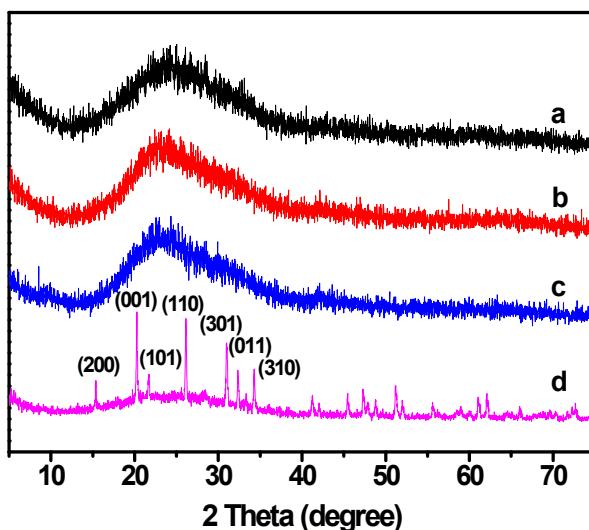
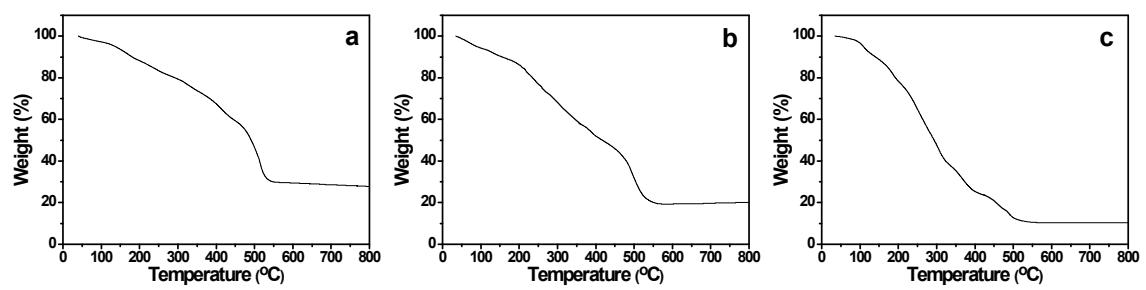


*Supporting information*

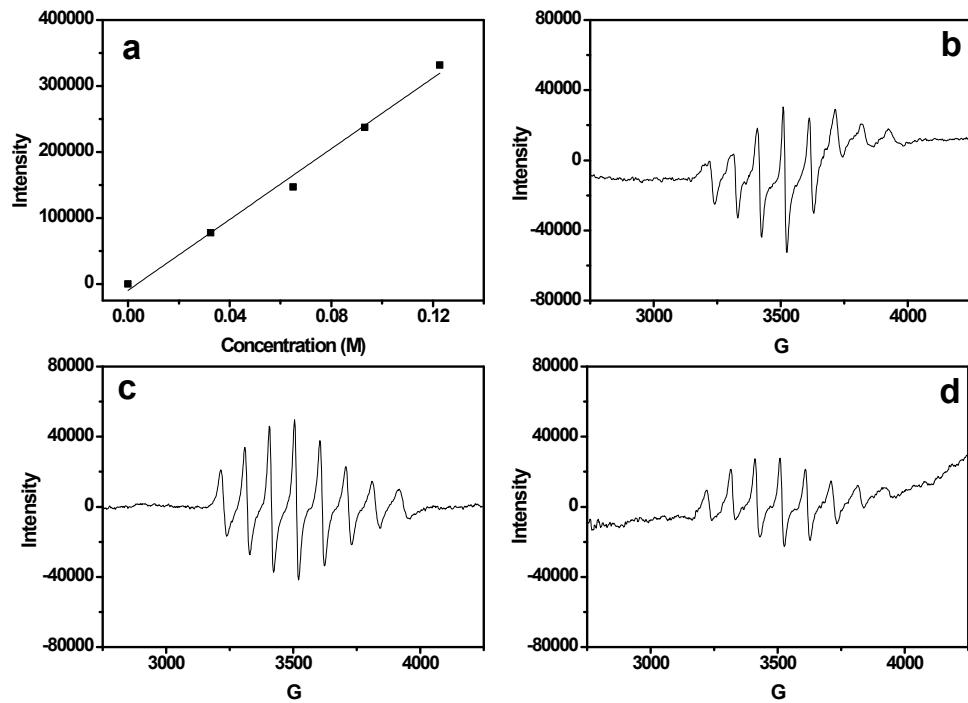
**Ionic Liquid-Stabilized Vanadium Oxo-clusters Catalyzing  
Alkane Oxidation by Regulating Oligovanadates**



