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Supporting information

Elucidating the Reaction Kinetics of Lithium-Sulfur Battery by *Operando* XRD Based on an Open-Hollow S@MnO₂ Cathode

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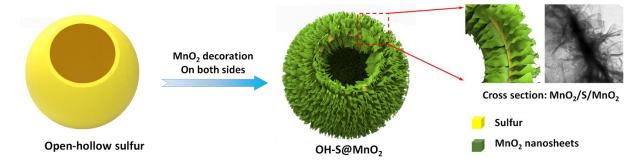


Fig. S1. Illustration of the preparation process of OH-S@MnO $_2$.

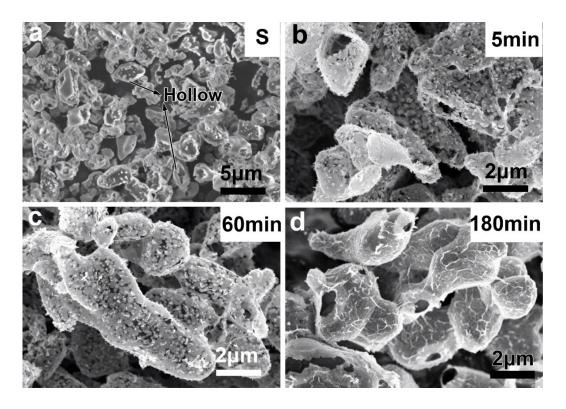
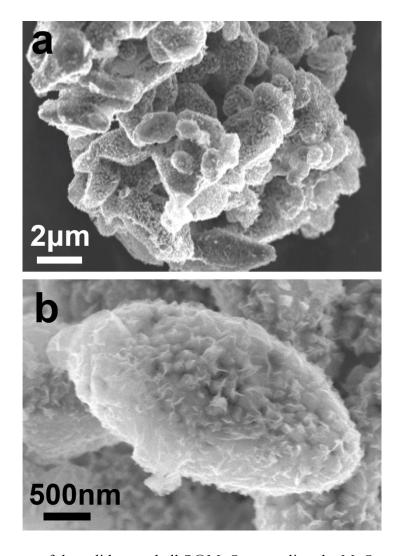


Fig. S2. The SEM images of OH-S@MnO₂ in different reaction time: (a) original S, (b) 5 min, (c) 60 min and (d) 180 min.



 $\label{eq:Fig.S3} \textbf{Fig. S3}. \ SEM \ images \ of the solid core-shell \ S@MnO_2, \ revealing \ the \ MnO_2 \ nanosheets \ coating \\ on \ the \ solid \ S \ spheroids.$

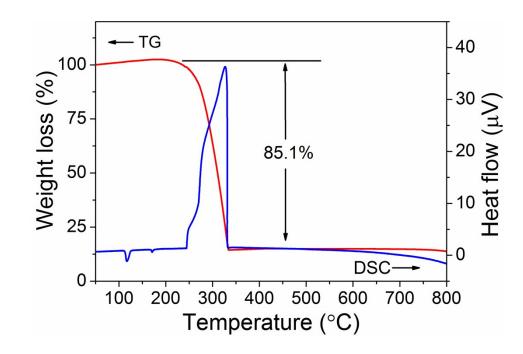


Fig. S4. TG/DSC analysis of CS-S@MnO₂ under Ar atmosphere, revealing the S content is around 85.1 wt%.

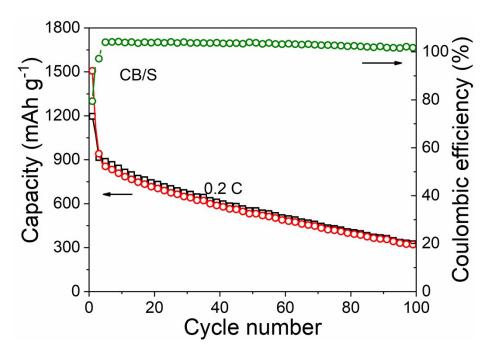


Fig. S5. Cycling performance of CB/S cathode at a current density of 0.2 C.

The coulombic efficiency of the CB/S electrode after 4 cycles is over 100%. The abormal coulomic efficiency is colsely related to the serious shuttling effect. Owing to the poor adsorption of carbon black, the polysulfides easily dissolve into the electrolyte during the discharge process, and then shuttle to the Li anode and react with Li metal to form irreversible Li₂S. Thus, the initial coulombic efficiency is quite low (~79%). Afterwards, the polysulfides shuttle back and forth, and thick Li₂S layer forms on the Li metal surface. After several cycles (3~4 cycles), during the discharge, due to the poor electrical contact between the polysulfides and cathode current collector, a large amount of polysulfides in the electrolyte cannot be reduced to Li₂S, leading to low discharge capacity; while in the recharge process, in addition to the decomposition of Li₂S on the cathode, a part of polysulfide in the electrolyte is also oxidized on the cathode/electrolyte interface. In this situation, the charge capacity is slightly higher than discharge capacity. Therefore, the coulombic efficiency is over 100% after the 3rd cycle.

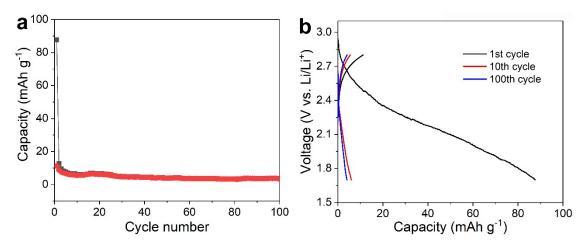


Fig. S6. (a) Cycling performance and (b) discharge-charge profiles of bare MnO_2 at 100 mA g^{-1} in the potential range of 1.7-2.8 V.

