

Supporting Information

Facile Electrochemical Co-Deposition of a Graphene/Cobalt Nanocomposite for Highly Efficient Water Oxidation in Alkaline Media: Direct Detection of Underlying Electron Transfer Reactions Under Catalytic Turnover Conditions

Si-Xuan Guo,^a Yuping Liu,^a Alan M. Bond*^a and Jie Zhang*^a
Esakki Karthik,^b Ilango Maheswaran,^b Senthil Kumar^b and Kanala L.N. Phani*^b

^a School of Chemistry, Monash University, Clayton, Vic 3800, Australia
E-mails: alan.bond@monash.edu, jie.zhang@monash.edu

^b Nanoscale Electrocatalysis & Sensor Research Group, Electrodes and Electrocatalysis Division, CSIR-Central Electrochemical Research Institute, Karaikudi, Tamilnadu, India
E-mail: klnphani@cecri.res.in

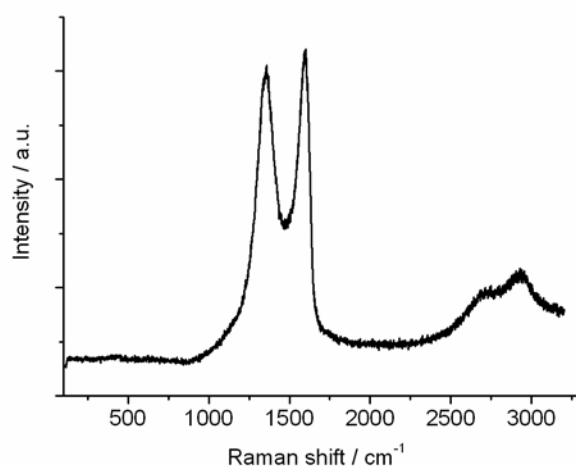


Fig. S1 Raman spectrum derived from thick graphene layers present on a graphene/cobalt nanocomposite modified FTO electrode after deposition at -1.4 V for 1000 s.

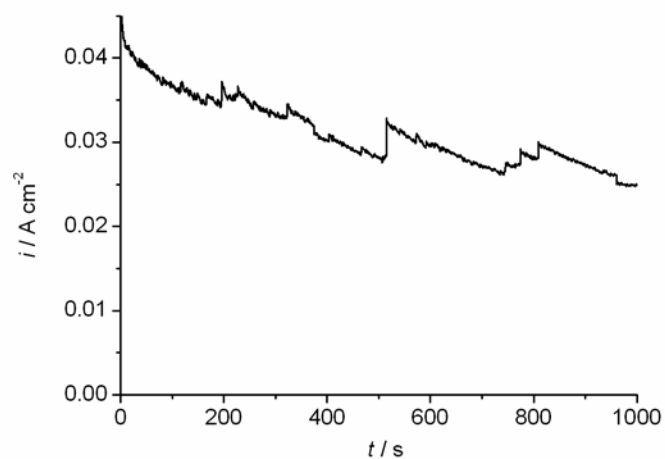


Fig. S2 Plot of catalytic current versus time during controlled potential electrolysis of a cobalt modified electrode in 1 M NaOH. Applied potential: + 0.8 V vs. Ag/AgCl. Cobalt deposition at -1.4 V for 1000 s in an aqueous solution containing 0.8 mM $\text{Co}(\text{NO}_3)_2$ and 0.1 M NaNO_3 .