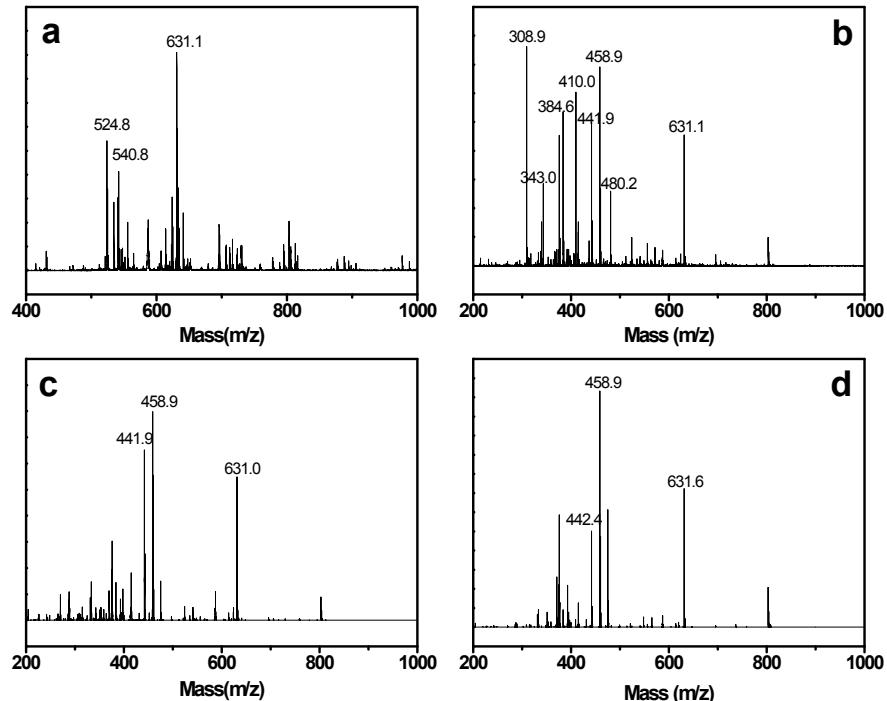
**Figure S1.** XRD patterns of IL [TBA][Pic]-stabilized V oxo-clusters. a) V-OC@IL-0.5, b) V-OC@IL-1, c) V-OC@IL-2, d) Commercial V<sub>2</sub>O<sub>5</sub>.



**Figure S2.** TGA patterns of IL [TBA][Pic]-stabilized V oxo-clusters. a) V-OC@IL-0.5, b) V-OC@IL-1, c) V-OC@IL-2.

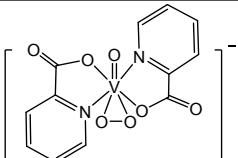
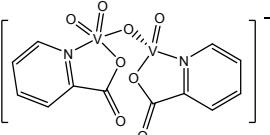
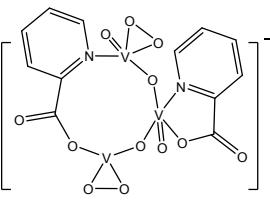
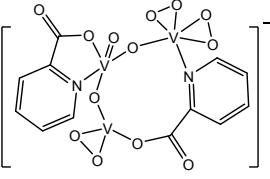
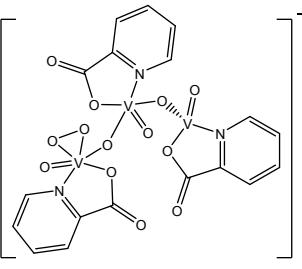
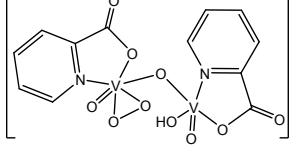
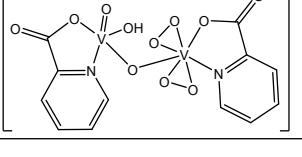


