Supplementary Information

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Fig. S1 ¹H NMR of samples (a) CuBTC and (b) $Cu_2O@HP-CuBTC (1.5)$.



Fig. S2 SEM images of Cu₂O@HP-CuBTC (x) (x=1, 2)



Fig. S3 ¹H NMR of samples $Cu_2O@HP-CuBTC$ (2) solution without washing.



Fig. S4. Composition analysis of $Cu_2O@HP-CuBTC$ (x) creation by hydrothermal reaction: L formation equation.



Fig. S5 Removal efficiencies of DBT and BT by CuBTC and Cu₂O@HP-CuBTC (x) (x = 1.0, 1.5, 2.0). The initial concentration of (a) DBT and (b) BT are 250 mg-S·L⁻¹ for 5h at 298 K.



Fig. S6. Comparison of adsorption kinetics and adsorption capacity of $Cu_2O@HP-CuBTC$ (1.5) and CuBTC: (a) Effect of contact time on the adsorption capacity with 1000 mg-S·L⁻¹ DBT. (b) Effect of the equilibrium concentration of DBT on the adsorption capacity after 5 h. (c) Effect of contact time on the adsorption capacity with 1000 mg-S·L⁻¹ BT.(d) Effect of the equilibrium concentration of BT on the adsorption capacity for 5 h at 298 K.



Fig. S7 Cycle-use performance of the Cu₂O@HP-CuBTC (1.5) in (a) DBT and (b) BT adsorption with 1000 mg-S·L⁻¹ DBT/BT at 298 K.



Fig. S8. (a) XRD of Cu₂O@HP-CuBTC (1.5) and Cu₂O@HP-CuBTC (1.5) after reaction (b) SEM image of Cu₂O@HP-CuBTC (1.5) after reaction

The linear form of the Langmuir and Freundlich adsorption isotherm equations are generally expressed as follows:

$$\frac{C_e}{q_e} = \frac{C_e}{q_{max}} + \frac{1}{K_L q_{max}}$$
$$lnq_e = lnK_F + \frac{1}{n}lnC_e$$

Where C_e is the equilibrium concentration of DBT and BT in the solution; q_e is the amount of DBT/BT adsorbed at equilibrium (mg-S·g⁻¹), q_{max} and K_L are the theoretical maximum adsorption capacity (mg-S·g⁻¹) and Langmuir adsorption equilibrium constant (L·mg⁻¹), respectively, and l/n and K_F are the heterogeneity factor and Freundlich constant [(mg·g⁻¹) (L·mg⁻¹)^{1/n}], respectively.



Fig. S9. Adsorption data simulation with (a) Langmuir and (b) Freundlich isotherm adsorption models on $Cu_2O@HP-CuBTC$ (1.5) and CuBTC with 250-1500 mg-S·L⁻¹ DBT for 5 h at 298 K.



Fig. S10. Adsorption data simulation with (a) Langmuir and (b) Freundlich isotherm adsorption models on $Cu_2O@HP-CuBTC$ (1.5) and CuBTC with 250-1500 mg-S·L⁻¹ BT for 5 h at 298 K.

Pseudo-first-order kinetic and Pseudo-second-order kinetic are expressed respectively as follows:

$$\ln (q_e - q_t) = \ln q_e - k_1 t$$
$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e}$$

Where q_t (mg-S·g⁻¹) is the adsorbed amount of adsorbate at time of t (min) and q_e is the amount of DBT/BT adsorbed at equilibrium (mg-S·g⁻¹). k_1 and k_2 are the pseudo-first-order and pseudo-second-order rate constant (mg·min·g⁻¹), respectively.



Fig. S11 Adsorption kinetic fitting with (a) pseudo-first-order model and (b) pseudosecond-order model on $Cu_2O@HP-CuBTC$ (1.5) and CuBTC with 1000 mg-S·L⁻¹DBT at 298 K.



Fig. S12 Adsorption kinetic fitting with (a) pseudo-first-order model and (b) pseudosecond-order model on $Cu_2O@HP-CuBTC$ (1.5) and CuBTC with 1000 mg-S·L⁻¹ BT at 298 K.