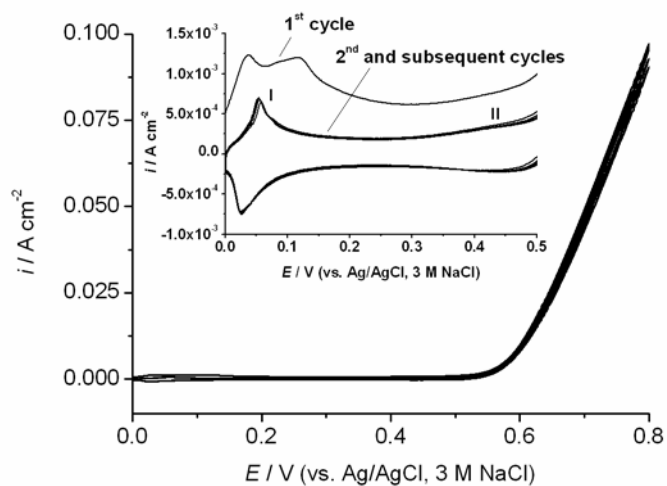
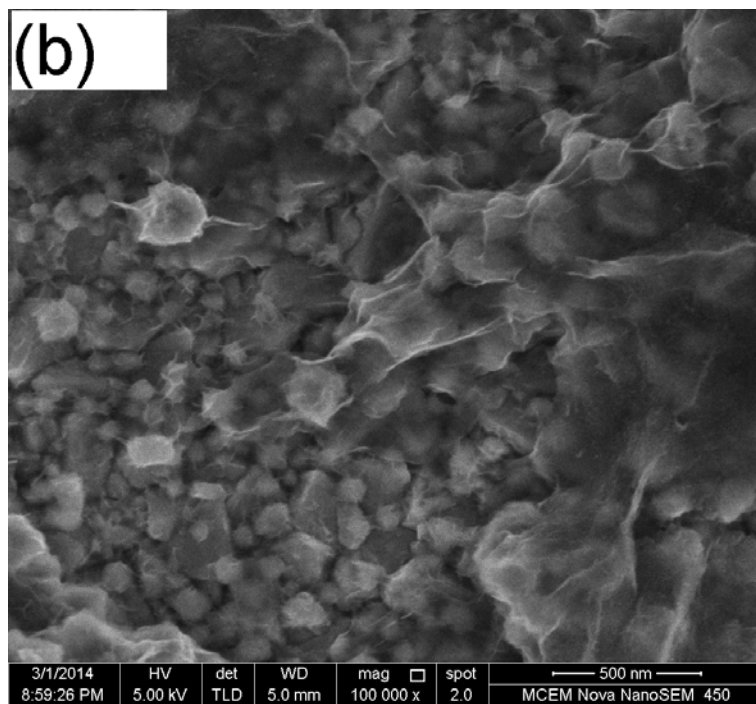
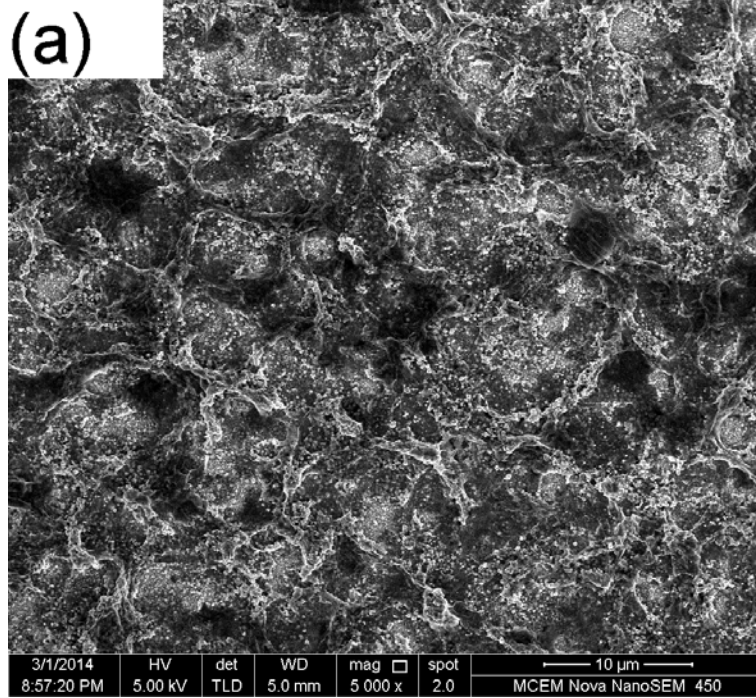


Fig. S3 Electrocatalytic water oxidation in aqueous 1 M NaOH electrolyte at a scan rate of 50 mV s^{-1} using a cobalt modified electrode, under conditions described in the main text. Inset shows the cobalt processes in the potential range of 0 – +0.5 V. Deposition of cobalt at -1.4 V for 1000 s in an aqueous 0.05 M phytic acid solution (pH 7) containing 0.8 mM $\text{Co}(\text{NO}_3)_2$.