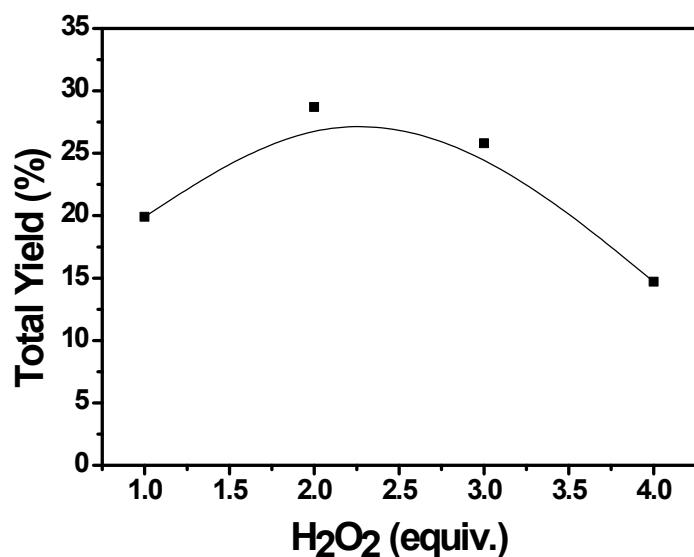
**Figure S3.** a) EPR signal intensity as a function of Vanadium (IV) concentration. The standard curve was achieved with the different concentrations (0.03 M–0.13 M) of VOSO<sub>4</sub> solution (V(IV)). b–d) EPR spectra of V-OC@IL-n (n=0.5,1,2) in H<sub>2</sub>O at 298 K. The concentration of V (IV) in the oxo-cluster was quantified by external standard method.



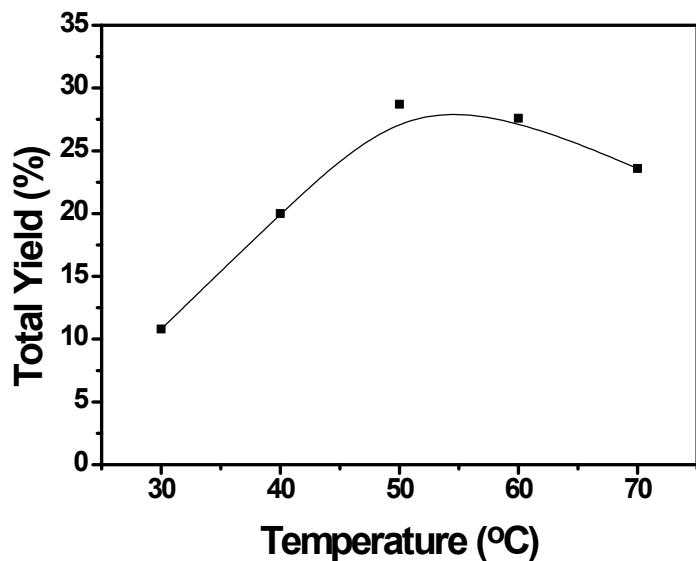
**Figure S4.** Mass spectra of the different catalysts. a) V-OC@IL-1; b) V-OC@IL-2; c) oxidizing species of V-OC@IL-1; d) The fresh solution was obtained by mixing  $\text{V}_2\text{O}_5$  and IL [TBA][Pic] in the presence of  $\text{H}_2\text{O}_2$  (molar ratio IL/V=1:1), and then subjected to MS characterization.

**Table S1. Possible structures of V oxo-cluster V-OC@IL-n (n=1 and 2) and the oxidizing species of V-OC@IL-1**

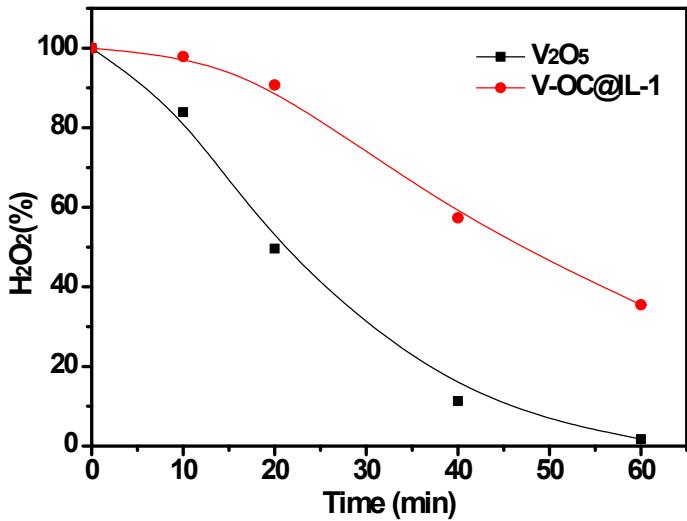
Entry	Mass (m/z)	Possible structure
1	343.0	$[\text{V}(\text{O})(\text{O-O})(\text{pic})_2]^-$ 
2	410.0	$[\text{V}_2(\text{O})_3(\mu-\text{O})(\text{pic})_2]^-$ 
3	524.8	$[\text{V}_3(\text{O})_2(\text{O-O})_2(\mu-\text{O})_2(\text{pic})_2]^-$ 
4	540.8	$[\text{V}_3(\text{O})(\text{O-O})_3(\mu-\text{O})_2(\text{pic})_2]^-$ 
5	631.1	$[\text{V}_3(\text{O})_3(\text{O-O})(\mu-\text{O})_2(\text{pic})_3]^-$ 
6	441.9	$[\text{V}_2(\text{O})_2(\text{O-O})(\text{OH})(\mu-\text{O})(\text{pic})_2]^-$ $[\text{M}-\text{H}]^-$ 
7	458.9	$[\text{V}_2(\text{O})(\text{O-O})_2(\text{OH})(\mu-\text{O})(\text{pic})_2]^-$ 



