

S1.1 BET surface area and pore size

As shown in Table S1, most of the prepared HTlcs have high surface area (greater than $100 \text{ m}^2 \text{ g}^{-1}$), the only exception being Cu-Al HTlcs ($59 \text{ m}^2 \text{ g}^{-1}$).

Fig. S3 shows the nitrogen physisorption isotherms and BJH pore size distributions for the HTlcs, $\text{M}^{2+}(\text{M}^{3+})\text{O}$ and MO materials. The isotherms of HTlcs and most of the $\text{M}^{2+}(\text{M}^{3+})\text{O}$ systems has the characteristic type IV shape indicating that they are mesoporous materials. Compared to the $\text{M}^{2+}(\text{M}^{3+})\text{O}$ systems, the pore size distributions of the HTlcs were narrower and the pore diameters were smaller. The BJH pore diameters and pore volumes confirmed that Cu(Fe)O was an non-porous material, which explained its low surface area. The BJH pore diameters and pore volumes also illustrated that most of the prepared MO were non-porous materials.

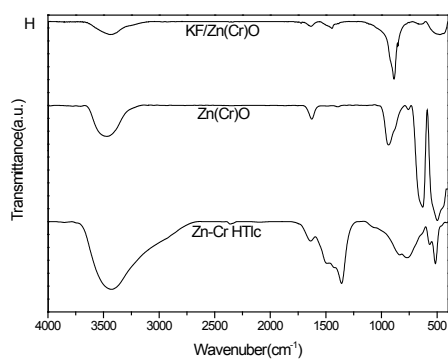
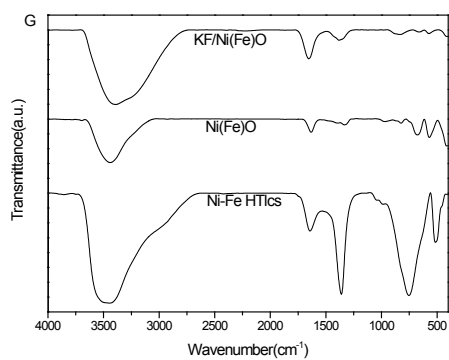
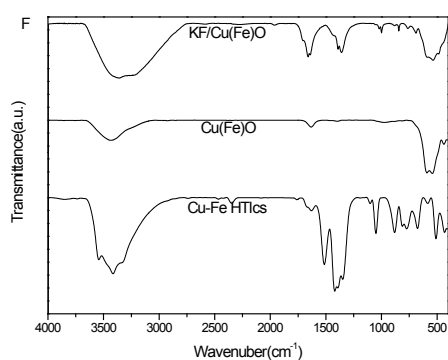
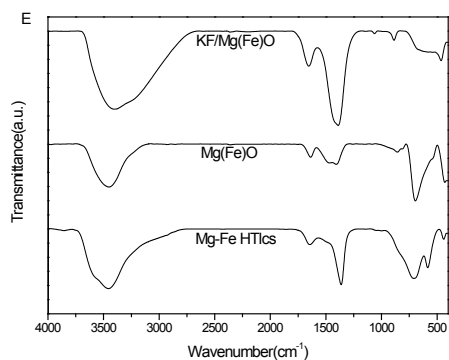
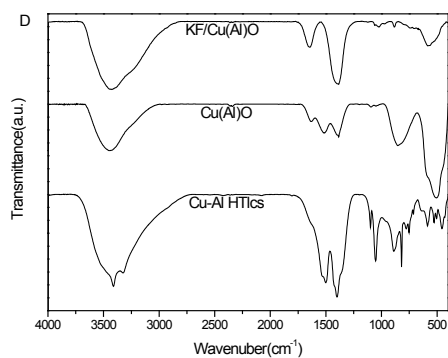
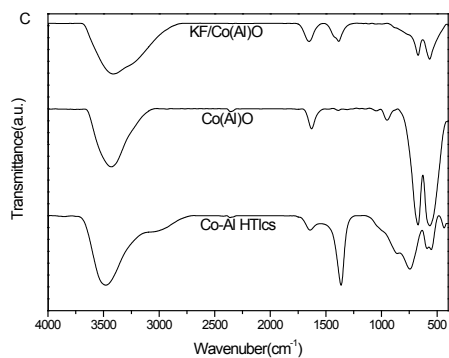
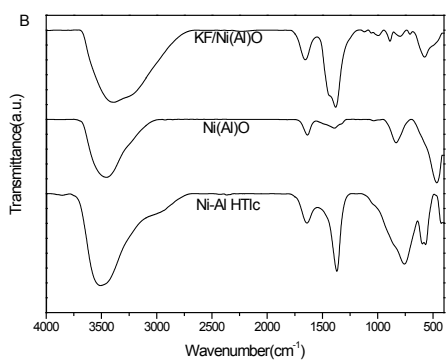
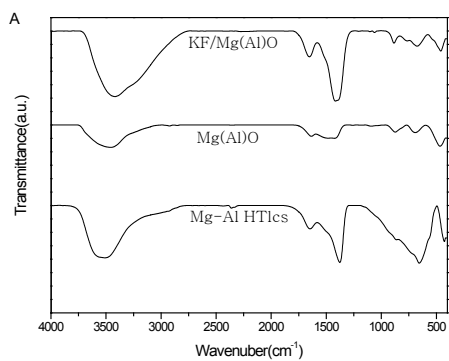
S1.2 The basic strengths and basicity of the catalysts

