# Inhibitory effect of $NO_2$ on the selective catalytic reduction of $NO_x$

### with NH<sub>3</sub> over one-pot synthesized Cu-SSZ-13 catalyst

Lijuan Xie, Fudong Liu, Kuo Liu, Xiaoyan Shi, Hong He\*

Research Center for Eco-Environmental Sciences, Chinese Academy of Sciences,

Beijing 100085, China

\*Corresponding author.

Fax: +86 10 62849123; Tel: +86 10 62849123;

E-mail: honghe@rcees.ac.cn (H. He)

## **Electronic Supplementary Information**

### 1. NH<sub>3</sub>-SCR performance of Cu<sub>3.9</sub>-SSZ-13 catalyst

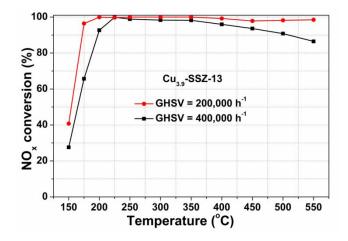


Fig. S1 NH<sub>3</sub>-SCR performance of the Cu<sub>3.9</sub>-SSZ-13 catalyst under different GHSVs.

Cu<sub>3.9</sub>-SSZ-13 catalyst exhibited excellent NH<sub>3</sub>-SCR performance in the whole temperature range, as shown in Fig. S1. The NO<sub>x</sub> conversion was higher than 95% from 175 to 550 °C under the GHSV of 200,000 h<sup>-1</sup>. When the GHSV was improved to 400,000 h<sup>-1</sup>, high NO<sub>x</sub> conversion (> 90%) was also achieved from 200-500 °C. In this study, the activity tests were carried out under a fixed GHSV of 400,000 h<sup>-1</sup>.

2. N<sub>2</sub>O formation over Cu<sub>3.9</sub>-SSZ-13 in "fast SCR" condition from 200 to 250  $^{\rm o}C$ 

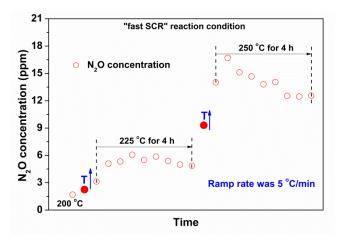


Fig. S2 N<sub>2</sub>O formation over Cu<sub>3.9</sub>-SSZ-13 in "fast SCR" condition from 200 to 250

°C.

#### 3. The effect of H<sub>2</sub>O on NH<sub>3</sub>-SCR performance of Cu<sub>3.9</sub>-SSZ-13

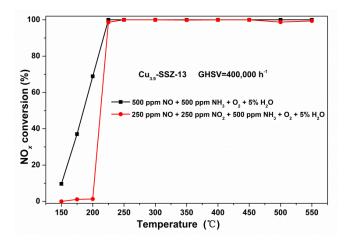
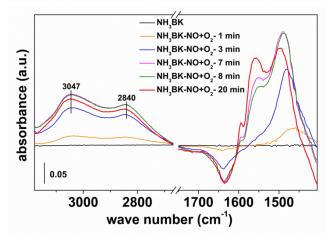


Fig. S3 NH<sub>3</sub>-SCR performance of Cu<sub>3.9</sub>-SSZ-13 under "standard" SCR and "fast"

SCR condition in the presence of 5% H<sub>2</sub>O.



#### 4. Reactions between pre-adsorbed species of NH<sub>3</sub> and NO + O<sub>2</sub>

Fig. S4 Reactions between pre-adsorbed  $NH_3$  species and  $NO + O_2$  at 120  $^{o}C$  on the

#### Cu<sub>3.9</sub>-SSZ-13 catalyst.

The reactions between pre-adsorbed species of NH<sub>3</sub> and NO + O<sub>2</sub> were carried out at 120 °C. As shown in Fig. S2, NH<sub>3</sub> species absorbed on Lewis acid sites (negative peak at ~ 1620 cm<sup>-1</sup>) were consumed firstly as soon as NO + O<sub>2</sub> was introduced, and nitrate species (positive peaks from 1500 to 1600 cm<sup>-1</sup>) formed on the sites free of NH<sub>3</sub> species. At the same time, NH<sub>4</sub>NO<sub>3</sub> (2840 and 3047 cm<sup>-1</sup>) was detected on the catalyst surface because of the quick reaction between NH<sub>4</sub><sup>+</sup> on Brønsted acid sites and nitrate species. With the introduction of NO + O<sub>2</sub>, the largest amount of NH<sub>4</sub>NO<sub>3</sub> was observed at 7 min. Although NH<sub>4</sub>NO<sub>3</sub> could be consumed by NO in the feed gas, large amount of NH<sub>4</sub>NO<sub>3</sub> still reserved on the catalyst surface after 20 min. It was obvious that the consumption speed of NH<sub>4</sub>NO<sub>3</sub> was much slower than its formation.