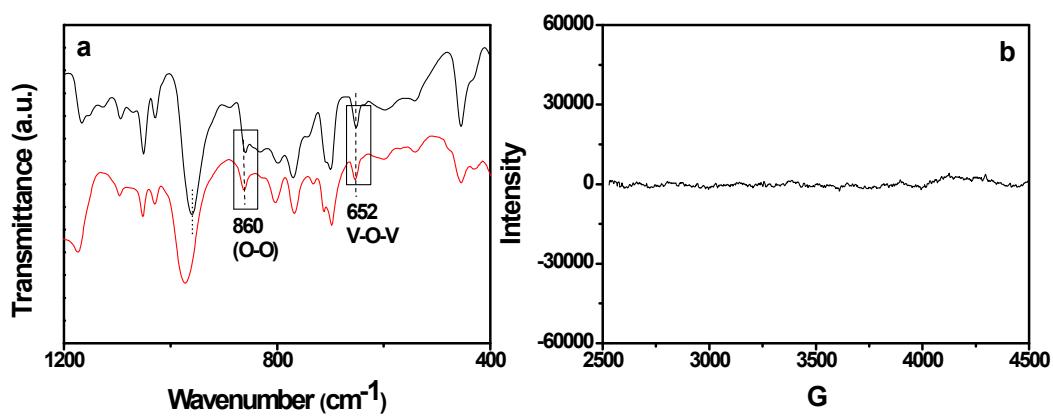
**Figure S5.** The effect of initial amount of  $\text{H}_2\text{O}_2$  on cyclohexane oxidation. Reaction conditions: cyclohexane (5.0 mmol),  $\text{H}_2\text{O}_2$  (30% aqueous solution), V-OC@IL-1 (10 mg),  $\text{CH}_3\text{CN}$  (3.0 mL), 50 °C, 1 h.



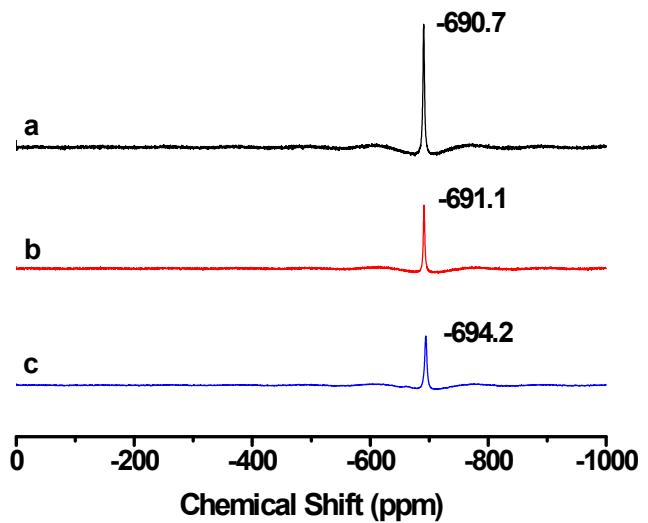
**Figure S6.** The effect of reaction temperature on cyclohexane oxidation. Reaction conditions: cyclohexane (5.0 mmol), H<sub>2</sub>O<sub>2</sub> (10.0 mmol, 30% aqueous solution), V-OC@IL-1 (10 mg), CH<sub>3</sub>CN (3.0 mL), 1 h.



