## Exploiting the dynamic properties of Pt on ceria for low temperature CO

## oxidation<sup>†</sup>

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## Supporting information



**Figure S1:** Diffraction pattern of the Pt/CeO<sub>2</sub> catalyst after an oxidation step for 1 h in 20% O<sub>2</sub> at 500 °C. All peaks correspond to the Fm-3m cubic structure of ceria (JCPDS 00-34-0394). Inset: zoom of the XRD pattern between 34 and 43°, the bar indicates the theoretical position of the more intense diffraction peak of Pt<sup>0</sup> (2 $\theta$  = 39.9°, JCPDS 00-004-802).



Figure S2: Pt 4f XPS spectrum of the Pt/CeO<sub>2</sub> catalyst at the reference state.



**Figure S3.** Impact of the REDOX sequence on the NO<sub>2</sub> yield of Pt/CeO<sub>2</sub>: a)  $\text{Red}_{500}/\text{Ox}_{500}$ , b)  $\text{Red}_{250}/\text{Ox}_{250}$  and c)  $\text{Red}_{250}/\text{Ox}_{RT}$ . Lean mixture:  $[C_3H_6] = 500$  ppm, [CO] = 1000 ppm, [NO] = 500 ppm,  $[O_2] = 10\%$  and  $[H_2O] = 10\%$ . Note that LOref curves in a), b) and c) are not identical due to slightly different Pt loadings in the SiC/catalyst mixtures.



**Figure S4.** Two successive LOref light-off curves : a) CO conversion b)  $C_3H_6$  conversion and c) NO<sub>2</sub> yield. Lean mixture:  $[C_3H_6] = 500$  ppm, [CO] = 1000 ppm, [NO] = 500 ppm,  $[O_2] = 10\%$  and  $[H_2O] = 10\%$ .



**Figure S5**. Impact of the presence of water on the LOref performances: a) CO conversion b)  $C_3H_6$  conversion and c) NO<sub>2</sub> yield. Lean mixture:  $[C_3H_6] = 500$  ppm, [CO] = 1000 ppm, [NO] = 500 ppm,  $[O_2] = 10\%$  and  $[H_2O] = 0$  or 10%.



Figure S6. CO and  $CO_2$  concentration profiles versus temperature during LO2 after a  $Red_{250}/Ox_{RT}$  sequence.



**Figure S7.** Impact of a lean/rich pulse cycling at 250 °C on the catalytic performances of Pt/CeO<sub>2</sub>: a) CO conversion b)  $C_3H_6$  conversion and c) NO<sub>2</sub> yield. The pulses sequence were composed of 30 s in 2% CO/He followed by 90 s in the lean mixture cycled for 1 h. Lean mixture :  $[C_3H_6] = 500$  ppm, [CO] = 1000 ppm, [NO] = 500 ppm,  $[O_2] = 10\%$  and  $[H_2O] = 10\%$ .



**Figure S8**. Representative STEM images of  $Pt/CeO_2$  a) after a reduction at 500 °C for 1 h in 10% H<sub>2</sub>/He and b) after a reduction at 250 °C for 1 h in 10% H<sub>2</sub>-He.



**Figure S9.** Particle size histogram of the Pt/CeO<sub>2</sub> catalyst after a reduction either at 250 °C or 500 °C for 1 h in 10% H<sub>2</sub>/He and after a pulse cycling at 250°C for 1 h (90 s in the lean mixture and 30 s in 2% CO/He). The size distribution was based on around 100 particles. Projected mean equivalent diameter: 0.83 nm ( $\sigma$ = 0.23 nm) after a reduction at 250 °C, 1.46 nm ( $\sigma$  = 0.33 nm) after a reduction at 500 °C and 1.30 nm ( $\sigma$  = 0.26 nm) after pulse cycling at 250°C.



**Figure S10.** Video of a Pt cluster produced after a  $\text{Red}_{250}/\text{Ox}_{250}$  at RT in high vacuum (High Resolution TEM mode).



