## Supporting Information

## for

# Ionic mesoporous polyamide enabling highly dispersive ultrafine Ru nanoparticles: synergistic stabilization effect and remarkable efficiency in levulinic acid conversion into $\gamma$-valerolactone 

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## Supplementary Experimental

## 1. Synthesis of carboxylic functional ionic monomers

Synthesis of DNph (Scheme S1): Nicotinic acid ( $1.24 \mathrm{~g}, 10 \mathrm{mmol}$ ) and $\alpha, \alpha^{\prime}$-dichloro- $p$-xylene ( 0.96 $\mathrm{g}, 5.5 \mathrm{mmol})$ were dissolved in acetonitrile $(30 \mathrm{~mL})$ at $95^{\circ} \mathrm{C}$ and then stirred for 24 h . The emerged white solid was isolated by filtration, washed with acetonitrile and dried at $50^{\circ} \mathrm{C}$ for 12 h to give the final product DNph ( $1.54 \mathrm{~g}, 73 \%$ yield).Found: N, $6.58 \%$; C, $56.06 \%$; H, $4.361 \%$; on theory: N, 6.64\%; C, $57.02 \%$; H, 4.30\%.


Scheme S1. Synthesis of 1,4-bis[(3-carboxypyridino)methyl]-phenyl dichloride (DNph).

Synthesis of DNph $\mathbf{2}_{\mathbf{2}}$ (Scheme S2): Nicotinic acid ( $1.24 \mathrm{~g}, 10 \mathrm{mmol}$ ) and 4,4'-bis(chloromethyl)bipheny $(1.38 \mathrm{~g}, 5.5 \mathrm{mmol})$ were dissolved in acetonitrile $(30 \mathrm{~mL})$ at $95^{\circ} \mathrm{C}$ and then stirred for 24 h . The emerged white solid was isolated by filtration, washed with acetonitrile and dried at $50^{\circ} \mathrm{C}$ for 12 h to give the final product $\mathrm{DNph}_{2}(1.77 \mathrm{~g}, 71 \%$ yield). Found: $\mathrm{N}, 5.51 \% ; \mathrm{C}, 61.40 \% ; \mathrm{H}, 4.55 \%$; on theory: N, 5.63\%; C, $62.78 \%$; H, 4.46\%.


Scheme S2. Synthesis of 4,4'-bis[(4-carboxypyridino)methyl]-biphenyl dichloride ( $\mathrm{DNph}_{2}$ ).

Synthesis of TNph (Scheme S3):Nicotinic acid (0.868 g, 7 mmol$)$ and 1,3,5$\operatorname{tris}($ bromomethyl $)$ benzene $(0.707 \mathrm{~g}, 2 \mathrm{mmol})$ were dissolved in acetonitrile $(30 \mathrm{~mL})$ at $95^{\circ} \mathrm{C}$ and then stirred for 24 h . The emerged white solid was isolated by filtration, washed with acetonitrile and dried at $50^{\circ} \mathrm{C}$ for 12 h to give the final product $\mathrm{TNph}(1.13 \mathrm{~g}, 78 \%$ yield). Found: N, $5.71 \% ; \mathrm{C}, 44.21 \% ; \mathrm{H}$, $3.37 \%$; on theory: N, $5.79 \%$; C, $44.65 \%$; H, $3.33 \%$.


Scheme S3. Synthesis of 1,3,5-tris[(3-carboxypyridino)methyl]-phenyl tribromide (TNph).

Synthesis of TIph (Scheme S4): Isonicotinic acid (1.24 g, 10 mmol ) and 1,3,5Tris(bromomethyl)benzene ( $1.96 \mathrm{~g}, 5.5 \mathrm{mmol}$ ) were dissolved in acetonitrile ( 30 mL ) at $95{ }^{\circ} \mathrm{C}$ and then stirred for 24 h . The emerged white solid was isolated by filtration, washed with acetonitrile and dried at $50^{\circ} \mathrm{C}$ for 12 h to give the final product $\operatorname{TIph}(2.30 \mathrm{~g}, 76 \%$ yield). Found: $\mathrm{N}, 5.64 \% ; \mathrm{C}, 44.51 \%$; H, 3.52\%; on theory: N, $5.79 \%$; C, $44.65 \%$; H, 3.33\%.


Scheme S4. Synthesis of 1,3,5-tris[(4-carboxypyridino)methyl]-phenyl tribromide (TIph).

## 2. Synthesis of ionic mesoporous polyamides

Synthesis of DNph-PTA (Scheme S5): A 50 mL flask was charged with DNph ( $0.286 \mathrm{~g}, 0.8 \mathrm{mmol}$ ) and dichloroethane ( $\mathrm{DEC}, 20 \mathrm{~mL}$ ), followed by dropwise addition of sulfoxide chloride ( $\mathrm{SOCl}_{2}, 0.2 \mathrm{~g}$, $1.7 \mathrm{mmol})$. The mixture was stirred at room temperature for 2 h and the suspension became a dark brown solution. Residual $\mathrm{SOCl}_{2}$ was removed by rotary evaporation. The obtained acyl chloride intermediate was dissolved in dry N-methyl pyrrolidone (NMP) ( 10 mL ), followed by dropwise addition of a solution of triethylamine (TEA, $0.1 \mathrm{~g}, 1 \mathrm{mmol}$ ) and bi-phenyl tetramine (PTA, 0.128 g , 0.6 mmol ) in 10 mL N,N-dimethylformamide (DMF) at $0{ }^{\circ} \mathrm{C}$. The mixture was heated at $140{ }^{\circ} \mathrm{C}$ for

24 h . The precipitate was isolated by filtration, washed with a mixture solution of methanol/water ( $\mathrm{v} / \mathrm{v}=1 / 1$ ), and then dried under vacuum to give a brown powder.


Scheme S5. Synthesis of DNph-PTA.