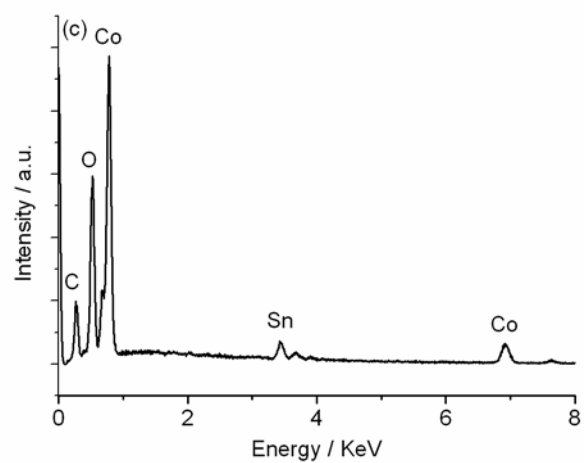


Fig. S4 SEM images (a, b) and EDX spectrum (c) obtained at a cobalt – graphene modified FTO electrode. Cobalt – graphene deposition at -1.4 V for 1000 s in an aqueous 0.05 M phosphate buffer solution (pH 7) containing 1 mg ml^{-1} graphene oxide and 0.8 mM $\text{Co}(\text{NO}_3)_2$.

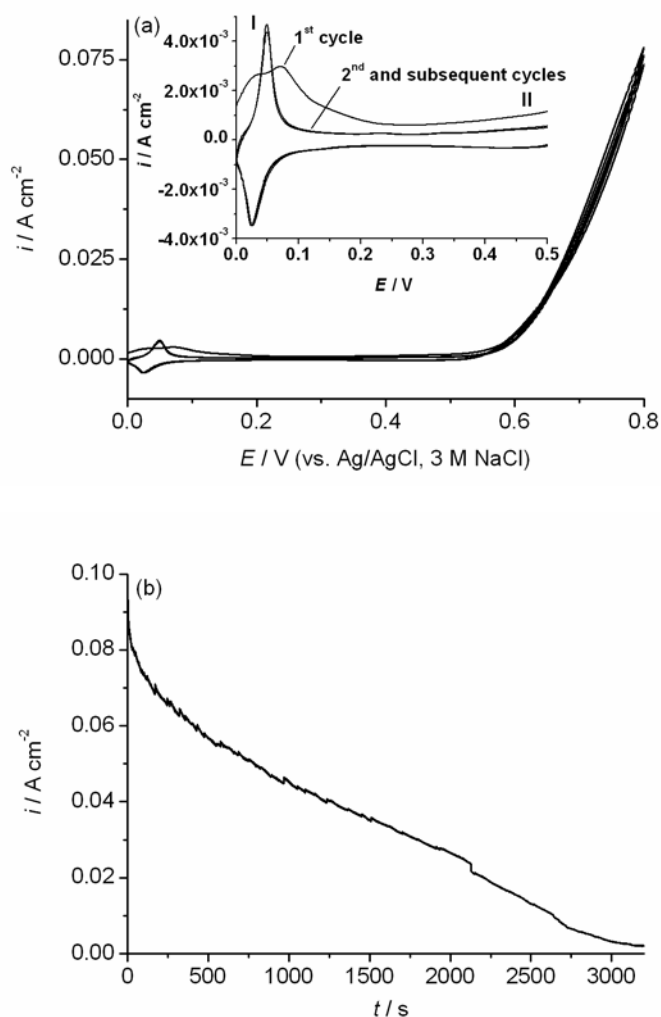


Fig. S5 (a) Cyclic voltammogram of electrocatalytic water oxidation by a cobalt – graphene modified GC electrode in aqueous 1 M NaOH electrolyte at a scan rate of 50 mV s^{-1} . Inset shows the cobalt processes in the potential range of 0 – +0.5 V. (b) Plot of catalytic current versus time during controlled potential electrolysis at the cobalt – graphene modified GC electrode in 1 M NaOH at a potential of +0.8 V. Cobalt – graphene deposition at -1.4 V for 1000 s in an aqueous 0.05 M phosphate buffer solution (pH 7) containing 1 mg ml^{-1} graphene oxide and $0.8 \text{ mM Co(NO}_3)_2$.