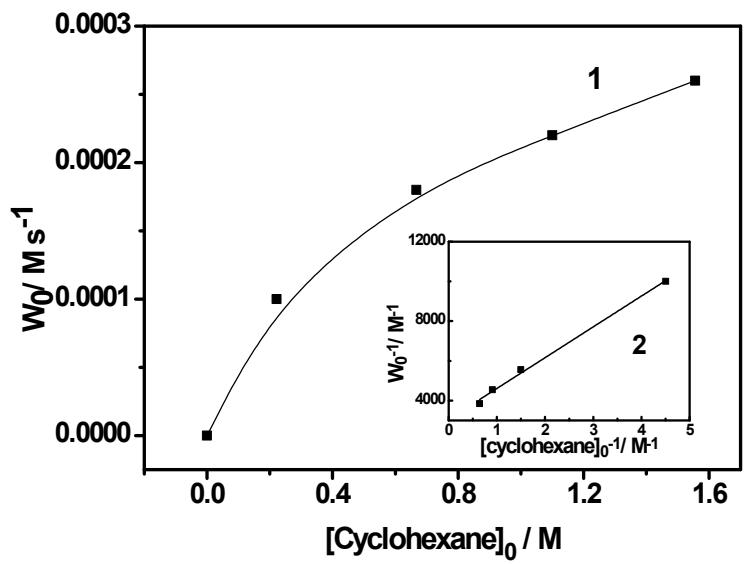
**Figure S7.** Hydrogen peroxide degradation curves over  $\text{V}_2\text{O}_5$  and  $\text{V-OC@IL-1}$ . Reaction conditions:  $\text{H}_2\text{O}_2$  (10.0 mmol, 30% aqueous solution), catalyst (0.1 mmol V),  $\text{CH}_3\text{CN}$  (3.0 mL), 50 °C.



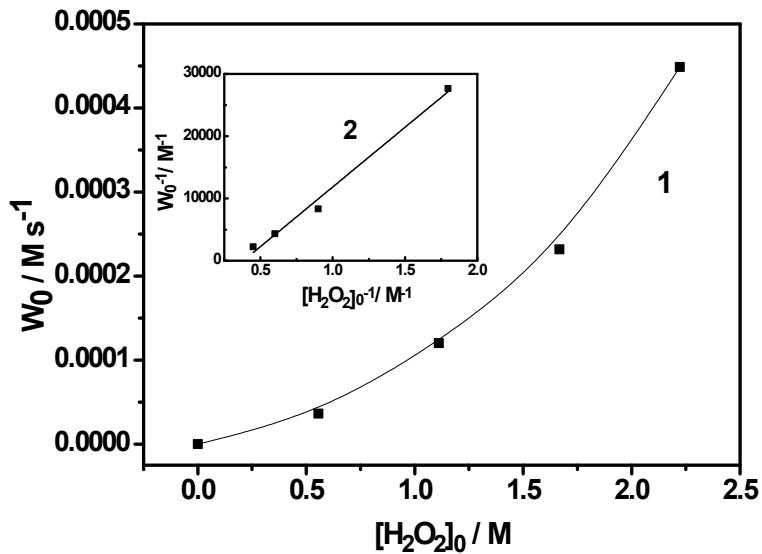
**Figure S8.** a) FT-IR spectra of V-OC@IL-1 (top) and its oxidizing species (bottom);  
b) EPR spectrum of the oxidizing species of V-OC@IL-1.



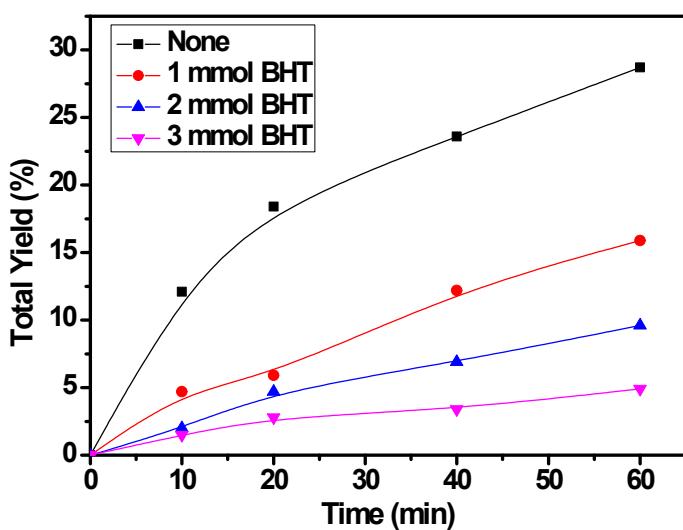
**Figure S9.**  $^{51}\text{V}$  NMR spectra of vanadium species prepared from  $\text{V}_2\text{O}_5$  under the action of  $\text{H}_2\text{O}_2$  in the presence of ionic liquid: a)  $[\text{TBA}][\text{OAc}]$ , b)  $[\text{BMIM}][\text{OAc}]$  and c)  $[\text{BMIM}][\text{BF}_4]$ , respectively.