Synthesis of DNph $\mathbf{2}_{\mathbf{2}}$-PTA (Scheme S6): A 50 mL flask was charged with $\mathrm{DNph}_{2}(0.397 \mathrm{~g}, 0.8$ mmol )and dichloroethane ( $\mathrm{DEC}, 20 \mathrm{~mL}$ ), followed by dropwise addition of sulfoxide chloride $\left(\mathrm{SOCl}_{2}\right.$, $0.2 \mathrm{~g}, 1.7 \mathrm{mmol}$ ). The mixture was stirred at room temperature for 2 h and the suspension became a dark brown solution. Residual $\mathrm{SOCl}_{2}$ was removed by rotary evaporation. The obtained acyl chloride intermediate was dissolved in dry N-methyl pyrrolidone (NMP) ( 10 mL ), followed by dropwise addition of a solution of triethylamine (TEA, $0.1 \mathrm{~g}, 1 \mathrm{mmol}$ ) and bi-phenyl tetramine (PTA, 0.128 g , 0.6 mmol ) in 10 mL N,N-dimethylformamide (DMF) at $0^{\circ} \mathrm{C}$. The mixture was heated at $140{ }^{\circ} \mathrm{C}$ for 24 h . The precipitate was isolated by filtration, washed with a mixture solution of methanol/water ( $\mathrm{v} / \mathrm{v}=1 / 1$ ), and then dried under vacuum to give a brown powder.


Scheme S6. Synthesis of $\mathrm{DNph}_{2}$-PTA.

Synthesis of TIph-PTA (Scheme S7): A 50 mL flask was charged with TIph ( $0.581 \mathrm{~g}, 0.8 \mathrm{mmol}$ ) and
dichloroethane ( $\mathrm{DEC}, 20 \mathrm{~mL}$ ), followed by dropwise addition of sulfoxide chloride $\left(\mathrm{SOCl}_{2}, 0.2 \mathrm{~g}, 1.7\right.$ mmol ). The mixture was stirred at room temperature for 2 h and the suspension became a dark brown solution. Residual $\mathrm{SOCl}_{2}$ was removed by rotary evaporation. The obtained acyl chloride intermediate was dissolved in dry N-methyl pyrrolidone (NMP) ( 10 mL ), followed by dropwise addition of a solution of triethylamine (TEA, $0.1 \mathrm{~g}, 1 \mathrm{mmol}$ ) and bi-phenyl tetramine (PTA, $0.128 \mathrm{~g}, 0.6 \mathrm{mmol}$ ) in 10 mL N,N-dimethylformamide (DMF) at $0{ }^{\circ} \mathrm{C}$. The mixture was heated at $140^{\circ} \mathrm{C}$ for 24 h . The precipitate was isolated by filtration, washed with a mixture solution of methanol/water ( $\mathrm{v} / \mathrm{v}=1 / 1$ ), and then dried under vacuum to give a brown powder.


Scheme S7. Synthesis of TIph-PTA.

Synthesis of TNph-PDA (Scheme S8): A 50 mL flask was charged with TNph ( $0.581 \mathrm{~g}, 0.8 \mathrm{mmol}$ ) and dichloroethane ( $\mathrm{DEC}, 20 \mathrm{~mL}$ ), followed by dropwise addition of sulfoxide chloride ( $\mathrm{SOCl}_{2}, 0.2 \mathrm{~g}$, 1.7 mmol ). The mixture was stirred at room temperature for 2 h and the suspension became a dark brown solution. Residual $\mathrm{SOCl}_{2}$ was removed by rotary evaporation. The obtained acyl chloride intermediate was dissolved in dry N-methyl pyrrolidone (NMP) ( 10 mL ), followed by dropwise addition of a solution of triethylamine (TEA, $0.1 \mathrm{~g}, 1 \mathrm{mmol}$ ) and para-phenylene diamine (PDA, 0.130 $\mathrm{g}, 1.2 \mathrm{mmol}$ ) in $10 \mathrm{~mL} \mathrm{~N}, \mathrm{~N}$-dimethylformamide (DMF) at $0^{\circ} \mathrm{C}$. The mixture was heated at $140^{\circ} \mathrm{C}$ for 24 h . The precipitate was isolated by filtration, washed with a mixture solution of methanol/water ( $\mathrm{v} / \mathrm{v}=1 / 1$ ), and then dried under vacuum to give a brown powder.


Scheme S8. Synthesis of TNph-PDA.

Synthesis of TNph-TAPB (Scheme S9): A 50 mL flask was charged with TNph ( $0.581 \mathrm{~g}, 0.8 \mathrm{mmol}$ ) and dichloroethane ( $\mathrm{DEC}, 20 \mathrm{~mL}$ ), followed by dropwise addition of sulfoxide chloride ( $\mathrm{SOCl}_{2}, 0.2 \mathrm{~g}$, $1.7 \mathrm{mmol})$. The mixture was stirred at room temperature for 2 h and the suspension became a dark brown solution. Residual $\mathrm{SOCl}_{2}$ was removed by rotary evaporation. The obtained acyl chloride intermediate was dissolved in dry N-methyl pyrrolidone (NMP) ( 10 mL ), followed by dropwise addition of a solution of triethylamine (TEA, $0.1 \mathrm{~g}, 1 \mathrm{mmol}$ ) and1,3,5-tris(4-aminophenyl)benzene (TAPB, $0.281 \mathrm{~g}, 0.8 \mathrm{mmol}$ ) in $10 \mathrm{~mL} \mathrm{~N}, \mathrm{~N}$-dimethylformamide (DMF) at $0^{\circ} \mathrm{C}$. The mixture was heated at $140^{\circ} \mathrm{C}$ for 24 h . The precipitate was isolated by filtration, washed with a mixture solution of methanol/water ( $\mathrm{v} / \mathrm{v}=1 / 1$ ), and then dried under vacuum to give a brown powder.


Scheme S9. Synthesis of TNph-TAPB.

