

Electronic Supplementary Information

Engineering effective structural defects of metal-organic frameworks to enhance their catalytic performances

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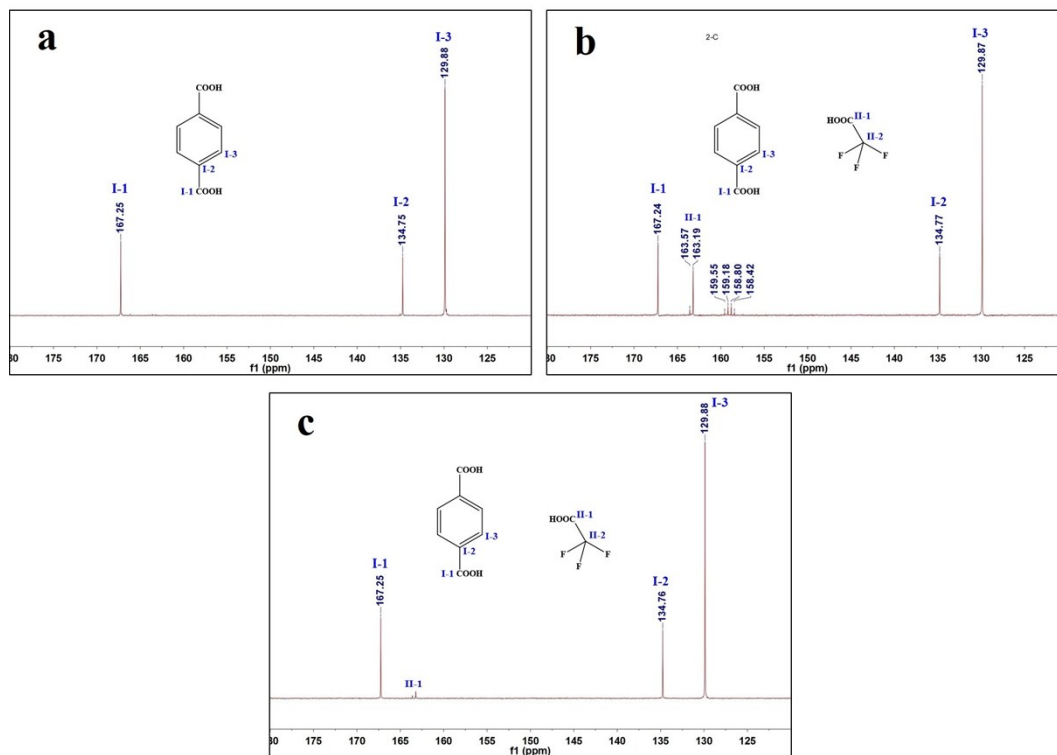
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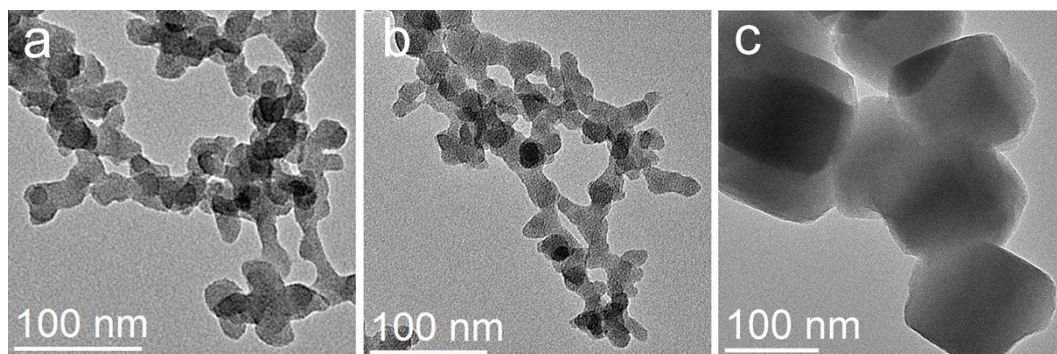


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Fig. S1 ^{13}C NMR spectra of acid-digested (a) UiO-66-DF, (b) UiO-66(1d), and (c) UiO-66(1d)-H2 samples. Note: 100 mg of UiO-66 sample was digested by a mixture of 47 wt.% HF (80 μL) and 1 mL of d_6 -DMSO. After centrifugation, the upper clear solution was transferred into a NMR tube and analyzed on a Bruker 600 MHz spectrometer (Ultrashield 600 PLUS).