CO_2 TPD measurements were performed to assess the base site strength and concentration. Fig.S4 shows the rate of CO_2 desorption, normalized to the sample loading, as a function of temperature for each $\text{M}^{2+}(\text{M}^{3+})\text{O}$ support and KF/ $\text{M}^{2+}(\text{M}^{3+})\text{O}$ -cn catalyst. The desorption profiles for the $\text{M}^{2+}(\text{M}^{3+})\text{O}$ supports showed one apparent desorption peak with a maximum at 100°C .

For all the KF/ $\text{M}^{2+}(\text{M}^{3+})\text{O}$ -cn samples, with the exception of KF/Co(Cr)O-cn, only a single apparent desorption feature with a maximum 100°C was observed. Above 100°C , there were no desorption peaks for KF/ $\text{M}^{2+}(\text{M}^{3+})\text{O}$ -cn. The desorption profiles for KF/ $\text{M}^{2+}(\text{M}^{3+})\text{O}$ -cn were similar to the corresponding supports, falsely implying that KF doping did not increase the basic strength of prepared KF/ $\text{M}^{2+}(\text{M}^{3+})\text{O}$ -cn catalysts. However, both the Hammett indicators measurements are

consistent with increase in base strength upon KF doping. This apparent anomaly could arise from the high basic strength of $\text{KF}/\text{M}^{2+}(\text{M}^{3+})\text{O-cn}$ resulting in CO_2 being so strongly adsorbed on its surface that it is not desorbed below 500 °C. This suggestion is consistent with the structure analysis in section 3.2. which showed that KOH was formed on the surface of $\text{KF}/\text{M}^{2+}(\text{M}^{3+})\text{O-cn}$ catalysts (Eq. (1)-(5)). The KOH formed would be expected to chemisorb CO_2 very strongly.

$\text{KF}/\text{Co}(\text{Cr})\text{O-cn}$ did not show a desorption peak at about 100 °C, illustrating that the number of base sites may be lower than that of the support alone. The reason for this may be similar to that for $\text{KF}/\text{Cr}_2\text{O}_3\text{-cn}$ (Eq. (6)).



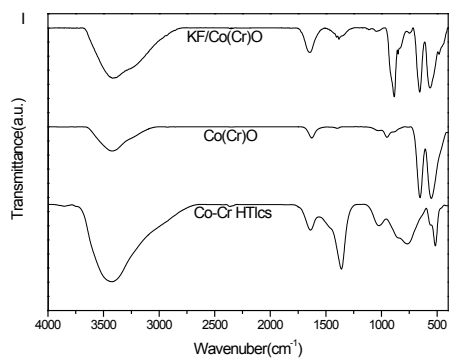


Fig. S1 FTIR spectra of HTlcs, $M^{2+}(M^{3+})O$ and $KF/M^{2+}(M^{3+})O$ -cn.