Synthesis of TNph-TAPM (Scheme S10): A 50 mL flask was charged with TNph ( $0.581 \mathrm{~g}, 0.8 \mathrm{mmol}$ ) and dichloroethane ( $\mathrm{DEC}, 20 \mathrm{~mL}$ ), followed by dropwise addition of sulfoxide chloride ( $\mathrm{SOCl}_{2}, 0.2 \mathrm{~g}$, 1.7 mmol ). The mixture was stirred at room temperature for 2 h and the suspension became a dark brown solution. Residual $\mathrm{SOCl}_{2}$ was removed by rotary evaporation. The obtained acyl chloride intermediate was dissolved in dry N-methyl pyrrolidone (NMP) ( 10 mL ), followed by dropwise addition of a solution of triethylamine (TEA, $0.1 \mathrm{~g}, 1 \mathrm{mmol}$ ) andtetra(4-aminophenyl)methane (TAPM, $0.228 \mathrm{~g}, 0.6 \mathrm{mmol}$ ) in $10 \mathrm{~mL} \mathrm{~N}, \mathrm{~N}$-dimethylformamide (DMF) at $0^{\circ} \mathrm{C}$. The mixture was heated at 140 ${ }^{\circ} \mathrm{C}$ for 24 h . The precipitate was isolated by filtration, washed with a mixture solution of methanol/water ( $\mathrm{v} / \mathrm{v}=1 / 1$ ), and then dried under vacuum to give a brown powder.


Scheme S10. Synthesis of TNph-TAPM.

Synthesis of TA-PTA (Scheme S11): A 50 mL flask was charged with trimesic acid (TA, $0.168 \mathrm{~g}, 0.8$ mmol )and dichloroethane ( $\mathrm{DEC}, 20 \mathrm{~mL}$ ), followed by dropwise addition of sulfoxide chloride ( $\mathrm{SOCl}_{2}$, $0.2 \mathrm{~g}, 1.7 \mathrm{mmol}$ ). The mixture was stirred at room temperature for 2 h and the suspension became a dark brown solution. Residual $\mathrm{SOCl}_{2}$ was removed by rotary evaporation. The obtained acyl chloride intermediate was dissolved in dry N-methyl pyrrolidone (NMP) ( 10 mL ), followed by dropwise addition of a solution of triethylamine (TEA, $0.1 \mathrm{~g}, 1 \mathrm{mmol}$ ) andbi-phenyl tetramine (PTA, $0.128 \mathrm{~g}, 0.6$ mmol) in 10 mL N,N-dimethylformamide (DMF) at $0{ }^{\circ} \mathrm{C}$. The mixture was heated at $140^{\circ} \mathrm{C}$ for 24 h . The precipitate was isolated by filtration, washed with a mixture solution of methanol/water ( $\mathrm{v} / \mathrm{v}=1 / 1$ ), and then dried under vacuum to give a brown powder.


Scheme S11. Synthesis of TA-PTA.

Synthesis of PDMBr (Scheme S12): 1-Vinylimidazole ( $5.00 \mathrm{~g}, 53.2 \mathrm{mmol}$ ) and $\mathrm{CH}_{2} \mathrm{Br}_{2}(4.62 \mathrm{~g}, 26.6$ mmol ) were dissolved in 5 mL THF. After stirring at room temperature for 1 h , the mixture was solvothermally treated at $100^{\circ} \mathrm{C}$ for 24 h . After cooling to room temperature, the obtained crude salt was washed with diethyl ether and dried under vacuum, giving the light yellow powder product, 3,3-methylene-divinylimidazole dibromide ([C1DVIM]Br). [C1DVIM]Br ( 0.3 g ), [C4MIM]Br (6g), $\mathrm{H}_{2} \mathrm{O}$
$(0.75 \mathrm{~mL})$ and AIBN $(0.03 \mathrm{~g})$ were placed in a Teflon-lined stainless steel autoclave. Subsequently, the above mixture was stirred for 2 h to give a homogeneous and transparent solution. The polymerization was triggered by statically heating at $100^{\circ} \mathrm{C}$ for 24 h . The solidified composite was washed with water and then dried under vacuum at $80^{\circ} \mathrm{C}$.


Scheme S12. Synthesis of PDMBr.

## Supplementary Fig.s



Fig. S1 ${ }^{1} \mathrm{H}$ NMR spectrum of DNph.


Fig. S2 ${ }^{1} \mathrm{H}$ NMR spectrum of $\mathrm{DNph}_{2}$.


Fig. S3 ${ }^{1} \mathrm{H}$ NMR spectrum of TNph.


Fig. S4 ${ }^{1} \mathrm{H}$ NMR spectrum of TIph.


Fig. $55{ }^{1} \mathrm{H}$ NMR spectrum of $\left[\mathrm{C}_{1} \mathrm{DVIM}\right] \mathrm{Br}$.


Fig. S6 FTIR spectra of DNph-PTA, DNph ${ }_{2}$-PTA and TIph-PTA.


Fig. S7 FTIR spectra of TNph-PDA, TNph-TAPB and TNph-TAPM.


Fig. S8 TG curves of DNph-PTA, DNph ${ }_{2}$-PTA, TNph-PTA, TIph-PTA, TNph-PDA, TNph-TAPB, and TNph-TAPM.


Fig. S9 XRD patterns of DNph-PTA, $\mathrm{DNph}_{2}$-PTA, TNph-PTA, TIph-PTA, TNph-PDA, TNph-TAPB, and TNph-TAPM.


Fig. S10 SEM images of (A) DNph-PTA, (B) DNph - PTA, (C) TIph-PTA, (D) TNph-PDA, (E) TNphTAPB, and (F) TNph-TAPM.


Fig. S11 SEMand elemental mapping images of N, O and Br for TNph-PTA.


Fig. $\mathbf{S 1 2}$ (A) $\mathrm{N}_{2}$ sorption isotherms and (B) pore size distribution curves of iMPAs. The synthetic procedure was same as TNph-PTA except by using solvents of (a) NMP ( 15 mL ), (b) DMF ( 15 mL ), (c) DMF/NMP ( $10 \mathrm{~mL} / 10 \mathrm{~mL}$ ), (d) DMF/NMP ( $5 \mathrm{~mL} / 10 \mathrm{~mL}$ ), (e) DMF/NMP ( $10 \mathrm{~mL} / 5 \mathrm{~mL}$ ), (f) THF/NMP ( $10 \mathrm{~mL} / 10 \mathrm{~mL}$ ), (g) TMB/NMP ( $10 \mathrm{~mL} / 10 \mathrm{~mL}$ ). Synthesis condition: TNph 0.8 mmol , PTA $0.6 \mathrm{mmol}, \mathrm{SOCl}_{2} 1.7 \mathrm{mmol}$, TEA $1 \mathrm{mmol}, 140^{\circ} \mathrm{C}, 24 \mathrm{~h}$.


