

## Supplemental Information

Selective oxidation of benzyl alcohol using *in situ* generated H<sub>2</sub>O<sub>2</sub> over hierarchical Au-Pd titanium silicalite catalysts.

Inés Moreno<sup>a,b</sup>, Nicholas F. Dummer<sup>a</sup>, Jennifer K. Edwards<sup>a</sup>, Mosaed Alhumaimess<sup>a</sup>, Meenakshisundaram Sankar<sup>a</sup>, Raul Sanz<sup>b</sup>, Patricia Pizarro<sup>b</sup>, David P. Serrano<sup>b,c</sup>, and Graham J. Hutchings<sup>\*a</sup>

<sup>a</sup> Cardiff Catalysis Institute, School of Chemistry, Cardiff University, Cardiff, CF10 3AT, UK.

<sup>b</sup> Department of Chemical and Energy Technology, ESCET, Rey Juan Carlos University, c/ Tulipán s/n, Móstoles, 28933, Madrid, Spain.

<sup>c</sup> IMDEA Energy Institute, Avda. Ramón de la Sagra, 3, Móstoles, 28935, Madrid, Spain.

\* Corresponding author. E-mail: hutch@cardiff.ac.uk

Keywords: Hierarchical titanium silicalite, TS-1, selective oxidation, benzyl alcohol, H<sub>2</sub>O<sub>2</sub>, direct synthesis, *in situ* oxidation.

**Table S1** Low temperature benzyl alcohol oxidation in autoclave reactor over various catalysts and the product distribution.

Catalyst	Conversion (%)	Selectivity (%)					Benzaldehyde production (mol/h/Kg <sub>cat</sub> ) <sup>1</sup>
		benzene	toluene	benzaldehyde	benzoic acid	benzyl benzoate	
TS-1 (XG-REF)	1.0	0	0	100	0	0	5
TS-1 (LG-12%)	1.0	0	0	100	0	0	5
AX	0.1	0	0	100	0	0	1
A12	0	-	-	-	-	-	0
APX	0.2	0	0	100	0	0	1
AP12	0.2	0	0	100	0	0	1
PX	0.1	0	0	100	0	0	1
P12	0.1	0	0	100	0	0	1

Conditions; 0-2°C, methanol (5.6 g), water (2.9 g), 2.3 mmol benzyl alcohol (0.25 g), 30 minutes, catalyst (10 mg), 25% O<sub>2</sub>/CO<sub>2</sub> (10.4 bar, 150 psi). <sup>1</sup> ±0.5 mol/h/Kg<sub>cat</sub>.