Sample	$\mathbf{S}_{\mathrm{BET}}$	Average Pore diameter	V /V
	$(m^2 \cdot g^{-1})$	(nm)	v micro/ v meso
CuBTC	1198.99	1.89	-
Cu ₂ O@HP-CuBTC (1)	1187.94	2.85	4.44
Cu ₂ O@HP-CuBTC (1.5)	1262.15	2.91	4.29
Cu ₂ O@HP-CuBTC (2)	1106.29	2.93	4.18

Table S1. Porosity properties of the prepared CuBTC materials

The specific surface area was calculated by employing the Brunauer–Emmett–Teller (BET) method in the range of relative pressure from 0.05 to 0.25. The average pore diameter was determined by the density functional theory method in the adsorption branch of the N₂ isotherm at 77 K. Total pore volume was determined using the adsorption branch of the isotherm at P/P₀ = 0.99. The mesopore volume (V_{meso}) was calculated from Barrett–Joyner–Halenda (BJH) desorption cumulative volume of pores between 1.70 and 300.00 nm diameter. The micropore volume (V_{micro}) was obtained by t-plot micropore analysis.

Table S2. Position (eV) and area of C1s region on CuBTC.

Peak	Position (eV)	Area
C-0	286.257	3202.401
C-C	284.803	20148.730
0-C=0	288.2	4951.440

Table S3. Position (eV) and area of C1s region on Cu₂O@HP-CuBTC (1.5).

Peak	Position (eV)	Area
C-0	286.215	3198.332
C-C	284.825	20702.900
0-C=0	288.174	4010.424

Adsorption model	Parameter	Sample	
		Cu ₂ O@HP-CuBTC	CuBTC
		(1.5)	
Langmuir	$K_L (L mg^{-1})$	0.014	0.008
	$q_{max} (mg-S g^{-1})$	65.20	49.58
	R ²	0.9956	0.9987
Freundlich	$K_{\rm F}$	13.01	4.572
	n	4.338	2.936
	R ²	0.9987	0.8348

Table S4. Isotherm parameters for adsorption of DBT onto Cu₂O@HP-CuBTC (1.5) and CuBTC at 298 K for 5 h

Table S5. Isotherm parameters for adsorption of BT onto Cu₂O@HP-CuBTC (1.5) and CuBTC at 298 K for 5 h

Adsorption isotherm	Parameter	Sample	
		Cu ₂ O@HP-CuBTC	CuBTC
		(1.5)	
Langmuir	$K_L (L mg^{-1})$	0.011	0.007
	$q_{max} (mg-S g^{-1})$	67.71	50.56
	R ²	0.9930	0.9983
Freundlich	K _F	11.07	4.119
	n	3.906	2.823
	R ²	0.9897	0.9483

Table S6 Kinetic parameters for adsorption onto $Cu_2O@HP-CuBTC$ (1.5) and CuBTC with 1000 mg-S·L⁻¹ DBT

Kinetic model	Parameter	Sample	
		Cu ₂ O@HP-CuBTC	CuBTC
		(1.5)	
Pseudo-first-order	k_1 (mg min g ⁻¹)	0.012	0.012
	$q_e (mg g^{-1})$	4.235	24.48
	R ²	0.3303	0.8794
Pseudo-second-order	$k_2 (mg \ min \ g^{-1})$	0.000034	0.000342
	$q_e (mg g^{-1})$	56.85	48.66
	\mathbb{R}^2	0.9934	0.9972

Table S7 Kinetic parameters for adsorption onto $Cu_2O@HP-CuBTC$ (1.5) and CuBTC

Kinetic model	Parameter	Sample	
		Cu ₂ O@HP-CuBTC	CuBTC
		(1.5)	
Pseudo-first-order	k_1 (mg min g ⁻¹)	0.005	0.013
	$q_e (mg g^{-1})$	8.117	13.49
	R ²	0.6424	0.7580
Pseudo-second-order	$k_2 (mg min g^{-1})$	0.000036	0.000228
	$q_e (mg g^{-1})$	54.80	46.82
	\mathbb{R}^2	0.9916	0.9986

with 1000 mg-S \cdot L⁻¹ BT