**Figure S11**: Variation of the O<sub>2</sub> consumption of the Pt/CeO<sub>2</sub> catalyst as a function of time at room temperature after a TPR (1% H<sub>2</sub>/He) up to 250°C (10°C/min) and a plateau at 250°C for 1 h in 10% H<sub>2</sub>/He.



**Figure S12**. a) Raw diffraction patterns of a fresh Pt/CeO<sub>2</sub> catalyst (in its reference state) recorded in air (blue) and in H<sub>2</sub> (red) as a function of the temperature between 25 and 750 °C.  $25^*$ : XRD recorded at 25°C in air or H<sub>2</sub> after the cooling from 750°C in the same atmosphere. b) Variation of the ceria lattice parameter extracted from a) between H<sub>2</sub> and air thermal treatment as a function of the temperature.



**Figure S13**: Variations of the CO conversion as a function of the temperature: LOref after an oxidation step for 1 h in 20% O<sub>2</sub> at 500 °C mixture, LO 2: after a Red<sub>250</sub>/Ox<sub>RT</sub> sequence and LO 3: after a Red<sub>250</sub>/Ox<sub>RT</sub> sequence but without any propene in the feed. Reactive mixture:  $[C_3H_6] = 0 / 500$  ppm, [CO] = 1000 ppm, [NO] = 500 ppm,  $[O_2] = 10\%$  and  $[H_2O] = 10\%$ .

Table S1 : Comparison of the CO oxidation rates and TOF (Turn-Over Frequency) values at 100°C for various  $Pt/CeO_2$  catalysts from literature and in this work.

Species and	Specific	Pt loading	Reaction	WHSV	rCO	TOF	Ref
conditioning	surface	(wt.%) and	conditions	(L·g <sup>-1</sup> ·catalyst·h <sup>-1</sup> )	(mmol/s/g	$(x10^{-2} s^{-1})$	
_	area	precursor			Pt)		
	(m²/g)						
Subnanometric	125	0.88	[CO]=1000	750	0.198	4-6	This work
thin Pt clusters		$Pt(NH_3)_4(NO_3)_2$	ppm, $[C_3H_6] =$			Estimated	
after $\text{Red}_{250}\text{Ox}_{\text{RT}}$			500 ppm, [NO]			for Pt	
			= 500 ppm,			between	
			$[U_2]^- = 10\%$			60 and	
			[1120] 1070			100%	
Pt nanoparticles	30	1	[CO]=1000	600	0.17	6	[1]
After redox		$Pt(NH_3)_4(NO_3)_2$	$ppm, [C_3H_6] =$			Estimated	
pulses at 250°C			500 ppm, [O <sub>2</sub> ]=			for a Pt	
			8%			dispersion	
Di O Di 1	0.0	0.07	[GO] 1000	2400	10	of 50%	[0]
Pt-O-Pt clusters	80	0.27	[CO]=1000	2400	10	196	[2]
at 200°C in 5%		H <sub>2</sub> PiCl <sub>6</sub>	ppm, $[O_2] = 5\%$ [H O] =				
$H_2$ and $a$			5% $[1120] = 5%$				
subsequent			No propene.				
exposure to			rio propene.				
CO/O <sub>2</sub> feed							
between 100 and							
185°C							
Single atom	25.6	1	[CO]=4000	200	0.181	3.5	[3]
After a steam		$H_2PtCl_6$	ppm, $[C_3H_6] =$				
treatment at			100 ppm, [NO]				
/50°C			= 500  ppm,				
			$[U_2]^- = 1070,$ $[H_2O] = 5\%$				
Nanoparticles	38	1	[CO]=1.9%.	232	1.05	20.6	[4]
after a calcination		$Pt(NH_3)_4(NO_3)_2$	$[O_2] = 1.3\%$			(calculated	
at 800°C 10 h and						from the	
a reduction at						total	
275°C for 1 h in						number of	
CO (8% in He)						Pt atoms)	

## References

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