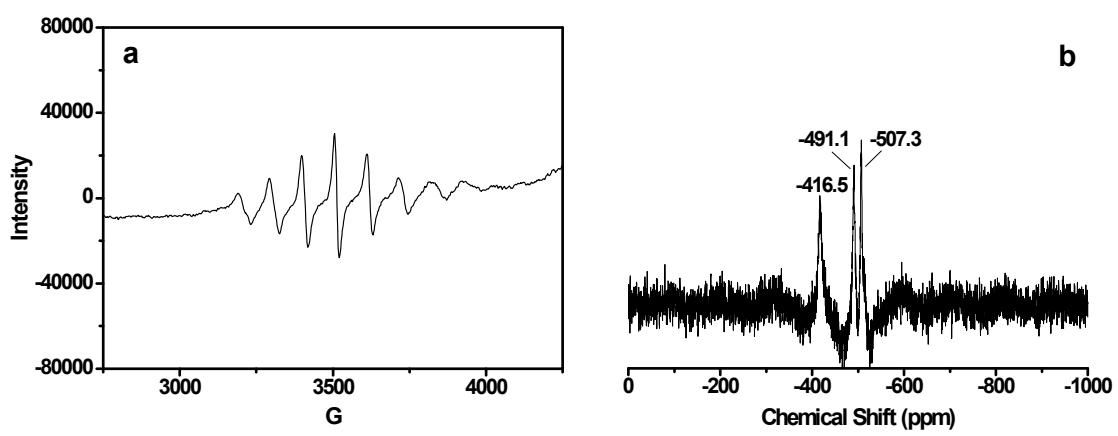
**Figure S10.** Oxidation of cyclohexane with hydrogen peroxide (2.22 M, 30 % aqueous solution) catalyzed by V-OC@IL-1 (0.004 M) in CH<sub>3</sub>CN at 50 °C (the total initial content of water in the reaction mixture was constant = 9.7 M). Dependence of the initial rate of oxygenate formation,  $W_0$ , on the initial concentration of cyclohexane is shown (curve 1). Linearization of curve 1 in coordinates  $[cyclohexane]_0^{-1}$ ,  $W_0$  is presented in line 2. Concentrations of cyclohexanone and cyclohexanol were determined after reduction of the aliquots with solid PPh<sub>3</sub>.



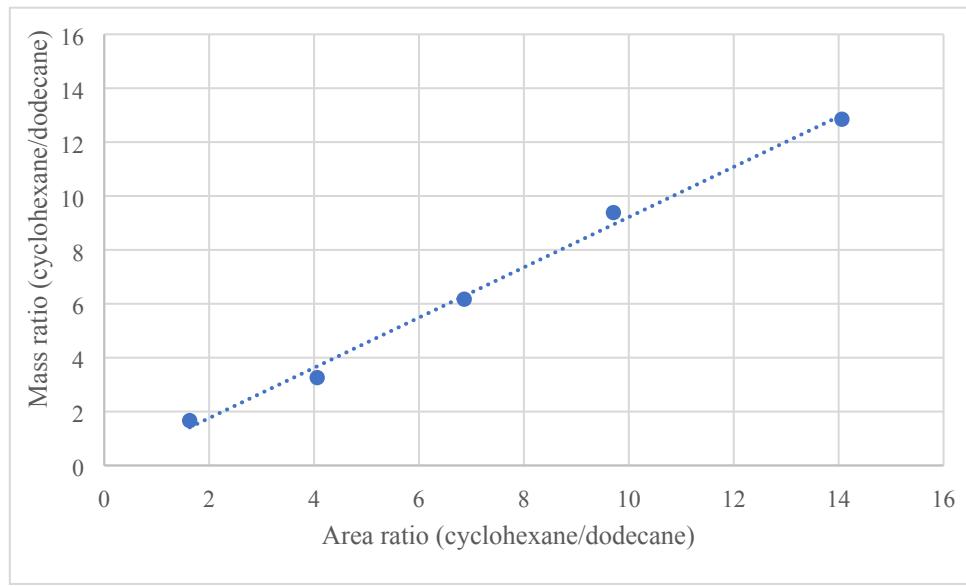
**Figure S11.** Oxidation of cyclohexane (1.11 M) with hydrogen peroxide (30 % aqueous solution) catalyzed by V-OC@IL-1 (0.004 M) in CH<sub>3</sub>CN at 50 °C (the total initial content of water in the reaction mixture was constant = 9.7 M). Dependence of the initial rate of oxygenate formation,  $W_0$ , on the initial concentration of H<sub>2</sub>O<sub>2</sub> is shown (curve 1). Linearization of curve 1 in coordinates  $[H_2O_2]_0^{-1}$ ,  $W_0$  is presented in line 2. Concentrations of cyclohexanone and cyclohexanol were determined after reduction of the aliquots with solid PPh<sub>3</sub>.