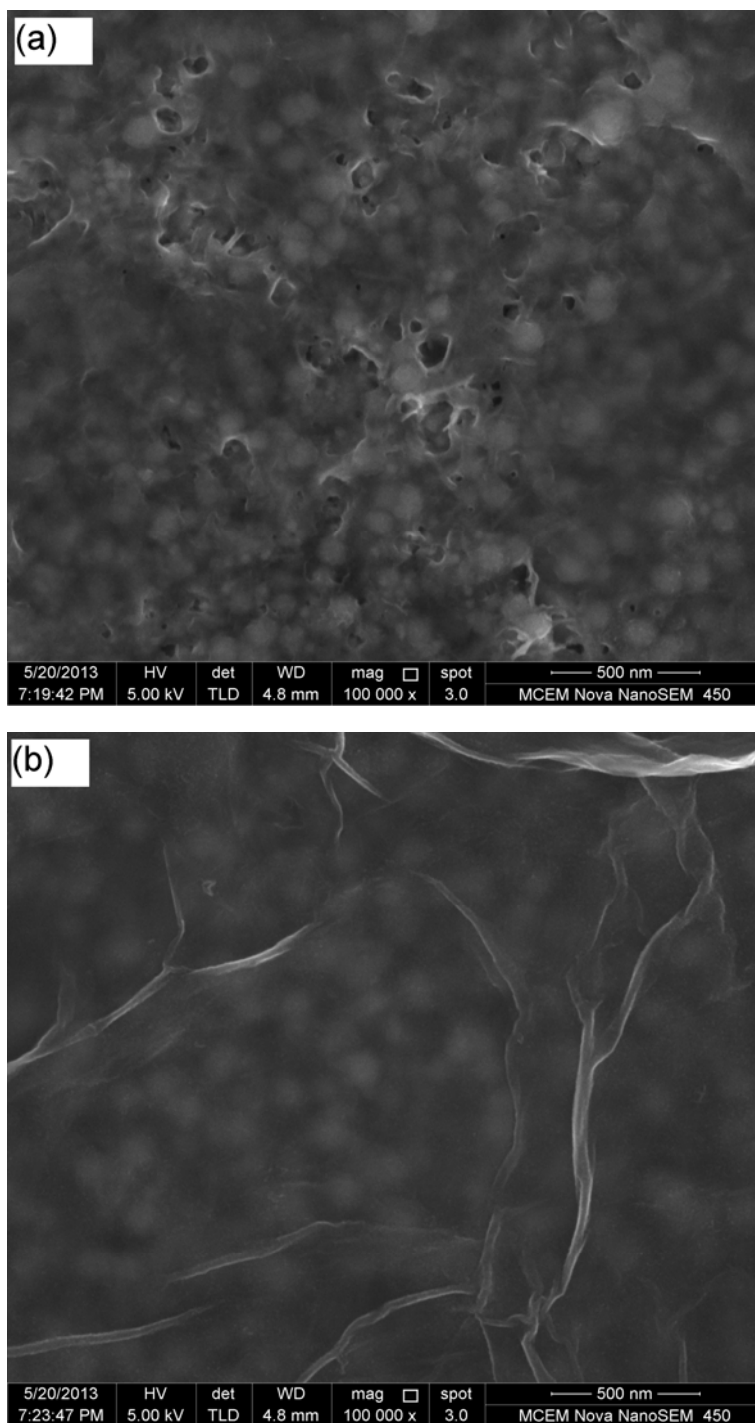


Fig. S6 SEM images of thin graphene layers showing holes (a) and intact thick layers (b) derived from a graphene/cobalt nanocomposite modified FTO electrode after controlled potential electrolysis at +0.8 V vs. Ag/AgCl for 1000 s in 1 M NaOH. Deposition of nanocomposite at -1.4 V for 1000 s.

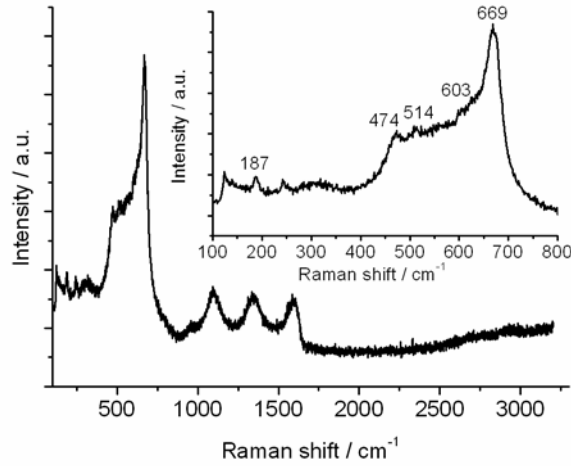


Fig. S7 Raman spectra obtained from a graphene/cobalt nanocomposite modified FTO electrode after controlled potential electrolysis in 1 M NaOH at +0.8 V for 1000s. Deposition of nanocomposite at -1.4 V for 1000 s.

Estimation of the change of OH⁻ concentration during water electrolysis under stationary conditions.

Assuming the faradaic efficiency of electrolysis is 100%, the amount of OH⁻ consumed (N) during electrolysis ($4 \text{ OH}^- \rightarrow \text{O}_2 + 2 \text{ H}_2\text{O} + 4 \text{ e}^-$) can be calculated from Faraday's law,

$$Q = \int_0^t I dt = nNF \quad (1)$$

where n is the number of electron transferred per OH⁻ which is one, I is the time dependent electrolysis current, t is the electrolysis time and F is Faraday's constant. In our case, I is almost constant during electrolysis (Fig. 7), therefore eq 1 can be simplified to,