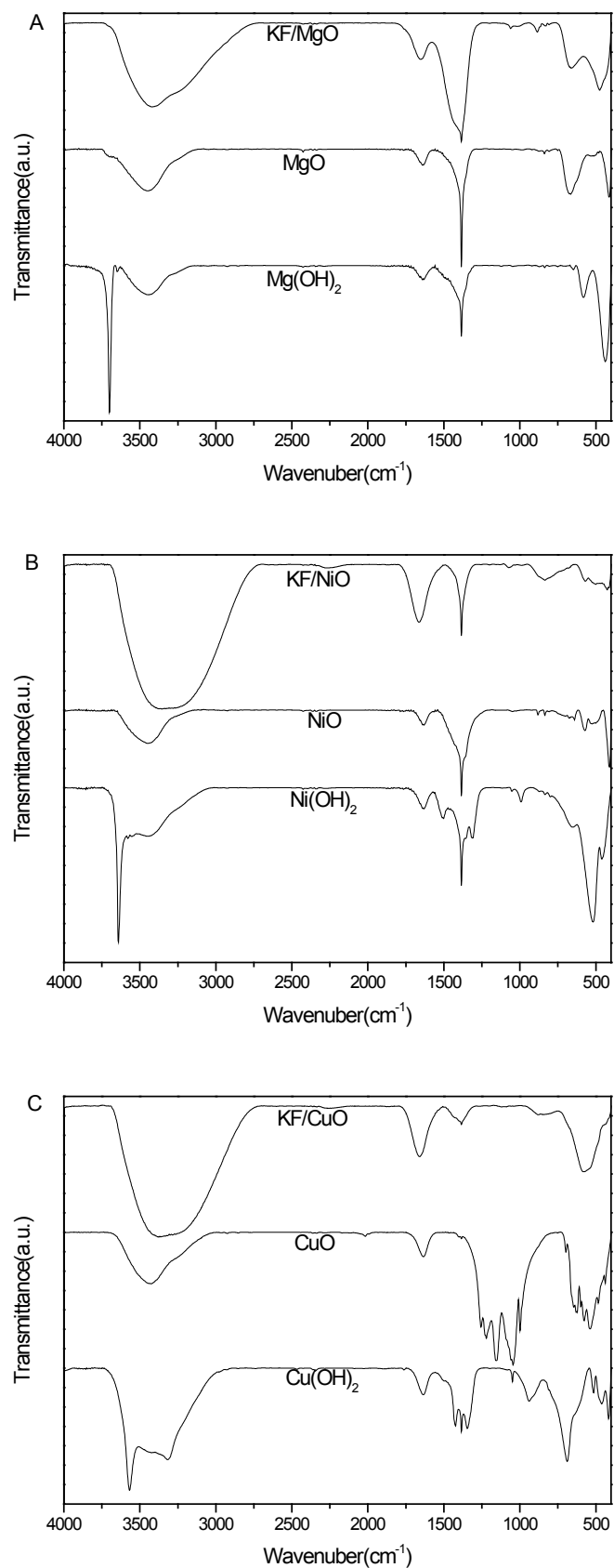


Fig. S2 FTIR spectra of M(OH)₂, MO and KF/MO-cn.