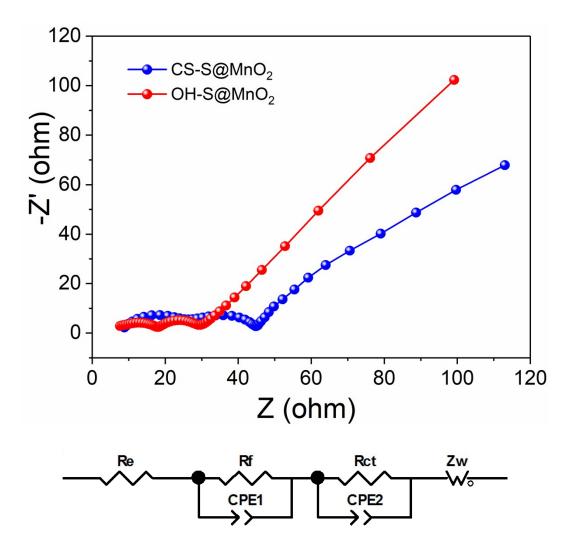


Fig. S7. Above: Nyquist plots of the CS-S@MnO₂ and OH-S@MnO₂ electrodes after 100 cycles, respectively. Below: Equivalent circuits used for Nyquist plots fitting.

Table S1. Kinetic parameters of the CS-S@MnO₂ and OH-S@MnO₂ electrodes.

Electrodes	R _e (ohm)	R_f (ohm)	R _{ct} (ohm)	CPE1 (F)	CPE2 (F)
CS-S@MnO ₂	7.8	20.2	15	1.4×10 ⁻⁵	2.0×10 ⁻⁴
OH-S@MnO ₂	5.7	12.8	9	1.5×10 ⁻⁵	2.3×10 ⁻⁴

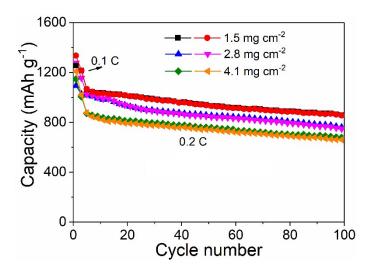


Fig. S8. Cycling performance of the OH-S@MnO $_2$ electrode with different sulfur loadings at the current density of 0.2 C.

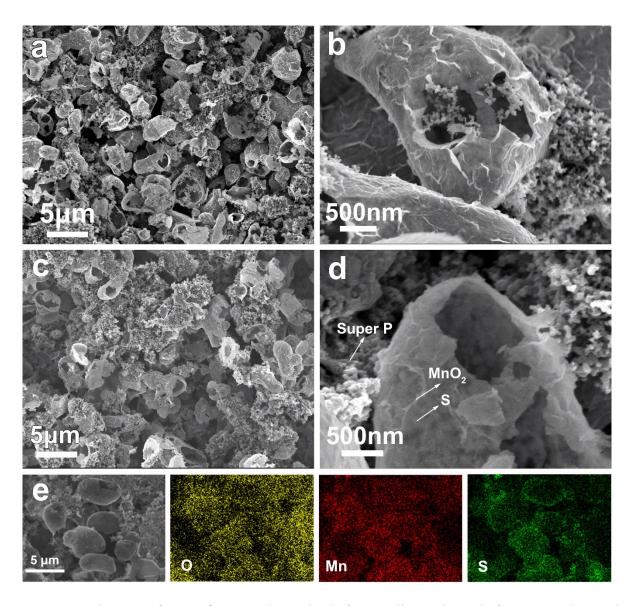


Fig. S9. SEM images of OH-S@MnO₂ electrodes before cycling (a-b) and after 100 cycles (c-d). (e) SEM-EDX elemental mapping inages of the OH-S@MnO₂ electrode after 100 cycles.

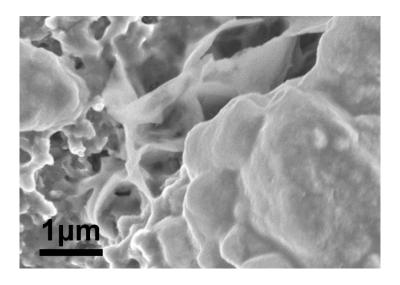


Fig. S10. The SEM image of SCS-MnO₂ electrode after 100 cycles.

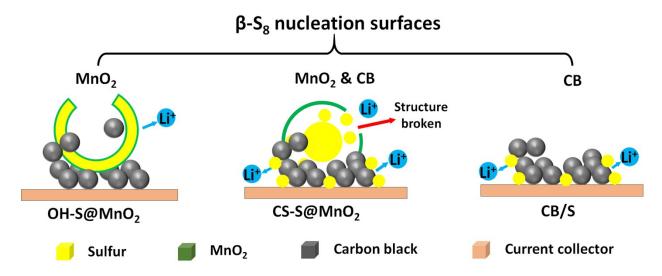


Fig. S11. Illustration of the β -S₈ nucleation in OH-S@MnO₂, CS-S@MnO₂ and CB/S cathodes with different surfaces.

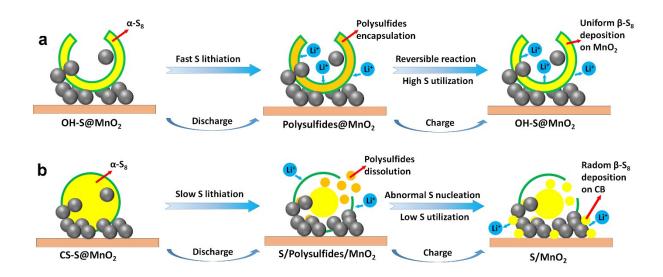


Fig. S12. The sulfur consumption and re-formation behaviors of OH-S@MnO₂ (a) and CS-S@MnO₂ (b).