$$N = \frac{It}{F} \quad (2)$$

To calculate how the consumption of OH⁻ affects the OH⁻ concentration in the solution adjacent to the electrode surface under stationary condition, the volume of the solution (V), where the concentration of OH⁻ is affected, is estimated based on the diffusion layer thickness ($L = \sqrt{\pi Dt}$) and electrode area (A),

$$V = LA = A\sqrt{\pi Dt} \quad (3)$$

where D is the diffusion coefficient of OH⁻.

The change of the average molar concentration of OH⁻ ($\Delta[\text{OH}^-]$) in the diffusion layer can then be estimated using equation 4 which is derived from eqs 2 and 3,

$$\Delta[\text{OH}^-] = \frac{1000N}{V} = \frac{1000It}{FA\sqrt{\pi Dt}} = \frac{1000i\sqrt{t}}{F\sqrt{\pi D}} \quad (4)$$

where $i = I/A$ is the current density.

Based on eq 4, the amount of OH^- consumed chronoamperometrically in 10 s is estimated to decrease the average OH^- concentration in the diffusion layer by ~ 0.36 M, using a current density of 0.14 A cm^{-2} (Fig. 4) and a diffusion coefficient of $5.3 \times 10^{-5} \text{ cm}^2 \text{ s}^{-1}$ for the OH^- ion (E. Samson, J. Marchand and K. A. Snyder, *Mater. Struct.*, 2003, **36**, 156-165.).