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Supplementary Information

Room temperature and atmospheric pressure aqueous partial oxidation of ethane to oxygenates over AuPd catalysts

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Experimental Section

Chemicals

Palladium(II) chloride (\geq 99.9%, PdCl₂), Gold(III) chloride trihydrate (\geq 99.9%, HAuCl₄·3H₂O), Sodium borohydride (99%, NaBH₄), Hydrogen peroxide solution (30 wt.%, H₂O₂), Ethanol (reagent grade), Acetaldehyde solution (40 wt.%), Acetic acid (\geq 99.7%), Glycolic acid (99%), Deuterium oxide (99.8 atom% D, D₂O), Phenol (99.0-100.5%), Dimethyl sulfoxide (\geq 99.9%, DMSO), Cerium(IV) sulfate (Ce(SO₄)₂) and Hydrochloric acid (37%, HCl) were purchased from Sigma-Aldrich. Formic acid (88%), Ferroin indicator (0.025 M) and Sodium hydroxide (NaOH) were purchased from Fisher Scientific. The 2 mg(Pd)/mL PdCl₂ acidic solution was prepared using 0.5 M HCl, and 2 mg(Au)/mL HAuCl₄ aqueous solution.

Catalyst Synthesis

AuPd nanoparticles were prepared through a modification of a method reported in the literature. ¹ 0.8775 mL PdCl₂ acidic solution (2 mg(Pd)/mL) and 1.625 mL HAuCl₄ solution (2 mg(Au)/mL) were added to a glass conical flask containing 207.2 mL deionized water. 1.65 mL of freshly prepared NaBH₄ aqueous solution (0.1 M) was injected into the solution under stirring (1000 rpm) as two 0.825 mL aliquots. The stirring speed of the produced dark brown colloidal suspension was kept at 1000 rpm for 30 minutes, and then the suspension was boiled vigorously (100 °C) under stirring (1000 rpm) until the suspension volume was between 20 and 25 mL. Of note, continuous stirring is critical to synthesize uniform colloids. After cooling down, the colloidal suspension was made up to 25 mL by adding deionized water. Finally, the as-prepared AuPd colloidal suspension (pH around 2.3) was stored in glass bottle. The suspension was sonicated uniformly prior to use. Au and Pd nanoparticles were prepared using similar processes as for AuPd. To maintain consistency across experiments, Pd nanoparticles were separated by centrifuge and dispersed in HCl aqueous solution (pH around 2.3) prior to use.

Catalyst Testing

A purpose-made PEEK reactor, constructed from Swagelok fittings, was used for all experiments. The reactor has a total volume of 24.5 mL. A Teflon-coated K-type thermocouple was inserted into the reaction liquid to directly measure the reaction temperature. No metal components were in contact with the reaction liquid. For experiments with H₂O₂ oxidant, 5 mL of colloidal catalyst (1 mg AuPd) and a specific amount of H₂O₂ were added to the reactor. Prior to testing, the PEEK reactor was sealed and purged with ethane (99.999%, Matheson) to remove air, and then pressurized with ethane to achieve the desired pressure, typically 1 bar. The reaction liquid was continuously stirred (1000 rpm) at room temperature (21 °C) using a magnetic stirrer for a specific period of time (usually 1 hour). For experiments at elevated temperatures, the reactor was heated and maintained at the desired reaction temperature. After the reaction, the reactor was cooled to a temperature below 15 °C in ice. The headspace gas was extracted using a gas-tight syringe for analysis.

In a typical continuous-feed semi-batch reactor experiment, described in the main text to maintain a low and steady H_2O_2 concentration, catalysts and initial 30 μ mol H_2O_2 (10 mM, 3 mL) were added to the reactor (initial 500 μ mol acetic acid was added for the corresponding acetic acid oxidation reaction). Then the reactor was connected to a gas-tight syringe pump. Prior to testing, the reactor was purged with ethane (for the ethane oxidation reaction) or nitrogen (for the acetic acid oxidation reaction) for 15 mins. The reactor was then sealed and the pressure was steady at 1 bar.