Fig. S13 SEM images of iMPAs. The synthetic procedure was same as that of TNph-PTA except by using solvents of (A) NMP 15 mL , (B) DMF 15 mL , (C) DMF/NMP ( $5 \mathrm{~mL} / 10 \mathrm{~mL}$ ), (D) DMF/NMP $(10 \mathrm{~mL} / 5 \mathrm{~mL})$, (E) THF/NMP $(10 \mathrm{~mL} / 10 \mathrm{~mL})$, and (F) TMB/NMP $(10 \mathrm{~mL} / 10 \mathrm{~mL})$, respectively.


Fig. S14 FTIR spectra of iMPAs. The synthetic procedure was same as TNph-PTA except for polymerization time of $3,6,12$, and 24 h , respectively.


Fig. $\mathbf{S 1 5}$ (A) $\mathrm{N}_{2}$ sorption isotherms and (B) pore size distribution curves of iMPAs. The synthetic procedure was same as TNph-PTA except for polymerization time of(a) 3 h , (b) 6 h , (c) 12 h , and (d) 24 h , respectively.


Fig. S16 (A) $\mathrm{N}_{2}$ sorption isotherms and (B) pore size distribution curves of (a) $\mathrm{Ru}_{0.5} @$ TNph-PTA, (b) $\mathrm{Ru}_{1.5} @ T \mathrm{Nph}-\mathrm{PTA}$, (c) Ru $\mathrm{u}_{5} @ T \mathrm{Nph}-\mathrm{PTA}$ and (d) Ru $\mathrm{s}_{8} @ T \mathrm{Tph}-\mathrm{PTA}$.


Fig. S17 (A) SEM and (B) SEM mapping images of $\mathrm{Ru}_{1.5} @ T \mathrm{Nph}-\mathrm{PTA}$.


Fig. S18 TG curves of TNph-PTA and Ru $u_{1.5} @$ TNph-PTA.


Fig. S19 FTIR spectra of TNph-PTA, Ru $\mathrm{u}_{1.5}(\mathrm{III}) @$ TNph-PTA and $\mathrm{Ru}_{1.5} @$ TNph-PTA.


Fig. S20 XRD patterns of TNph-PTA and Ru $u_{1.5} @$ TNph-PTA.


Fig. S21 TEM images of (A) Ru/C, (B) $\mathrm{Ru}_{1.5} @ T N p h-P T A-N$, (C) Ru $\mathrm{u}_{1.5} @ T A-P T A$, and (D) $\mathrm{Ru}_{1.5} @ \mathrm{PDMBr}$.


Fig. $\mathbf{S 2 2} \mathrm{N}_{2}$ sorption isotherm of TNph-PTA-N.


Fig. S23 $\mathrm{N}_{2}$ sorption isotherm of $\mathrm{Ru}_{1.5} @$ TNph-PTA-N.


Fig. S24 $\mathrm{N}_{2}$ sorption isotherms (inset: pore size distribution curves) of TA-PTA.


Fig. S25 $\mathrm{N}_{2}$ sorption isotherm (inset: pore size distribution curve) of $\mathrm{Ru}_{1.5} @ T A-P T A$.


Fig. S26 $\mathrm{N}_{2}$ sorption isotherm (inset: pore size distribution curve) of PDMBr.


Fig. $\mathbf{S 2 7} \mathrm{N}_{2}$ sorption isotherm (inset: pore size distribution curve) of $\mathrm{Ru}_{1.5} @$ PDMBr.


Fig. S28 (A) survey scan, (B) C 1s, (C) N 1s, (D) O 1s, and (E) Ru 3p XPS spectra of Ru $\mathrm{p}_{1.5} @ T A-P T A$.


Fig. S29 (A) survey scan, (B) C 1s, (C) N 1s, (D) Ru 3p XPS spectra of Ru $\mathrm{u}_{1.5} @$ PDMBr.


Fig. $\mathbf{S 3 0}$ (A) survey scan, (B) C 1s, (C) N 1s, (D) O 1s, and (E) Ru 3p XPS spectra of Ru/C.


Fig. S31 Recyclability of $\mathrm{Ru}_{1.5} @ T \mathrm{Tph}-\mathrm{PTA}$ for hydrogenation of LA to GVL. Reaction conditions: 1 $\mathrm{mmol} \mathrm{LA}, 4 \mathrm{~mL}$ water, $\mathrm{LA} / \mathrm{Ru}=350,70^{\circ} \mathrm{C}, 4 \mathrm{~h}, 1 \mathrm{MPa}$.


Fig. S32 Kinetic curves of the fresh catalyst (solid lines) and recovered catalyst (dashed line, the $5^{\text {th }}$ run). Reaction conditions: $1 \mathrm{mmol} \mathrm{LA}, 4 \mathrm{~mL}$ water, $\mathrm{LA} / \mathrm{Ru}=350,4 \mathrm{~h}, 1 \mathrm{MPa} 150^{\circ} \mathrm{C}$.


Fig. S33 (A) SEM and (B) TEM image of recovered $\mathrm{Ru}_{1.5} @$ TNph-PTA.


Fig. S34 $\mathrm{N}_{2}$ sorption isotherm (inset: pore size distribution curve) of recovered $\mathrm{Ru}_{1.5} @$ TNph-PTA.








Fig. S35 Hydrogenation and dehydration of LA to produce GVL. In this system Path 1 was occurred.


Fig. S36 GC-MS analysis of the liquid phase after reaction. Reaction conditions: catalyst $\mathrm{Ru}_{1.5} @ \mathrm{TNph}-$ PTA 19 mg , LA 10 mmol , water $4 \mathrm{~mL}, \mathrm{LA} / \mathrm{Ru}=3500,150^{\circ} \mathrm{C}, 1 \mathrm{~h}, 1 \mathrm{MPa}$.


Fig. S37 Time resolved conversion and yield in $\mathrm{Ru}_{1.5} @ T \mathrm{TNph}-\mathrm{PTA}$ catalyzed conversion of LA into GVL at (A) $70{ }^{\circ} \mathrm{C}$ and (B) $50^{\circ} \mathrm{C}$. Reaction conditions: $1 \mathrm{mmol} \mathrm{LA}, 4 \mathrm{~mL}$ water, $\mathrm{LA} / \mathrm{Ru}=350,4 \mathrm{~h}, 1$ MPa .


