

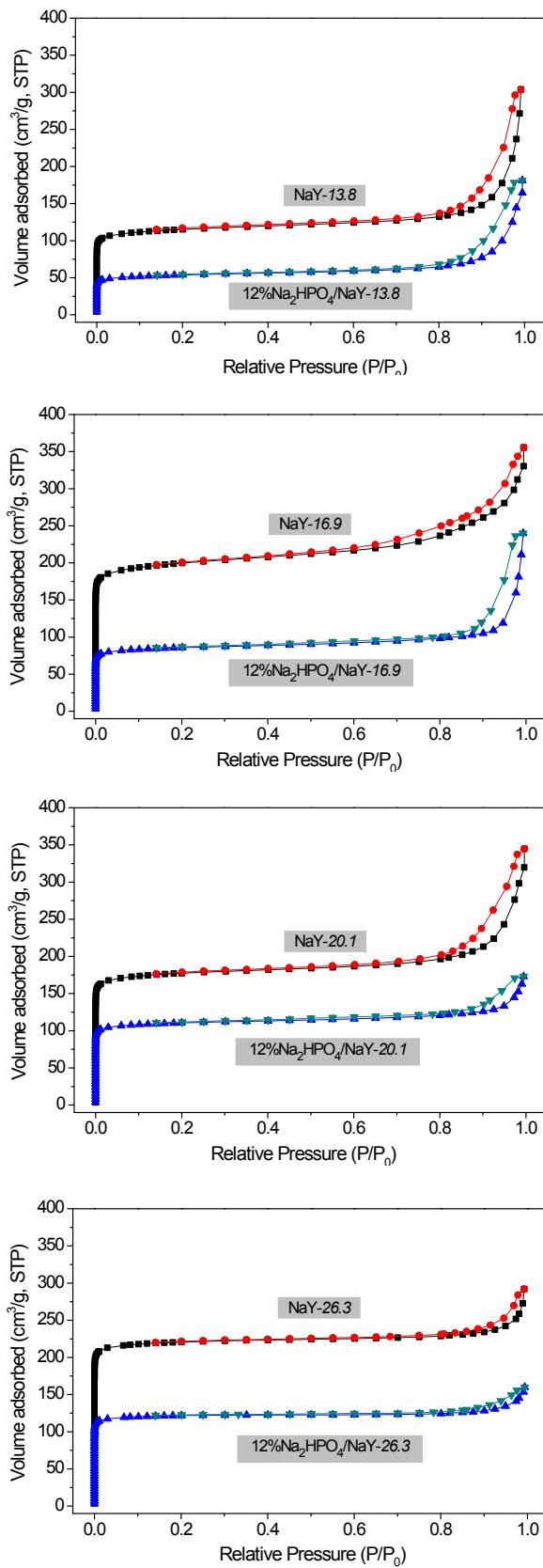
## Electronic Supplementary Information

**Table S1.** Comparison of the representative catalyst systems in LA dehydration

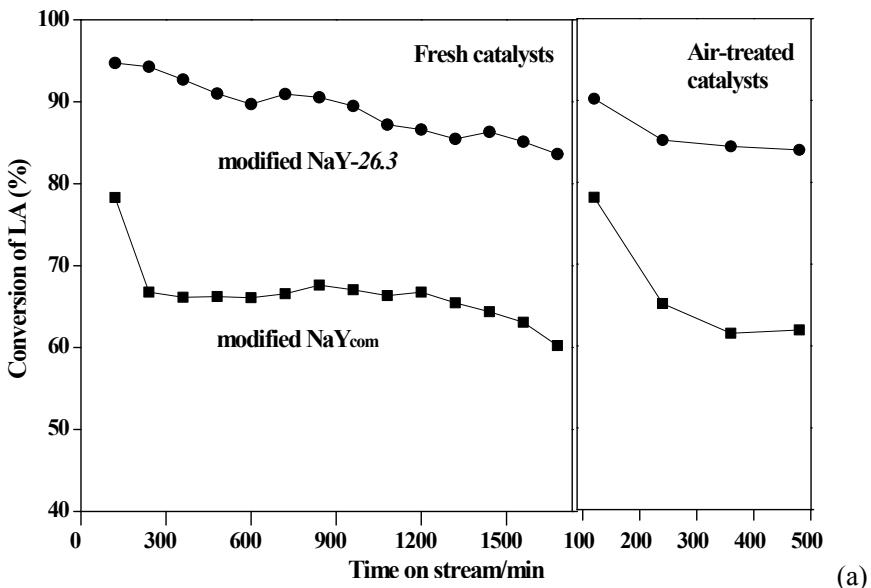
Research Work	Catalyst System	LA Feedstock Concentration (wt %)	LA Conv. (%)	AA Yield (%)	Reaction Temp. (°C)
Reference 9	CuSO <sub>4</sub> /Na <sub>2</sub> SO <sub>4</sub>	10	80	54	400
Reference 10	NH <sub>3</sub> -treated AlPO <sub>4</sub>	22	100	43.3	340
Reference 11	Phosphates + NaHCO <sub>3</sub>	20	89	58	350
Reference 12b,d	Phosphates	34	/	36	350
Reference 17a	Calcium hydroxyapatite	50	100	60	375
Reference 17b	Barium sulfate	20	99.8	74	400
Reference 22	NaNO <sub>3</sub> /SBA-15	37	97	44.8	360
Reference 25d	KI/NaY <sub>com</sub>	29	97.6	67.9	325
Reference 26	Na <sub>2</sub> HPO <sub>4</sub> /NaY <sub>com</sub>	34	85	56.6	340
This work	Na <sub>2</sub> HPO <sub>4</sub> /NaY-20.1	34	93.5	74.3	340

