

## SUPPORTING INFORMATION

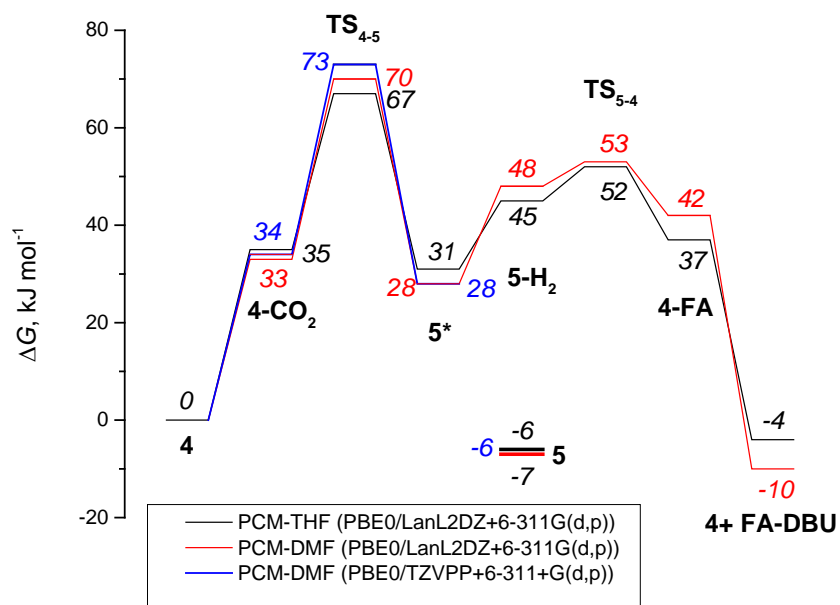
# **Mechanism of CO<sub>2</sub> Hydrogenation to Formates by Homogeneous Ru-PNP Pincer Catalyst: from a Theoretical Description to Performance Optimization**

Georgy A. Filonenko,<sup>[a,b]</sup> Emiel J.M. Hensen,<sup>[a,b]</sup> and Evgeny A. Pidko<sup>[a,b],\*</sup>

[a] Inorganic Materials Chemistry group, Department of Chemical Engineering and Chemistry, Eindhoven University of Technology, P.O. Box 513, 5600 MB Eindhoven, The Netherlands

[b] Institute for Complex Molecular Systems, Eindhoven University of Technology, P.O. Box 513, 5600 MB Eindhoven, The Netherlands

Corresponding author: Evgeny A. Pidko ([e.a.pidko@tue.nl](mailto:e.a.pidko@tue.nl))

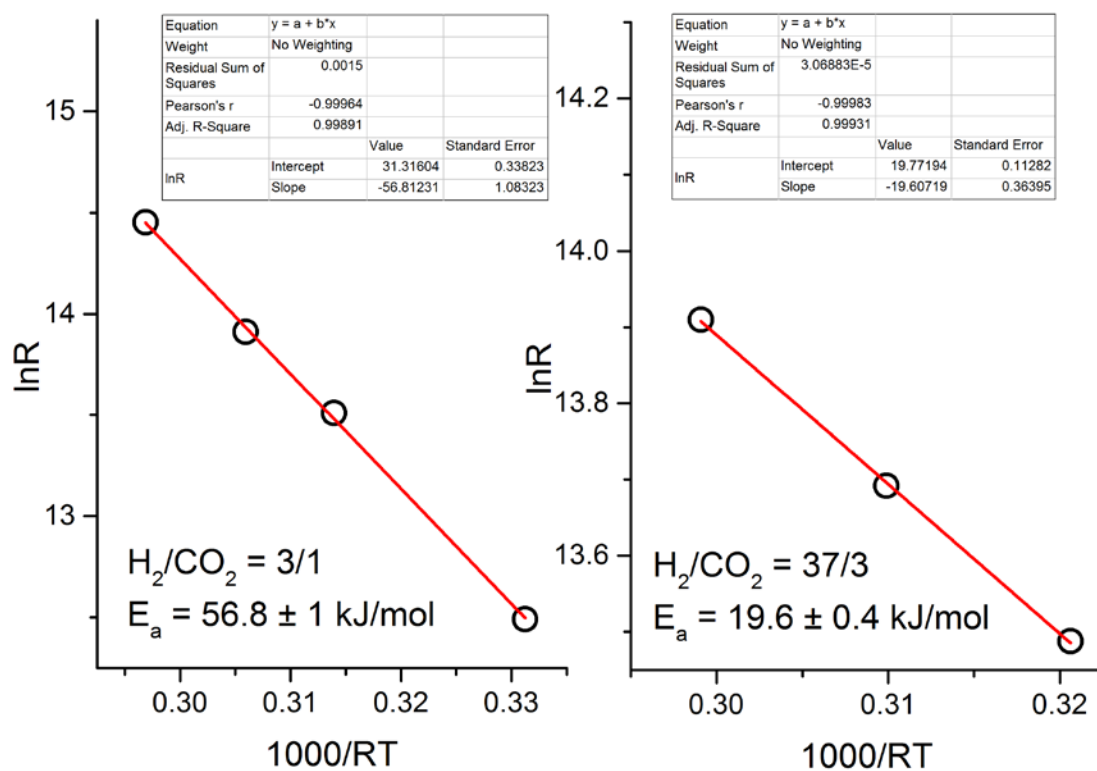


**Figure S1.** A comparison of Gibbs free energy diagrams for catalytic cycle **I** calculated using PCM model for THF and DMF solvents using standard basis sets and extended basis set combination for the PCM-DMF solvent system (these methodologies were employed for the full geometry optimization and normal mode analysis of all reaction intermediates and transition states, relative Gibbs free energy values are given in italic in  $\text{kJ mol}^{-1}$ ).

**Table S1.** Summary of the small-scale  $\text{CO}_2$  hydrogenation experiments with **1** ( $p(\text{H}_2/\text{CO}_2) = 1/1$ ) = 40 bar).<sup>a</sup>

Solvent	Base	TON	Formic acid-to-base ratio
THF	DBU	12829	0.381
THF	$\text{KO}^t\text{Bu}$	728	0.217
DMF	DBU	38642	1.147
DMF	$\text{KO}^t\text{Bu}$	649	0.194

<sup>a</sup> - Conditions: 70°C, 2h, 40 bar equimolar  $\text{H}_2/\text{CO}_2$ , 0.1 mmol catalyst, 3ml solvent.



**Figure S2.** Arrhenius plots for hydrogenation of  $CO_2$  over **1** at different  $H_2$  partial pressures.

Initial rates were used for determination of  $E_a$ . Since the rate law was not known, the pre-exponential values could not be determined accurately.