

Electronic Supplementary Information

Ordered mesoporous carbon catalyst for dehydrogenation of propane to propylene

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1. Experimental section

1.1. Synthesis

The preparation of the ordered mesoporous carbon (OMC) materials was from the reference by a low-temperature autoclaving method based on organic-organic self-assembly [S1]. In a typical synthesis, 3.3 g of resorcinol and 2.5 g of F127 was dissolved in a mixture of 20 ml water and 20 ml ethanol. 0.2 g of 37% hydrochloric acid was then added to the above solution. After one hour of stirring, 2.5 g of 37% formaldehyde solution was added dropwise under tempestuously stirring. The reaction mixture was further vigorously stirred for another one hour and then transferred to a Teflon-lined autoclave and heated at 50 °C for 4 days. The obtained product was collected by filtration, washed with water and dried, and then carbonized at 600 °C for 6 h. The final product was denoted as OMC-1. While the molar ratio of formaldehyde to resorcinol is fixed at 2:1, autoclaving for 3 days, the synthesized carbon was denoted as OMC-2.

The CMK-3 ordered mesoporous carbon was synthesized using mesoporous silica of SBA-15 ($S_{\text{BET}} = 648 \text{ m}^2 \text{g}^{-1}$, $D_{\text{BJH}} = 9.4 \text{ nm}$) as a hard template [S2]. Typically, mesoporous silica was impregnated with sucrose solution in the presence of sulfuric acid and dried at

80 °C and subsequently at 160 °C. Then the impregnation/drying step was repeated once. The obtained sample was carbonized under nitrogen atmosphere at 900 °C for 4 h. The resultant mesoporous carbons were obtained by stirring carbon/silica composition in HF acid (20 wt%) for 24 h to remove the silica frameworks, filtering, washing and drying at 100 °C overnight.

CNTs were prepared as the reference mentioned [S3]. The procedure was conducted in a horizontal quartz tube in a furnace. A ceramic boat containing Catalyst powder (Co/SiO₂) was placed in the center of the quartz tube. When the furnace temperature was increased gradually to 700 °C, a mixed gas of N₂ and C₂H₂ was allowed to flow into the reaction tube. After the multiwall nanotubes (MWNT) growth for *ca.* 20 min, the specimen was cooled down to room temperature under ambient N₂. The obtained powder of Co/SiO₂/CNTs composite was treated with a HF aqueous solution and nitric acid at room temperature in order to extract the nanotubes by dissolution of SiO₂ and cobalt particles. The residues were then separated by filtration, washed with distilled water and dried at 100 °C.

1.2. Characterization

Transmission electron microscopy (TEM) measurements were performed on a Philips Tecnai F20 microscope at 200 kV. All samples subjected to TEM measurements were ultrasonically dispersed in ethanol and drop-cast onto copper grids covered with carbon film. Powder X-ray diffraction (XRD) pattern was recorded using a Rigaku D/max-2500 diffractometer, with Cu K α radiation ($\lambda = 1.5406 \text{ \AA}$) at a scanning rate of 0.01 °/s. Small angle X-ray scattering (SAXS) experiments were performed on a Bruker Nanostar small angle X-ray scattering system. Nitrogen adsorption and desorption isotherms were measured on a Quantachrome NOVA 2000e sorption analyzer at 77 K. Before measurements, the samples were degassed in a vacuum at 200 °C for at least 6 h. The

Brunauer-Emmett-Teller (BET) method was utilized to calculate the specific surface areas (S_{BET}), the pore size distributions were derived from the adsorption branches of isotherms using Non-Local Density functional they (NLDFT) method, and the total pore volumes (V_{total}) were estimated from the adsorbed amount at a relative pressure P/P_0 of 0.980. X-ray photoelectron spectroscopy (XPS) measurements were performed on a Kratos Axis Ultra DLD (delay line detector) spectrometer equipped with a monochromatic Al K-X-ray source (1486.6 eV). All XPS spectra were recorded using an aperture slot of $300\mu\text{m} \times 700\mu\text{m}$, survey spectra were recorded with a pass energy of 160 eV, and high-resolution spectra with a pass energy of 40 eV. The temperature program desorption (TPD) profiles were obtained from CHEMBET-3000 with a custom built set-up, consisting of a U-shaped tubular micro-reactor, placed inside an electrical furnace. The mass flow rate of the helium carrier gas (20 mL/min) and the heating rate of the furnace (5 K/min) were controlled with appropriate units.