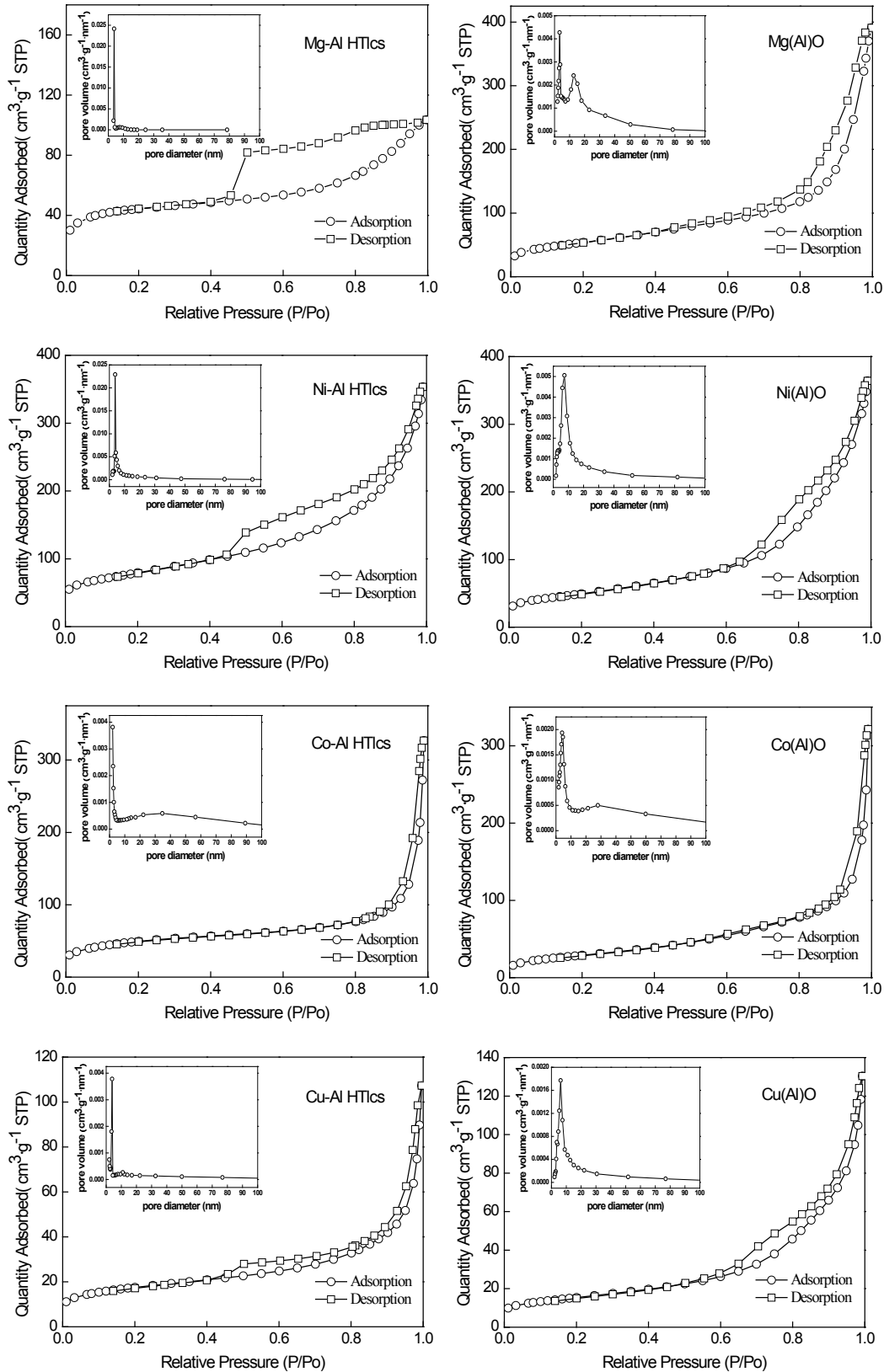


Fig.S3-continued