**Table S2** H<sub>2</sub>O<sub>2</sub> productivity at 2°C of various catalysts.

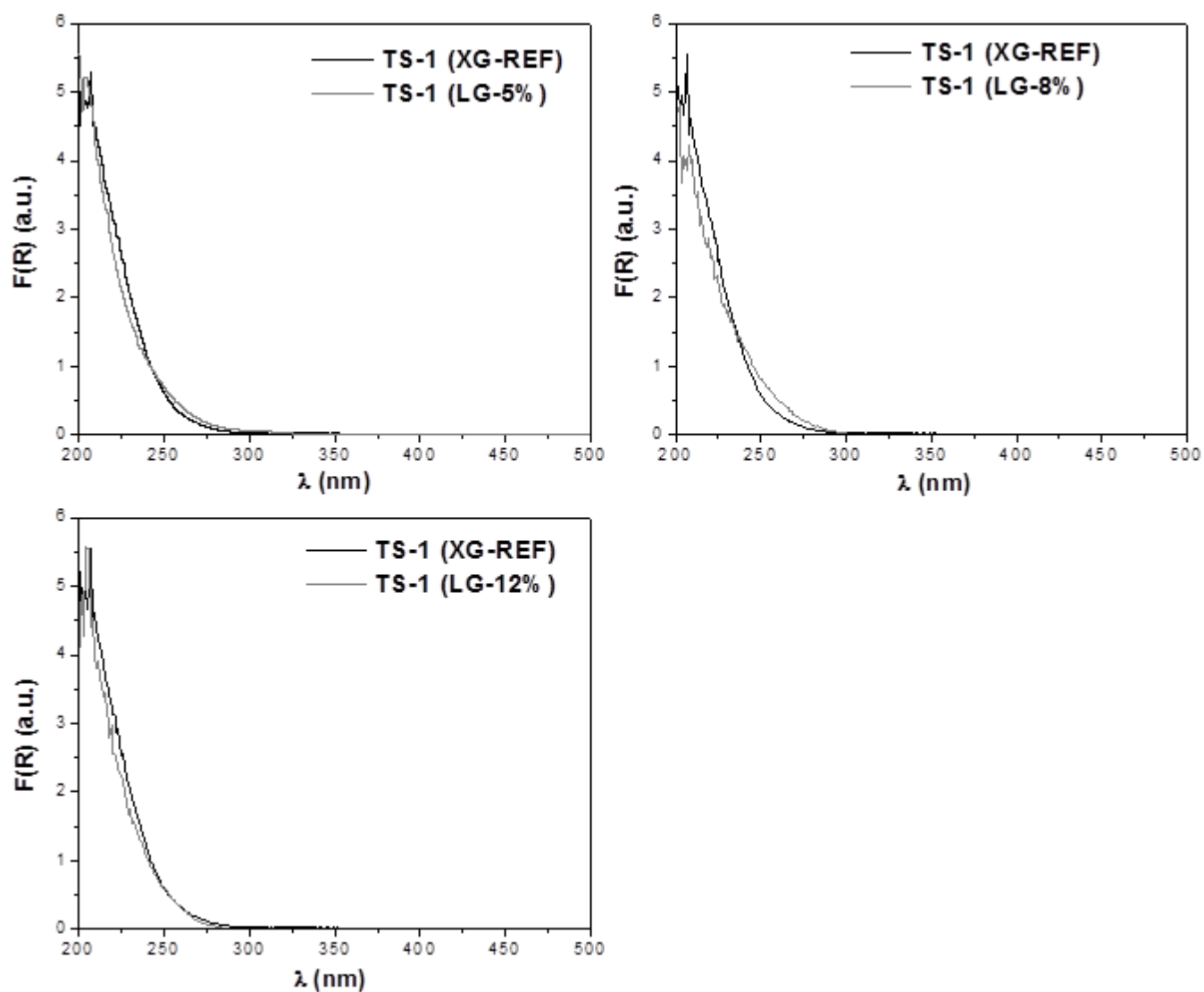
<b>Catalyst</b>	<b>Productivity (mol<sub>H<sub>2</sub>O<sub>2</sub></sub>/h/Kg<sub>cat</sub>)<sup>1</sup></b>	<b>H<sub>2</sub>O<sub>2</sub> (wt.%)</b>
TS-1 (XG-REF)	0	0
TS-1 (LG-12%)	0	0
AX	0	0
A12	0	0
APX	34	0.07
AP12	25	0.05
PX	6	0.01
P12	15	0.03

Conditions; 0-2°C, methanol (5.6 g), water (2.9 g), 30 minutes, catalyst (10 mg), 5 % H<sub>2</sub>/CO<sub>2</sub> (28.96 bar, 420 psi), 25% O<sub>2</sub>/CO<sub>2</sub> (10.4 bar, 150 psi). <sup>1</sup> ±0.5 mol/h/Kg<sub>cat</sub>.

**Table S3** H<sub>2</sub>O<sub>2</sub> productivity at 30°C of various catalysts.

<b>Catalyst</b>	<b>Productivity (mol<sub>H<sub>2</sub>O<sub>2</sub></sub>/h/Kg<sub>cat</sub>)<sup>1</sup></b>	<b>H<sub>2</sub>O<sub>2</sub> (wt.%)</b>
TS-1 (XG-REF)	0	0
TS-1 (LG-12%)	0	0
AX	0	0
A12	0	0
APX	124	0.25
AP5	96	0.19
AP8	84	0.17
AP12	95	0.19
DAPX	12	0.02
DAP12	40	0.08
PX	16	0.03
P12	77	0.15

Conditions; 30°C, methanol (5.6 g), water (2.9 g), 30 minutes, catalyst (10 mg), 5 % H<sub>2</sub>/CO<sub>2</sub> (28.96 bar, 420 psi), 25% O<sub>2</sub>/CO<sub>2</sub> (10.4 bar, 150 psi). <sup>1</sup> ±0.5 mol/h/Kg<sub>cat</sub>.



**Fig. S1** Comparison DR UV/Vis spectroscopy of hierarchical TS-1 samples and TS-1 reference zeolite (calcined).