1.3. Catalytic testing

Catalytic tests were performed in a stainless steel, fixed-bed flow microreactor at atmospheric pressure, and the catalyst load was 400 mg. The gas reactant contained 5 vol% propane and a balance of nitrogen (total flow rate = 40 cm³/min). The hydrocarbon reaction products were analyzed with an on-line gas chromatograph with a 6-m column of Porapak Q and a flame ionization detector (FID). Propane (C₃H₈) conversion and selectivity to products have been calculated as follows:

$$\text{C}_3\text{H}_8 \text{ Conversion (mol \%)} = \frac{\text{moles of C}_3 \text{ reacted}}{\text{moles of C}_3 \text{ fed}} \times 100$$

$$\text{Selectivity (mol \%)} = \frac{\text{moles of product i formed}}{\text{moles of C}_3 \text{ reacted}} \times \left(\frac{N_i}{N_{C_3}} \right) \times 100$$



Scheme 1. Dehydrogenation of propane over mesoporous carbons.

Table S1. Kinetic parameters for dehydrogenation of propane over mesoporous carbons^a

Sampl e	Dehydrogenation rate at 873 K ^b		Hydrogen yield	
	(mmol/g/h)	(mmol/m ² /h) ^c	(mmol/g/h)	(mmol/m ² /h) ^c
OMC-1	118	0.19	107	0.17
OMC-2	127	0.21	112	0.20
CMK-3	87	0.07	79	0.06
CNTs ^d	21.2	0.10	17.7	0.08
GC ^d	16.4	4.1	13.7	3.4

^a Reaction conditions: 0.40 g, 873 K, 2% propane in nitrogen, 40 mLmin⁻¹. ^b The dehydrogenation reaction rate was depict as propylene formation. ^c Normalized by specific surface area of used sample in steady state. ^d The data showed is the initial reaction rate.

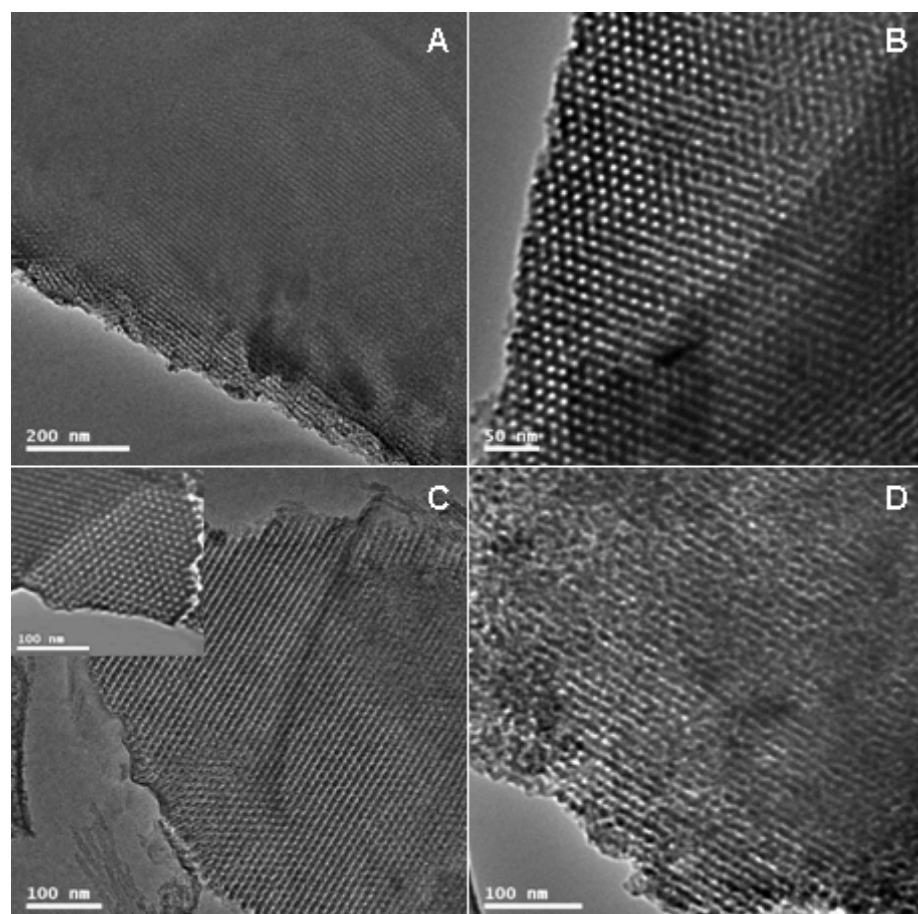


Fig. S1. Transmission electron microscopy (TEM) of the fresh carbon catalysts: (A, B) ordered mesoporous carbon OMC-1; (C) CMK-3; (D) mesoporous carbon OMC-2.