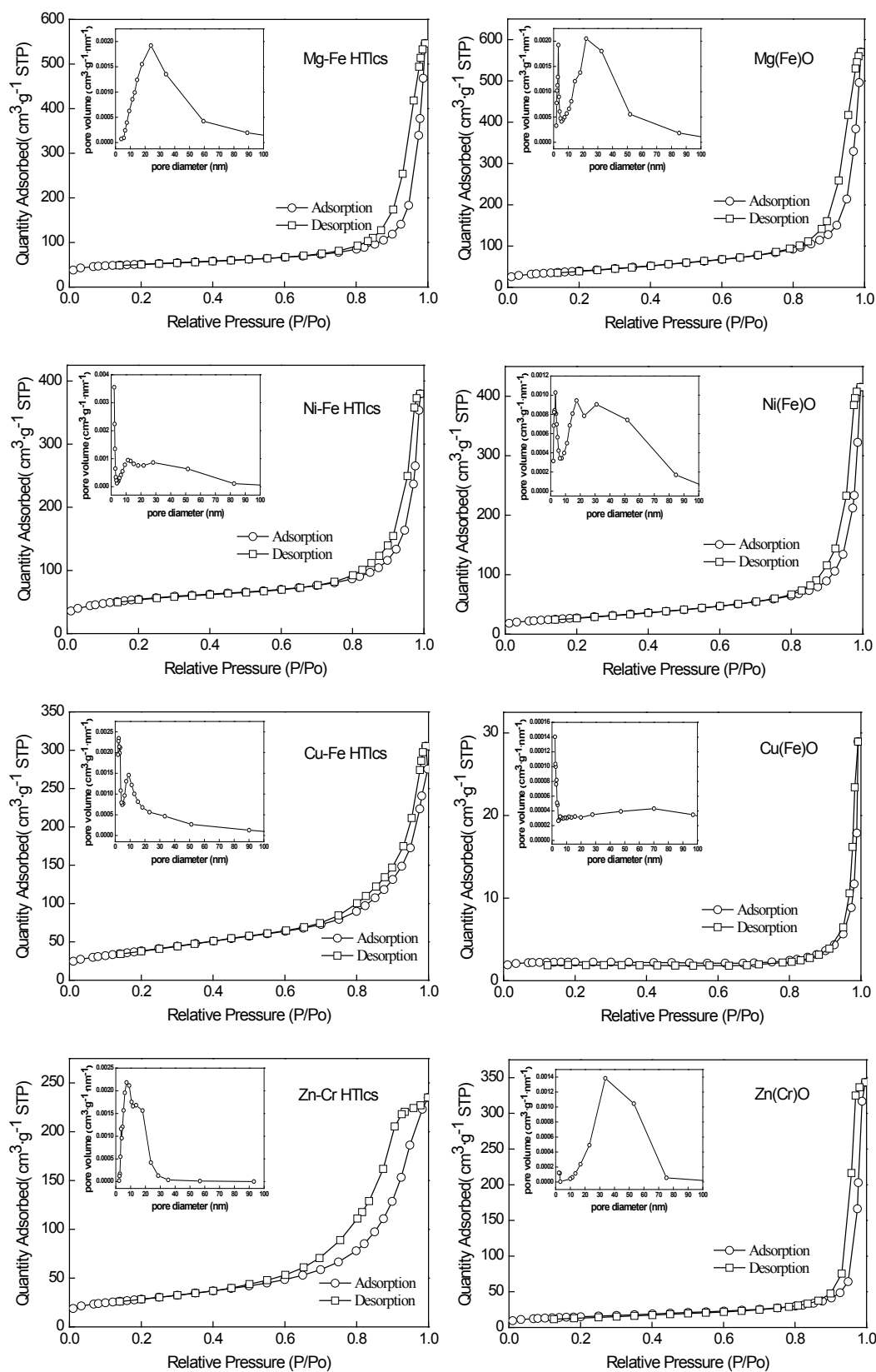


Fig.S3-continued