After 1 h of reaction, 470 µmol H₂O₂ in 2 mL of water was continuously added to the reactor by syringe pump during the following 49 h of reaction time.

Product Analysis

The gas phase products were analyzed by GC (Agilent GC7980) equipped with TCD and FID detectors (Helium as carrier gas). Residual H_2O_2 concentration was determined by titration with acidified $Ce(SO_4)_2$ solution using 8 μ L ferroin indicator.^{2,3} The liquid phase products were analyzed by 1H-NMR (Bruker 400 MHz NMR) using water suppression technique to decrease the dominant water signal. DMSO (1 mM) and phenol (8 mM) were used as internal standards.⁴ Typically, 500 μ L liquid product was mixed with 40 μ L standards (DMSO and phenol) aqueous solution and 60 μ L D_2O for the measurement. The measurements for ethanol, methanol, acetaldehyde, acetic acid, formic acid, and glycolic acid were calibrated from purchased standards following procedures reported in the literature (Figure S2a).⁴

To quantify ethyl hydroperoxide, liquid solutions containing only ethyl hydroperoxide were reduced using prepared fresh 0.05 M NaBH₄ solution. After this, the reduced liquid products were analyzed by 1H-NMR. Considering that ethanol was the only reduction product, the amount of ethyl hydroperoxide was related directly to the total amount of ethanol. This procedure was robust and formed the basis of an ethyl hydroperoxide calibration curve (Figure S2b). Notably, considering both ethyl hydroperoxide and ethanol have three peaks located at around 1.07 ppm due to the signal of protons from CH₃CH₂- in 1H NMR spectrum, the areas of the peaks located at 3.96 ppm (CH₃CH₂- of ethyl hydroperoxide) and 3.56 ppm (CH₃CH₂- of ethanol) were calculated to quantify the amount of ethyl hydroperoxide and ethanol, respectively. Methyl hydroperoxide was quantified using analogous methods (Figure S2c).

Catalyst Characterization

X-ray diffraction (XRD) patterns were recorded on a Bruker D8 Advanced Diffractometer with Cu K_{α} radiation. X-ray photoelectron spectroscopy (XPS) data were collected on a Thermo ESCALAB 250Xi instrument equipped with a monochromatic Al $K\alpha$ (hv = 1486.6 eV)) source, and all XPS spectra were calibrated using C 1s peak at 284.8 eV as the reference. ICP-atomic emission spectroscopy (Agilent 725ES) was used for analysis Au/Pd molar ratio. Scanning electron microscopy (SEM) images and electron dispersive X-ray spectroscopy (EDXS) results were obtained on a JSM-5600 LV instrument. Scanning transmission electron microscopy (STEM) images were collected on a JEOL 2100-F-AC operated at 200 kV, and samples were prepared on copper grids coated with ultra-thin holey carbon films.

Computational Methods

Density Funcitonal Theory calculations (as implemented in the Vienna *Ab-initio* Simulation Package)⁵ are used to study the C-H bond activation reaction. The AuPd(111) surface is modelled as a four-layer metal slab, consisting of a (4 x 4) fcc unit cells with 19 Å vacuum spacing between the periodic images. All calculations are performed using the RPBE functional⁶ with Grimme's D3(BJ)⁷ method to account for the dispersion interactions. The transition states are determined using the climbing-image nudged elastic band approach.⁸ All calculations use a 400 eV plane-wave cutoff and (3 x 3 x 1) k-point grid. A force threshold of 0.03 eV/Å is used for the geometry optimizations.