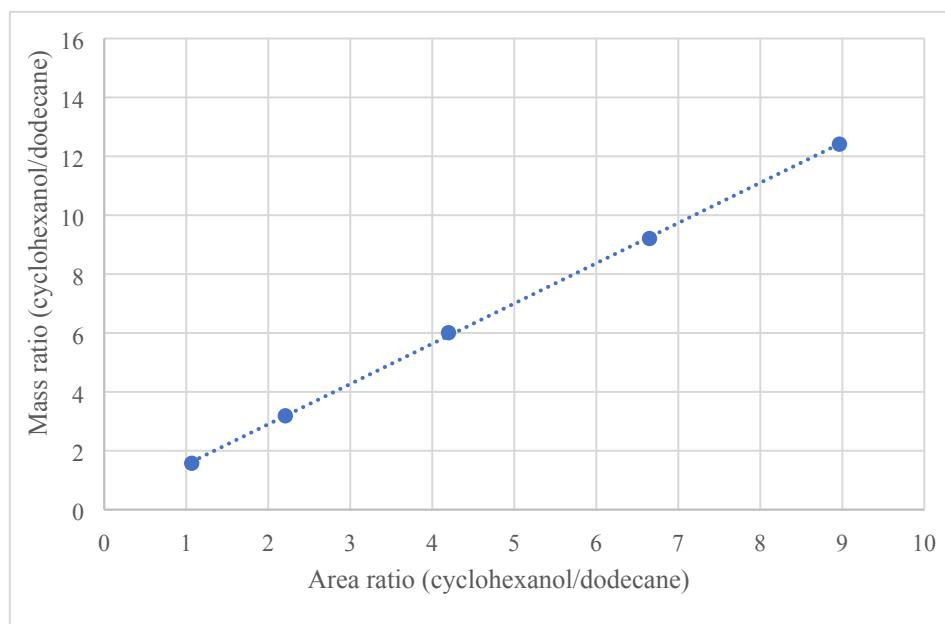
**Figure S12.** The effect of butylated hydroxytoluene (BHT) amount on the oxidation of cyclohexane. Reaction conditions: cyclohexane (5.0 mmol), H<sub>2</sub>O<sub>2</sub> (10.0 mmol, 30% aqueous solution), V-OC@IL-1(0.4 mol%), CH<sub>3</sub>CN (3.0 mL), 50 °C.



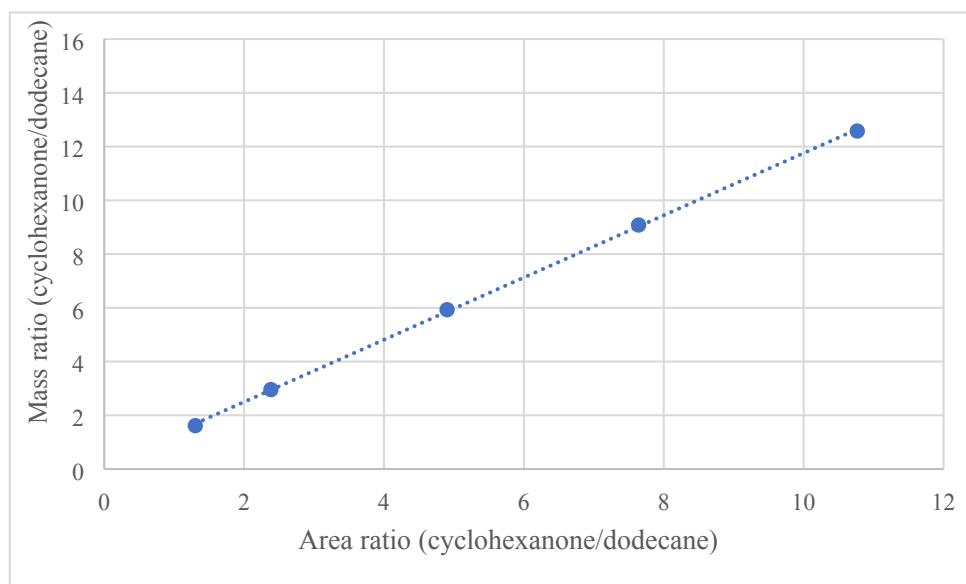
**Figure S13.** EPR spectrum (a) and  $^{51}\text{V}$  NMR spectrum (b) of the recovered V-OC@IL-1 catalyst.