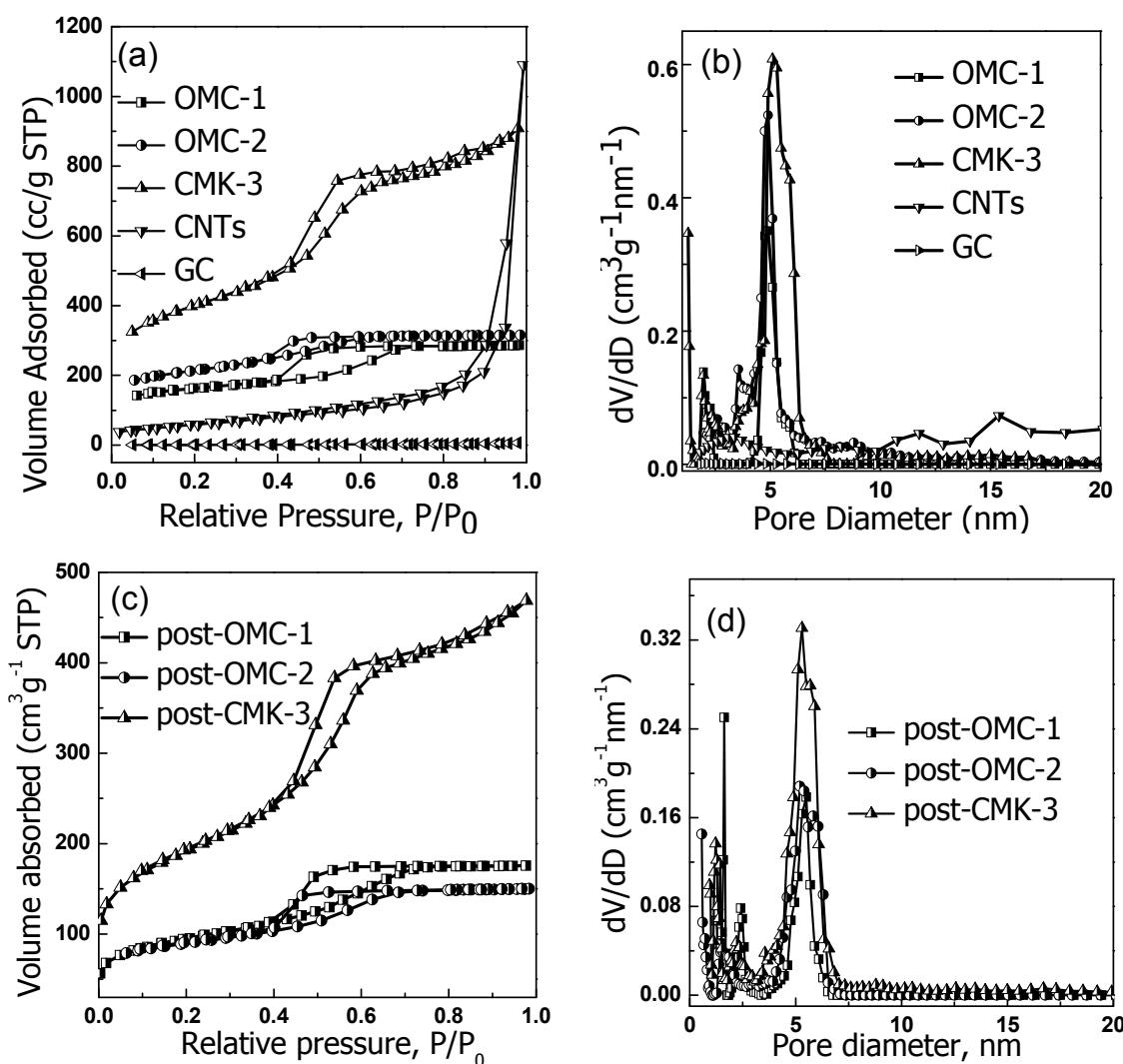


Fig. S2. Nitrogen sorption isotherms and the corresponding pore size distribution curves of different carbon catalysts before (a,b) and after (c,d) reaction.