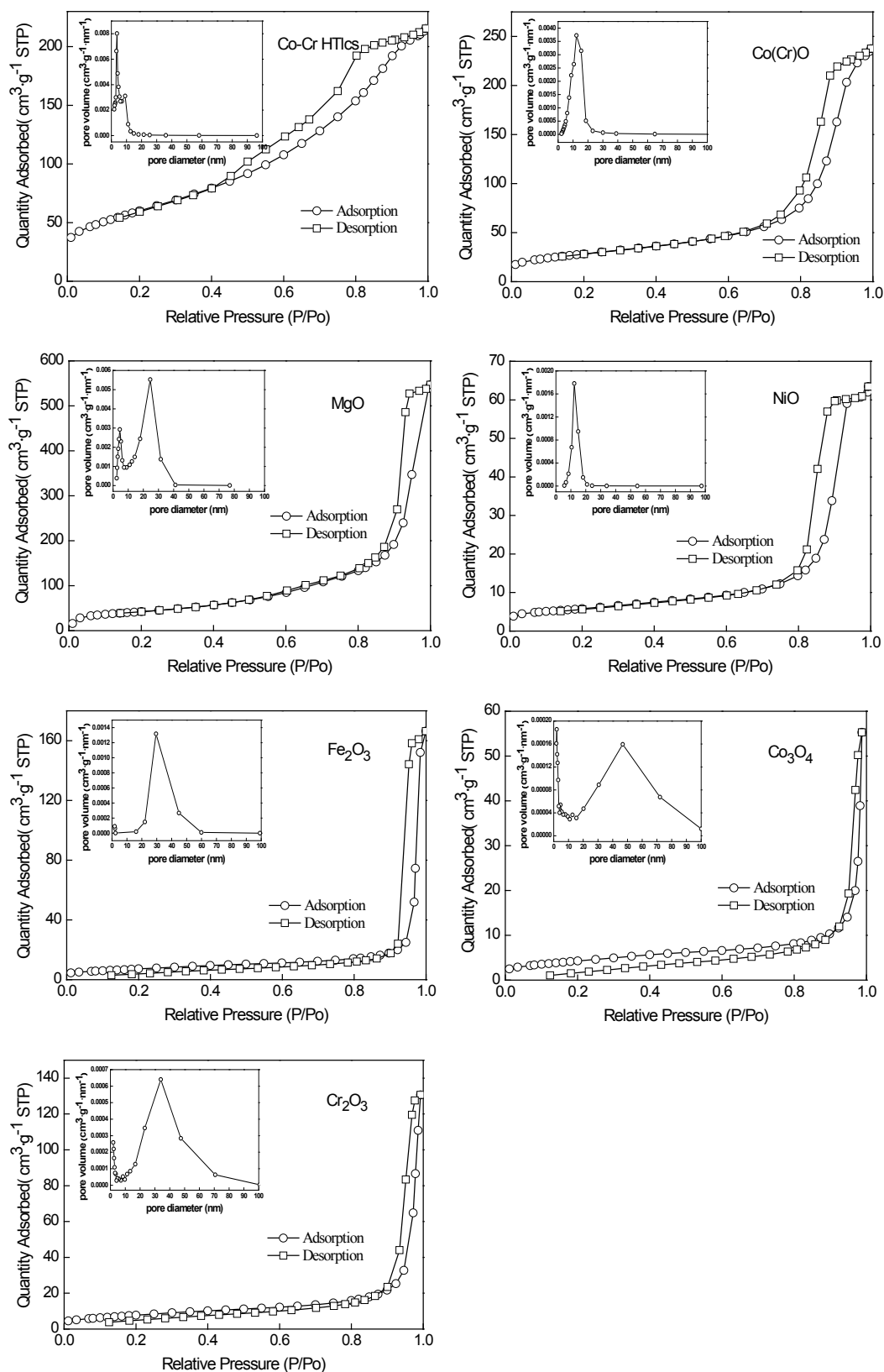
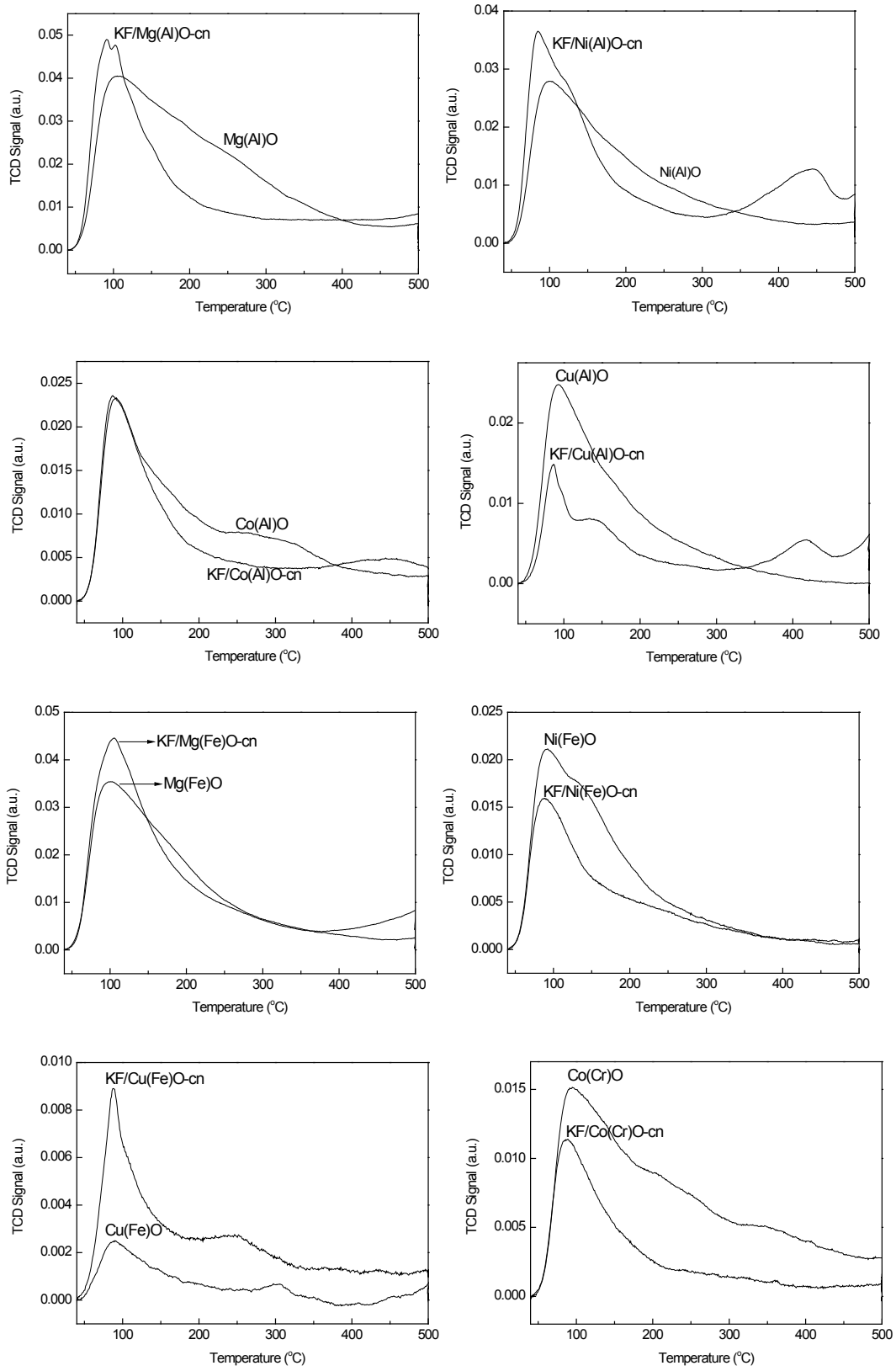