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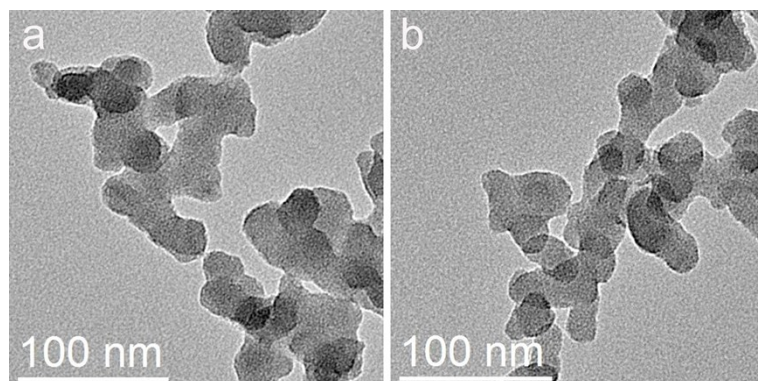


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3 **Fig. S2** Low-magnitude transmission electron microscopy (TEM) images of (a) UiO-66(1d), (b) UiO-
4 66(3d), and (c) UiO-66-DF.

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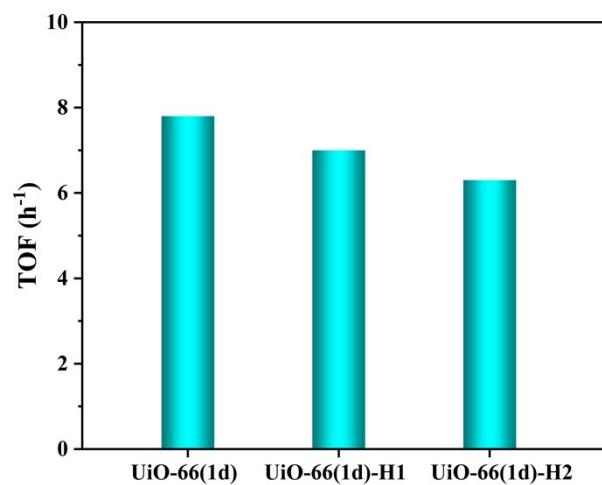


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3 **Fig. S3** Low-magnitude TEM images of (a) UiO-66(1d)-H1 and (b) UiO-66(1d)-H2.

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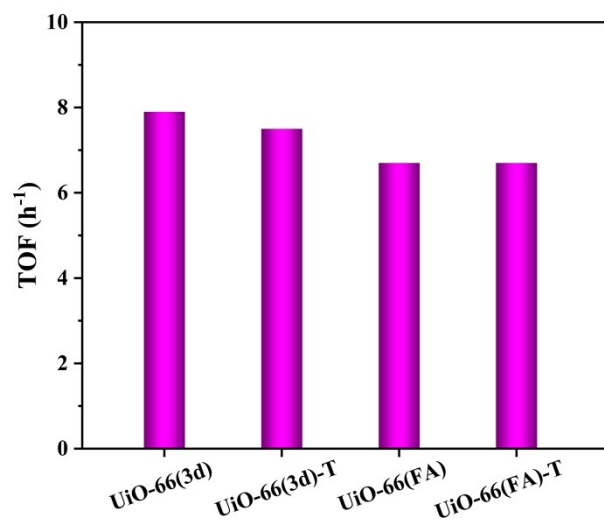
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3 **Fig. S4** Turnover frequency (TOF) for UiO-66(1d), UiO-66(1d)-H1, and UiO-66(1d)-H2, where TOF was
4 calculated based on the number of converted cyclohexanone per open metal site per reaction time and the
5 number of open metal site was considered equal to the amount of TFA modulator in defective UiO-66.