Typical type-IV isotherms with a clear condensation step at $P/P_0 = 0.5 - 0.7$ can be observed for samples OMC-1, OMC-2 and CMK-3, which is associated with the filling of mesopores due to capillary, with a narrow pore size distribution centered around 5 nm. Meanwhile, the large volume adsorbed at the lower $P/P_0 = 0 - 0.1$ suggests the presence of microporosity of CMK-3 (Table 1). The capillary condensation of N_2 molecules at high relative pressure $P/P_0 = 0.9 - 1.0$ indicates the existence of pore system with small size and/or structural defects in the carbon walls of CNTs [S4], in accord with the broad pore size distribution ranging from 3 – 20 nm. Graphite carbon has a surface area as low as $4 \text{ m}^2\text{g}^{-1}$, indicating the absence of pores.

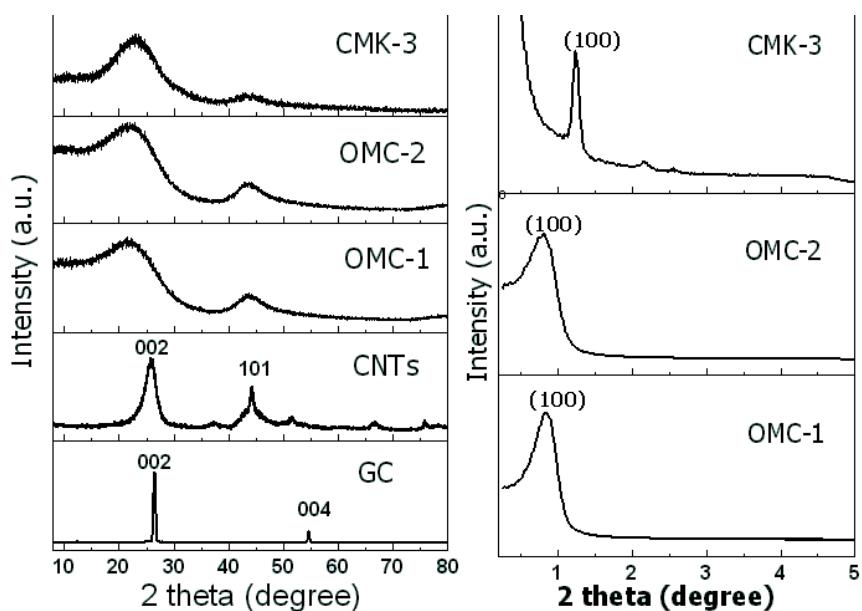


Fig. S3. Wide-angle XRD patterns (*left*) and the SAXS patterns (*right*) of different carbon catalysts.

From the wide angle XRD patterns, it can be clearly seen that GC exhibits two very sharp diffraction peaks at 26.5° (2θ) and 54.5° (2θ), which can be indexed to (002) and (004) reflection of the graphite lattice respectively (PDF 08-0415). CNTs represent a carbon with a high degree of graphitization, containing two intense diffraction peaks at 2θ value of 26° (2θ) and 44.2° (2θ), which can be assigned to (002) and (101) diffractions of the graphitic framework. In contrast, all the mesoporous carbon catalysts show two broad peaks at ca. 24° (2θ) and ca. 44° (2θ). These peaks are assigned to diffractions from the (002), (100) planes of graphite [S5], indicating the partially graphitic pore walls. In the low-angle reflections, a sharp and narrow diffraction peak is visible in all three mesoporous carbon samples, corresponding to the two-dimensional hexagonal periodicity of the pore systems, which is consistent with the TEM images.