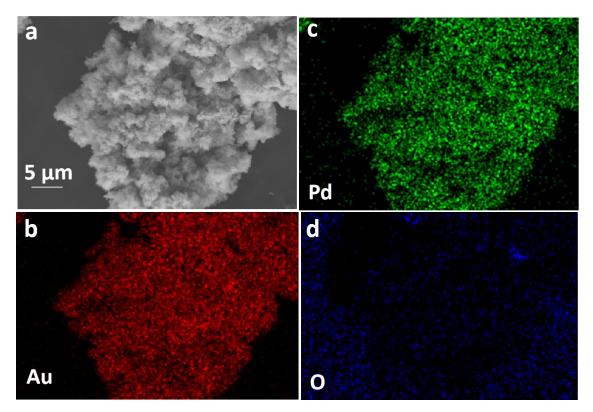


Figure S1. SEM-EDX elemental mapping of AuPd.

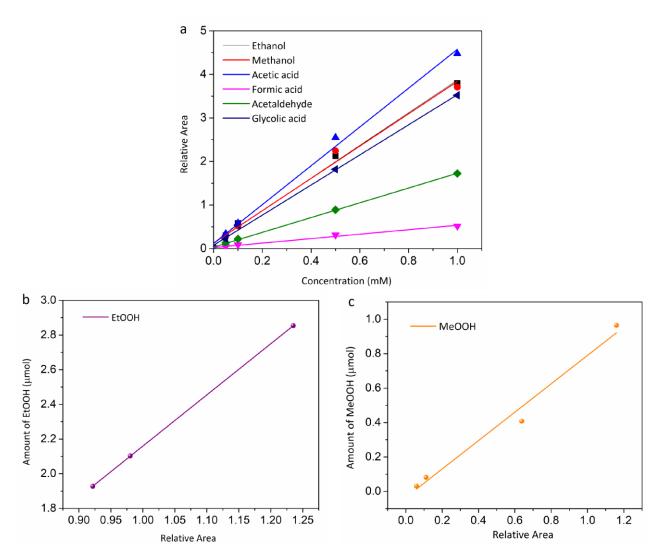


Figure S2. Standard calibration curves for products. (a) Ethanol, methanol, acetaldehyde, acetic acid, formic acid, glycolic acid; (b) ethyl hydroperoxide; (c) methyl hydroperoxide.

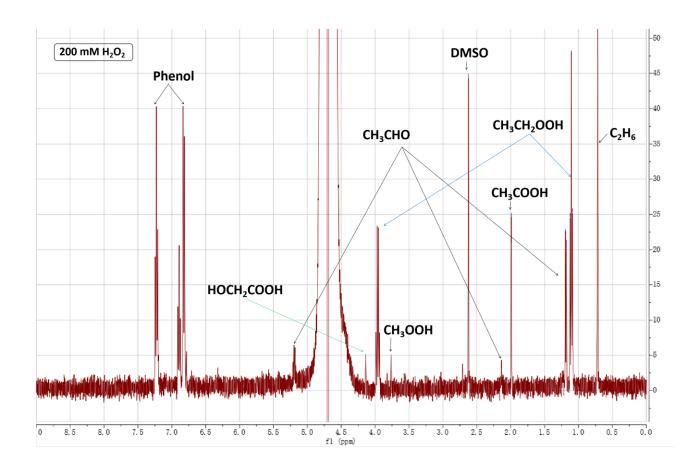


Figure S3. Typical 1H-NMR spectrum for liquid products. This spectrum corresponds to products of the oxidation of C_2H_6 using AuPd with $[H_2O_2]_{initial} = 200$ mM. Reaction conditions: 5 mL; 1 mg AuPd; 1 bar C_2H_6 ; 21 °C; 1 h; 1000 rpm.

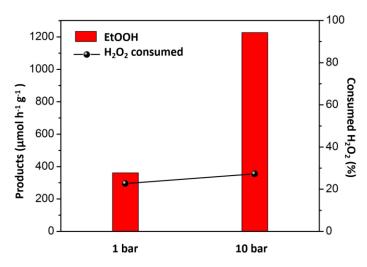


Figure S4. Comparison of catalytic activity of AuPd for C_2H_6 oxidation performed at 1 bar C_2H_6 (Gain factor = 0.0318) and 10 bar C_2H_6 (Gain factor = 0.0899). Gain factor is defined as mol oxygenates/mol H_2O_2 consumed. Reaction conditions: 5 mL; 1 mg AuPd; 1 bar or 10 bar C_2H_6 ; 21 °C; 1 h; 1000 rpm; $[H_2O_2]_{initial} = 10$ mM.