**Table S2.** Quantified areas of the overall desorption peaks for the unloaded and loaded NaY<sub>com</sub> and NaY-*n*

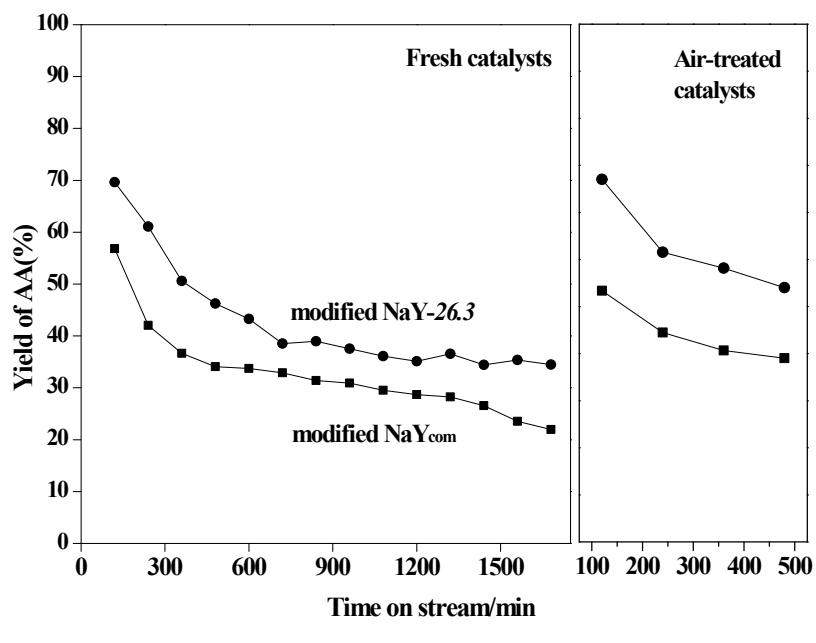
Samples	NaY <sub>com</sub>	NaY-13.8	NaY-16.9	NaY-20.1	NaY-26.3
Unloaded	267	238	240	284	308
Loaded	213	220	210	214	249



**Fig. S1.** The isotherms liner plots of NaY-*n* and 12%Na<sub>2</sub>HPO<sub>4</sub>/NaY-*n*.

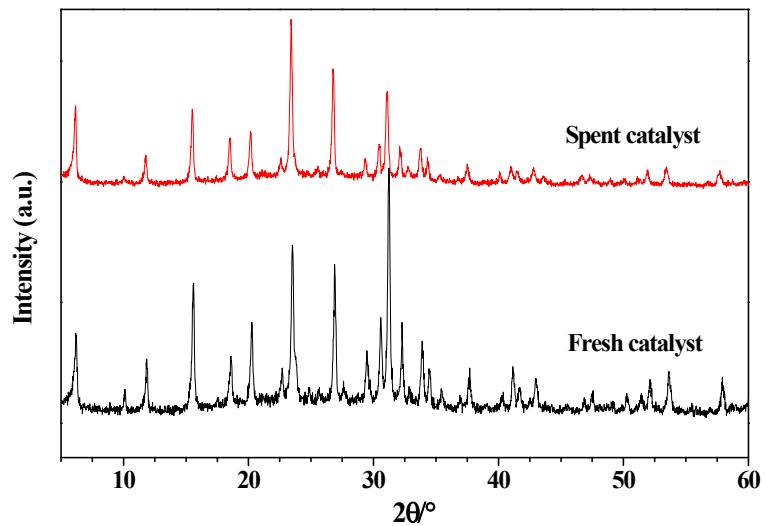


(a)



(b)

**Fig. S2.** (a) Conversion of LA and (b) yield of AA as a function of time on stream over  $\text{Na}_2\text{HPO}_4$  modified  $\text{NaY}_{\text{com}}$  and  $\text{NaY-26.3}$ : the fresh catalysts subject to a period of 1700 min reaction, and the air-treated catalysts subject to a period of 480 min reaction. Reaction temperature = 340 °C, LA concentration = 34 wt %, and  $\text{N}_2$  carrier flow rate = 30 ml/min.



**Fig. S3.** XRD patterns of the fresh and used  $\text{Na}_2\text{HPO}_4/\text{NaY-26.3}$ .