## **Supplementary Information**

"Encapsulated Ionic Liquids (ENILs): From continue to discrete liquid phase" by Jose Palomar,\* Jesus Lemus, Noelia Alonso, Jorge Bedia, Miguel A. Gilarranz and Juan J. Rodriguez.

## **Experimental details**

Subsmicrocapsule  $C_{Cap}$  synthesis: The carbon submicrocapsules were synthesized by template method<sup>[1]</sup>. A solid core and mesoporous shell aluminosilicate (SCMS) were used as template. The solid core were achieved following the Störb synthesis<sup>[2]</sup>, a volume of 15 mL of tetraethoxysilane (TEOS) was added to a reaction medium formed by 12.6 mL of ammonia aqueous solution (20%, v), 185 mL of ethanol and 20.3 mL of deionized water. The mixture was maintained at 303 K with vigorous stirring during 1 hour to achieve a colloidal solution of silica spheres. A mixture containing 12.5 mL of TEOS and 5 mL of octadecyltrimethoxysilane (C18TMS), was added to the colloidal solution to form the mesoporous shell around them<sup>[3]</sup>. After 1 hour of reaction, the spheres formed were isolated by filtration and calcined at 823 K for 6 h under an air atmosphere. The silica spheres were impregnated by a solution consisting on 0.27 g of Al<sub>3</sub>6H<sub>2</sub>O in 0.3 mL of deionized water. This step was repeated one more time. The powder resulting was dried in air at 353 K and calcined at 823 K for 5 h in air to form SCMS aluminosilicate. A phenol-formaldehyde resin has been used as carbon precursor to obtain carbon submicrocapsules. A mixture of 0.374 g of phenol per gram of template was heated at 373 K for 14 h under 150 mm of Hg static vacuum (rotavapor equipment). Then, 0.238 g of paraformaldehyde per g of SCMS was added and maintain during 24 h under static vacuum at 403 K to obtain a phenol-formaldehyde resin into the SCMS template. This material was heated to 433 K at rate of 1 K/min and held at that temperature for 5 h under a nitrogen flow of 100 NmL/min in a vertical furnace (i.d. 26 mm, length 12 cm). Then, the temperature was raised up to 1123 K with a heat rate of 5 K/min and held at that temperature for 7 h. The resulting carbon aluminosilicate was washed with HF (48%, v) to generate the carbon submicrocapsules.

*Incipient wetness:* The submicrocapsules ( $C_{cap}$ ) were filled of IL by means of a direct impregnation, dissolving the IL in acetone. To prevent hydration, IL and acetone were kept in their original tightly closed bottles in a desiccator before use. Impregnation was carried out mixing 1 ml of IL dissolved in acetone for each 100 mg of submicrocapsules. IL concentration in acetone solution was adjusted to obtain different IL loadings on the support. To ensure a homogeneous penetration of the IL solution into the pores, the IL solution was added drop by drop over the surface of the C<sub>cap</sub>. Then, synthesized ENIL materials were stored at 333 K during 24 h prior to their use. After evaporation of acetone, the ENIL contains from 20 to 83% (w/w) of IL phase.

Characterization: The porous structure of supports and ENIL materials was characterized by means of nitrogen adsorption-desorption isotherms at 77 K using a Micromeritics apparatus (Tristar II 3020 model) and mercury porosimetry using Quantachrome apparatus (PM-3310 model). Before adsorption-desorption experiments, samples were outgassed at 423 K under a residual pressure lower than  $10^{-3}$  Pa. The BET equation was applied to determine the BET surface area (A<sub>BET</sub>) and Dubinin-Radushkevich equation for micropore volume (0-2 nm). The external or non-micropore area  $(A_s)$  was obtained from the t-method. The difference between the volume of  $N_2$  (as liquid) at 0.95 relative pressure and the micropore volume was taken as mesopore volume (2-50 nm). In the mercury porosimetry measurements the estimation of pore diameter from the applied pressure was based on the Washburn equation. The surface tension of mercury was taken as 4.8×10<sup>-3</sup> N/cm and the mercury contact angle as 141°. The macropore volume was estimated in the 50-100 nm range. Elemental analyses (EA) of C<sub>cap</sub> and ENILs were carried out in a Perkin-Elmer analyzer (210 CHN model) to obtain C, and N elemental percentages. Thermogravimetric analyses (TGA) of IL and ENIL materials were conducted in a Mettler Toledo Instruments (TGA/SDTA851e model) under nitrogen with a heating rat of 10°C/min. The accuracy of temperature and mass measurements was 0.1 K and  $10^{-3}$ mg, respectively. A dynamic method was used with a temperature range from 323 to 873 K at a heating rate of 10 K min<sup>-1</sup> while purging with 50 ml min<sup>-1</sup> of dry nitrogen. The mass of the sample placed in TGA analyses were between 4 and 12 mg. In all TGA runs, aluminum pans with a capacity of 70 ml were used.