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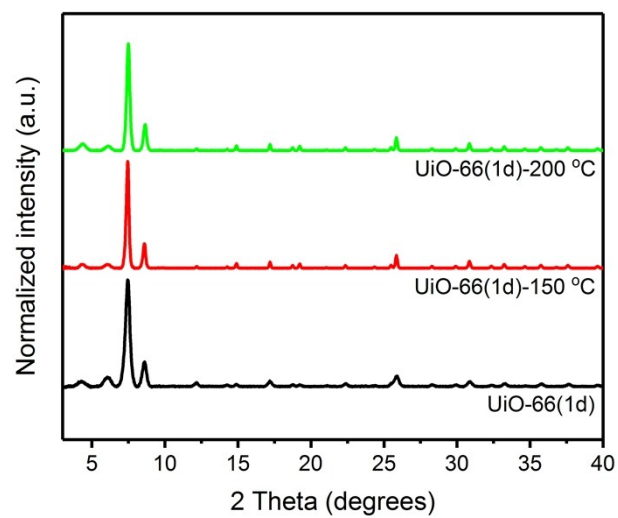
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3 **Fig. S5** Turnover frequency (TOF) for UiO-66(3d), UiO-66(3d)-T, UiO-66(FA), and UiO-66(FA)-T, where
4 TOF was calculated based on the number of converted cyclohexanone per open metal site per reaction time
5 and the number of open metal site was considered equal to the total amount of modulator (TFA and FA) in
6 defective UiO-66.

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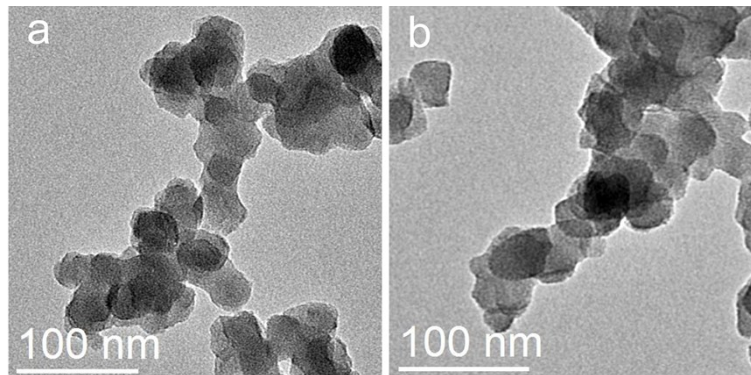


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3 **Fig. S6** PXRD patterns of UiO-66(1d), UiO-66(1d)-150°C, and UiO-66(1d)-200°C.

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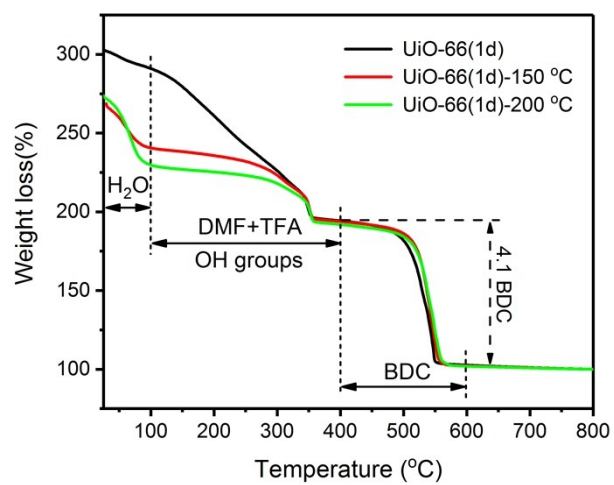
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3 **Fig. S7** Low-magnitude TEM images of (a) UiO-66(1d)-150°C and (b) UiO-66(1d)-200°C.

