

## Co-processing CH<sub>4</sub> and Oxygenates on Mo/HZSM-5: 2. CH<sub>4</sub>/CO<sub>2</sub> and CH<sub>4</sub>/HCOOH Mixtures

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### Supplementary Information

The tabulated results presented in Table S.1 show the observed product distribution and conversion for co-processing CO<sub>2</sub>/CH<sub>4</sub>, CH<sub>3</sub>COOH/CH<sub>4</sub>, and HCOOH/CH<sub>4</sub> mixtures at 950 K. All data reported were recorded at 11 ks time-on-stream.

**Table S.1:** CH<sub>4</sub> conversion and product carbon selectivity for DHA reactions over Mo/H-ZSM-5 catalyst at 950 K, CH<sub>4</sub> flow rate 12.0 cm<sup>3</sup> min<sup>-1</sup>, CH<sub>4</sub>:Ar = 9:1, catalyst loading 1 g with Mo:Al<sub>f</sub> = 0.25, and time-on-stream 11 ks.

Oxygenate	CO <sub>2</sub>	AA	FA
O*/CH <sub>4</sub> (/10 <sup>-5</sup> )	1.8	1.5	1.7
CH <sub>4</sub> conversion (%) <sup>a</sup>	8.6	6.3	8.2
Selectivity (%) <sup>b</sup>			
CO	62.0	54.1	41.2
C <sub>2</sub> H <sub>4</sub>	1.0	1.3	1.5
C <sub>2</sub> H <sub>6</sub>	1.1	1.2	1.6
C <sub>6</sub> H <sub>6</sub>	22.6	29.5	36.7
C <sub>7</sub> H <sub>8</sub>	1.0	1.4	1.7
C <sub>10</sub> H <sub>8</sub>	11.1	11.6	15.6
C <sub>10</sub> <sup>+</sup>	1.2	0.9	1.5

$$^a \text{Conv}_{CH_4} = \frac{F_{CH_4}^{Inlet} - F_{CH_4}^{Outlet}}{F_{CH_4}^{Inlet}} \quad ^b \% S_i = \frac{n_i * F_i}{\sum_i n_i * F_i}$$