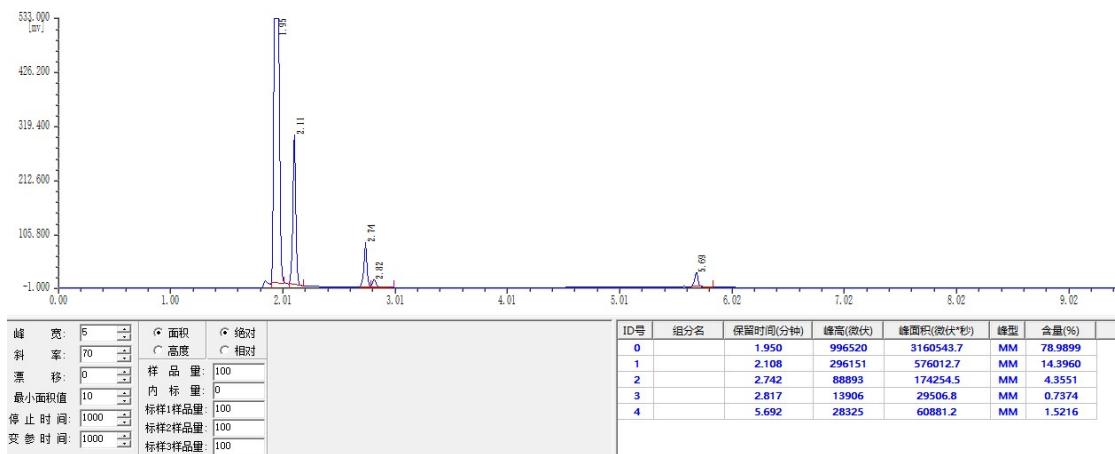
**Figure S14.** GC calibration line for cyclohexane with dodecane as internal standard.



**Figure S15.** GC calibration line for cyclohexanol with dodecane as internal standard.



**Figure S16.** GC calibration line for cyclohexanone with dodecane as internal standard.



**Figure S17.** Chromatogram example of reaction solution. The cyclohexane and the products are identified as follows (retention times in parentheses): cyclohexane (2.11 min), cyclohexanol (2.74 min), cyclohexanone (2.82 min), dodecane (internal standard, 5.69 min).

**Table S2.** Comparison of the V-OC@IL-1 catalyst with those reported catalytic systems in the selective oxidation of cyclohexane.

Catalysts	Reaction conditions	Yield of KA oil (%)	Ref.
None or Co complex (industrial production)	160–170 °C, air	<5	S1
$[\{\text{Cu}(\text{Hdea})(\text{H}_2\text{dea})\}_2(\mu_2\text{-H}_2\text{pma})] \cdot 3\text{H}_2\text{O}$	50 °C, 5 h, $\text{H}_2\text{O}_2$ , $n(\text{H}_2\text{O}_2)/n(\text{cyclohexane}) = 5$	33.5	S2
$[\text{Cu}(\kappa\text{ONN}'\text{-HL})(\text{NO}_3)(\text{DMF})](\text{NO}_3)\cdot\text{H}_2$	50 °C, 3 h, $\text{H}_2\text{O}_2$ , pyridine, $n(\text{H}_2\text{O}_2)/n(\text{cyclohexane}) = 5$	21.6	S3
$[\text{VO}(\text{OCH}_3)(5\text{-Cl-quin})_2]$	50 °C, 1 h, $\text{H}_2\text{O}_2$ , $n(\text{H}_2\text{O}_2)/n(\text{cyclohexane}) = 4.3$	39	S4
CuSBdiAP	70 °C, 3 h, $\text{H}_2\text{O}_2$ , $n(\text{H}_2\text{O}_2)/n(\text{cyclohexane}) = 1.5$	27.68	S5
CeCr/NC-500	60 °C, 5 h, $\text{H}_2\text{O}_2$ , $n(\text{H}_2\text{O}_2)/n(\text{cyclohexane}) = 2$	53.9	S6
Cl-PCFe	150 °C, 2 h, 1.0 MPa $\text{O}_2$	12.1	S7
Co-MgAlO	150 °C, 2 h, 0.6 MPa $\text{O}_2$	7.5	S8
AC	125 °C, 8 h, 1.5 MPa $\text{O}_2$	5.3	S9
$\text{C}_6\text{MHImHSO}_4\text{-Co/ZSM-5}$	150 °C, 3 h, 1.5 MPa air	8.9	S10
V-OC@IL-1	50 °C, 1 h, $\text{H}_2\text{O}_2$ , $n(\text{H}_2\text{O}_2)/n(\text{cyclohexane}) = 2$	28.7	This work

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