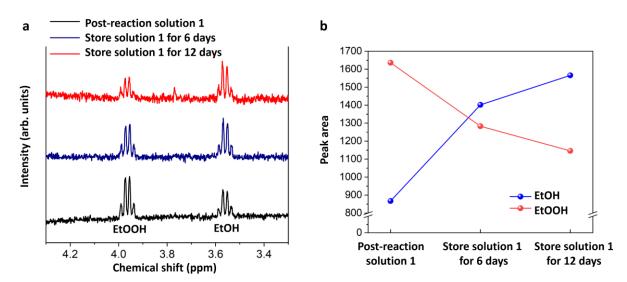


Figure S5. (a) Typical 1H-NMR spectra for low concentrations of liquid products. Solution 1 results from C_2H_6 oxidation over AuPd at 50 °C with 100 mM $[H_2O_2]_{initial}$ for 1 h. (b) Normalized peak areas of EtOOH and EtOH associated with solution 1 after reaction and after storage of the solution for 6 and 12 days. The peak areas of products are normalized to peak area of the internal standard DMSO.

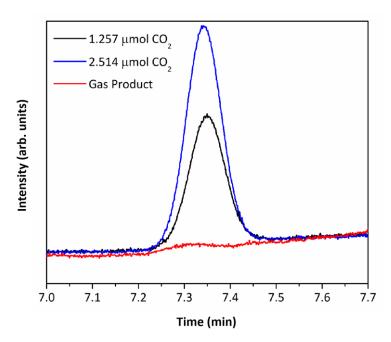


Figure S6. GC curve analyzing CO_2 in the gas phase after reaction over AuPd. CO_2 was nearly undetectable in the gas phase when compared with the calibration results for minute quantities of CO_2 .

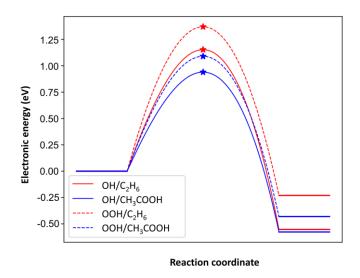


Figure S7. DFT calculations of activation barriers of C₂H₆ and CH₃COOH over AuPd surfaces.

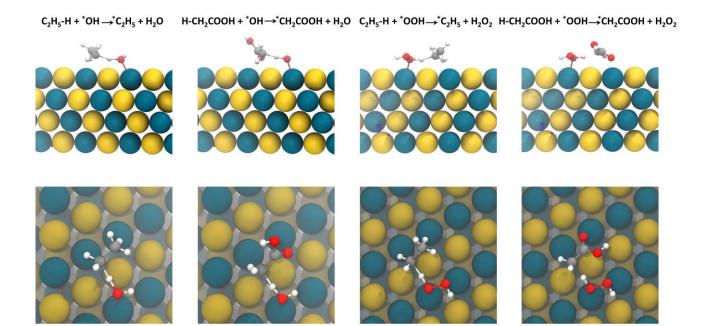


Figure S8. Front and top view for the structures of reaction intermediates and transition states (TS) involved in C_2H_6 and CH_3COOH activation by *OH and *OOH, respectively, over AuPd surfaces. Yellow: Au; dark green: Pd; gray: C; white: H; red: O.

Table S1. Results of elemental analysis of AuPd.