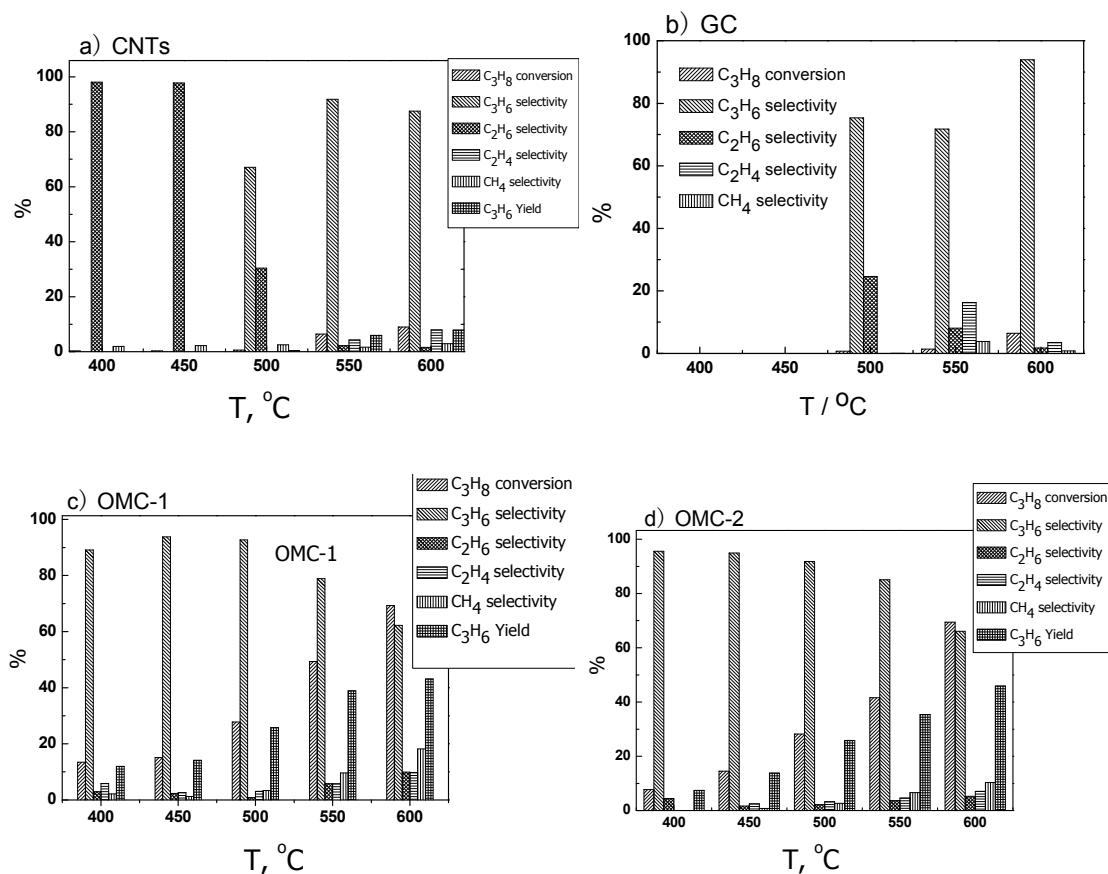


Fig. S4. Dependence of catalytic activity on the reaction temperature during the dehydrogenation of propane over nanostructured carbons, (a) CNTs, (b) GC, (c) OMC-1, (d) OMC-2. Although the higher selectivity to propylene occurred at higher temperature range, both carbon nanotubes and graphite carbon show poor catalytic activity. In contrast, the OMC-x can preferably catalyze the dehydrogenation reaction.