Fig. S38 Plots of $\ln \left(\mathrm{C}_{\mathrm{t}} / \mathrm{C}_{0}\right)$ vs. reaction time in $\mathrm{Ru}_{1.5} @ T \mathrm{Tph}-\mathrm{PTA}$ catalyzed conversion of LA into GVLat (A) $150^{\circ} \mathrm{C}$, (B) $100^{\circ} \mathrm{C}$, (C) $70^{\circ} \mathrm{C}$, (D) $50^{\circ} \mathrm{C}$.Reaction conditions: $1 \mathrm{mmol} \mathrm{LA}, 4 \mathrm{~mL}$ water, $\mathrm{LA} / \mathrm{Ru}=350,4 \mathrm{~h}, 1 \mathrm{MPa}$.


Fig. S39 Plots of $\ln (\mathrm{k})$ against $\mathrm{T}^{-1}$ for LA hydrogenation. Reaction conditions: 1 mmol LA, 4 mL water,LA/Ru=350, $4 \mathrm{~h}, 1 \mathrm{MPa}$.

Table S1. Element analyses

| Entry | Sample | $\mathrm{N} \%$ | $\mathrm{C} \%$ | $\mathrm{H} \%$ |
| :---: | :--- | :---: | :---: | :---: |
| 1 | DNph-PTA | 16.51 | 47.90 | 5.37 |
| 2 | DNph $_{2}$-PTA | 14.84 | 56.38 | 7.10 |
| 3 | TNph-PTA | 13.89 | 54.18 | 3.98 |
| 4 | TIph-PTA | 8.45 | 53.94 | 4.23 |
| 5 | TNph-PDA | 10.95 | 51.31 | 3.65 |
| 6 | TNph-TAPB | 9.54 | 61.76 | 4.78 |
| 7 | TNph-TAPM | 11.30 | 55.99 | 5.48 |
| 8 | Ru $_{1.5} @$ ONph-PTA | 13.41 | 54.09 | 3.81 |

Table S2. Synthetic conditions and textural properties ${ }^{a}$

| Entry | Solvent | Volume $(\mathrm{mL})^{b}$ | $\mathrm{S}_{\mathrm{BET}^{c}}$ <br> $\left(\mathrm{~m}^{2} \mathrm{~g}^{-1}\right)$ | $\mathrm{Vp}^{d}$ <br> $\left(\mathrm{~cm}^{3} \mathrm{~g}^{-1}\right)$ | $\mathrm{Dp}^{e}$ <br> $(\mathrm{~nm})$ |
| :---: | :--- | :---: | :---: | :---: | :---: |
| 1 | NMP | 15 | 122 | 0.61 | 20.1 |
| 2 | DMF | 15 | 25 | 0.10 | 15.6 |
| 3 | DMF/NMP | $10 / 10$ | 150 | 0.78 | 20.8 |
| 4 | DMF/NMP | $5 / 10$ | 94.2 | 0.45 | 19.2 |
| 5 | DMF/NMP | $10 / 5$ | 47.7 | 0.22 | 18.8 |
| 6 | THF/NMP | $10 / 10$ | 26.1 | 0.09 | 13.4 |
| 7 | TMB/NMP | $10 / 10$ | 42.4 | 0.31 | 29.1 |

$a_{\mathrm{i}}$ MPAs synthesized through the condensation of TNph and PTA by using different solvents. Synthesis condition: TNph 0.8 mmol , PTA $0.6 \mathrm{mmol}, \mathrm{SOCl}_{2} 1.7 \mathrm{mmol}$, TEA $1 \mathrm{mmol}, 140{ }^{\circ} \mathrm{C}, 24 \mathrm{~h} .{ }^{b}$ Solvent volume in the synthesis system. ${ }^{c} \mathrm{BET}$ surface area. ${ }^{d}$ Total pore volume. ${ }^{e}$ Average pore diameter.

Table S3. Synthetic conditions and textural properties ${ }^{a}$

| Entry | Reaction time (h) | Production <br> yield (\%) | $\mathrm{S}_{\mathrm{BET}^{b}}$ <br> $\left(\mathrm{~m}^{2} \mathrm{~g}^{-1}\right)$ | $\mathrm{Vp}^{c}$ <br> $\left(\mathrm{~cm}^{3} \mathrm{~g}^{-1}\right)$ | $\mathrm{Dp}^{d}$ <br> $(\mathrm{~nm})$ |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | 3 | 19.4 | 1.4 | - | - |
| 2 | 6 | 50.3 | 18 | 0.135 | 29.3 |
| 3 | 12 | 58.3 | 22 | 0.07 | 13.3 |
| 4 | 24 | 61.1 | 150 | 0.78 | 20.8 |

$a_{\mathrm{i}}$ MPAs synthesized through the condensation of TNph and PTA by different polymerization time. ${ }^{b}$ BET surface area. ${ }^{c}$ Total pore volume. ${ }^{d}$ Average pore diameter.

Table S4. Textural properties

| Entry | Sample | Ru (wt\%) | $\begin{gathered} \mathrm{S}_{\mathrm{BEE}{ }^{a}} \\ \left(\mathrm{~m}^{2} \mathrm{~g}^{-1}\right) \end{gathered}$ | $\begin{gathered} \mathrm{Vp}^{b} \\ \left(\mathrm{~cm}^{3} \mathrm{~g}^{-1}\right) \end{gathered}$ | $\begin{gathered} \mathrm{Dp}^{c} \\ (\mathrm{~nm}) \end{gathered}$ |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | $\mathrm{Ru}_{0.5} @$ TNph-PTA | 0.51 | 84 | 0.56 | 15.3 |
| 2 | $\mathrm{Ru}_{5}$ @TNph-PTA | 3.82 | 60 | 0.31 | 13.9 |
| 3 | Ru8@TNph-PTA | 5.68 | 49 | 0.29 | 12.7 |
| 4 | $\mathrm{Ru} / \mathrm{C}$ | 5 | 808 | 0.41 | 2 |
| 5 | TNph-PTA-N | - | 5 | 0.02 | - |
| 6 | $\mathrm{Ru}_{1.5} @$ TNph-PTA-N | 1.25 | 3 | 0.01 | - |
| 7 | TA-PTA | - | 80 | 0.61 | 30.2 |
| 8 | Ru1.5@TA-PTA | 1.23 | 69 | 0.54 | 26.5 |
| 9 | PDMBr | - | 121 | 0.68 | 22.4 |
| 10 | $\mathrm{Ru}_{1.5} @ \mathrm{PDMBr}$ | 1.62 | 94 | 0.51 | 15.9 |
| 11 | Reused $\mathrm{Ru}_{1.5} @$ TNph-PTA | 1.44 | 85 | 0.39 | 14.8 |

${ }^{a}$ BET surface area. ${ }^{b}$ Total pore volume. ${ }^{c}$ Average pore diameter.