	ICP-AES				
Elements	Unn. (ωt.%)	Norm. (ωt.%)	Atom. (at.%)	Error (ωt.%)	$(mg/L)^{[b]}$
0	1.60	2.25	18.07	0.4	n.d.
Pd	23.16	32.48	39.27	0.8	11
Au	46.56	65.28	42.65	1.8	21

	XPS ^[c]					
Elements	Au	Pd	С	О		
Atom. (at.%)	26.26	24.74	20.14	28.86		

[[]a] The Au-Pd molar ratio is determined to be 1.086 by EDX analysis.

[[]b] The Au-Pd molar ratio is determined to be 1.027 by ICP-AES characterization. n.d. = not determined.

[[]c] The Au-Pd molar ratio is determined to be 1.061 by XPS analysis.

Table S2. Overview of articles in major journals on heterogeneous ethane oxidation, and associated conditions.

Catalyst	Reaction conditions ^[a]	Initial H ₂ O ₂ concentration	Reference
AuPd	21 °C and 1 bar	0.001-0.5 M; <i>In</i> situ production ^[b]	This work
Fe- and Cu- containing ZSM-5	50 °C and 5-30 bar	0.1-1 M	J. Am. Chem. Soc., 2013, 135 , 11087–11099
Fe/ZSM-5	30-60 °C and 20 bar; 50 °C and 1-30 bar	0.06-0.3 M	J. Catal., 2015, 330 , 84–92
Fe/ZSM-5	30 °C and 5 bar	0.5 M or 1 M	Chem. Sci., 2014, 5, 3603-3616
H-ZSM-5	77-120 °C and 30-35.5 bar	0.1-0.4 M	Appl. Catal. A: General, 2013, 456 , 82–87
Rh ₁ O ₅ /ZSM-5	50-80 °C and 15 bar; 50 °C and 1.5-15 bar	0.5-2.5 M	ACS Sustainable Chem. Eng., 2019, 7 , 4707–4715
TS-1	60 °C and 30 bar	0.116 M	Tetrahedron Lett., 2006, 47, 3071–3075
Pd/C	70-110 °C and 34.5 bar	<i>In situ</i> production	J. Am. Chem. Soc., 1992, 114 , 7308–7310
(FePc)2N/SiO2; (FePctBu)2N/SiO2	60 °C and 32 bar	0.339 M	J. Organomet. Chem., 2015, 793 , 139–144

[[]a] Reaction temperature and initial ethane pressure.

[[]b] H₂O₂ generated in situ.

Table S3. Additional experiments for comparison with AuPd nanoparticle catalysts.^[a]

			Products (µmol)			Total		
		H_2O_2				O_2	liquid	H_2O_2
		amount	EtOOH	CH ₃ CHO	CH ₃ COOH	produced	products	consumed
Entry	Catalyst	(µmol)				(µmol)	(µmol)	(%)
1 ^[b]	PdCl ₂ /HAuCl ₄	50	0	0	0	0	0	0
2 ^[c]	AuPd	50	0.43	0	0	2.54	0.43	22.2

[[]a] Reaction conditions: 1 bar C_2H_6 ; 21 °C; 1 h; 1000 rpm.

[[]b] Entry 1: Homogeneous metal chloride precursor solutions (3.3 μ mol of PdCl₂ and 3.3 μ mol of HAuCl₄ in 5 mL of water).

[[]c] Entry 2: 5 mL; 1 mg AuPd (6.6 μ mol of metals).

Table S4. Comparison of catalytic activity of AuPd catalyst for C₂H₆ oxidation.^[a]

		H_2O_2			Total liquid		
		concentration	Reaction	O ₂ produced	products	H ₂ O ₂ consumed	Gain
Entry	Oxidant	(mM)	time (h)	$(\mu mol)^{[c]}$	(µmol)	(µmol)	factor ^[d]
1	H_2O_2	0	1	0	0	0	0
2	H_2O_2	1	1	n.d.	0.15	2.9	0.0525
3	H_2O_2	10	1	2.54	0.43	11.1	0.0383
4	H_2O_2	30	1	13.27	0.94	95.1	0.0098
5	H_2O_2	100	1	68.55	2.87	318.2	0.0090
6	H_2O_2	200	1	172.19	7.71	663.6	0.0116
7	H_2O_2	500	1	319.45	1.22	1609	0.0008
8	H_2O_2	10	2	5.65	1.26	22.2	0.0569
9	H_2O_2	10	4	5.99	2.06	33.3	0.0619
10	H_2O_2	10	8	10.51	2.83	43.3	0.0654
11 ^[b]	H_2/O_2	n.d.	1	n.d.	4.32	n.d. ^[e]	n.d.

