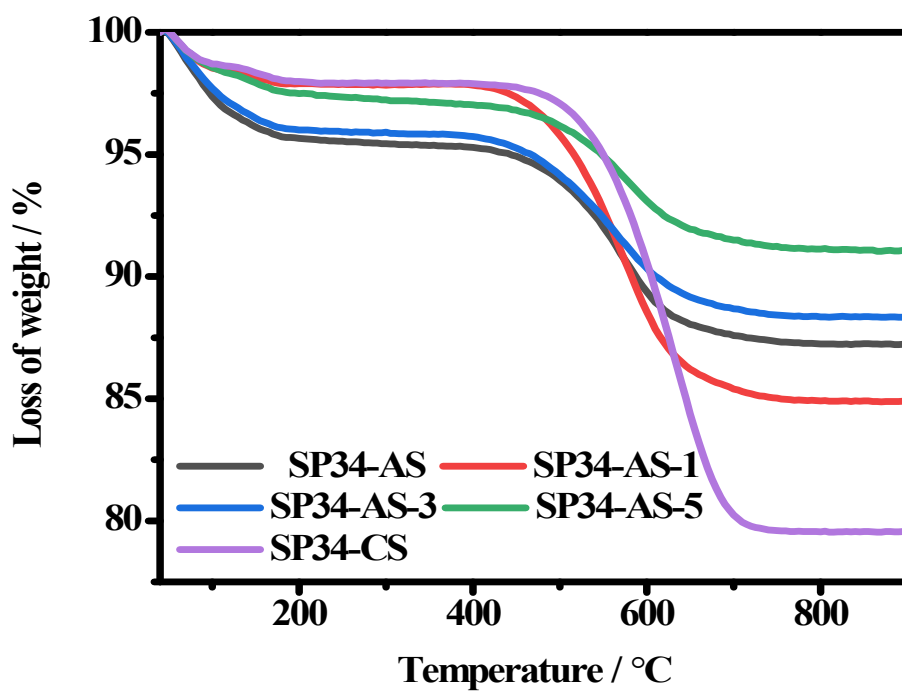


Fig. S6 TG curves of SP34-AS, SP34-AS-1, SP34-AS-3, SP34-AS-5 and SP34-CS.



Table S1 The acid site density of prepared samples

Sample	SP34-AS	SP34-AS-1	SP34-AS-3	SP34-AS-5	SP34-CS
Acid site density (mmol/g)	0.23	0.33	0.28	0.34	0.43

Table S2 Product selectivity (%) of MTO reaction over various catalysts.

Catalysts	Lifetime /min <sup>a</sup>	C <sub>1</sub>	C <sub>2</sub> <sup>=</sup>	C <sub>2</sub>	C <sub>3</sub> <sup>=</sup>	C <sub>3</sub>	C <sub>4</sub>	C <sub>4</sub> <sup>=</sup>	C <sub>2</sub> <sup>=</sup> +C <sub>3</sub> <sup>=</sup>	C <sub>2</sub> <sup>=</sup> ~C <sub>4</sub> <sup>=</sup>	Carbon balance
SP34-CS	450	1.64	23.51	1.73	34.31	14.05	4.48	13.55	57.82	71.37	98%
SP34-AS	120	1.44	28.61	0.35	39.80	4.67	4.45	14.50	68.41	82.91	95%
SP34-AS-1	240	1.34	27.24	0.73	40.71	4.34	4.75	14.56	67.95	82.51	97%
SP34-AS-3	330	1.58	31.03	0.56	39.61	4.13	4.33	12.96	70.64	83.60	98%
SP34-AS-5	60	1.01	27.07	0.39	40.09	3.94	5.10	15.97	67.16	83.13	94%

Reaction conditions : WHSV = 0.5 h<sup>-1</sup>, T = 400°C, catalyst weight = 1.0 g and 1 atm.

<sup>a</sup> Catalyst lifetime is defined as the reaction duration with methanol conversion higher than 95%.

Table S3 Variation of coke formation in methanol conversion over SAPO-34.

Samples	SP34-AS	SP34-AS-1	SP34-AS-3	SP34-AS-5	SP34-CS
coke (% g/gcat)	8.05	12.93	7.38	5.91	18.34
TOS (min)	120	240	330	60	450
R <sub>coke</sub> (mg/min)	0.67	0.54	0.22	0.99	0.41
P <sub>coke</sub> (g/gMeOH)	0.08	0.06	0.03	0.12	0.05

$R_{\text{coke}} \text{ (mg/min)} = \text{Coke amount (mg)} / \text{reaction time (min)}$ ,

$P_{\text{coke}} \text{ (g/g)} = \text{Coke amount (g)} / \text{methanol feedstock (g)}$ .