Table S5. Dispersion and specific active surface area of Ru in catalysts

|  | Dispersion (\%) | Ru metal S. A. $\left(\mathrm{m}^{2} \mathrm{~g}^{-1}\right)^{\mathrm{a}}$ | Average particle size (nm) | $\begin{aligned} & \text { GVL } \\ & (\%) \end{aligned}$ | Yield |
| :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathrm{Ru}_{0.5} @$ TNph-PTA | 37 | 134.2 | 1.71 | 97.8 |  |
| $\mathrm{Ru}_{1.5} @ \mathrm{TNph}-\mathrm{PTA}$ | 35 | 126.9 | 1.82 | 96.3 |  |
| $\mathrm{Ru}_{5} @$ TNph-PTA | 31 | 112.4 | 2.15 | 94.5 |  |
| Ru_@TNph-PTA | 29 | 105.1 | 2.07 | 93.7 |  |
| Ru1.5@TNph-PTA-N | 23 | 83.4 | 3.21 | 64.8 |  |
| $\mathrm{Ru}_{1.5} @ \mathrm{PDMBr}$ | 28 | 101.5 | 2.48 | 87.4 |  |
| $\mathrm{Ru}_{1.5} @$ TA-PTA | 25 | 90.7 | 2.60 | 70.5 |  |
| $\mathrm{Ru} / \mathrm{C}$ | 16 | 59.9 | 12.3 | 43.8 |  |
| Reused $\mathrm{Ru}_{1.5} @ \mathrm{TNph}-$ PTA | 33 | 119.7 | 2.08 | 94.3 |  |

${ }^{\text {a }}$ specific active surface area of Ru.

Table S6. The surface chemical state of Ru species and the proportion of $\mathrm{Ru}(0)$

|  |  | $\mathrm{Ru}_{1.5} @ T N p h-P T A$ | $\mathrm{Ru}_{1.5} @$ PDMBr | $\mathrm{Ru}_{1.5} @$ TA-PTA | $\mathrm{Ru} / \mathrm{C}$ |
| :--- | :--- | :---: | :---: | :---: | :---: |
| B.E. <br> (eV) | $\mathrm{Ru}(0)$ | $\mathrm{Ru}(\mathrm{III})$ | $484.4 / 462.2$ | $484.4 / 462.2$ | $484.4 / 462.2$ |
|  | $\mathrm{~A}_{(\mathrm{Ru}(0))} / \mathrm{A}_{(\mathrm{Ru}(\mathrm{III}))}$ | $70.7 \% / 29.3 \%$ | $62.1 \% / 37.9 \%$ | $54.5 \% / 45.5 \%$ | $38.4 / 462.2$ |

Table S7. Hydrogenation of LA into GVL ${ }^{a}$

| Entry Samples | $\mathrm{Ru} \mathrm{wt} \%$ | Particle size <br> $(\mathrm{nm})$ | Conv. <br> $(\%)$ | Yield <br> $(\%)$ | $\mathrm{TON}^{b}$ | $\mathrm{TOF}^{c}\left(\mathrm{~h}^{-1}\right)$ | $\mathrm{STY}^{d}$ |
| :--- | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | $\mathrm{Ru} / \mathrm{C}$ | 5.00 | 12.3 | 21.7 | 8.5 | 297 | 891 |
| 2 | $\mathrm{Ru}_{8} @ \mathrm{TNph}-P T A$ | 5.68 | 2.07 | 48.3 | 21.4 | 749 | 2247 |
| $3^{e}$ | $\mathrm{Ru} / \mathrm{C}$ | 5.00 | 12.3 | 15.9 | 5.6 | 979 | 2937 |
| $4^{e}$ | $\mathrm{Ru}_{8} @ \mathrm{TNph}-\mathrm{PTA}$ | 5.68 | 2.07 | 29.2 | 11.9 | 2082 | 6246 |

${ }^{a}$ Reaction conditions: $10 \mathrm{mmol} \mathrm{LA}, 4 \mathrm{~mL}$ water, $\mathrm{LA} / \mathrm{Ru}=3500,150{ }^{\circ} \mathrm{C}, 20 \mathrm{~min}, 1 \mathrm{MPa} .{ }^{b}$ Turnover number $(\mathrm{TON})=\mathrm{mol}$ GVL obtained) $/(\mathrm{mol} \mathrm{Ru}) .{ }^{c}$ Turnover frequency $(\mathrm{TOF})=(\mathrm{mol} \mathrm{GVL}$ obtained $) /(\mathrm{mol} \mathrm{Ru} \times \mathrm{h}) .{ }^{d}$ Space time yield $(\mathrm{STY})=(\mathrm{g}$ GVL obtained $) /(\mathrm{gcatalyst} \times \mathrm{h}) .{ }^{e} 50 \mathrm{mmol}$ LA (LA/Ru=17500).