 $NH_3$  capture tests in TGA: Ammonia absorption experiments were carried out in the TGA analyzer at atmospheric pressure and temperatures of 293 and 313 K using 20 mg of IL sample amount. The balance has a weight range of 0–1000 mg with a resolution of 0.1 mg. The temperature of the sample was maintained constant with a regulated external thermostat bath (Huber minisat 125). Gas–liquid-solid equilibrium and kinetic data of ammonia in ENIL materials and neat IL were obtained at 293 K and 0.1 MPa, in a  $NH_3/N_2$  gas flow of 100 N cm<sup>3</sup>/min, 80% (volume) of  $NH_3$  and monitoring the increment on weight of the sample. Desorption experiments were carried out at the absorption temperature and pressure under dry nitrogen flow (100 N cm<sup>3</sup>/min).

 $NH_3$  capture tests in fixed-bed column: The sorption of ammonia was also evaluated in a continuous flow system, which consists of a quartz fixed-bed column (1/4 inch diameter), coupled to a quadrupole mass analyzer (OmniStar/ThermoStar). Experiments were conducted under following operating condition: 293K of temperature, 2000 ppmv of inlet ammonia concentration, 20 N cm<sup>3</sup> /min of gas flow, atmospheric pressure and 8 cm of height of adsorbent/absorbent material (C<sub>cap</sub>, ENIL-R<sub>2</sub> and ENIL-R<sub>4</sub>). Ammonia detection was carried out utilizing a single quadrupole mass analyzer. The signal selected in order to quantify the amount of NH<sub>3</sub> in the gas outlet of the reactor was an ion current of 14.98A. Desorption experiments were performed after 50 minutes of NH<sub>3</sub> sorption on ENIL materials. A N<sub>2</sub> flow of 20 N cm<sup>3</sup> /min was passing through the column with the exhausted ENIL materials at 293 K,

during 30 minutes and then the temperature was raised at 343 K during 20 minutes and 0.1MPa for the completed regeneration. The regenerative cycles were conducted three times.

## REFERENCES

- 1 Yoon, S. B. and Sohn, K. and Kim, J. Y. and Shin, C. and Yu, J., Hyeon, T., Adv Mater, 2002, 14, pp. 19-21.
- 2 Stober, W. and Fink, A., Bohn, E., J. Colloid Interface Sci., 1968, 26, pp. 62.
- 3 Buchel, G. and Unger, K. K.and Matsumoto, A., Tsutsumi, K., Adv Mater, 1998, 10, pp. 1036.

**Figure S1** (a) Nitrogen adsorption-desorption isotherms at 77K and (b) Pore size distribution (6 to 100nm) from Hg porosimetry of carbon submicrocapsules ( $C_{Cap}$ ) and encapsulated ionic liquid (ENIL- $R_n$ ) materials with increasing amounts of OmimPF<sub>6</sub> (0-80% w/w).



Figure S2 Normalized derivative thermogravimetric curves (DTG) obtained under nitrogen atmosphere at a heating rate of 10 °C/min, for EtOHmimBF<sub>4</sub> and ENIL-R<sub>n</sub> materials prepared with different amount of this IL.







**Table S1.** Results of  $NH_3$  capture with the ionic liquid (IL) EtOHmimBF<sub>4</sub> and ENIL-R<sub>n</sub> materials prepared with this IL obtained in thermogravimetric tests at 293 K, 1 atm and 0.08 MPa  $NH_3$  partial pressure, where the ammonia absorption capacity of IL-based system is expressed per unit mass of IL.

	Thermogravimetric tests   Pseudo-second order model $\frac{t}{q_t} = \frac{1}{kq_s^2} + \frac{t}{q_s}$				
	$q_s$	k	$R^2$		
IL	101	3.5.10-3	0.999		
ENIL R <sub>2</sub>	106	7.1.10-3	0.998		
ENIL R <sub>4.2</sub>	104	12.8·10 <sup>-3</sup>	0.999		
$\boldsymbol{q}_s \ (\mathrm{mg} \cdot \mathrm{g}^{-1}); \boldsymbol{k} \ (\mathrm{mg} \cdot \mathrm{g}^{-1} \cdot \mathrm{min}^{-1})$					

**Table S2.** Results of  $NH_3$  adsorption-desorption with ENIL- $R_4$  material obtained in fixed bed reactor tests at 293 K, 2000 ppmv of inlet ammonia concentration, 20 N cm<sup>3</sup>/min of gas flow, atmospheric pressure in bed column of 8 cm of height and 1/4 inch diameter.

Cycle	t <sub>0,5</sub>	$\mathbf{q}_{\mathbf{s}}$	$\mathbf{q}_{\mathbf{s}}$
	(min)	( <b>mg</b> •g <sup>-1</sup> )	(mg·cm <sup>-3</sup> )
1	20.4	1.85	0.22
2	19.8	1.80	0.21
3	20.2	1.83	0.22