[[]a] Typical reaction conditions: 5 mL; 1 mg AuPd; 1 bar C_2H_6 for entries 1 to 10; 21 °C; 1000 rpm. For all entries, CO_2 in the gas phase is in trace amounts (<1 μ mol) and could not be quantified by GC-TCD.

[[]b] $P_{H2} = 0.1$ bar, $P_{N2} = 0.9$ bar, $P_{C2H6} = 1$ bar, $P_{O2} = 0.4$ bar.

[[]c] The amount of O₂ was determined by GC.

[[]d] Gain factor is defined as mol of total amount of oxygenates/mol of H₂O₂ consumed.

[[]e] After reaction, 3.4 μ mol H₂O₂ left. n.d. = not determined.

Table S5. Product quantification for C_2H_6 oxidation over AuPd at 50 $^{\circ}C.^{[a]}$

	H_2O_2		Proc	lucts (µmol)		O_2	Total liquid	H_2O_2
	concentration	EtOOH	EtOH	CH ₃ CHO	CH₃COOH	produced	products	consumed
Catalyst	(mM)	Lioon	LiOII	CH3CHO		(µmol)	(µmol)	(µmol)
AuPd	100	2.29	1.13	1.31	0.16	178	4.89	440
AuPd	200	3.00	0.91	2.09	0.29	274	6.29	800
AuPd	500	0.64	0.20	0.57	0.15	792	1.56	2140

[[]a] Reaction conditions: 5 mL; 1 mg AuPd; 2 bar C_2H_6 ; 50 °C; 1 h reaction time; 1000 rpm.

Table S6. Comparison of catalytic activity of Pd, Au and AuPd catalysts for ethane oxidation and acetic acid oxidation in semi-batch continuous-H₂O₂-feed reactions. ^[a]

				CO_2	Total liquid	H_2O_2	
Entry	Catalyst	Reactant ^[b]	Conversion (%) ^[c]	produced (μmol) ^[d]	products (µmol)	consumed (µmol)	Gain factor ^[e]
1	Pd	CH ₃ COOH	1.00	3.47	1.54	460	n.d.
2	Au	CH ₃ COOH	1.22	5.37	0.71	180	n.d.
3	AuPd	CH ₃ COOH	3.25	12.32	3.91	450	n.d.
4	Pd	C_2H_6	0.58	n.d. ^[f]	4.63	468	0.0099
5	Au	C_2H_6	0.48	n.d.	3.82	400	0.0096
6	AuPd	C_2H_6	0.82	n.d.	6.51	420	0.0155

[[]a] Reaction conditions: Pd, Au, or AuPd colloid (6.6 μ mol of metals); 1 bar N₂ for entries 1 to 3, and 1 bar C₂H₆ for entries 4 to 6; 21 °C; 50 h; 1000 rpm; 500 μ mol H₂O₂.

[[]b] 500 µmol CH₃COOH or 1 bar C₂H₆ (795 µmol) as reactant.

[[]c] Conversion = (mol of total amount of oxygenates + mol of CO₂ produced)/mol of reactant in the reactor.

[[]d] The amount of CO₂ produced was determined by GC.

[[]e] Gain factor is defined as mol of total amount of oxygenates/mol of H₂O₂ consumed.

[[]f] For entries 4 to 6, CO_2 in the gas phase is in trace amounts (<1 μ mol) and can not be quantified by GC-TCD. n.d. = not determined.

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