Fig. S3 Physisorption isotherms and BJH pore size distribution for HTlcs, $\text{M}^{2+}(\text{M}^{3+})\text{O}$ and MO .



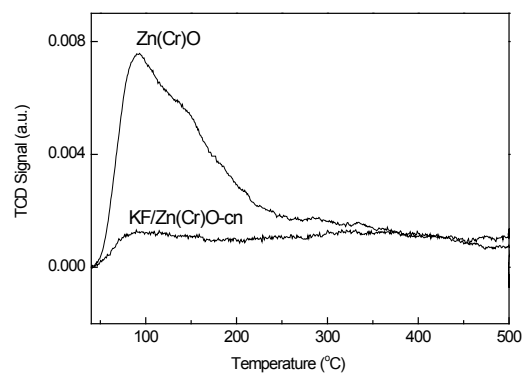


Fig.S4 TPD profiles of CO₂ adsorbed on M²⁺(M³⁺)O and KF/M²⁺(M³⁺)O-cn materials.

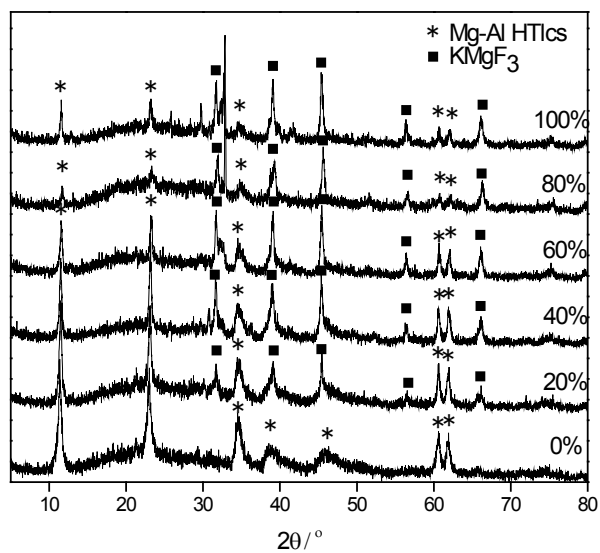


Fig. S5 XRD patterns of KF/Mg-Al HTlcs with different loading amount of KF.

Table S1 Nitrogen physisorption data of HTlcs

Entry	Catalyst	Surface Area (m ² g ⁻¹)	Pore Volume (cm ³ g ⁻¹)	Average pore width (Å)
1	Mg-Al HTlcs	140	0.16	45
2	Ni -Al HTlcs	272	0.55	73
3	Co-Al HTlcs	166	0.51	180
4	Cu-Al HTlcs	59	0.17	120
5	Mg-Fe HTlcs	164	0.85	278
6	Ni-Fe HTlcs	182	0.59	181
7	Cu-Fe HTlcs	139	0.47	122
8	Zn-Cr HTlcs	100	0.36	107
9	Co-Cr HTlcs	216	0.33	52