Table S8. Comparison of supported catalysts in hydrogenation of LA to GVL

| Entry | Catalysts | $\begin{gathered} \mathrm{Ru} \\ (\mathrm{wt} \%) \end{gathered}$ | $\begin{gathered} \mathrm{T} \\ \left({ }^{\circ} \mathrm{C}\right) \end{gathered}$ | $\begin{gathered} \mathrm{H}_{2} \\ (\mathrm{MPa}) \end{gathered}$ | Solvent | Yield ${ }^{a} /$ Yield ${ }^{b}$ | TOF ${ }^{\text {c }}$ | $\begin{gathered} \mathrm{STY}^{d} \\ \left(\mathrm{~g}_{\mathrm{GVL}} \mathrm{~g}_{\text {catalast }^{-1}} \mathrm{~h}^{-1}\right) \end{gathered}$ | Ref. |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | $\mathrm{Ru}-\mathrm{Pd} / \mathrm{TiO}_{2}$ | 1.0 | 200 | 4.0 | 1,4-dioxane | 99.6/- | 2160 | - | S1 |
| 2 | $\mathrm{Ru} / \mathrm{ZrO}_{2}$ | 1.0 | 150 | 3.0 | $\gamma$ - <br> octalactone | 100/94.3 | 936 | 3.83 | S2 |
| 3 | 2RuAl-SEA | 2.0 | 220 | 1.38 | 1,4-dioxane | -/- | 2484 | 4.06 | S3 |
| 4 | 0.300Ru-CNF | 0.27 | 150 | 4.5 | solvent-free | 95/62 | 956 | 3.13 | S4 |
| 5 | $\mathrm{Ru} / \mathrm{ZrO}_{2} @ \mathrm{C}$ | 0.85 | 140 | 1.0 | water | 96.4/88.4 | 482 | 2.35 | S5 |
| 6 | Ru-HAP | 4.9 | 70 | 0.5 | water | 99/89 | 14.9 | 5.00 | S6 |
| 7 | Ru/MIL-101(Cr) | 5.0 | 70 | 1.0 | water | 86/52 | 71.6 | 4.40 | S7 |
| 8 | Ru/SMS | 4.6 | 70 | 0.5 | water | 95.6/- | 50 | 0.66 | S8 |
| 9 | $\mathrm{Ru} / \mathrm{Mg}-\mathrm{LaO}$ | 5.0 | 130 | 1.2 | water | 99/- | 87 | 4.52 | S9 |
| 10 | $\mathrm{Ru}_{1.5} @ \mathrm{TNph}-\mathrm{PTA}$ | 1.46 | 150 | 1.0 | water | 96.3/94.3 | 84.3 | 1.42 | This <br> work |
|  | Ru $\mathrm{l}_{8}$ @TNph-PTA | 5.46 |  |  |  | 98.8/- | 462 | 19.0/411 ${ }^{\text {e }}$ |  |

${ }^{a}$ Yield of the fresh catalyst. ${ }^{b}$ Yield of the spent catalyst after several recycling runs and " - " means that the reusability was currently unclear.
${ }^{c}$ Turnover frequency $(\mathrm{TOF})=\mathrm{mol} \mathrm{GVL} /(\mathrm{mol} \mathrm{Ru} \times \mathrm{h}) .{ }^{d}$ Space time yield $=\mathrm{g} \mathrm{GVL} /($ gcatalyst $\times \mathrm{h}) .{ }^{e}$ under reaction time of 20 min.

## Details for the comparison of Ru catalysts in LA conversion to GVL

Table S8 lists the reaction conditions and catalytic performance of typical efficient Ru-based catalysts in the hydrogenation of LA into GVL. Though directly comparing the catalytic performances of different catalysts is difficult because of the variation of the reaction conditions (substrate amount, solvent, pressure, temperature, etc.), reasonable comparison can be made by comprehensively considering the activity (conversion, yield, TOF and STY etc.) and stability under similar reaction conditions. Various supported Ru and Ru alloy NPs exhibited high efficiency by using organic solvent or under solvent-free condition. However, the recycling performance of many systems was unclear or suffered from apparent deactivation. Noticeably, Ru NPs on iMPAs in this work maintained the activity in a five-run test under both saturated conversion (Fig. 5A) and moderate conversion (Fig. S31), which is additionally reflected by the almost identical kinetic curve of $\mathrm{Ru}_{1.5} @$ TNph-PTA in the $5^{\text {th }}$ run to that in the $1^{\text {st }}$ run (Fig. S32) plus the calculation of the cumulative TON and average TOF (Table S9 and S10, as seen below). Particularly, the combination of robust Ru NPs and high loading over the catalyst Ru $\mathrm{R}_{8}$ @TNph-PTA ( $5.68 \mathrm{wt} \%$ ) endow both high yield, turnover frequency (TOF) and space time yield (STY). The STY value was $19.0 \mathrm{~g}_{\mathrm{GVL}} \mathrm{g}_{\text {catalyst }}{ }^{-1} \mathrm{~h}^{-1}$ under complete conversion (>99) and dramatically increased to be $411 \mathrm{~g}_{G V L} \mathrm{~g}_{\text {catalyst }}{ }^{-1} \mathrm{~h}^{-1}$ within the initial stage (conversion: $30 \%$, reaction time: 20 min ), significantly exceeding previous ones under similar conditions. Besides, the reaction occurred under relatively low $\mathrm{H}_{2}$ pressure and by using water the solvent that is favorable from the green and sustainable perspective. The comparison above indicates that Ru NPs iMPAs in this work serves as the effective and stable heterogeneous catalyst for hydrogenation of LA to GVL.

Table S9. Recycling of Ru $\mathrm{u}_{1.5} @$ TNph-PTA in hydrogenation of LA into GVL

| Run | Yield | TON | Cumulative TON | Average TOF |
| :--- | :---: | :---: | :---: | :---: |
| 1 | 96.3 | 337 | 337 | 84.3 |
| 2 | 95.5 | 334 | 671 | 83.9 |
| 3 | 95.7 | 335 | 1006 | 83.8 |
| 4 | 95.1 | 333 | 1339 | 83.7 |
| 5 | 94.3 | 330 | 1669 | 83.5 |

Reaction conditions: $1 \mathrm{mmol} \mathrm{LA}, 4 \mathrm{~mL}$ water, $\mathrm{LA} / \mathrm{Ru}=350,4 \mathrm{~h}, 1 \mathrm{MPa}, 150^{\circ} \mathrm{C}$.
Table S10. Recycling of $\mathrm{Ru}_{1.5} @$ TNph-PTA in hydrogenation of LA into GVL

| Run | Yield | TON | Cumulative TON | Average TOF |
| :---: | :---: | :---: | :---: | :---: |
| 1 | 76.2 | 259 | 259 | 64.7 |
| 2 | 75.7 | 257 | 516 | 64.5 |
| 3 | 75.4 | 257 | 773 | 64.4 |
| 4 | 75.1 | 256 | 1029 | 64.3 |
| 5 | 75.3 | 256 | 1285 | 64.3 |

Reaction conditions: $1 \mathrm{mmol} \mathrm{LA}, 4 \mathrm{~mL}$ water, $\mathrm{LA} / \mathrm{Ru}=350,4 \mathrm{~h}, 1 \mathrm{MPa}, 70^{\circ} \mathrm{C}$.