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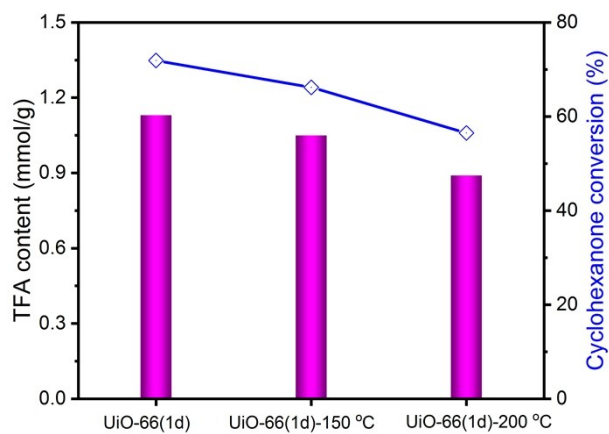


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3 **Fig. S8** TGA curves of UiO-66(1d), UiO-66(1d)-150°C, and UiO-66(1d)-200°C.

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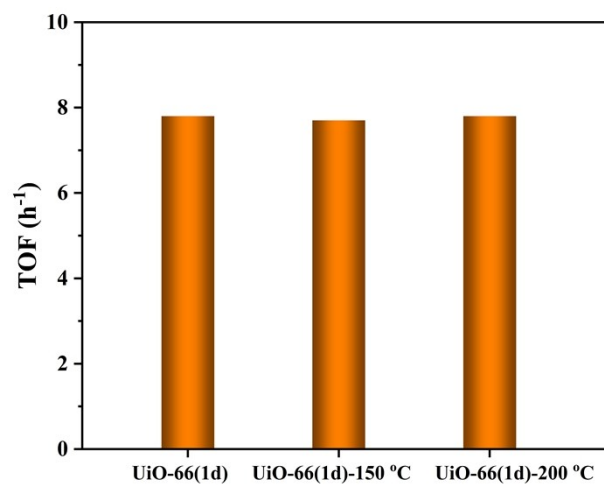
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3 **Fig. S9** Catalytic performances of UiO-66(1d), UiO-66(1d)-150°C, and UiO-66(1d)-200°C in
4 cyclohexanone conversion along with their TFA contents after digestion. Reaction conditions: 180 mg of
5 cyclohexanone, 315 mg of dodecane as internal standard, 550 mg of isopropanol, 15 mg of solid catalyst,
6 10 mL of toluene, 105 °C for 10 h.

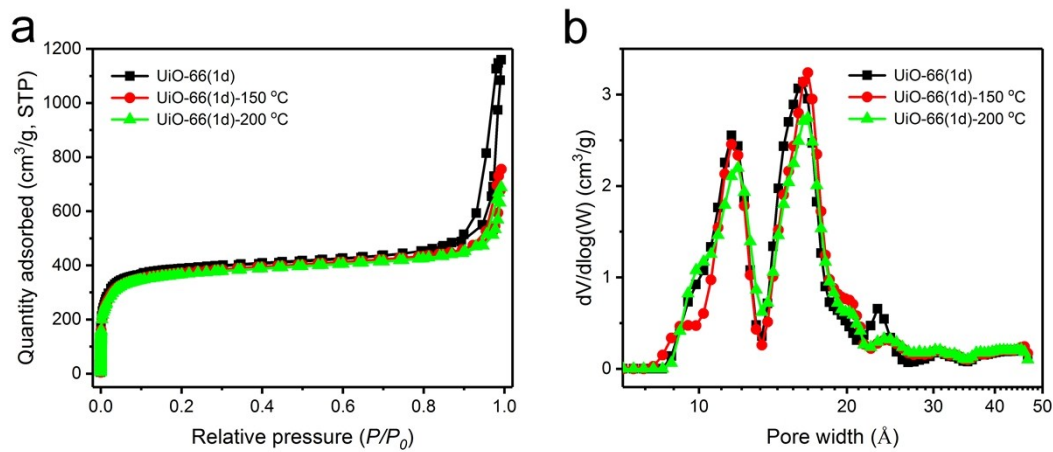
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3 **Fig. S10** Turnover frequency (TOF) for parent and heated UiO-66 catalysts, where TOF was calculated based
4 on the number of converted cyclohexanone per open metal site per reaction time and the number of open
5 metal site was considered equal to the amount of TFA modulator in defective UiO-66.

