

## Electronic Supplementary Information

### Multi-walled carbon nanotube and carbide-derived carbon supported metal phthalocyanines as cathode catalysts for microbial fuel cell application

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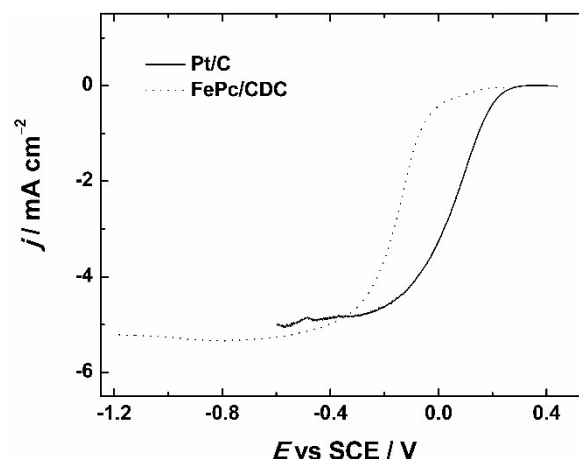
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#### A comparison of the RDE results



**Fig. S1** Comparative RDE voltammetry curves for  $\text{O}_2$  reduction on FePc/CDC (loading of  $0.4 \text{ mg cm}^{-2}$ ) and Pt/C (Pt loading of  $40 \text{ } \mu\text{g cm}^{-2}$ ) catalysts recorded in  $\text{O}_2$ -saturated  $0.1 \text{ M}$  PBS containing  $0.1 \text{ M}$   $\text{K}_2\text{SO}_4$  (pH 7) ( $\omega = 1900 \text{ rpm}$ ,  $\nu = 10 \text{ mV s}^{-1}$ ).

#### Cost analysis (INR - ₹, USD - \$ and $1 \text{ ₹} = 0.014 \text{ \$}$ )

Total cathode surface area =  $120 \text{ cm}^2$

#### ➤ Cost calculation for M-1 (with FePc/MWCNT)

Cost of FePc/MWCNT =  $85.2 \text{ \$ g}^{-1}$

Catalyst loading =  $0.2 \text{ mg cm}^{-2}$

Total catalyst required =  $24 \text{ mg}$

Total cost of FePc/MWCNT used =  $85.2 \text{ \$ g}^{-1} \times 24 \text{ mg} = \mathbf{2.05 \text{ \$ (A1)}}$

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➤ *Component used for preparation of catalyst ink*

Cost of activated carbon, @0.5 mg cm<sup>-2</sup> = 60 mg = 0.003 \$

Nafion 117 dispersion (5% in alcohol) = 3.3 \$

Acetone as solvent = 1.146 \$

Total cost = **4.45 \$ (B)**

➤ *Cost for reactor and electrode*

Cost of clayware reactor is ₹ 10/- and cost of required carbon felt is approx. ₹ 80 /-

Total = ₹ 90/- ≈ **1.35 \$ (C)**

So, Total cost of construction of M-1 = **A1+B+C ≈ 7.85 \$**

➤ **Cost calculation for M-2 (with CoPc/MWCNT)**

Cost of CoPc/MWCNT = 81.5 \$ g<sup>-1</sup>

Catalyst loading = 0.2 mg cm<sup>-2</sup>

Total catalyst required = 24 mg

Total cost of CoPc-MWCNT used = 81.5 \$ g<sup>-1</sup> × 24 mg = **1.96 \$ (A2)**

So, Total cost of construction of M-2 = **A2+B+C ≈ 7.76 \$**

➤ **Cost calculation for M-3 (with FePc/CDC)**

Cost of FePc-CDC = 31.5 \$ g<sup>-1</sup>

Catalyst loading = 0.4 mg cm<sup>-2</sup>

Total catalyst required = 48 mg

Total cost of FePc-MWCNT used = 31.5 \$ g<sup>-1</sup> × 48 mg = **1.51 \$ (A3)**

So, Total cost of construction of M-3 = **A3+B+C ≈ 7.31 \$**

➤ **Cost calculation for M-Pt (10 wt.% Pt on Vulcan XC72)**

Cost of catalyst = 105 \$ g<sup>-1</sup> (Sigma-Aldrich)

Catalyst loading = 0.5 mg cm<sup>-2</sup>

Total catalyst required = 60 mg

Total cost of 10 wt.% Pt on Vulcan XC72 used = 105 \$ g<sup>-1</sup> × 60 mg = **6.30 \$ (A4)**

Total cost of construction of M-Pt = **A4+B+C ≈ 12.10 \$**

32.7 mW m<sup>-2</sup> power is generated from M-1 having net power output = (32.7×0.120)/7.85 = **0.50 mW \$<sup>-1</sup>**

42.2 mW m<sup>-2</sup> power is generated from M-2 having net power output = **0.65 mW \$<sup>-1</sup>**

58.5 mW m<sup>-2</sup> power is generated from M-3 having net power output = **0.96 mW \$<sup>-1</sup>**

62.1 mW m<sup>-2</sup> power is generated from M-Pt having net power output = **0.62 mW \$<sup>-1</sup>**

Ratio of the cost of Pt to catalyst FePc/MWCNT = (6.30/1.96) ≈ **3.2**

Ratio of the cost of Pt to catalyst CoPc/MWCNT = (6.30/2.05) ≈ **3.1**

Ratio of the cost of Pt to catalyst FePc/CDC = (6.30/1.51) ≈ **4.2**