Table S11. Calculation of minimized energy

| Object | Structureformula | Optimized configuration | Minimized energy ( $\mathrm{kcal} \mathrm{mol}^{-1}$ ) |
| :---: | :---: | :---: | :---: |
| TNph-PTAunit (Model I) |  |  | Stretch: 0.8239 <br> Bend: 3.4592 <br> Stretch-Bend: 0.1374 <br> Torsion:1.7683 <br> Non-1,4VDW: 4.5152 <br> 1,4 VDW: 14.9770 <br> Charge/Charge:-72.2915 <br> Charge/Dipole: 2.4331 <br> Dipole/Dipole: -6.7552 <br> TotalEnergy:-50.9327 kcal mol ${ }^{-1}$ |
| TNph-PTAunit $+\mathrm{Ru}$ |  |  | Stretch: 1.1127 <br> Bend: 4.4123 <br> Stretch-Bend: 0.2434 <br> Torsion: -10.0539 <br> Non-1,4 VDW: 1.8860 <br> 1,4 VDW: 17.8202 <br> Charge/Charge: -72.6749 <br> Charge/Dipole: -0.4884 <br> Dipole/Dipole: 1.9526 <br> Total Energy: -55.7900 $\mathbf{k c a l ~ m o l}^{-1}$ |
| PDMBr unit (Model II) |  |  | Stretch: 0.9580 <br> Bend: 28.2796 <br> Stretch-Bend: 0.0083 <br> Torsion: -1.2943 <br> Non-1,4 VDW: 25.3578 <br> 1,4 VDW: 6.5745 <br> Charge/Charge: -267.5262 <br> Charge/Dipole: -6.7967 <br> Dipole/Dipole: 0.0143 <br> Total Energy: - $\mathbf{2 1 4 . 4 2 4 7} \mathbf{~ k c a l ~ m o l}^{-1}$ |
| PDMBr unit + Ru |  |  | Stretch: 0.9522 <br> Bend: 28.2855 <br> Stretch-Bend: 0.0055 <br> Torsion: -1.3030 <br> Non-1,4 VDW: 23.7017 <br> 1,4 VDW: 6.5708 <br> Charge/Charge: -267.5271 <br> Charge/Dipole: -6.7760 <br> Dipole/Dipole: 0.0142 <br> Total Energy: -216.0761 $\mathbf{k c a l ~ m o l}^{-1}$ |


| TA-PTA unit (Model III) |  |  | Stretch: 0.5737 <br> Bend: 6.5607 <br> Stretch-Bend: 0.0658 <br> Torsion: 0.3964 <br> Non-1,4 VDW: 0.2506 <br> 1,4 VDW: 9.7154 <br> Dipole/Dipole: -9.4292 <br> Total Energy: 8.1335 kcal mol $^{-1}$ |
| :---: | :---: | :---: | :---: |
| TA-PTA unit $+\mathrm{Ru}$ |  |  | Stretch: 0.9205 <br> Bend: 4.0620 <br> Stretch-Bend: 0.1722 <br> Torsion: - 13.5249 <br> Non-1,4 VDW: -3.0473 <br> 1,4 VDW: 16.0513 <br> Dipole/Dipole: 1.3947 <br> Total Energy: $6.0284 \mathbf{~ k c a l ~ m o l}^{-1}$ |

Table S12.Total minimized energy and stabilization energy

| Object | TNph-PTA $\left(\mathbf{k c a l} \mathbf{~ m o l}^{-1}\right)$ |  | PDMBr $\left(\mathbf{k c a l} \mathbf{~ m o l}^{-\mathbf{1}}\right)$ |  | TA-PTA $\left(\mathbf{k c a l ~ m o l}^{\mathbf{- 1}}\right)$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | MTE | SE | MTE | SE | MTE | SE |
| RUS | -50.9327 | - | -214.4247 | - | 8.1335 | - |
| RUS +Ru | -55.7900 | -4.5873 | -216.0761 | -1.6514 | 6.0284 | -2.1051 |

## REFERENCE

S1 W. Luo, M. Sankar, A. M. Beale, Q. He, C. J. Kiely, P. C. A. Bruijnincxand M. Weckhuysen, Nat. Coттип., 2015, 6, 6540-6549.

S2 J. Ftouni, A. Munoz-Murillo, A. Goryachev, J. P. Hofmann, E. J. M. Hensen, L. Lu, C. J. P. Kiely, C. A. Bruijnincx and B. M. Weckhuysen, ACS Catal., 2016, 6, 5462-5472.

S3 S. Cao, J. R. Monnier and J. R. Regalbuto, J. Catal., 2017, 347, 72-78.
S4 Y. Yang, C. J. Sun, D. E. Brown, L. Q. Zhang, F. Yang, H. R. Zhao, Y. Wang, X. H. Ma, X. Zhang, and Y. Ren, Green Chem., 2016, 18, 3558-3566.

S5 W. Cao,W. Luo, H. Ge, Y. Su, A. Wang and T. Zhang, Green Chem., 2017, 19, 2201-2211.
S6 M. Sudhakar, K. M. Lakshmi, J. V. Swarna, R. Kishore, K. V. Ramanujachary and A. Venugopal, Catal. Commun., 2014, 50, 101-104.

S7 Y. Guo, Y. Li, J. Chen, and L. Chen, Catal. Lett., 2016, 146, 2041-2052.
S8 Y. Kuwahara, Y. Magatani and H. Yamashita, Catal. Today, 2015, 258, 262-269.
S9 J. V. Swarna, M. Sudhakar, K. S. Naveen and A. Venugopal, RSC Adv., 2015, 5, 9044-9049.