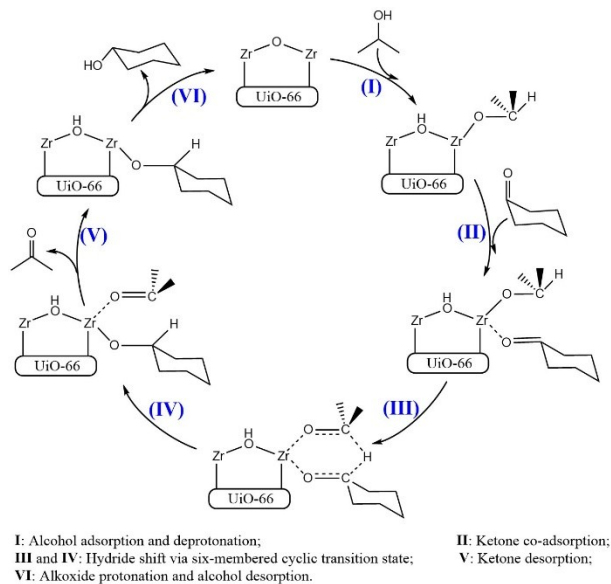
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3 **Fig. S11** (a) Nitrogen adsorption/desorption isotherms and (b) pore size distribution of UiO-66(1d), UiO-
 4 66(1d)-150°C, and UiO-66(1d)-200°C.

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3 **Scheme S1** Proposed reaction pathway of cyclohexanone conversion over effective open metal sites in
 4 defective UiO-66 catalyst. Note: The deprotonized BDC linker and TFA modulator coordinated to Zr metal
 5 site was omitted and activation of IPA and cyclohexanone was assumed to proceed on the same open metal site.

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2 **Table S1** BET surface areas and pore volumes of various UiO-66 samples derived from the isotherms.

Entry	Samples	BET surface area (m ² /g) ^a	Total pore volume (cm ³ /g) ^b
1	UiO-66(1d)	1518	0.71
2	UiO-66(3d)	1694	0.74
3	UiO-66-DF	1025	0.39
4	UiO-66(1d)-H1	981	0.62
5	UiO-66(1d)-H2	953	0.47
6	UiO-66(1d)-150°C	1451	0.67
7	UiO-66(1d)-200°C	1422	0.66

^a Surface area calculated in the P/P_0 range of 0.005 to 0.05. ^b Total pore volume collected at $P/P_0 = 0.8$.

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2 **Table S2** Controlling nucleation of UiO-66 in various synthetic conditions.

Entry	Solvent	Temperature (oC)	Crystallinity	UiO-66
1	DMF	80	Yes	Yes
2	DMF/H ₂ O (5:5, V/V)	80	Yes	Yes with impurity
3	DMF/H ₂ O (5:5, V/V)	60	Yes	Yes with impurity
4	DMF/H ₂ O (2:8)	80	Yes	Yes with impurity
5	DMF/H ₂ O (0.5/9.5)	80	No	-

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2 **Table S3** Conversion of cyclohexanone in the presence of other catalysts.^a

Entry	Catalyst	TFA content (mmol/g) ^b	Conversion (%)
1	TFA	-	4.8
2	BDC	-	2.6
3	UiO-66-DF	-	4.0
4	UiO-66(1d)	1.13	71.9
5	UiO-66(1d)-H2	0.35	17.9
6	UiO-66-DF+TFA ^c	-	5.1
7	UiO-66-DF+TFA ^d	-	9.8
8	UiO-66(1d)-H2+TFA ^d	-	18.3
9	UiO-66-DF-T ^e	0.11	13.9
10	UiO-66(1d)-H2-T ^e	0.42	30.6

^a Reaction conditions: 180 mg of cyclohexanone, 315 mg of dodecane as internal standard, 550 mg of isopropanol, 15 mg of solid catalyst, 10 mL of toluene, 105 °C for 10 h. ^b Measured by HPLC after digestion of solid catalyst. ^c 1.93 mg of TFA, which was equal to that in UiO-66(1d), was added as co-catalyst. ^d 19.3 mg of TFA was added as co-catalyst. ^e Solid catalyst was treated with TFA thrice via PSE method.

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