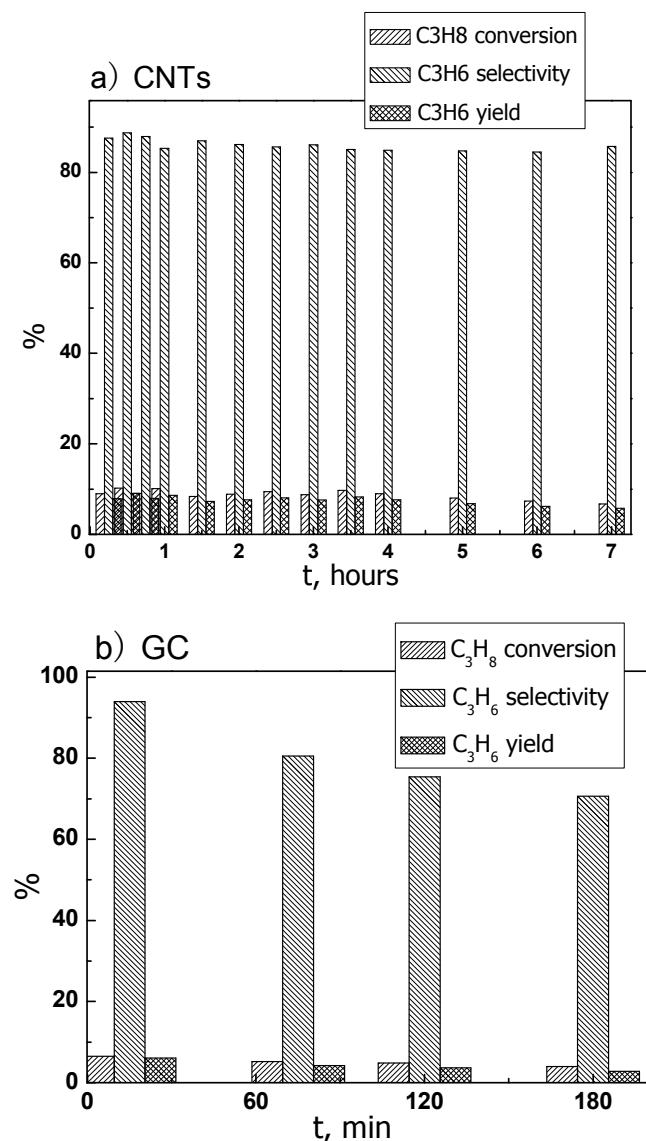


Fig. S5. Propane conversion, propylene selectivity and yield as a function of time on stream obtained at 873 K on a) CNTs and b) GC. Both carbon nanotubes and graphite carbon show poor stability.

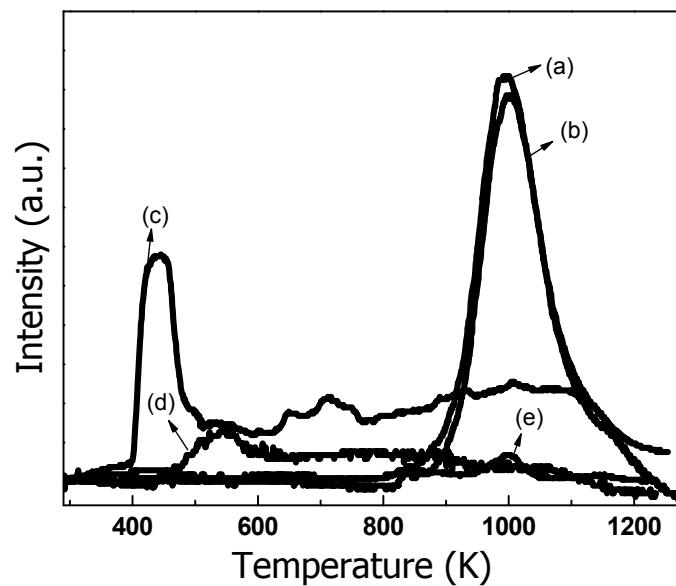


Fig. S6. TPD profiles of different mesoporous carbons before reaction: (a) OMC-1, (b) OMC-2, (c) CMK-3, (d) CNTs, (e) GC.

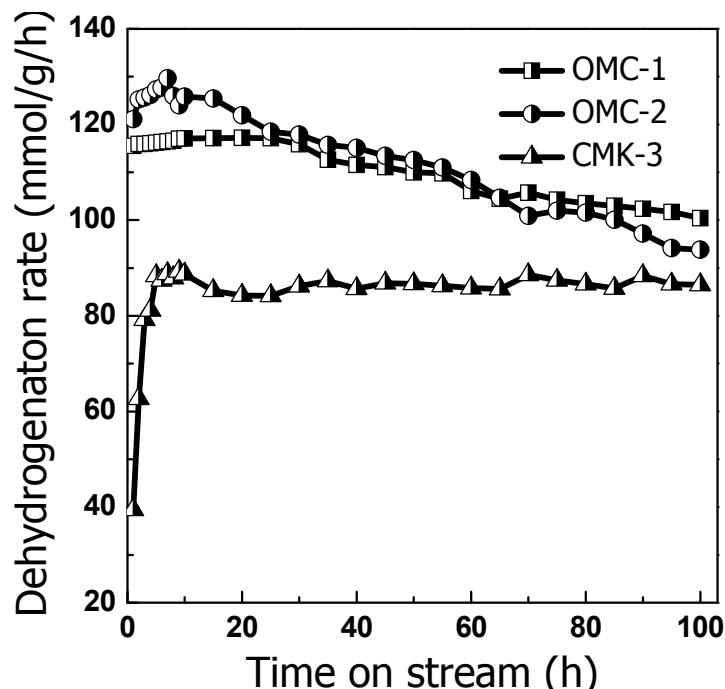


Fig. S7. Reaction rates for the dehydrogenation of propane over different mesoporous carbons. Reaction conditions: 0.40 g, 873 K, 2% propane in nitrogen, 40 mL/min.

References

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